ปัจจัยที่มีผลต่อสภาพเลือกจำเพาะและค่าการแยกในไมเซลลาร์อิเล็กโทรไคเนทิก โครมาโทกราฟีและคะพิลลารีอิเล็กโทรโครมาโทกราฟี

นางสาวชนิดา พวงพิลา

วิทยานิพนธ์นี้เป็นส่วนหนึ่งของการศึกษาตามหลักสูตรปริญญาวิทยาศาสตรคุษฎีบัณฑิต สาขาวิชาเคมี คณะวิทยาศาสตร์ จุฬาลงกรณ์มหาวิทยาลัย ปีการศึกษา 2554

ลิขสิทธิ์ของจุฬาลงกรณ์มหาวิทยาลัย บทคัดย่อและแฟ้มข้อมูลฉบับเต็มของวิทยานิพนธ์ตั้งแต่ปีการศึกษา 2554 ที่ให้บริการในคลังปัญญาจุฬาฯ (CUIR) เป็นแฟ้มข้อมูลของนิสิตเจ้าของวิทยานิพนธ์ที่ส่งผ่านทางบัณฑิตวิทยาลัย

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FACTORS AFFECTING SELECTIVITY AND RESOLUTION IN MICELLAR ELECTROKINETIC CHROMATOGRAPHY AND CAPILLARY ELECTROCHROMATOGRAPHY

Miss Chanida Puangpila

A Dissertation Submitted in Partial Fulfillment of the Requirements for the Degree of Doctor of Philosophy Program in Chemistry Department of Chemistry Faculty of Science Chulalongkorn University Academic Year 2011 Copyright of Chulalongkorn University

Thesis Title	Factors Affecting Selectivity and Resolution in Micellar
	Electrokinetic Chromatography and Capillary
	Electrochromatography
Ву	Miss Chanida Puangpila
Field of Study	Chemistry
Thesis Advisor	Associate Professor Thumnoon Nhujak, Ph.D.

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ชนิดา พวงพิลา : ปัจจัยที่มีผลต่อสภาพเลือกจำเพาะและค่าการแยกในไมเซลลาร์ อิเล็กโทรไคเนทิกโครมาโทกราฟีและคะพิลลารีอิเล็กโทรโครมาโทกราฟี. (FACTORS AFFECTING SELECTIVITY AND RESOLUTION IN MICELLAR ELECTROKINETIC CHROMATOGRAPHY AND CAPILLARY ELECTROCHROMATOGRAPHY) อ.ที่ปรึกษาวิทยานิพนธ์หลัก: รศ. คร. ธรรมนูญ หนูจักร, 99 หน้า.

งานวิจัขนี้เกี่ยวข้องกับแบบจำลองทางทฤษฎีของสภาพเลือกจำเพาะของการแขก สำหรับสารที่มีประจุในไมเซลลาร์อิเล็กโทรไกเนทิกโครมาโทกราฟี (MEKC) และการ เปรียบเทียบสภาพเลือกจำเพาะของมอนอลิตที่ไม่มีประจุสำหรับการแขกเพปไทด์และโปรตีน ในคะพิลลารีอิเล็กโทรโครมาโทกราฟี (CEC) ได้สร้างสมการและแบบจำลองทางทฤษฎี สำหรับสภาพเลือกจำเพาะของการแขก (α_{MEKC}) ใน MEKC โดยที่ α_{MEKC} สัมพันธ์กับตัวแปรที่ ไม่มีหน่วยได้แก่ สภาพเลือกจำเพาะของการเกลื่อนที่ (α_{cze}) ในคะพิลลารีโซน อิเล็กโทรฟอริซิส (CZE) และสภาพเลือกจำเพาะของรีเทนชัน (α_k) ใน MEKC เมื่อ α_{cze} และ α_k นิขามเป็นอัตราส่วนของกวามสามารถในการเคลื่อนที่ทางไฟฟ้าใน CZE และอัตราส่วน ของรีเทนชันแฟกเตอร์ใน MEKC สำหรับสารสองชนิดที่มีประจุ ตามลำคับ ด้วอย่างเช่น การ แขกของสารที่มีประจุใน MEKC สามารถเพิ่ม α_{MEKC} ได้เมื่ออัตราส่วนของสภาพเลือกจำเพาะ (ρ) มากกว่า 1.0 ($\rho = \alpha_k/\alpha_{\text{cze}}$) ในขณะที่ α_{MEKC} ลดลงเมื่อ $\rho \leq 1.0$ เมื่อใช้อัลกิลเบนซีนเป็น สารทดสอบพบว่าก่า α_{MEKC} ที่ได้จากการทดลองสอดกล้องกับการทำนายตามแบบจำลองของ α_{MEKC}

นอกจากนี้ได้เตรียม CEC คอลัมน์ประเภทมอนอลิตที่ไม่มีประจุที่มีหมู่เกาะอัลคิลเป็น C8-, C12- และ C16- โดยโคพอลิเมอไรเซซันของมอนอเมอร์ที่มีหมู่ฟังก์ชันเป็น C8-เมทราคริเลต, C12-อะคริเลต และC16-เมทราคริเลต ตามลำดับ กับสารเชื่อมโยงข้าม เพนแทรีไทรทอลไทรอะคริเลต C16-มอนอลิตให้ประสิทธิภาพ (N) สำหรับแยกอัลคิล เบนซีนดีกว่า (N เท่ากับ 200,000, 162,000, 150,000 เพลต/เมตร สำหรับ C16-, C12- และ C8-มอนอลิต ตามลำดับ) และให้ประสิทธิภาพสำหรับแยกทริปทิกเพปไทค์แมปปิงดีกว่า อย่างไรก็ตาม C8-มอนอลิตให้ประสิทธิภาพสำหรับแยกโปรตีนได้ดีกว่า (N เท่ากับ 332,000, 236,000, 225,000 เพลต/เมตร สำหรับ C8-, C12- และ C16-มอนอลิต ตามลำดับ)

ภาควิชา	เคมี	ถายมือชื่อนิสิต
สาขาวิชา	เคมี	_ถายมือชื่ออ.ที่ปรึกษาวิทยานิพนธ์หลัก
ปีการศึกษา <u></u>	2554	

497 22641 23 : MAJOR CHEMISTRY KEYWORDS : CAPILLARY E LECTROCHROMATOGRAPHY/ CHARGED COMPOUNDS/ MICELLAR ELECTROKINETIC C HROMATOGRAPHY/ NEUTRAL MONOLITHS/ SEPARATION SELECTIVITY

CHANIDA PUANGPILA: FACTORS AFFECTING SELECTIVITY AND RESOLUTION IN MICELLAR ELECTROKINETIC CHROMATOGRAPHY AND CAPILLARY ELECTROCHROMATOGRAPHY. ADVISOR: ASSOC.PROF. THUMNOON NHUJAK, Ph.D., 99 pp.

This work involves the theoretical models of separation s electivity for charged an alytes in micellar electrokinetic ch romatography (MEKC), a nd comparison of selectivity of neutral monoliths for peptides and proteins separation in cap illary electrochromatography (CEC). Equations and theoretical models for MEKC separation selectivity (α_{MEKC}) were established, in which α_{MEKC} is related to di mensionless va lues of mobility selectivity (α_{CZE}) in c apillary zone electrophoresis (CZE) and r etention s electivity (α_k) in MEKC, and where α_{CZE} and α_k are defined as the ratio of electrophoretic mobility in CZE and the ratio of retention factor in MEKC for two charged analytes, r espectively. For example, MEKC separation of two charged analytes can enhance α_{MEKC} when the selectivity ratio (ρ) is greater than 1.0 ($\rho = \alpha_k/\alpha_{CZE}$), while lower α_{MEKC} is obtained with $\rho \leq 1.0$. Using alkylparabens as t est an alytes, ex cellent a greement w as f ound between the observed α_{MEKC} and prediction according to the theoretical models of α_{MEKC} .

In a ddition, neutral monolithic CEC columns with C8-, C12- and C16alkyl moieties were prepared by the copolymerization of the functional monomers C8-methacrylate, C 12-acrylate and C16-methacrylate, r espectively with the crosslinker pentaerythritol tr iacrylate. The C 16-monolith provided better separation e fficiency (N) for alkylbenzenes (N of 200,000, 162,000, 150,000 plates/m for C 16-, C 12- and C 8-monoliths, r espectively), a nd yielded better separation for tryptic peptide mapping. However, the C8-monolith provided better separation efficiency for proteins (N of 332,000, 236,000, 225,000 plates/m for C8-, C12- and C16-monoliths, respectively).

Department :	Chemistry	Student's Signature
Field of Study :	Chemistry	Advisor's Signature
Academic Year :	2011	

ACKNOWLEDGEMENTS

First of a ll, I wish to express my gratitude t o m y advisor, A ssociate P rofessor Dr. Thumnoon Nhujak, for his professionalism, suggestion, and critical reading. My special thanks are extended to the thesis examiners for their valuable comments and suggestions.

I am grateful to Professor Dr. Ziad El Rassi for his instruction during my one year research on C EC work in his lab at the Department of Chemistry, Oklahoma S tate University. I am also grateful to the members of his research group for their support, cheerful and friendship.

Furthermore, I s pecially t hank t o a ll m embers of S eparation a nd C hromatography Research Unit for their valuable suggestions. Also, I wish to thank all members of CE g roup f or t heir he lpfulness a nd encouragement. Moral s upports a nd c heerful willingness of my friends are truly appreciated. Thanks are also extended to everyone who has contributed suggestions and supports throughout this research.

I thankfully a cknowledge the Rachadaphiseksomphot Endowment and the Graduate School, C hulalongkorn U niversity f or t he f inancial s upport a nd the Center f or Petroleum, P etrochemicals, an d A dvanced M aterials for i nternational conference support. The financial support also imparted of the Institute for the Promotion of the Teaching Science and Technology, Thailand. All research facilities and partial grant, provided b y t he D epartment of C hemistry, C hulalongkorn U niversity a re appreciatively and thankfully acknowledge.

Finally, I am eternally grateful to my beloved parents and my brother for their love, encouragement and supports through to the end.

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LIST OF ABBREVIATIONS AND SYMBOLS

ABs	alkylbenzene
ACN	acetonitrile
AIBN	2,2'-azobisisobutyronitrile
APKs	alkyl phenyl ketones
BGE	background electrolyte
BP	butylparaben
CE	capillary electrophoresis
CEC	capillary electrochromatography
CGE	capillary gel electrophoresis
CIEF	capillary isoelectric focusing
CITP	capillary isotachophoresis
CZE	capillary zone electrophoresis
C8-methacrylate	octyl methacrylate
C12-acrylate	dodecyl acrylate
C16-methacrylate	cetyl methacrylate
DAD	diode array detector
DB	dodecylbenzene
EDMA	ethylene dimethacrylate
EG	ethylene glycol
EOF	electroosmotic flow
EP	ethylparaben
EtOH	ethanol
GC	gas chromatography
HPLC	high-performance liquid chromatography
i.d.	internal diameter
IP	isomethylparaben
MEKC	micellar electrokinetic chromatography
NaOH	sodium hydroxide
NAs	nitroalkanes

NMM	naphthyl methacrylate monolith
ODM	octadecyl monolith
PETA	pentaerythritol triacrylate
p <i>I</i>	isoelectric point
PP	propylparaben
PTFE	polytetrafluoroethylene
RP-CEC	reversed-phase capillary electrochromatography
RSD	relative standard deviation
SDS	sodium dodecyl sulphate
[SDS]	concentration of sodium dodecyl sulphate
С	concentration of analyte
Ε	electric field strength
е	electronic charge
${F}_{ m E}$	applied electric force
F_{F}	frictional force
Н	plate height
H_{aq}	plate height due to intermicelle mass transfer in aqueous
	phase
$H_{\rm col}$	plate height due to column
H _{det}	plate height due to detection
H_{f}	plate height due to maldistribution of flow
$H_{ m inj}$	plate height due to injection
H _{joule}	plate height due to thermal dispersion
H_1	plate height due to longitudinal diffusion
$H_{\rm mc}$	plate height due to sorption-desorption kinetics in micelle
	phase
H_{\min}	minimum plate height
H_{p}	plate height due to mass transfer resistance in the pore
$H_{\rm pd}$	plate height due to polydispersity of micelle phase
$H_{\rm t}$	plate height due to thermal dispersion
Κ	distribution constant
Ka	acid distribution constant

k	retention factor
L	total capillary length
l	length of capillary to detector
l _{inj}	length of analyte injected
Ν	number of theoretical plate, or peak efficiency
\overline{N}	average efficiency
n _{aq}	amount of analyte in aqueous phase
<i>n</i> _{mc}	amount of analyte in micelle phase
ΔP	pressure difference across the capillary
$Q_{ m inj}$	quantity of sample injected
R _s	resolution
r	internal capillary radius
<i>r</i> _h	hydrodynamic radius
t _{eo}	migration time of EOF
t _{ep}	migration time c orresponding to th e e lectrophoretic
	mobility of the charged analyte
t _{inj}	injection time
t _m	migration time
t _{mc}	migration times of micelle phase
to	retention time of EOF marker
u _{opt}	optimum flow velocity
V	applied voltage
V _{inj}	volume of sample injected
Veo	electroosmotic velocity
v _{ep}	electrophoretic velocity
v_{net}	total electrophoretic velocity
v_{s}	observed velocity of the analyte
v_{sc}	observed velocity of micelle phase
w _b	peak width at base
Wh	peak width at half height
x _{aq}	mole fraction of analyte in aqueous phase

$x_{ m mc}$	mole fraction of analyte in micelle phase
Ζ	charge of anion
α	selectivity
α_{CZE}	mobility selectivity in CZE
α_{dis}	degree of ionization
α_k	retention selectivity in MEKC
α_{m}	separation selectivity or mobility selectivity
α_{MEKC}	separation selectivity in MEKC
3	permittivity
ф	volume of aqueous phase to pseudo stationary phase
η	viscosity
μ	electrophoretic mobility
μ_{eo}	electroosmotic mobility
μ_{eff}	effective electrophoretic mobility
μ_{mc}	mobility of micelle phase
μ_{MEKC}	effective electrophoretic mobility of fully charged analyte
	in MEKC
μ_{net}	total mobility
μ_0	electrophoretic mobility at CZE conditions
$\overline{\mu}$	average effective electrophoretic mobility
Δμ	difference in the mobility for two analytes
σ	standard deviation of peak in distance unit
σ^2	peak variance
τ	standard deviation of peak in time unit
ζ	zeta potential
ρ	selectivity ratio

CHAPTER I

INTRODUCTION

1.1 Introduction to Capillary Electrophoresis

Capillary electrophoresis (CE) is a separation technique in which the analytes are separated in a capillary containing an electrolyte under the influence of a pplied electric field. The separation principle is based on the difference in electrophoretic mobility of analytes depending on the charged-to-size ratio [Khaledi, 1998; Camilleri, 1993]. The wide applications of CE have been demonstrated by its ability to separate both charged and ne utral analytes, small and large molecules such as peptides and proteins. Several advantages of CE include high separation efficiency, simple sample preparation, short analysis time, and low sample and solvent consumption [Hansen *et al.*, 2003; McEvoy *et al.*, 2007].

