

การผลิตค่านักมั่นต์จากยางรถยนต์ใช้แล้วโดยการกรองดูดด้วยไอน้ำร้อนยาดซิ่ง
และควรบ่อน้ำออกให้หมดในเครื่องปฏิกรณ์แบบเบตัน

นางสาวยนพร ล้อทอง



สถาบันวิทยบริการ
พัฒนาผลิตภัณฑ์ทางวิทยาศาสตร์

วิทยานิพนธ์นี้เป็นส่วนหนึ่งของการศึกษาตามหลักสูตรปริญญาวิทยาศาสตร์ธรรมชาติ
สาขาวิชาปีโครงการและวิทยาศาสตร์พอลิเมอร์
บัณฑิตวิทยาลัย จุฬาลงกรณ์มหาวิทยาลัย
ปีการศึกษา 2541

ISBN 974-639-473-8

ลิขสิทธิ์ของบัณฑิตวิทยาลัย จุฬาลงกรณ์มหาวิทยาลัย

**PRODUCTION OF ACTIVATED CARBON FROM USED TIRES BY
SUPERHEATED STEAM AND CARBON DIOXIDE ACTIVATION
IN A FIXED BED REACTOR**

Miss Thanapon Lortong

**A Thesis Submitted in Partial Fulfillment of the Requirements
for the Degree of Master of Science
Program of Petrochemical and Polymer Science**

**Graduate School
Chulalongkorn University**

Academic Year 1998

ISBN 974-639-473-8

Thesis Title PRODUCTION OF ACTIVATED CARBON FROM USED TIRES BY SUPERHEATED STEAM AND CARBON DIOXIDE ACTIVATION IN A FIXED BED REACTOR

By Miss Thanapon Lortong

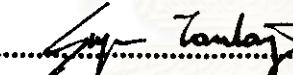
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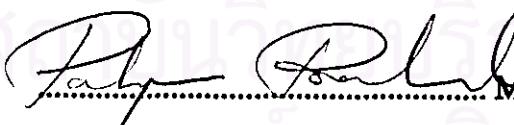
Accepted by the Graduate School, Chulalongkorn University in Partial
Fulfillment of the Requirements for the Master's Degree


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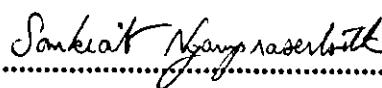
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ชนาพร ล้อหอง : การผลิตถ่านกัมมันต์จากยางรถยนต์ใช้แล้วโดยการกระตุ้นด้วยไอน้ำร้อนภายใต้
และค่ารับอนไดออกไซด์ในเครื่องปฏิกรณ์แบบเบด涅่ (PRODUCTION OF ACTIVATED CARBON
FROM USED TIRES BY SUPERHEATED STEAM AND CARBON DIOXIDE ACTIVATION IN A FIXED
BED REACTOR) อ.ที่ปรึกษา : ผศ.ดร.ธราพงษ์ วิทิตศานต์, 123 หน้า. ISBN 974-639-473-8.

งานวิจัยนี้เป็นการศึกษาการผลิตถ่านกัมมันต์จากยางรถยนต์ใช้แล้ว โดยกระบวนการการผลิตที่ประกอบด้วยการคาวน์ในร์ แล้วกระตุ้นด้วยไอน้ำร้อนภายใต้และค่าวอนไดออกไซด์ในเครื่องปฏิกรณ์แบบเบด涅่ เส้นผ่านศูนย์กลาง 100 มิลลิเมตร ค่าวอนในร์ยางรถยนต์ใช้แล้วที่อุณหภูมิ 360°C เป็นเวลา 80 นาที ด้วยอัตราการในทดสอบอากาศ 0.52 g/min ถ่านขาวที่ได้มีร้อยละผลิตภัณฑ์ 41.40% , ปริมาณค่าวอนคงตัว 62.67% , ปริมาณเด็ก 16.30% และปริมาณสารระเหย 22.13% . จากนั้นนำถ่านขาวที่ได้ไปกระตุ้นด้วยไอน้ำร้อนภายใต้และค่าวอนไดออกไซด์ ภาวะที่เหมาะสมในการกระตุ้น คือ ถ่านขาวขนาด $0.60-1.18$ มิลลิเมตร ที่อุณหภูมิ 800°C เป็นเวลา 45 นาที ใช้อัตราการในทดสอบอากาศ 0.27 g/min , อัตราการในทดสอบค่าวอนไดออกไซด์ 2.0 g/min และไอน้ำร้อนภายใต้ พบร่วมถ่านกัมมันต์ที่ได้มีร้อยละผลิตภัณฑ์ 27.99% , ความหนาแน่นเชิงปริมาตร 0.3590 g/cm^3 , ปริมาณเด็ก 21.05% , ค่าการดูดซึบโซเดียม 598.79 mg/g , ค่าการดูดซึบเมทิลเคนสูตร 247.08 mg/g , พื้นที่ผิวน้ำ $658.75 \text{ m}^2/\text{g}$, พื้นที่ผิวน้ำที่น้ำมันดินไม่ให้พร่อง $424.27 \text{ m}^2/\text{g}$, พื้นที่ผิวภายในอก $234.48 \text{ m}^2/\text{g}$ และเส้นผ่านศูนย์กลางรูกรุนเฉลี่ย 22.24 ซังติเมตร