According to separation mechanism [Grossman *et al.*, 1992; Khaledi, 1998], CE can be classified i nto s ix basic modes including capillary z one electrophoresis (CZE), micellar electrokinetic chromatography (MEKC), capillary electrochromatography (CEC), capillary gel electrophoresis (CGE), capillary i sotachophoresis (CITP) and capillary is oelectric focusing (CIEF). This work involves the first three modes that will be briefly mentioned in this section.

CZE is a basic mode of CE that commonly used for separation of charged analytes. Its separation me chanism is based on the difference in electrophoretic mobility of analytes due to their different charge-to-size r atio, as shown in Figure 1.1a. The background electrolytes (BGE) used in CZE are typically buffers such as phosphate, borate and acetate.

1.2 Introduction to Micellar Electrokinetic Chromatography

MEKC is another mode of CE in which BGE contains a surfactant, such as sodium dodecyl s ulphate (SDS), t o f orm m icelles or micellar p hase acting a s a ps eudostationary p hase, s imilar to a s tationary p hase in h igh-performance l iquid chromatography (HPLC). The major benefit of MEKC is that allows the separation of both neutral and charged analytes. The s eparation m echanism o f n eutral analytes depends only on t he difference in partitioning of t he an alytes b etween an aqueous phase and a pseudo s tationary phase of m icelles w hile t he s eparation of c h arged analytes in MEKC depends on t he difference in either m icellar partitioning or their electrophoretic mobilities.



Figure 1.1 Separation mechanism in (a) CZE, (b) MEKC and (c) CEC. Adapted from Andrea and Brown [1997].

1.3 Introduction to Capillary Electrochromatography and Monolithic Columns

CEC is a separation t echnique combining the t wo modern l iquid-phase s eparation techniques, namely HPLC and CE. Therefore, the separation principle is based on a dual m echanism whereby n eutral an alytes are s eparated according t o d ifferent partitioning of the analytes between mobile phase and stationary phase while charged analytes a dditionally a s eparation m echanism b ased on t he d ifference i n t heir electrophoretic mobilities. Using the same s tationary phase i n a cap illary column, CEC provides h igher e fficiency due to f lat f low profile in C EC [Dittmann, and Rozing, 1997], while parabolic flow profile in HPLC. The columns used in CEC can be c ategorized into t hree types including the open-tubular c olumns, the packed columns and monolithic columns. There are limitations of the first two column types, such as tedious packing procedure for packed c olumn, bubble formation due to the present of frits in packed column and low phase ratio for open-tubular columns [Dong *et al.*, 2009].

The monolithic columns are increasingly interested in recent years due in major part to the ease of the *in situ* polymerization in a capillary to form a continuous porous structure. Therefore, the monolithic columns can effectively overcome the above mentioned problems of packed columns. Furthermore, the much higher phase ratio of monolithic column than that of the open-tubular column [Dong *et al.*, 2009].

Monolithic c olumns c an b e c lassified in to tw o ma in c ategories, i. e. silica-based monoliths and organic polymer-based monoliths. The former is prepared using the sol-gel technology creating a continuous sol-gel network throughout the column. The latter is u sually p repared v ia v inyl p olymerization in s ingle s tep w ithin a c apillary column by the polymerization of an organic functional monomer in the presence of a crosslinker, i nitiator and por ogens [Legido-Quigley *et a l.*, 2003; Klodzinska *et a l.*, 2006]. A wide va riety of m onomers c an be us ed s uch a s, a crylamide, acrylate, methacrylate an d s tyrene [Stulik *et a l.*, 2006; Eeltink *et a l.*, 2006]. This provides monolithic stationary phases with difference in surface chemistries. The main benefit of us ing or ganic p olymer-based m onoliths is stable ev en under ex treme pH

conditions, which could not tolerated by silica-based monoliths [Legido-Quigley *et al.*, 2003].

In this dissertation, we will focus on ne utral organic polymer-based monoliths which are void of a ny fixed c harges on the monolithic s tationary phases. The n eutral monolith without a ny c harged monomers will prevent the electrostatic interaction between charged analytes and stationary phases that allows the separation of a wide range of neutral and charged an alytes. The successful applications of C EC with neutral monolith to the separation of charged analytes especially for the proteins and peptides separation have been accomplished [Okanda, and E1R assi, 2005; Karenga, and E1Rassi, 2008, 2010a, 2010b, 2011c].

1.4 Previous Work on Separation Selectivity in MEKC and RP-CEC of Proteins and Peptides Separation

Typically, t he s eparation of t wo a nalytes i n c hromatography a nd e lectrokinetic chromatography such as MEKC can be expressed by separation selectivity (α) and resolution (R_s). In MEKC, R_s related to α , retention factor (k) and efficiency (N), therefore, t he h igher t he s eparation s electivity, t he g reater t he resolution of t wo analytes, r esulting i n t he be tter s eparation. The s eparation m echanism of n eutral analytes i n MEKC d epends onl y on t he di fference i n m icellar p artitioning of t he analytes. The MEKC separation selectivity (α_{MEKC}) for neutral analytes or retention selectivity (α_k) is defined as the ratio of k, i.e. $\alpha = k_2/k_1$ where $k_2 \ge k_1 > 0$. The higher t he d ifference i n k or hi gher s eparation s electivity provides t he better separation. In case of charged analytes with a difference in electrophoretic mobility (μ_0) of analytes at CZE conditions, the MEKC separation is based on the differences in both k and μ_0 . Therefore, α_{MEKC} for two charged analytes is defined as the ratio of effective e lectrophoretic mobility of two f ully c harged analytes, i .e. $\alpha_{MEKC} = \mu_{MEKC,2}/\mu_{MEKC,1}$ with $k_2 \ge k_1 > 0$. Factors affecting separation selectivity in MEKC include micellar buffer components, such as types and concentrations of surfactant,

organic s olvent, and p H, and p arameters o f CE i nstrument, s uch as t emperature [Riekkola *et al.*, 1997].

In pr evious w ork, the a ddition of s urfactant t o t he M EKC buf fer may r esult in improved s eparation f or amino aci ds [Iadarola *et a l.*, 2008], inorganic a nions [Riekkola *et al.*, 1997], dianisine [Mallampati *et al.*, 2005], anacardic acids [Česla *et al.*, 2006] and statins [Damić *et al.*, 2010], with respect to CZE separation. But the lower degree of separation in MEKC than that in CZE was reported for preservatives [Huang *et al.*, 2003]. These dual effects are similar to those seen in chiral separation using du al c yclodextrins a s reported i n our pr evious w ork [Nhujak *et a l.*, 2005]. However, s eparation s electivity and e lectrophoretic m obility or der i n MEKC f or charged analytes have not been explained.

CEC employing or ganic polymer-based monolithic stationary phases is one of the modes in CE that used as an effective separation method for charged species such as proteins and peptides. Customarily, the monolithic stationary phases with the fixed surface charges have been intentionally introduced to support the electroosmotic flow (EOF) [Bedair, and El Rassi, 2002, 2003; Augustin et al., 2008; Feng et al., 2009]. This leads to the nuisance electrostatic interaction between charged analytes and the stationary phases, which caused either band broadening or irreversible binding of charged analytes. To overcome above problems, the neutral nonpolar monoliths for reversed-phase CEC (RP-CEC) have been developed for charged analytes separation [Okanda, and El Rassi, 2005; Karenga, and El Rassi, 2008, 2010a, 2010b, 2010c]. In this case, the EOF generated from the adsorption of mobile phase ions to the neutral monolithic surface. The magnitude of the E OF c an be c onveniently adjusted by changing the p H a nd a cetonitrile c ontent of t he m obile phase. In a ddition, t he separation selectivity, retention and magnitude of the EOF have been modulated by mixed ligand m onolithic c olumns [Karenga, and E I R assi, 2011a] as w ell as segmented m onolithic c olumns c onsisting of o ctadecyl a nd na phthyl monolithic segments [Karenga, and El Rassi, 2011b].

In previous work, the neutral monoliths for RP-CEC have been developed in the aim of s eparating bi omolecules, i .e. pr oteins and pe ptides, but t hese ne utral monoliths were not effective in CEC of proteins and peptides [Dong *et al.*, 2005; Li *et al.*, 2004; Zhang *et al.*, 2003]. The success of preparing a series of neutral nonpolar monoliths with surface bond C17 [Okanda, and E1 R assi, 2005], C18 [Karenga, and E1 R assi, 2008] and naphthyl ligands [Karenga, and E1 R assi, 2010c] for RP-CEC of proteins and pe ptides was r eported. Up-to-date, the d eveloping n eutral nonpolar monoliths with v arying *n*-alkyl c hain lengths (i.e. C8, C12 and C16) for RP-CEC of ch arged analytes such as proteins and peptides have not been reported previously.

1.5 Aim and Scope

In t his t hesis, s eparation selectivity in M EKC and C EC w as in vestigated f or separation of particular analytes. As previous mentioned in Section 1.4, the better degree of s eparation in M EKC t han that in CZE w as o btained f or s ome charged analytes, while the lower separation for other charged analytes was reported, as well as the reversed order of electrophoretic mobility for charged analytes in MEKC was obtained with respect to CZE separation. These dual effects are similar to those seen in chiral separation using dual cyclodextrins as reported in our previous work [Nhujak et al., 2005]. The addition of surfactant to the MEKC buffer may result in improved or reduced separation for charged analytes. This behavior implies that an increase in the surfactant concentration in the MEKC buffer can affect the separation selectivity for the charged analytes separation. In preliminary study, it is interesting to establish theoretical models for separation selectivity in MEKC (α_{MEKC}) to explain a change in separation and e lectrophoretic mobility order of fully charged analytes in MEKC based on mobility s electivity in CZE (α_{CZE}), retention s electivity in MEKC (α_k), selectivity r atio ($\rho = \alpha_k / \alpha_{CZE}$) and t he or der of $|\mu|$ in C ZE a nd k in M EKC. Therefore, the aims of this work a re to develop theoretical models for α_{MEKC} of charged analytes and to compare the observed and the predicted α_{MEKC} over a wide range of SDS concentration ([SDS]) and k values. The experiment will be carried out using test analytes as four alkylparabens and MEKC buffer containing SDS surfactant in a 10 m M disodium tetraborate buffer at pH 10.2 to afford almost fully negatively charged parabens. It is expected that this work will be very useful for explanation of a change, an increase or a d ecrease, of α_{MEKC} and electrophoretic mobility order of fully charged analytes in MEKC when SDS surfactant is added into the MEKC buffer. In r ecent y ear, t he CEC e mploying organic pol ymer-based m onolithic stationary phases is increasing used for separation of charged species i.e. proteins and peptides due to the ease of *in situ* polymerization in the capillaries. However, the potentials of CEC in the separation of proteins and peptides are still dormant due to the lack of suitable stationary phases. Since a few work have been reported the neutral nonpolar monoliths for R P-CEC of c harged s pecies including proteins and peptides in the absence of electrostatic interactions with the fixed surface charges. Therefore, further objective is to develop t wo di fferences ne utral nonpol ar monolithic c olumn s eries which designated as A and B column series. Each series consisting of three columns at varying *n*-alkyl chain length such as C8, C12 and C16 which were prepared by the copolymerization of the functional monomers C8-methacrylate, C12-acrylate or C16methacrylate with the crosslinking monomer pentaerythritol triacrylate and a ternary porogenic solvent made of cyclohexanol, ethylene glycol and water to yield monoliths with surface bound C 8, C 12 and C 16 c hains. In t he A c olumns s eries, t he composition of f unctional m onomers a nd c rosslinker w as a djusted t o y ield comparable chromatographic retention while in the B columns series, the composition of functional m onomers a nd c rosslinker was ke pt c onstant y ielding va riable chromatographic retention.

In or der t o characterize the two d ifferences eries monolithic c olumns, t he two columns series w ere d emonstrated in t he s eparation of n eutral an alytes s uch as alkylbenzenes, a lkyl phenyl ke tones, ni troalkanes, a nilines and phe nols as w ell as charged species such as proteins and peptide mapping. It is expected that some of these developed monolithic c olumns series will be suitable for proteins or peptides separation. In a ddition, the effect of d ifferent *n*-alkyl c hain l ength monoliths with surface bound C 8, C 12 and C 16 c hains on the separation of proteins and peptide mapping will be clarified.

CHAPTER II

THREORY OF CE MEKC AND CEC

2.1 CE Instrumentation



Figure 2.1 Schematic diagram of a basic CE instrument. Adapted from Weinberger [1993].

The schematic diagram of a typical CE in strument is shown in F igure 2.1. A CE system in cludes a capillary, high vol tage pow er supply, electrodes, buf fer vials and detector. The separation column is made of a narrow bore bare fused silica capillary for CZE and MEKC, and a narrow bore fused silica capillary containing the stationary phase in the case of CEC, ranging in diameter from 10 to 200 μ m and length from 20 to 100 cm. The high voltage power supply is applied to drive the separation, allowing voltages up between -30 a nd + 30 kV. Two e lectrodes us ed c ommonly m ade of platinum wire. A UV-Vis detector with wavelength selection from 190 to 700 nm is widely used detector. A cooling system is required for controlling temperature of the capillary and reducing Joule heating.

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Two different methods are basically used to introduce the sample into the capillary either hydrodynamic injection or electrokinetic injection. *The hydrodynamic injection* is based on pr essure differences between the inlet and outlet ends of the capillary. This different pr essure c an be a chieved by various methods s uch a s gravimetric, overpressure, and vacuum. The length of the sample zone injected (l_{inj}) into the capillary by the hydrodynamic method is given by the following equation [Khaledi, 1998]

$$l_{\rm inj} = \frac{\Delta P r^2}{8\eta L} t_{\rm inj} \tag{2.1}$$

where ΔP is the pressure difference between the inlet and outlet ends of capillary, r is the radius diameter of capillary, t_{inj} is the injection time, η is the liquid viscosity, and L is the capillary length. The volume (V_{inj}) and the amount (Q_{inj}) of analyte injected can be calculated using the following equations

$$V_{\rm inj} = \frac{\Delta P \pi r^4}{8 \eta L} t_{\rm inj} \tag{2.2}$$

and

$$Q_{\rm inj} = \frac{\Delta P \pi r^4}{8 \eta L} t_{\rm inj} C \tag{2.3}$$

where *C* is the analyte concentration. The pressure injection is widely used in CE. Since the injection is based on the pressure difference, it is universally applied to all kinds of s ample matrices without a ny bi as on the sample compounds. Therefore, pressure injection has better reproducibility and greater control over the amount of sample injected into the capillary. *In electrokinetic injection*, the sample is introduced into the capillary by applying high voltage over a short period of time. Analyte ions will migrate into the capillary due to the combination of electrophoretic migration of the ions and electroosmotic flow of the sample solution. The length of sample zone introduced into the capillary during electrokinetic injection is given by the equation

$$l_{\rm inj} = (v_{\rm eo} + v_{\rm ep})t_{\rm inj} \tag{2.4}$$

where v_{eo} is the electroosmotic velocity of the bulks olution and v_{ep} is the electrophoretic v elocity. Since each analyte h as a d ifferent m obility and electrokinetic injection is biased, therefore, this method gives the concentration of the injected s ample is d ifferent f rom that o f the o riginal s ample. However, t he electrokinetic injection is preferable to introduce the analytes i nto the s eparation monolith with very low porosity to avoid the extremely high backpressure.

2.2 Electrophoretic Mobility [Grossman, and Colburn, 1992; Camilleri, 1993]

The two p rimary factors that affect e lectrophoretic migration in CE in clude the applied electric force (F_E) and the frictional force (F_F). When a voltage V is applied across a capillary of length L containing the BGE, each charged analytes will migrate toward the electrode in the direction opposite polarity to its direction of the electric force F_E

$$F_{\rm E} = zeE \tag{2.5}$$

where z is the charge of an ion, e is the fundamental electronic charge, and E is the electric field strength (E = V/L, where V is the applied voltage across L is the total length of capillary).

According to charged a nalytes m igrate because of the applied electric force. This migration is resisted by the frictional force $F_{\rm F}$

$$F_{\rm F} = 6\pi r_{\rm h} \eta v_{\rm ep} \tag{2.6}$$

where η is the viscosity of the medium, r_h is the hydrodynamic radius of the ion, and v_{ep} is the electrophoretic velocity of the ion. Then, the acceleration of the ion will proceed until F_E is balanced by F_F , giving the equation:

$$zeE = 6\pi r_{\rm h} \eta v_{\rm ep} \tag{2.7}$$

The electrophoretic mobility, μ (m² V⁻¹ s⁻¹) is defined as the electrophoretic velocity of anion migrating in BGE under the influence of an applied electric field and relates to parameters as the equation

$$\mu = \frac{V_{\rm ep}}{E} = \frac{ze}{6\pi\eta r_{\rm h}}$$
(2.8)

With respect to Equation 2.8, electrophoretic mobility depends on the charge-to-size ratio of an ion, $z/r_{\rm h}$. Furthermore, it also depends on charge density of the analytes, ionic strength, viscosity of electrolyte, and temperature.

2.3 Electroosmosis [Grossman, and Colburn, 1992; Camilleri, 1993]

In addition to the electrophoretic mobility of analytes, the analytes will migrate along the capillary toward the detector by EOF. The EOF, as shown in Figure 2.2, is the movement of a m edium toward the electrode when the voltage is applied. In the presence of the BGE, especially, a buffer at pH > 2, silanol groups at the surface of the bare fused silica capillary ionize to negatively charged (-Si-O⁻) as the Equation 2.9 and 2.10. In c ases of packed or monolithic c olumns, the charged may arise from charged mo ieties that might b e in tentionally incorporated t o s upport the E OF. Furthermore, the adsorption of the ions from the mobile phase c reates an adsorbed layer of ions on the solid surface.

-SiOH (s) + H₂O (l)
$$\implies$$
 -SiO⁻ (s) + H₃O⁺ (aq) (2.9)

or

SiOH (s) + OH⁻ (aq)
$$\implies$$
 -SiO⁻ (s) + H₂O (l) (2.10)

Under these conditions, and when the surface is in contact with a buffer, some BGE cations are at tracted at the n egative s urface of the cap illary to form an electrical double l ayer, as shown in F igure 2.2. One la yer is tightly bound by e lectrostatic force, called the Stern layer, while other BGE cations are more loosely bound, called the diffusion l ayer. Moreover, the r est of the excess BGE cations are in the bulk solution. When the voltage is applied, the excess BGE cations both in the diffusion

layer and bulk solution migrate towards cathode and carry water or solvent molecules to the same direction. This phenomenon is called *electroosmosis*, and the migration of water or solvent molecules is called *electroosmotic flow* (EOF).



Figure 2.2 Electroosmotic flow (EOF). Adapted from Andrea et al. [1997].

The d irection of E OF i s i nfluenced b y s ign of the z eta p otential (ζ), the electric potential a t t he s hear p lane of t he doubl e l ayer. For a n egatively charged s olid surface, the zeta potential is negative and consequently, the EOF is cathodal and *vice versa*. The zeta potential is directly related to the velocity of electroosmotic flow, v_{eo} , as the equation

$$v_{\rm eo} = -\frac{\varepsilon\zeta}{4\pi\eta}E\tag{2.11}$$

where ε is the permittivity, and η is the viscosity of the liquid in the double layer. These values may be different from those in the bulk solution [Kenndler, 1998]. The electroosmotic mobility, μ_{eo} , can be defined as the velocity of electroosmotic flow versus the applied electric field as the equation

$$\mu_{\rm eo} = \frac{v_{\rm eo}}{E} = -\frac{\varepsilon\zeta}{4\pi\eta}$$
(2.12)

In case of a bare fused silica capillary, the value of ζ is negative, and therefore, μ_{eo} has a positive sign. From the internal capillary surface, v_{eo} increases with increasing distance, a nd is constant at t he di stance of a pproximately 15 nm from t he w all.

Typically, the capillary used in CE has 20 t o 1 00 μ m i. d. (20000 t o 1 00000 nm). Thus, it can be said that v_{eo} is constant throughout the capillary radius [Grossman, and Colburn, 1992].

Since EOF is generated at the capillary wall, and it is uniformly distributed along the capillary, there is no pressure drop within the capillary. This results in a flat profile of the bulk flow which does not directly contribute to the zone broadening. The flat flow profile in CE contrasts to the parabolic profile generated by laminar flow driven by a pressure gradient in HPLC (Figure 2.3), resulting in high efficiency and resolution in CE than HPLC.



Figure 2.3 Flow profiles in CE and HPLC. Adapted from Chankvetadze [1997].

In the presence of the EOF, the n et v elocity, v_{net} , of the analyte is the sum of the electrophoretic v elocity of the analyte and the electropsmotic velocity as E quation 2.13 and Figure 2.4

$$v_{\rm net} = v_{\rm ep} + v_{\rm eo} \tag{2.13}$$

It should a lso be not ed that a t hi gh E OF, bot h a nions a nd c ations m igrate t o the detection window. For cations, $v_{ep,+}$ and v_{eo} are in the same direction to the cathode at the detection window. The higher the ion charges and the smaller the ion size, the faster the migration toward the cathode. For anions, $v_{ep,-}$ has the direction toward the anode. However, the anions can migrate to the cathode, b ecause $v_{eo} > v_{ep,-}$. The

higher the ion c harges and the s maller the ion s ize, the s maller the n et velocity. Neutral molecules migrate toward the cathode only due to EOF, and cannot be separated.



Figure 2.4 Migration behavior of the analytes. Adapted from Li [1992].

The net electrophoretic mobility ($\mu_{net} = \mu + \mu_{eo}$), μ_{eo} and μ can be calculated from an electropherogram using the following equations

$$\mu_{\rm net} = \frac{v_{\rm net}}{E} = \frac{lL}{Vt_{\rm m}}$$
(2.14)

$$\mu_{\rm eo} = \frac{v_{\rm eo}}{E} = \frac{lL}{Vt_{\rm eo}}$$
(2.15)

$$\mu = \mu_{\rm net} - \mu_{\rm eo} = \frac{lL}{V} \left(\frac{1}{t_{\rm m}} - \frac{1}{t_{\rm eo}} \right)$$
(2.16)

where t_m and t_{eo} are the mig ration time s o f the a nalyte a nd th e E OF ma rker, respectively, *l* is the length of the capillary to detector, *L* is the total length of capillary and *V* is the applied voltage.

2.4 Retention and Separation Selectivity in MEKC

Overview of MEKC is given in Section 1.2. In this section, more theoretical details of M EKC are d iscussed. A r etention f actor or cap acity factor (k) is one of the characteristics t hat i ndicates r etention b ehavior of an alytes i n ch romatography and

electrokinetic ch romatography s uch as M EKC. The r etention f actor in M EKC is defined as the ratio of total moles of analyte in the micelle phase $(n_{\rm mc})$ versus those in the aqueous phase $(n_{\rm aq})$ [Miola *et al.*, 1998] as the following equation

$$k = \frac{n_{\rm mc}}{n_{\rm aq}} = K\phi \tag{2.17}$$

where *K* is t he di stribution c onstant be tween t he t wo ph ases, t he r atio of t he concentration of the solute in the micelle phase to that in the aqueous phase, and ϕ is the phase r atio, the ratio of the volume of the aqueous phase to that of the micelle phase. The higher the retention factor, the stronger the retention or the partitioning of analytes in the micelle phase.

In M EKC, the obs erved e lectrophoretic m obility of analyte A (μ) is a sum of the electrophoretic mobility of a nalyte A (μ _A) and the electrophoretic mobility of the micelle phase (μ _{mc}) [Camilleri, 1993] as the equation

$$\mu = x_{\rm aq}\mu_{\rm A} + x_{\rm mc}\mu_{\rm mc} \tag{2.18}$$

where x_{aq} and x_{mc} are the mole fractions of an alyte in aqueous and micelle phase, respectively.