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ภาควิชา.....
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ปีการศึกษา.....

ลายมือชื่อนักศึกษา นิตยา ลือกova
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ลายมือชื่ออาจารย์ที่ปรึกษาร่วม

3970646623 : MAJOR PETROCHEMISTRY

KEY WORD:

USED TIRE / ACTIVATED CARBON / FIXED BED REACTOR

THANAPON LORTONG : PRODUCTION OF ACTIVATED CARBON

FROM USED TIRES BY SUPERHEATED STEAM AND CARBON DIOXIDE

ACTIVATION IN A FIXED BED REACTOR. THESIS ADVISOR : ASSIST. PROF.

THARAPONG VITIDSANT, Ph.D. 123 pp. ISBN 974-639-473-8.

This research was the study of the production of activated carbon from used tires by the processes of carbonization and activation with superheated steam and carbon dioxide in a fixed bed reactor with the diameter of 100 mm. The used tires were carbonized at 350°C for 60 min with the air flow rate of 0.52 nl/min. The characteristics of the resulted chars were yield of 41.40 %, fixed carbon of 62.57 %, ash of 15.30 % and volatile matter of 22.13 %. Then, the chars were activated with superheated steam and carbon dioxide. The optimum condition for activation was 0.60-1.18 mm of the chars size at 900°C for 45 min with air at a flow rate of 0.27 nl/min, carbon dioxide at a flow rate of 2.0 nl/min and superheated steam. The resulted activated carbon obtained yield of 27.99 %, bulk density of 0.3590 g/cm³, ash of 21.05 %, iodine number of 598.79 mg/g, methylene blue number of 247.08 mg/g, B.E.T. surface area of 658.75 m²/g, micropore area of 424.27 m²/g, external area of 234.48 m²/g and average pore diameter of 22.24 Å.

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ACKNOWLEDGEMENT

The author wishes to express her deepest appreciation to her advisor, Assistant Professor Tharapong Vitidsant, Ph.D., for his invaluable guidance, advice and encouragement throughout this research. In addition, she is also grateful to Associate Professor Supawan Tantayanon, Ph.D., Professor Pattarapan Prasassarakich, Ph.D., Assistant Professor Prapaipit Chamsuksai Ternai, Ph.D., and Assistant Professor Somkiat Ngamprasertsith, Ph.D., for serving as a chairman and the members of thesis committee, respectively, whose comments have been especially valuable.

Appreciations are also expressed to the Faculty of science, Chulalongkorn University for granting a teaching assistance fellowship during 1995-1997, the Graduate School for the financial support in part of this research work and also the Department of Chemical Technology, Chulalongkorn University for providing equipment and chemicals.

A deep affectionate gratitude is acknowledged to my parents for their love, understanding, encouragement and social support throughout the entire study. With them, the author would never have been able to achieve this goal.

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ABBREVIATIONS

T	:	Temperature (°C)
t	:	Time (min)
% Y	:	% Yield
% M	:	% Moisture
% VM	:	% Volatile matter
% FC	:	% Fixed carbon
BD	:	Bulk density (g/cm ³)
IA	:	Iodine number (mg/g)
MB	:	Methylene blue number (mg/g)
S _{B.E.T.}	:	B.E.T. surface area (m ² /g)
S _{micro}	:	Micropore area (m ² /g)
S _{external}	:	External surface area (m ² /g)
S _{Langmuir}	:	Langmuir surface area (m ² /g)
V _{total}	:	Total pore volume (cm ³ /g)
V _{micro}	:	Micropore volume (cm ³ /g)
V _{non-micro}	:	Non-micropore volume (cm ³ /g)

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