In the case of charged analyte A, μ is given by

$$\mu = x_{aq}\mu_A + x_{mc}\mu_{mc} = \frac{n_{aq}}{n_{aq} + n_{mc}} + \frac{n_{mc}}{n_{aq} + n_{mc}}\mu_{mc}$$
(2.19)

From Equations 2.17 to 2.19, μ can be expressed by

$$\mu = \left(\frac{1}{1+k}\right)\mu_{\rm A} + \left(\frac{k}{1+k}\right)\mu_{\rm mc}$$
(2.20)
In the presence of high EOF, the total mobility ($\mu_{net} = \mu + \mu_{eo}$) in Equation 2.20 is given by

$$\mu_{\text{net}} = \left(\frac{1}{1+k}\right) \mu_{\text{A}} + \left(\frac{k}{1+k}\right) \mu_{\text{mc}} + \mu_{\text{eo}}$$
(2.21)

Therefore, the retention factor of the charged analyte in MEKC with high EOF can be calculated from an electropherogram using the equation [Téllez, Fuguet, and Rosés 2007a, 2007b; Camilleri, 1993]

$$k = \frac{\mu - \mu_{\rm A}}{\mu_{\rm mc} - \mu} \tag{2.22}$$

where μ and μ_A are electrophoretic mobility of a nalyte in M EKC and a t zero concentration of SDS or CZE, respectively, and μ_{mc} is the electrophoretic mobility of micelle m arker. It should be m entioned that E quation 2.22 is written in terms of absolute r ather t han n et el ectrophoretic m obility b ecause μ_{eo} is a c onstant f or a ll species.

It is important to note that MEKC has three different modes based on the direction of v_{eo} , the obs erved ve locity of m icellar phase (v_{sc}) and the obs erved ve locity of the analyte (v_s). In the nor mal e lution mode, v_{eo} and v_{sc} have i dentical d irection and $|v_{eo}| > |v_{sc}|$. In the case that v_{eo} and v_{sc} have opposite direction and v_{eo} being opposite to v_s , this mode is called reversed elution mode. In the last mode, restricted elution mode in which v_s being opposite to v_{sc} and v_{eo} and v_{sc} have opposite direction [Pyell, 2006].

As pr eviously m entioned i n S ection 1. 4, separation s electivity (α) is a nother characteristic u sed f or describing the d egree o f s eparation of two analytes in chromatography and electrokinetic chromatography such as MEKC. The separation selectivity in MEKC (α_{MEKC}) for two fully charged analytes is defined as the ratio of the effective electrophoretic mobilities, with $k_2 \ge k_1 > 0$.

$$\alpha_{\text{MEKC}} = \mu_{\text{MEKC},2} / \mu_{\text{MEKC},1}$$
(2.23)

where $\mu_{MEKC,1}$ and $\mu_{MEKC,2}$ are the effective electrophoretic mobilities of the analyte 1 and analyte 2, respectively.

2.5 Retention in CEC [Dittmann et al., 2000]

Although the concept of retention in CEC is similar to HPLC, it should be noted that the retention of s olute in CEC depends on both partitioning and electromigration, while the retention in HPLC due only to the difference in stationary phase partitioning that can be described by following equation

$$t_{\rm R,LC} = t_{\rm o}(1 + k_{\rm LC}) \tag{2.24}$$

where $t_{R,LC}$ and t_o are the mig ration times of the r etained an alyte and u nretained analyte in HPLC, respectively, and k_{LC} is the retention factor in HPLC. In CEC, the retention of analyte is based on partitioning and electrophoresis, therefore, Equation 2.20 needs to be modified to:

$$t_{\rm R,CEC} = t_{\rm o} (1 + k_{\rm LC}) \left(\frac{t_{\rm ep}}{t_{\rm ep} + t_{\rm o}} \right)$$
 (2.25)

where $t_{R,CEC}$ and t_o are the migration times of the retained analyte and unretained or uncharged an alyte in CEC s eparation, r espectively, and k_{LC} is the r etention factor associated w ith stationary pha se and mobile pha se partitioning, and t_{ep} is the migration time of analyte due to electrophoretic mobility. The first part of Equation 2.25 describes t he c hromatographic r etention. T he s econd part de scribes the modulation of analyte due to electromigration. In the case of neutral analytes, since they be ar no charge, t herefore, their r etention de pends only on t he difference i n partitioning be tween t he stationary pha se a nd mobile pha se. The value of t_{ep} in Equation 2.25 is equal t o infinity and E quation 2.25 is r educed t o Equation 2.24. Therefore, the retention factor for neutral analyte in CEC is given by

$$k_{\rm CEC} = \frac{t_{\rm R,CEC} - t_{\rm o}}{t_{\rm o}}$$
(2.26)

The k values in CEC can be obtained in the range between -1 and ∞ , where k = 0 refers to the analyte that not interacts with the stationary phase and migrates with the EOF, k = -1 refers to the analyte that retains in the stationary phase and migrates before the EOF, and $k = \infty$ refers to the analyte that more interacts with the stationary phase.

2.6 Resolution in CE

In CE, a resolution (R_s) of two analytes is defined as the ratio of the difference in their migration times to their peak width at base as the equation

$$R_{\rm s} = \frac{t_{\rm m2} \cdot t_{\rm m1}}{0.5(w_{\rm b1} + w_{\rm b2})} \tag{2.27}$$

It follows from Equations 2.27 and 2.16 that, R_s can be related to the mobility and the average number of theoretical plates, \overline{N} , as the equation

$$R_{\rm s} = \frac{1}{4} \left(\frac{\Delta \mu}{\overline{\mu} + \mu_{\rm eo}} \right) \sqrt{\overline{N}}$$
(2.28)

where $\Delta \mu$ is the difference in the mobility, $\mu_2 - \mu_1$, for two analytes, and $\overline{\mu}$ the average electrophoretic mobility of t he analytes. For two a nalytes with s ame direction of μ Equation 2.28 may be rearranged to relate to the resolution R_s to the efficiency term, the selectivity term, and the mobility term as expressed in Equation 2.29

$$R_{\rm s} = \left(\frac{\sqrt{\overline{N}}}{4}\right) \left(\frac{\alpha_{\rm m} - 1}{\alpha_{\rm m}}\right) \left|\frac{\mu_2}{\overline{\mu} + \mu_{\rm eo}}\right|$$
(2.29)

where α_m is the separation selectivity or mobility selectivity, which is defined as the ratio of effective electrophoretic mobilities for two analytes s uch as μ_2/μ_1 for $|\mu_2| > |\mu_1|$. In MEKC with normal elution mode, the resolution equation for neutral analytes can be expressed to relate to the retention term in Equation 2.30

$$R_{\rm s} = \frac{\sqrt{\overline{N}}}{4} \left(\frac{\alpha_{\rm k} - 1}{\alpha_{\rm k}} \right) \left(\frac{k_2}{1 + k_2} \right) \left(\frac{1 - \frac{t_{\rm eo}}{t_{\rm mc}}}{1 + \left(\frac{t_{\rm eo}}{t_{\rm mc}} \right) k_1} \right)$$
(2.30)

where α_k is the retention selectivity which is defined as the ratio of the retention factor, e.g. k_2/k_1 and $k_2 \ge k_1 > 0$, t_{eo} and t_{mc} are the migration times of an EOF marker or a n unretained c ompound and a micelle marker, r espectively. With the nor mal elution mode of MEKC separation of fully charged analytes due only to the difference in mic ellar p artitioning a nd n ot in their e lectrophoretic mo bilities, the resolution equation is given by Equation 2.31:

$$R_{\rm s} = \left(\frac{\sqrt{N}}{4}\right) \left(\frac{\alpha_{\rm k} - 1}{\alpha_{\rm k}}\right) \left(\frac{k_2}{1 + \bar{k}}\right) \left(\frac{1 + t_{\rm eo} / t_{\rm ep} - t_{\rm eo} / t_{\rm mc}}{1 + t_{\rm eo} / t_{\rm ep} + (t_{\rm eo} / t_{\rm mc}) \bar{k}}\right)$$
(2.31)

where t_{ep} is the migration time corresponding to the electrophoretic mobility of the charged analyte, and $t_{ep} = t_{ep2} = t_{ep1}$ for this case.

Similar to the resolution in MEKC in Equation 2.30, the resolution in CEC for neutral analyte can be expressed to relate to the efficiency term, selectivity term and retention term in Equation 2.32

$$R_{\rm s} = \frac{\sqrt{\overline{N}}}{4} \left(\frac{\alpha - 1}{\alpha}\right) \left(\frac{k_2}{1 + k_2}\right) \tag{2.32}$$

where k_2 is the retention factor of more retained analyte, α is the selectivity which is defined as the ratio of the retention factor, e.g. k_2/k_1 and $k_2 \ge k_1 > 0$

2.7 Preparation and Factors Affecting Morphology and Porosity of Monoliths

Organic polymer-based monoliths are prepared in a single step within the confines of a capillary column by the polymerization of an organic functional monomer in the presence of a crosslinker, initiator and porogens [Merhar *et al.*, 2003]. The functional monomer defines the monolith polarity while the porogens, monomer-to-crosslinker ratio and polymerization temperature control the monoliths morphology [Urban, and Jandera, 2008]. Monoliths are associated with two main types of pores: (i) the flow-through pores and (ii) the mesopores filled with "stagnant" mobile phase in which the solute molecules migrate to access the active adsorption sites. To get large surface area and retention, a significant number of smaller pores should be incorporated into the polymer. Micropores with sizes smaller than 2 nm contribute most significantly to the overall surface area followed by mesopores ranging from 2 to 50 nm [Urban, and J andera, 2008]. The larger flow-through pores (macropores) are essential to allow liquid to flow through at a reasonably low pressure and contribute very little to the overall surface area [Viklund *et al.*, 1996].

The polymerization can be initiated through the application of heat, UV radiation [Li, Tolley, and Lee 2009; Rohr *et al.*, 2003; Tan, Benetton, and Henion, 2003], gamma radiation [Sáfrány *et a l.*, 2005; Beiler *et a l.*, 2007] or r edox r eagents [Petra, Holdscaronvendová *et al.*, 2003; Cantó-Mirapeix *et al.*, 2008]. Once decomposed, the initiator initiates the polymerization and as the polymer chains grow, their solubility in the reaction mixture decreases and the polymer chains precipitate to form nuclei. Thermodynamically, the monomers are better solvents for the formed polymer than the porogens and the nuclei therefore become swollen with monomers. As a result of the monomer c oncentration in the nuclei is kinetically preferred. Further polymerization leads to an increase in the size of the nuclei to microglobules, which then aggregate to form clusters. As the microglobules continue to grow and crosslink to each other the final m orphological s tructure is f ormed. This process I eads t o t wo-phase s ystem consisting of a white colored c ontinuous solid m onolith a nd i nert I iquid por ogens filling the por es. Once the por ogens are washed out, the volume oc cupied by the

porogens then corresponds to the volume of the macropores [Vlakh, and Tennikova, 2007]. While varying the monomer-crosslinker ratio or type of initiator can change the composition and rigidity of the monolith, the alteration of the porogen affects only the porous structure of the final polymer. The porogens can either be good or poor solvents for the polymer. The mechanism of pore formation using porogens has been described a s follows. At t he b eginning of the pol ymerization, t he s olution i s homogeneous until the growing and crosslinked polymer chains precipitates and falls out of the solution. If the por ogen is a good solvent for the final polymer, phase separation is delayed and the resultant pores are smaller. Alternatively in the presence of a poor solvent, phase separation occurs early leading to large pores [Peters, Svec, and Fréchet, 1999]. While there is no standard way of choosing the right composition of porogens and the right porogen composition has to be based on trial and error, a reduction of m onomer/crosslinker r atio r epresents a s traight f orward m ethod t o increase p ore s ize and decrease p ressure d rop during o peration (in HPLC), t his approach how ever, de creases t he hom ogeneity a nd r igidity of t he m acroporous polymer [Vlakh, and Tennikova, 2007].

2.8 Efficiency and Band Broadening in CE

The parameters of peak efficiency used in CE are characterized similarly to those in chromatography. Theoretically, an electrophoretic peak in CE are assumed to have a Gaussian peak with standard deviation, σ in the distance units and τ in time units, as shown in Figure 2.5. The width of the peak at base, w_b , may be obtained by drawing lines at t angents t o the points of inflection, and m easuring the s eparation be tween these two points. The w_b is given by

$$w_{\rm b} = 4\sigma \quad \text{or} \quad w_{\rm b} = 4\tau \tag{2.33}$$

and the peak width at half height, w_h , is given by

$$w_{\rm h} = 2.354\sigma \text{ or } w_{\rm h} = 2.354\tau$$
 (2.34)

Peak efficiency (*N*) is also related to σ and τ as the equation

$$N = \left(\frac{l}{\sigma}\right)^2 = \left(\frac{t}{\tau}\right)^2 \tag{2.35}$$

It follow from Equations 2.33 to 2.35, *N* can be calculated from an electropherogram, according to the equation



$$N = 16 \left(\frac{t_{\rm m}}{w_{\rm b}}\right)^2 = 5.54 \left(\frac{t_{\rm m}}{w_{\rm h}}\right)^2$$
(2.36)

Figure 2.5 Gaussian peak.

In MEKC, peak broadening c an be expressed by peak variance (σ^2) or theoretical plate height (*H*) as similarly explained in chromatography as the equation [Terabe *et al.*, 1989]

$$\sigma^2 = Hl \tag{2.37}$$

Analogous to chromatography, H in MEKC also relates to N and l as the equation [Khaledi, 1998]

$$H = \frac{l}{N} \tag{2.38}$$

According to Equation 2.38, the higher the efficiency, the smaller the plate height or peak broadening. In this work, peak broadening in MEKC will be discussed in terms of H. The total H can be described as the sum of plate height caused by five main contributions as the equation

$$H = H_1 + H_{mc} + H_{aq} + H_t + H_{pd}$$
 (2.39)

where H_1 , H_{mc} , H_{aq} , H_t and H_{pd} are t he pl ate he ight generated by l ongitudinal diffusion, s orption-desorption ki netics in the ps eudo s tationary ph ase s olubilisation, intermicelle mass transfer in the aqueous phase, thermal dispersion and polydispersity of the pseudo stationary phase, respectively.

However, H_{mc} is negligible for analytes having strong partitioning into the ps eudo stationary p hase. H_1 increases with i ncreasing r etention t ime a nd hi gh di ffusion coefficient o f analytes. H_{aq} and H_{pd} decrease with i ncreasing s urfactant concentration. H_t increases with increasing the conductivity of BGE, capillary radius and applied voltage.

Similar to total H in MEKC, the total H in CEC can be expressed as

$$H = H_{\rm inj} + H_{\rm det} + H_{\rm col} + H_{\rm joule}$$
(2.40)

where H_{inj} , H_{det} , H_{col} , and H_{joule} are the plate height generated by injection, detection, column and thermal dispersion, respectively.

Joule heating causes non-uniform temperature gradients and local changes in viscosity that lead to band broadening. However, this effect can be minimized by using low conducting s upporting e lectrolytes in the m obile phase, na rrow bor e capillaries for efficient h eat dissipation, field s trengths that a re 1 000 V/cm or less, and c ontrolled column t emperature. The c ontribution of b and broadening i n bot h pressure an d electrodriven s eparations has be en thoroughly studied and it has be en r eported that plate height contributions from H_{inj} , H_{det} and H_{joule} were all negligible compared to H_{det} [Wen, A siaie, and Horváth, 1999]. Therefore, it can be as sumed that the total plate height is determined by the passage of the sample through the column. In CEC, factors affecting H_{col} include; maldistribution of flow (H_f), longitudinal diffusion (H_1) and mass transfer resistance in the pore (H_p). After dropping the negligible terms and substituting these terms in Equation 2.40, total H can be expressed as

$$H = H_{\rm f} + H_{\rm l} + H_{\rm p} \tag{2.41}$$

On substituting the c orresponding parameters that define plate height c ontributions into Equation 2.41, we obtain the van Deemter equation, which is usually represented in a simplified manner by summing up the constants (A, B and C) for a given set of conditions and relates each plate height contributor in terms of mobile phase velocity as:

$$H = \mathbf{A} + \frac{\mathbf{B}}{\mathbf{u}} + \mathbf{C}\mathbf{u} \tag{2.42}$$

Figure 2.6 shows a typical van Deemter plot and the relative plate height contributions of each term in the van Deemter equation as a function of mobile phase velocity. As shown in Figure 2.6, the optimum flow velocity (u_{opt}) produces the minimum plate height (H_{min}) . Longitudinal diffusion term, B/u, depends on the nature of the solute and an increase in the mobile phase flow velocity can minimize this term. The mass transfer r esistance i n t he p ores, C u, increases w ith i ncreasing m obile pha se f low velocity. This d iffusion m ass transfer resistance i s d ecreased i n C EC d ue t o t he generated E OF w ithin the flow through por es, which i ncreases the ki netics of the mass transfer [Wen, Asiaie, and Horváth, 1999]. The highest gain in CEC separation

efficiency results from decreasing the maldistribution of flow (the A term) observed in pr essure dr iven f low i n pa cked c olumns, w hich i s know n a s "Eddy diffusion" [Gidding, 1991]. The pl ug f low p rofile i n C EC c auses the "A" term to b ecome negligible i n d etermining t he o verall s eparation ef ficiency. Once t he broadening effects i n bot h t he A and C t erms of t he va n D eemter e quation a re r educed, efficiencies t hat a re 5-10 t imes be tter t han t hose obt ained i n pr essure-driven m ode under the same conditions are obtained.



Figure 2.6 Illustration of the plate height (H) contribution to each van Deemter term and the resulting observed plot of H as a function of mobile phase linear velocity.

CHAPTER III

THEORETICAL MODELS OF SEPARATION SELECTIVITY FOR CHARGED COMPOUNDS IN MICELLAR ELECTROKINETIC CHROMATOGRAPHY

3.1 Introduction

In chromatography and electrokinetic chromatography such as MEKC, the degree of separation of two analytes can be described by separation selectivity and resolution. The higher the resolution, the better the separation. To obtain high resolution, the high difference in k or high separation selectivity is required. As described in Section 2.6, with the normal elution mode of MEKC separation for two neutral analytes, the separation depends only on a d ifference in their electrophoretic mobilities. The resolution of two analytes depends on the retention selectivity, α_k , which is defined as the ratio of k such as k_2/k_1 . The higher the α_k , the better the resolution. In the case of MEKC separation of fully charged an alytes due only t o the difference i n m icellar partitioning and not in their electrophoretic mobilities, the resolution depends only on α_k as shown in Equations 2.30 and 2.31 in Section 2.6. The higher the difference in k or higher separation s electivity, the higher the resolution, resulting in the better separation.

It can be seen in Equations 2.30 and 2.31 that the separation selectivity may be now referred to the retention selectivity. In case of charged analytes with a difference in electrophoretic mobility (μ_0) of analytes at CZE conditions, the MEKC separation is based on t he di fferences i n bot h k and μ_0 , and the s eparation s electivity for two charged analytes in MEKC, α_{MEKC} , is defined as the ratio of effective electrophoretic mobility of two fully charged analytes, i.e. $\alpha_{MEKC} = \mu_{MEKC,2}/\mu_{MEKC,1}$ with $k_2 \ge k_1 > 0$. Factors affecting separation selectivity in MEKC include micellar buffer components,

such as t ypes an d co ncentrations of s urfactant, or ganic s olvent, a nd pH, a nd parameters of CE instrument, such as temperature [Riekkola *et al.*, 1997].

Typically, sodium dode cyl s ulphate (SDS) is t he m ost w idely used as a n i onic surfactant in MEKC because it is inexpensive and available in highly purified form. Separation s electivity can b e al tered b y ad ding the SDS s urfactant i nto t he MEKC buffer [Riekkola *et al.*, 1997; Mallampati *et al.*, 2005; Česla *et al.*, 2006; Iadarola *et al.*, 2008; Damić *et al.*, 2010].

In pr evious w ork, t he a ddition of s urfactant t o t he M EKC buf fer m ay r esult i n improved MEKC separation for amino acids [Iadarola *et al.*, 2008], inorganic anions [Riekkola *et al.*, 1997], dianisine [Mallampati *et al.*, 2005], anacardic acids [Česla *et al.*, 2006] and statins [Damić *et al.*, 2010], with respect to CZE separation. B ut the lower degree of separation in MEKC than that in CZE was reported for preservatives [Huang *et al.*, 2003]. These dual effects are similar to those seen in chiral separation using du al c yclodextrins a s reported in our pr evious w ork [Nhujak *et a l.*, 2005]. However, s eparation s electivity and e lectrophoretic m obility or der i n MEKC f or charged analytes have not been explained.

In o rder t o ex plain the separation s electivity and electrophoretic m obility o rder in MEKC for charged an alytes with differences in μ_0 , the a ims of this section are to establish theoretical models of MEKC separation selectivity (α_{MEKC}) which is related to t he dimensionless values of mobility s electivity (α_{CZE}) in C ZE and r etention selectivity (α_k) in M EKC, and t o c ompare t he observed and pr edicted separation selectivity in M EKC. The pr oposed α_{MEKC} models were classified based on t he ranges of α_{CZE} , α_k , selectivity ratio ($\rho = \alpha_k/\alpha_{CZE}$) and the order of $|\mu|$ in CZE and k in MEKC. C E s eparations with nor mal e lution m ode were p erformed in t wo buf fer systems: (1) CZE with 10 mM disodium tetraborate buffer at pH 10.2, and (2) MEKC with 20 to 60 mM SDS surfactant in a 10 mM disodium tetraborate buffer at pH 10.2, and the test analytes used were alkylparabens.





isomethylparaben (IP)

ethylparaben (EP)





propylparaben (PP)

butylparaben (BP)

Figure 3.1 Chemical structures of p arabens: is omethylparaben, e thylparaben, propylparaben and butylparaben.

3.2 Experimental

3.2.1 Chemicals

The following test analytes in a class of alkylparabens were purchased from Sigma-Aldrich (Steinheim, G ermany): is omethylparaben (methyl *m*-hydroxybenzoate; I P), ethylparaben (ethyl *p*-hydroxybenzoate; E P), pr opylparaben (propyl *p*-hydroxybenzoate; PP), and but ylparaben (butyl *p*-hydroxybenzoate; BP). Sodium hydroxide and disodium tetraborate decahydrate (Na₂B₄O₇.10H₂O) were supplied by Fluka (Buchs, S witzerland), S DS f rom S igma (St. L ouis, M O, U SA), all or ganic solvents obt ained f rom Merck (Dramstadt, G ermany), and d odecylbenzene/micellar marker (M) from Sigma-Aldrich (Steinheim, Germany).

3.2.2 CE conditions

CE experiments were carried out with a Beckman Coulter MDQ-CE system equipped with a photo-DAD scanning from 190 to 300 nm and monitoring at 220 nm. The data handling system comprised an IBM PC and 32 Karat Software. The uncoated fused-silica c apillary 40.2 c m in le ngth (30 cm to d etector) \times 50 μ m i.d. (Polymicro Technologies, AZ, USA) was used for CZE and MEKC separations, thermostated at 25 °C. V oltage w as s et at 15 kV . A sample solution w as i ntroduced b y 0.5 ps i pressure i njection f or 3 s . Prior to each d aily an alysis, t he cap illary was r insed sequentially for 15 m in with m ethanol, 0.1 M NaOH, water, and a r unning buffer. Between consecutive runs, the capillary was flushed with 0.1 M NaOH and then with a running buffer, each for 2 m in. After analysis, each day, the capillary was rinsed with water and E tOH for 5 m in each, and then 0.1 M NaOH and water for 10 m in each. All experiment runs were performed in duplicate.

3.2.3 Preparation of buffer solutions

The electrophoretic mobilities were determined in two buffer systems: (1) CZE with 10 mM disodium tetraborate buffer, adjusted to pH 10.2 with 1.0 M NaOH, and (2) MEKC with 20 to 60 m M SDS in a 10 m M disodium tetraborate buffer at pH 10.2. All buffers were prepared using Milli-Q water, sonicated for 30 min, and then filtered through 0.45 μ m PTFE filters prior to use.

3.2.4 Preparation of analytes

Each t est an alyte w as s eparately d issolved in 5 m L of a cetonitrile, and t hen each analyte solution was diluted with Milli-Q water in a 10 m L volumetric flask to give 1000 ppm stock solutions. Stock solutions of DB and thiourea were also separately dissolved in ethanol, and then diluted to 20000 ppm with Milli-Q water. A working standard solution containing 20 to 60 ppm of each test analyte, 30 ppm thiourea and 150 ppm DB were prepared by diluting each of the stock solutions with a 1.0 m M

borate buf fer. All s olutions were f iltered t hrough 0.45 μ m P TFE filters p rior to analysis.

3.2.5 Charged compounds separation in CZE

3.2.5.1 Determination of pK_a values of alkylparabens

Stock s olution of 100 m M disodium t etraborate was p repared b y w eighing an appropriate a mount of disodium te traborate and then dissolved with Milli-Q water, adjust to pH 10.2 with 1.0 M NaOH. Solution of 10 mM disodium tetraborate buffer was prepared by diluting appropriate amounts of 100 mM disodium tetraborate buffer with the Milli-Q water.

The borate buffers with valous pHs from 7.8 to 10.2 were prepared by adjusting a 10 mM Na $_2B_4O_7$ buffer with a 1.0 M NaOH or H₃BO₃ solution to desire pH. The values of effective electrophoretic mobility, μ_{eff} , in CZE conditions of each paraben were measured and calculated us ing E quation 2.16. The ap parent p K_a values of parabens w ere d etermined b y p lotting 1/ μ_{eff} versus 10^{-pH} ([H₃O⁺]) and r esults ar e shown in Section 3.3.1.2.

3.2.5.2 Separation of alkylparabens in CZE at pH 10.2 of borate buffer

Simultaneous s eparation of alkylparabens w as c arried out with a 10 m M disodium tetraborate buffer at pH 10.2 and other CE conditions as in Section 3.2.2. In the case of normal e lution mode, μ_{eff} of each p araben can b e cal culated f rom electropherograms u sing t he E quation 2.16 and t he r esults are s hown in S ection 3.3.1.3. Each value of α_{CZE} was obtained from the ratio of μ_{eff} for two analytes i.e. $\alpha_{CZE} = \mu_2/\mu_1$. Results are also shown in Section 3.3.1.3.

3.2.6 Charged compounds separation in MEKC

Equations and theoretical models were p roposed for MEKC separation s electivity (α_{MEKC}) of two charged analytes using data of mobility selectivity in CZE, retention selectivity in MEKC, the order of $|\mu|$ in CZE and k in MEKC. Details are discussed in Section 3.3 .2. Experimental and p redicted values of α_{MEKC} for two charged analytes in MEKC were compared as shown in Section 3.3.2.3. The experiment was carried out using 10 mM Na₂B₄O₇ buffer at pH 10.2 and various concentrations of SDS. Results are shown in Figures 3.5.

3.3 Results and Discussion

3.3.1 Charged compounds separation in CZE

3.3.1.1 BGE conditions

All test analytes such as IP, BP, PP and EP are weak acid compounds (Figure 3.1) with pK_a values of 9.2 for IP [Piršelová, Baláž, and Schultz, 1996] and 8.4 for other parabens [Wilson, and Gisvold, 1998]. Therefore, a background electrolyte at basic pH was selected to allow separation of all parabens as negatively charged compounds. Typically, CZE separation of acid compounds is performed using a borate buffer at pH 8.2 to 10.2. In previous work, the separation of preservatives such as BP, PP and EP was carried out in the borate buffer at pH 9.0 [Huang *et al.*, 2003]. In this work, borate bu ffer at pH 10.2 w as chosen to a fford a lmost f ully ne gatively charged analytes, and the degrees of ionization of all parabens were determined and the details were discussed in Section 3.3.1.2.

3.3.1.2 Degrees of ionization and apparent pK_a values of alkylparabens

As previous mentioned in Section 3.2.5.1, the test analytes, parabens such as IP, BP, PP an d E P, ar e esters o f h ydroxybenzoic a cid w ith H O-C₆H₄COOR. T hese

compounds contain an –OH group that expresses a weak acid, and therefore they can be dissociated to c arry a negative charge ($^{-}OC_{6}H_{4}COOR$), especially at pH > p K_{a} . The degree of ionization (α_{dis}) for each analyte depends on the pH of the BGE and the p K_{a} of the analyte in the BGE at the experimental ionic strength. The parabens in their fully charged f orm a re s eparated i n t his e xperiment, i n or der t o a void interpretation of results of micelle partitioning for mixtures of neutral and ionic form of parabens. Therefore, the p K_{a} value of each paraben needs to be determined under these experimental conditions in order to choose particular pH of the buffer providing fully charged analytes.

In the case of a weak acid, HA, the protolysis of this neutral acid can be expressed by giving equation [Khaledi, 1998].

$$HA + H_2O = H_3O^+ + A^-$$
 (3.1)

The acid dissociation constant, K_a , at a given ionic strength is given by equation.

$$K_{\rm a} = \frac{\left[\mathrm{H}_{3}\mathrm{O}^{+}\right]\mathrm{A}^{-}}{\left[\mathrm{H}\mathrm{A}\right]} \tag{3.2}$$

The acid dissociation c onstant, K_a , may b e d etermined b y C E [Cai *et a l.*, 1992]. When the weak acid analyte is partially ionized due to the equilibrium at a given pH, the effective electrophoretic mobility, μ_{eff} , depends on the degree of ionization, α_{dis} , and the electrophoretic mobility of fully charge, μ_0 , as the equation.

$$\mu_{\rm eff} = \alpha_{\rm dis} \mu_0 \tag{3.3}$$

For the case of a monovalent weak acid with a certain pK_a , the degree of ionization, α_{dis} , is connected to the pH of the BGE by

$$\alpha_{dis} = \frac{\left[A^{-}\right]}{\left[A^{-}\right] + \left[HA\right]} = \frac{1}{1 + 10^{pKa-pH}}$$
(3.4)

From Equation 3.1 to 3.4, μ_{eff} of a monovalent weak acids depends on the pH of BGE by equation.

$$\mu_{\rm eff} = \frac{\mu_0}{1 + 10^{pKa - pH}} \tag{3.5}$$

It is possible to obtain a linear Equation 3.6, by taking the inverse of Equation 3.5

$$\frac{1}{\mu_{\rm eff}} = \frac{1}{K_{\rm a}\mu_0} \left[H_3 O^+ \right] + \frac{1}{\mu_0}$$
(3.6)

Equation 3.6 is a linear relationship whereby a plot of $1/\mu_{eff}$ against $[H_3O^+]$ yield a straight line with a Y-intercept of $1/\mu_0$ and a slope of $1/K_a\mu_0$. The p K_a value follows using the equation

$$pK_{a} = \log \frac{\text{slope}}{\text{intercept}}$$
(3.7)

The apparent pK_a values of each paraben were determined by measuring μ_{eff} of each paraben in CZE as a procedure described in Section 3.2.5.1. From the linear fitting of $1/\mu_{eff}$ versus 10^{-pH} in Figure 3.2, Table 3.1 s ummarizes the values of slope, $1/K_a\mu_0$, and Y-intercept, $1/\mu_0$, experimental and the lite rature pK_a values of each p araben. The slightly smaller apparent pK_a than literature pK_a^{o} values are seen, where the latter is obtained from the zero ionic strength. S trictly speaking, $pK_a^{o} = pK_a + (-\log \gamma_A -)$, where the γ_A - is activity coefficient for A⁻ at a given ionic strength, and always less than 1.0. Therefore, pK_a less than pK_a^{o} value is reasonable.

The borate buffer used in this work has the limit of buffering capacity in the pH range of $pK_a\pm 1$, where the pK_a of boric acid is 9.2. Therefore, the pH 10.2 was chosen to obtain buffering capacity and afford almost fully charged analytes with the degrees of ionization of 0.96 f or IP and 0.99 for other parabens, calculated using the apparent pK_a values in Table 3.1 and Equation 3.4.



Figure 3.2 Plots of $1/\mu_{eff}$ as a function of $[H_3O^+]$ for BP, PP, and EP in (a), IP in (b). CE c onditions: uncoated f used s ilica 50 µm i .d. × 40.2 c m (30 c m t o de tector), temperature 2.5 °C, BGE, 10 m M disodium bor ate buffer at a range of pH values, voltage 15 kV, 0.5 psi pressure injection for 3 s and UV detection at 220 nm.

paraeti						
Analyte		Intercept (1/µ0)	pKa			
	Slope			Literature		
	$(1/K_a\mu_0)$		This work	(at zero ionic		
				strength)		
IP	-2.63×10^{8}	-0.414	8.80	9.2		
BP	-4.43×10^{7}	-0.468	7.98	8.4		
PP	-4.40×10^{7}	-0.443	8.00	8.4		
EP	-4.00×10^{7}	-0.427	7.97	8.4		

Table 3.1 Slope, Y-intercept, experimental and the literature pK_a values of for each paraben

3.3.1.3 Electrophoretic mobility and separation selectivity

Simultaneuos separation of IP, BP, PP and EP in CZE was carried out as a procedure described in Section 3.2.5.2. Figure 3.3 shows an example of electropherogram for separation of these parabens in CZE. As seen in Figure 3.3, the CZE separation, in which the el ectrophoretic m obility v ectors o f n egatively ch arged p arabens ar e opposite t o an E OF vector, the migration time order EP > PP > BP > IP with the effective electrophoretic mobilities μ of -2.25, -2.13, -2.03 and -2.00 10^{-8} m²V⁻¹s⁻¹, respectively, indicates the $|\mu|$ order EP > PP > BP > IP, in line with the charge-to-size ratio for homologous series EP > PP > BP. The smaller $|\mu|$ for IP than other parabens may be due to the smaller degree of ionization, and/or larger hydrodynamic size of IP. The values of α_{CZE} can be calculated from the ratio of μ for each p air of an alytes, resulting in the α_{CZE} values of 0.888, 1.066 and 0.953 for IP/EP, PP/IP and BP/PP, respectively. It can be seen from Figure 3.3 that separation of BP, PP and EP was achieved under CZE conditions, while partial separation was obtained for IP and BP.



Figure 3. 3 Electropherogram of s eparation of IP, B P, PP a nd E P using CZE. CE c onditions: unc oated f used s ilica 50 μ m i .d. \times 40.2 c m (30 cm t o d etector), temperature 25 °C, BGE, 10 mM disodium borate buffer adjusted to pH 10.2 with 1.0 M NaOH, voltage 15 kV, 0.5 ps i pressure injection for 3 s and UV detection at 220 nm.

3.3.2 Charged compounds separation in MEKC

3.3.2.1 Principle of charged compounds separation in MEKC

In MEKC, effective electrophoretic mobilities of two fully charged analytes, μ_{MEKC} , are given by Equations 3.8 and 3.9 [Camilleri, 1993].

$$\mu_{(\text{MEKC},1)} = \left(\frac{\mu_{0,1} + k_1 \mu_{\text{mc}}}{1 + k_1}\right)$$
(3.8)

$$\mu_{(\text{MEKC},2)} = \left(\frac{\mu_{0,2} + k_2 \mu_{\text{mc}}}{1 + k_2}\right)$$
(3.9)

where μ_0 is the electrophoretic mobility at zero concentration of SDS or under CZE conditions, and μ_{mc} is the electrophoretic mobility of the micelle marker. Subscripts 1 and 2 refer to the analytes 1 and 2, respectively.

As previously mentioned in Section 3.1, the retention selectivity (α_k) in MEKC is defined as the ratio of k, such as k_2/k_1 , and therefore k_2 is given by Equation 3.10

$$k_2 = \alpha_k k_1 \tag{3.10}$$

In CZE, the mobility selectivity (α_{CZE}) is defined as the ratio of μ_0 , such as $\mu_{0,2}/\mu_{0,1}$, and therefore $\mu_{0,2}$ is given by Equation 3.11

$$\mu_{0,2} = \alpha_{\rm CZE} \mu_{0,1} \tag{3.11}$$

The separation selectivity in MEKC (α_{MEKC}) is the ratio of μ_{MEKC} with $k_2 \ge k_1 > 0$. From μ_{MEKC} values in Equations 3.8 and 3.9, α_{MEKC} can be rewritten as

$$\alpha_{\text{MEKC}} = \frac{\mu_{(\text{MEKC},2)}}{\mu_{(\text{MEKC},1)}} = \left(\frac{\mu_{0,2} + k_2 \mu_{\text{mc}}}{\mu_{0,1} + k_1 \mu_{\text{mc}}}\right) \left(\frac{1 + k_1}{1 + k_2}\right)$$
(3.12)

From Equations 3.10 and 3.11, α_{MEKC} can be expressed by the equation

$$\alpha_{\text{MEKC}} = \left(\frac{\alpha_{\text{CZE}}\beta + \alpha_{k}k_{1}}{\beta + k_{1}}\right) \left(\frac{1 + k_{1}}{1 + \alpha_{k}k_{1}}\right)$$
(3.13)

where $\beta = \mu_{0,1}/\mu_{mc}$

3.3.2.2 Theoretical models of separation selectivity

 α_{MEKC} in Equation 3.1.3 may be rearranged to relate to the ratio of α_k/α_{CZE} as the equation

$$\alpha_{\text{MEKC}} = \alpha_{\text{CZE}} \left(\frac{\beta + \frac{\alpha_k}{\alpha_{\text{CZE}}} k_1}{\beta + k_1} \right) \left(\frac{1 + k_1}{1 + \alpha_k k_1} \right)$$
(3.14)

	Order of μ in			_	Assumed values	
Туре	CZE and <i>k</i> in MEKC	α_{CZE}	α_k	ρ	α_{CZE}	α_k
Ι	Same	$\alpha_{CZE} \geq 1$	$\alpha_k > \alpha_{CZE} \geq 1$	ρ > 1	1.1	1.2-3.3
II	Same	$\alpha_{CZE} > 1$	$\alpha_{CZE} \geq \alpha_k \geq 1$	$\rho \le 1$	1.5	1.0-1.5
III	Reversed	$\alpha_{CZE} < 1$	$\alpha_k \geq 1 > \alpha_{CZE}$	ρ>1	0.8	1.0-6.4
IV	Co-migration	$\alpha_{CZE} = 1$	$\alpha_k = \alpha_{CZE} = 1$	ρ = 1	_	_

Table 3.2 Types of theoretical models for α_{MEKC}

In order to describe and predict separation of charged analytes in MEKC, theoretical models of α_{MEKC} for two charged analytes in E quation 3.14 a re firstly proposed in this work, and classified into four types as listed in Table 3.2, based on the ranges of α_{CZE} , α_k , ρ and the order of $|\mu|$ in CZE and *k* in MEKC.

It should be noted that α_k is always ≥ 1.0 . In the case of Types I and II where the value of $\alpha_{CZE} > 1.0$, the same order of $|\mu|$ in CZE and k in MEKC, e.g. $k_2 > k_1$ and $|\mu_2| > |\mu_1|$. In case of Type III, the value of $\alpha_{CZE} < 1.0$ refers to the reversed order of $|\mu|$ in CZE and k in MEKC, e.g. $k_2 > k_1$ and $|\mu_2| < |\mu_1|$. Type IV, where $\alpha_k = 1.0$ and $\alpha_{CZE} = 1.0$, indicates co-migration of t wo charged a nalytes a nd t herefore, no resolution is obtained using either CZE or MEKC. In order to simply predict the values of α_{MEKC} for two charged analytes, the value of β in Equation 3.14 is assumed to be equal to 0.5. Figure 3.4 shows plots of the α_{MEKC} model of Types I–III over a wide range of k_1 . Practically, an increase in k may be obtained by an increase in the concentration of SDS ([SDS]) in an MEKC buffer.

Figure 3.4a is firstly considered. At a fixed value ρ except in the case $\rho \approx 1.0$, for example, $\alpha_k = 1.2, 1.4, 1.7, 2.2$ and 3.3 r espectively, the value of α_{MEKC} increases with an increase in k_1 to a maximum value, and then decreases at higher values of k_1 . At a fixed value of k_1 , the higher the value of α_k , the greater the value of α_{MEKC} . The k_1 giving the maximum α_{MEKC} value decreases as the value of α_k increases. It can be

concluded from the α_{MEKC} model of Type I, with the same order of $|\mu|$ in CZE and k in MEKC for charged analytes that higher α_k than α_{CZE} can improve α_{MEKC} for two charged analytes in MEKC.

In contrast to Type I, the α_{MEKC} model of Type II, where $\alpha_k \leq \alpha_{CZE}$, in Figure 3.4b shows that the value of α_{MEKC} decreases with an increase in k_1 , implying poorer separation for two charged analytes in MEKC. The addition of SDS surfactant in the BGE leads to a decrease of α_{MEKC} for two charged analytes.

Finally, the reversed order of $|\mu|$ in CZE and k in MEKC for two charged analytes as shown in F igure 3. 4c is discussed. It is seen that, the theoretical α_{MEKC} for the Type III m odel s tarts f rom l ess t han 1.0 ($1/\alpha_{MEKC} > 1.0$) t o ne ar 1.0 (poorer separation) with increasing k_1 and then higher than 1.0 (better separation) at higher k_1 values. At an α_{MEKC} of 1.0, the value of k_1 is given by Equation 3.15

$$k_{1} = \frac{(1 - \alpha_{CZE})}{(\alpha_{CZE} - \alpha_{k}) + (\alpha_{k} - 1)/\beta}$$
(3.15)

The small value of α_k gives a higher k_1 at α_{MEKC} 1.0, which is consistent with the bottom line for α_{MEKC} of 0.99 in Figure 3.4c. It should be noted that for a theoretical value of α_{CZE} or $\alpha_{MEKC} < 1.0$, the practical separation selectivity is equal to $1/\alpha_{CZE}$ or $1/\alpha_{MEKC}$. Therefore, an i ncrease i n k_1 may result i n a r eversed o rder o f electrophoretic mobility for two charged analytes in MEKC.

As can be seen in Figure 3.4, the theoretical model of α_{MEKC} can be employed to describe t he s eparation of t wo charged an alytes. The g reater t he α_{MEKC} value $(\alpha_k > 1.0)$, the greater the resolution. The better separation selectivity in MEKC over CZE c an be obtained for t he α_{MEKC} Type I ($\alpha_k > \alpha_{CZE}$), or T ype III m odels $(\alpha_k >> \alpha_{CZE}, \text{ or } \alpha_k > 1/\alpha_{CZE})$ at appropriate values of k_1 .

It should be noted that the direction of EOF velocity and total velocity does not affect the el ectrophoretic m obility o f an alytes an d m icelles, an d t he r etention f actor o f analytes i n MEKC. Owing to independence of t he v alues o f α_m and α_k with th e direction of these velocities, our proposed selectivity models can be used for MEKC with nor mal, r eversed a nd r estricted m odes c lassified b y the direction of EOF and total velocity as details given in Section 2.4.



Figure 3.4a Theoretical models of α_{MEKC} of two charged analytes in MEKC. Type I: $\alpha_k > \alpha_{CZE} \ge 1.0, \ \rho > 1.0.$ α_{MEKC} is obtained using E quation 3.14 a nd data in Table 3.2. a-e refer to the values of α_k for 1.2, 1.4, 1.7, 2.2, and 3.3, respectively.



Figure 3.4b Continued. Type II: $\alpha_{CZE} \ge \alpha_k \ge 1.0$, $\rho \le 1.0$. a-c refer to the values of α_k for 1.0, 1.2, and 1.5, respectively.



Figure 3.4c Continued. Type III: $\alpha_k \ge 1.0 > \alpha_{CZE}$, $\rho > 1.0$. a-e refer to the values of α_k for 1.0, 1.6, 3.2, 4.8 and 6.4, respectively.

3.3.2.3 Experimental and predicted values of a_{MEKC} in MEKC

Figure 3.5 shows an example of electropherograms of simultaneous separation of test analytes in MEKC using various concentrations of SDS. The retention factors for negatively charged p arabens, calculated using Equation 2.22 a nd Figure 3 .5, ar e shown in Table 3.3. The values of *k* were obtained in the order BP > PP > IP > EP, which are consistent with the magnitude order of octanol-water distribution constants in this series BP > PP > EP [Poouthree *et al.*, 2007; Golden, G andy, and V ollmer, 2005; Tavares *et al.*, 2009]. As seen in Figure 3.5c for MEKC separation with 60 mM SDS, the order of migration time or $|\mu_{MEKC}|$ is obtained to be BP > PP > IP > EP, while different orders are obtained in MEKC at 20 mM SDS (Figure 3.5a): BP > PP > EP > IP, and in CZE (Figure 3.3): EP > PP > BP > IP. These differences in migration behavior can be explained using the separation selectivity models in Section 3.3.2.2.

Figure 3.6 shows the observed and predicted values of α_{MEKC} for parabens in MEKC over a wide range of [SDS] (Figure 3.6a) and k_1 values (Figure 3.6b). The former is useful t o consider the [SDS] giving t he a chieve r esolution of a ll s olutes a nd t he reversed m igration, w hereas the l atter i s us eful t o c ompare t he obs erved a nd t he

predicted model without known [SDS]. The predicted values of α_{MEKC} at different [SDS] (6.0 to 60 m M) were calculated using data in Table 3.3 and Equation 3.14. Table 3.3 also lists the mobility s electivity, r etention s electivity, r etention factor, selectivity ratio, and p redicted models of α_{MEKC} . As previously mentioned, f or MEKC separation of a particular analyte pair, such as P P and IP, k_1 refers to the retention factor for the solute with smaller k, such as k_{IP} . U sing a wide r ange of [SDS] (20 to 60 mM), the observed k_1 can be plotted against [SDS] to derive a linear calibration pl ot, a llowing predicted values of k_1 at various [SDS] to be obtained. Using data in Table 3.3 and Equation 3.14, the observed values of α_{MEKC} in Figure 3.6 were found to be in good a greement with the predicted values, indicating that Equation 3.14 c an be used for prediction of the α_{MEKC} values over a wide range of [SDS] and k_1 .

Pair	Solute	$k_1 = a[SDS]+b$	α_{CZE}	α_k	β	ρ	Types of model for α_{MEKC} in MEKC
IP/EP	EP	0.00236[SDS]-0.013	0.888	$k_{\rm IP}/k_{\rm EP}$	0.575	ρ > 1.0	III
PP/IP	IP	0.00871[SDS]-0.028	1.066	$k_{\mathrm{PP}}/k_{\mathrm{IP}}$	0.511	ρ > 1.0	Ι
BP/PP	PP	0.01004[SDS]-0.035	0.953	$k_{\mathrm{BP}}/k_{\mathrm{PP}}$	0.544	ρ > 1.0	III
	BP	0.03068[SDS]-0.057	-	-	-		-

Table 3.3 Mobility selectivity (α_{CZE}), retention selectivity (α_k), retention factor (k_1), selectivity ratio (ρ), and types of α_{MEKC} model



Figure 3.5 Electropherograms of separation of IP, BP, PP and EP in MEKC using (a) 20, (b) 40, and (c) 60 mM SDS in a 10 mM $Na_2B_4O_7$ buffer adjusted to pH 10.2 with 1.0 M NaOH. CE conditions: uncoated fused silica 50 µm i.d. × 40.2 cm (30 cm to detector), temperature 25 °C, voltage 15 kV, 0.5 psi pressure injection for 3 s and UV detection at 220 nm.



Figure 3.6 Observed (symbols) and predicted (solid lines) values of α_{MEKC} for two charged analytes in MEKC. (a) Various concentrations of SDS and (b) various values of k_1 . Symbols \bullet , \bullet , and \blacktriangle refer to pairs of BP/PP, PP/IP, and IP/EP, respectively. Predicted values are obtained using Equation 3.14 and data as listed in Table 3.3.

According to electropherograms in Figure 3.5 and data in Table 3.3, the same order of $|\mu|$ in CZE and k in MEKC was obtained for PP/IP, and therefore $\alpha_{CZE} > 1.0$ and $\alpha_{MEKC} > 1.0$. Although the ρ value is greater than 1.0, a slight d ecrease in the observed and predicted values of α_{MEKC} with an increase in [SDS] and k_1 is due to small calculated v alues of ρ between 1.032 and 1.072 f or 10 t o 60 m M S DS. Therefore, a change in α_{MEKC} for PP/IP in MEKC is consistent with the α_{MEKC} model of Type I described in Section 3.3.2.2 with small values of ρ .

Owing to the reversed order of $|\mu|$ in CZE and k in MEKC for IP/EP and BP/PP, and the theoretical value of α_{CZE} being less than 1.0, the reversed $|\mu|$ order for IP/EP and BP/PP at high [SDS] and at low or zero [SDS] is consistent with the α_{MEKC} Type III model. At an α_{MEKC} value of 1.0, t he predicted values of k_1 in Fi gure 3.6b ar e estimated to be 0.003 for BP/PP at very low [SDS], and 0.052 for IP/EP which is in good agreement with the observed k_1 of 0.064. It should be noted that, employing Equation 3.15 with an average α_k of 3.831 f or IP/EP at 6.0 t o 60 m M S DS, the predicted values of k_1 of 0.057 g iving α_{MEKC} of 1.0 are found to be good agreement with value of k_1 of 0.052 in Figure 3.6b.

3.4 Conclusion

Micellar el ectrokinetic chromatography (MEKC) i s o ne o f t he m odes i n cap illary electrophoresis w hich i s performed b y the addition of a surfactant i nto the running buffer, t o form m icelles a cting as a ps eudo-stationary pha se. T he s eparation of charged co mpounds i n M EKC de pends on t he di fference i n e ither m icellar partitioning o r th eir electrophoretic mo bilities (μ). M EKC s eparation s electivity (α_{MEKC}), defined as the ratio of their μ , is one of the characteristics used to describe separation o f t wo an alytes. In or der t o e xplain t he s eparation s electivity a nd electrophoretic mobility or der of f ully charged a nalytes i n M EKC, e quations a nd theoretical models for α_{MEKC} which is related to the dimensionless values of mobility selectivity (α_{CZE}) in c apillary z one el ectrophoresis (CZE) and r etention s electivity

(α_k) in MEKC were established, where α_{CZE} and α_k are defined as the ratio of μ in CZE a nd t he r atio of r etention f actor (k) i n M EKC f or t wo c harged a nalytes, respectively. Theoretical models for α_{MEKC} can be classified into four types based on the order of $|\mu|$ in CZE, k in MEKC and the selectivity ratio ($\rho = \alpha_k/\alpha_{CZE}$). The α_{MEKC} Type I (the same order of $|\mu|$ in CZE and k in MEKC with $\rho > 1.0$), MEKC separation of two charged analytes can enhance α_{MEKC} up to the maximum value with increasing the SDS concentration, while the α_{MEKC} Type II (the same order of $|\mu|$ in CZE and k in MEKC than CZE is obtained with $\rho \le 1.0$ ($\alpha_{CZE} \ge \alpha_k \ge 1.0$). The α_{MEKC} Type III (the reversed order of $|\mu|$ in CZE and k in MEKC with $\rho > 1.0$) can give the reversed order of the μ in MEKC results in worse s eparation in MEKC than CZE. F or the α_{MEKC} Type IV with α_{CZE} of 1.0 and α_k of 1.0 ($\rho = 1.0$), no resolution is obtained in either CZE or MEKC. Using four alkylparabens as test analytes, excellent a greement was found between the observed α_{MEKC} and the proposed α_{MEKC} models of test analytes in MEKC over a wide range of SDS concentrations and values of k.

CHAPTER IV

INVESTIGATION OF NEUTRAL MONOLITHIC CAPILLARY COLUMNS WITH VARYING *n*-ALKYL CHAIN LENGTHS IN CAPILLARY ELECTROCHROMATOGRAPHY

4.1 Introduction

CEC employing organic polymer-based monolithic stationary phases is increasingly used as an effective separation method due in major part to the ease of the *in situ* polymerization of vinyl-based monomers in capillaries and microchannels [Eeltink, and Svec, 2007; Karenga, and El Rassi, 2011c; Svec, 2009, 2010], which has allowed the realization of tailor made stationary phases for the separation of a wide range of species [Faure et al., 2008; Karenga, and El Rassi, 2010a; Lu et al., 2009]. Recently, and t o w iden t he s cope of applications o f C EC t o e ncompass bi omolecules i.e. peptides and proteins, El R assi's r esearch group has introduced a series of n eutral nonpolar monoliths with surface bound C 17, C18 and naphthyl ligands for RP-CEC of charged species (including proteins and peptides) in the absence of electrostatic interactions with fixed surface charges while a ffording relatively moderate EOF velocity [Karenga, and El Rassi, 2008, 2010a, 2010b, 2010c; Okanda, and El Rassi, 2005]. Customarily, the fixed surface charges have been intentionally introduced to support the EOF [Lu et al., 2009; Augustin et al., 2008; Bedair, and El Rassi, 2002, 2003], a f act that led to the nuisance el ectrostatic interactions, which c aused ei ther band broadening or i reversible binding of charged solutes such a sproteins and peptides. In the new generation of neutral no npolar monoliths [Karenga, and E1] Rassi, 2008, 2010a, 2010b, 2010c; Okanda, and E1 R assi, 2005], the EOF resulted from t he a dsorption of mobile phase i ons t o t he ne utral m onolithic s urface, t hus imparting this surface with the zeta potential required to support the EOF necessary for s olute t ransport across t he c olumn. The magnitude of t he E OF ha s b een conveniently adjusted by the pH and A CN c ontent of t he m obile ph ase. The

This work has been published in Electrophoresis DOI 10.1002/elps.201200018.

separation s electivity, r etention a nd m agnitude of t he E OF ha ve be en f urther modulated b y m ixed ligands (i.e. C18/naphthyl ligands) m onolithic c olumns [Karenga, and E I R assi, 2011a] as well as by segmented monolithic columns consisting of octadecyl and na phthyl monolithic segments [Karenga, and El R assi, 2011b]. Although other researchers have also developed neutral monoliths for RP-CEC [Dong et al., 2004; Li et al., 2004; Zhang et al., 2003], these were s parse attempts a nd t he de scribed ne utral m onoliths were not e ffective i n t he C EC of peptides and proteins. Briefly, in the first attempt, Zhang et al. [Zhang et al., 2003] developed a neutral monolith, which was prepared by the copolymerization of butyl methacrylate and ethylene dimethacrylate (EDMA). This neutral monolith exhibited a weak E OF, and therefore, the separation of small acidic solutes was achieved through their differential electromigration. Similarly, a n eutral monolithic column was prepared by the copolymerization of lauryl methacrylate and EDMA that was applied to RP-CEC of ionic analytes whereby their separation was realized with their electrophoretic mobility as the driving force [Dong et al., 2004]. In another report, a monolithic c apillary c olumn whose i nner w all grafted with p olyethyleneimine to support the generation of an annular EOF was developed [Li et al., 2004]. The actual monolith was made by in situ copolymerization of vinylbenzene chloride and EDMA. This monolith permitted the separation of short peptides at pH 2.5 where the peptides are also positively charged as the an nular polyethyleneimine coating to avoid electrostatic attractions between the peptides and the annular coating.

As a continuation of this recent efforts in developing neutral nonpolar monoliths for the R P-CEC of ch arged s pecies in t he ab sence of electrostatic i nteractions, t wo different neutral nonpolar monolithic columns series (designated as A and B columns series) each consisting of three columns at varying *n*-alkyl chain length (i.e. C8, C12 and C 16) w ere pr epared a nd c haracterized ove r a w ide r ange of m obile pha se composition. In the A columns series, the composition of the functional monomers and c rosslinker w as a djusted t o yield c omparable c hromatographic r etention regardless of the alkyl chain length while in the B columns series, the composition of the f unctional m onomers a nd c rosslinker w as ke pt c onstant yielding va riable chromatographic r etention. The t wo c olumns s eries were d emonstrated in th e separation of neutral (nonpolar and polar) and charged species such as proteins and peptide mapping.

4.2 Experimental

4.2.1 Reagents and materials

Pentaerythritol tr iacrylate (PETA), dodecyl ac rylate (C12-acrylate), 2,2 'azobisisobutyronitrile (AIBN), 3 -(trimethoxysilyl)propyl m ethacrylate, be nzene, alkylbenzenes (ABs), alkyl phe nyl k etones (APKs), ni troalkanes (NAs), phe nols, anilines, and analytical-grade acetone were purchased from Aldrich (Milwaukee, WI, USA). Octyl methacrylate (C8-methacrylate) and cetyl methacrylate (C16methacrylate) were from Polysciences (Warrington, PA, USA). Cyclohexanol was purchased from J.T. Baker (Phillipsburg, NJ, USA). Ethylene glycol (EG), HPLCgrade acetonitrile (ACN), and nitric acid were from Fischer Scientific (Fair Lawn, NJ, USA). The following proteins were purchased from Sigma (St. Louis, MO, USA): chicken egg w hite l ysozyme, e quine he art c ytochrome C, bovi ne pa ncreas ribonuclease A, ov albumin, and bovi ne pancreas α -chymotrypsin. TPCK trypsin from bovine pancreas was also purchased from Sigma (St. Louis, MO, USA). Equine heart c ytochrome C tryptic di gestion w as p erformed a fter p rotein r eduction a nd alkylation using the Promega protocol. Buffer solutions were prepared using sodium phosphate monobasic from Mallinckrodt (Paris, KY, USA).

4.2.2 CE conditions

The i nstruments us ed i n t his i nvestigation w ere a P/ACE 2200 a nd P/ACE 5510 system CE from Beckman (Fullerton, CA, USA) equipped with a fixed wavelength UV de tector, and a phot odiode a rray d etector, r espectively. All e lectrochromatograms w ere r ecorded w ith a p ersonal c omputer r unning G old P/ACE s oftware. T he uncoated f used-silica c apillary 2 7 c m in length (20 c m t o detector) × 100 μ m i.d. (Polymicro T echnologies, A Z, U SA) w as us ed f or C EC separations, thermostated at 25 °C. The samples w ere i njected electrokinetically at

various times and applied voltages, which are stated in the figure captions. Prior to CEC separation each day, the monolithic column was conditioned with the running buffer using a syringe pump for 30 m in. Thereafter, the column was placed in the CEC in strument for conditioning at the running vol tage until a stable current and baseline were observed.

4.2.3 Column fabrication

The fabrication of organic polymer based-monolithic column can be divided into two main steps and the details as describes in Sections 4.2.3.1 and 4.2.3.2. The monomers used in the process of column fabrication are shown in Figure 4.1



pentaerythritol triacrylate (PETA)

3-(trimethoxysilyl)propyl methacrylate

Figure 4.1 Chemical structures of monomers used in the column fabrication: octyl methacrylate (C8-methacrylate), dodecyl acrylate (C12-acrylate), cet yl methacrylate (C16-methacrylate), pentaerythritol triacrylate (PETA), and 3-(trimethoxysilyl)propyl methacrylate.

4.2.3.1 Column pretreatment

Prior to the polymerization step, the inner wall of the fused-silica capillary was treated with 1.0 M sodium hydroxide for 30 min, flushed with 0.1 M hydrochloric acid for 30 min, a nd t hen r insed with w ater f or 30 m in. The c apillary i nner w all w as t hen allowed to react with a solution of 50% v/v of 3-(trimethoxysilyl)propyl methacrylate in acet one f or 6 h at r oom t emperature t o v inylize t he i nner wall o f th e c apillary. Finally, t he c apillary w as r insed w ith a cetone a nd t hen dr ied with a s tream of nitrogen. The process of column pretreatment is shown in Figure 4.2.



Figure 4.2 Schematic diagram of column pretreatment procedure.
4.2.3.2 In situ polymerization

Polymerization s olutions w ere pr epared f rom *n*-alkyl a crylate o r m ethacrylate functional monomers with C8, C12, or C16 alkyl chains, the crosslinking monomer PETA a nd po rogenic s olvents, a nd all m ixed i nt her atio o f 20:80 w /w monomers/porogenic solvents. The mixtures of monomers were weighed in different ratios, and then dissolved in a ternary por ogenic solvent consisting of cyclohexanol and ethylene glycol in various ratios at constant 3.6 wt% water, the details as shown in Table 4.1. AIBN (1.0 wt% with respect to monomers) was added to the solution as the free radical initiator. The polymerization solutions was then mixed with a vortex mixer to obtain clear solutions, and degassed with ni trogen for 10 m in. A 30 c m pretreated capillary (see Section 4.2.3.1) was filled with the polymerization solution up to 21 cm by immersing the inlet of the capillary in the solution vial and applying vacuum to the capillary outlet. The capillary ends were then sealed using GC septa, and the capillary was put in a 60 °C GC oven for 12 h. The resulting monolith was washed w ith a n 80: 20 v/v a cetonitrile:water m ixture us ing a n H PLC pum p. A detection window was created at 1 to 2 mm after the end of the polymer bed using a thermal wire stripper. Finally, the column was cut to a total length of 27 cm with an effective length of 20 cm. The overall process is shown in Figure 4.3.

Column/monolith designation	<i>n</i> -Alkyl chain length monomer		DI ()	EOF	k		
	designation	mmol ^a	Plates/m [*]	(mm/s)	pentyl benzene	hexyl benzene	heptyl benzene
1A ^c	C8	0.58	150,000	1.15	1.94	2.71	3.82
2A ^c	C12	0.47	162,000	1.10	1.86	2.64	3.75
3A ^c	C16	0.26	200,000	1.03	1.62	2.42	3.40
$1B^d$	C8	0.48	128,000	0.90	1.58	2.21	3.12
$2B^d$	C12	0.48	93,000	0.90	1.94	2.78	4.01
$3B^d$	C16	0.48	62,000	0.86	2.52	3.66	5.35

Table 4.1 Composition of t he pol ymerization s olutions us ed i n the pre paration of t he different monolithic c olumns. Capillary c olumn, 27 c m t otal l ength, 20 c m e ffective length \times 100 µm i.d.; mobile phase, 75% ACN (v/v) in 1.0 mM sodium phosphate buffer, pH 7.0; voltage, 15 kV.

^aAmount of *n*-alkyl monomer used in the polymerization mixture.

^bThe average values taken for benzene and the first seven alkylbenzenes series.

^cPolymerization solutions contained 0.07, 0.13, and 0.15 mmol PETA for the monolithic columns 1A, 2A, and 3A, respectively (i.e. the A columns series).

^dPolymerization solutions contained 0.07 mmol PETA (i.e. the B columns series).



Figure 4 .3 Schematic d iagram o f co lumn f abrication. Adapted f rom Svec *et a l*. [2000].

4.2.4 Preparation of mobile phase

The CEC mobile phase solutions were prepared by pipetting the appropriate amounts of stock aqueous solution of 100 mM phosphate buffer into a 25 mL volumetric flask, followed by adding appropriate volumes of ACN. Thereafter, the final solution was made up to 25 mL with DI water. All buffers were sonicated for 30 min prior to use. It should be note that the stock aqueous solution of 100 mM phosphate buffer was prepared by adjusting a phos phate buffer with a 1.0 M phos phoric a cid or 1.0 M NaOH solution to desire pH.

4.2.5 Preparation of analytes

An appropriate amount of each analytes was separately dissolved in ACN in a 5 mL volumetric flask to give 0.1 M stock solutions. Stock solution of thiourea was also separately dissolved in DI water in a 5 mL volumetric flask to give 0.1 M stock solutions. Each protein was separately dissolved at a concentration of 5.0 m g/mL in DI water. The mixture of proteins at the concentration of 1.0 mg/mL was obtained by diluting 5.0 m g/mL of each proteins and and 1.0 mM thiourea, and then diluting the

mixture with a running mobile phase. Other working standard solutions of each set of test analytes containing 2.0 mM of each test analytes and 1.0 mM thiourea were also prepared by diluting each of the stock solutions with a running mobile phase. All solutions were sonicated for 10 min prior to CEC analysis.

The pr eparation of t he s amples o f peptides was done b y t ryptic digestion of cytochrome C after r eduction and a lkylation following the Promega protocol. The stock s olution of t he di gest p rotein w as m ade in D I water b efore d iluting it in a concentration of 1.0 mg/mL for CEC analysis.

4.3 Results and Discussion

4.3.1 Column fabrication and characterization

4.3.1.1 Porogens and monomers composition

Very r ecently, a neutral oc tadecyl m onolith (ODM) with C18 c hains for e nhanced retention and selectivity has developed [Karenga, and El Rassi, 2008]. In their work, a ternary porogenic solvent made of cyclohexanol, ethylene glycol (EG), and water in the r atio 75.7: 20.7:3.6 wt% pr oved t o be t he opt imal por ogen t o obt ain a n O DM monolith with reasonable EOF and high separation efficiency. Initially, in the present investigation, the C16 monolith was prepared by free radical polymerization using two different initiators, AIBN (1.0 wt% with r espect t o m onomers) and ni tric a cid [Wang et a l., 2010] (0.06 m mol), and a ternary porogenic s olvent i ntroduced by Karenga and El Rassi [Karenga, and El Rassi, 2008] and made of cyclohexanol, EG, and water in the ratio 75.7: 20.7:3.6 w t% for the former in itiator and in the ratio 82.5:14.9:2.5 wt% for the latter initiator. Using 30:70 %wt of monomers (functional monomer and PETA crosslinker) to porogen, the latter monolithic column with the nitric a cid i nitiator pr ovided hi gh s eparation e fficiency o f 145,000 pl ates/m f or benzene and ABs (Figure 4.4a), and up to 204,000 plates/m for proteins (Figure 4.4b), while the former column with the AIBN initiator gave very low permeability in a pressure d riven flow a nd l ow s eparation e fficiency i n C EC. H owever, t he l atter monolithic column (i.e. that prepared in the presence of nitric acid) was not stable, and therefore, A IBN was chosen as the free radical initiator for fabricating further columns throughout the study.

In an attempt to produce C8-, C12-, and C16- monolithic columns with acceptable permeability us ing a p ressure dr iven f low, pol ymerization s olutions w ith hi gher content in por ogen in the ratio of monomers to por ogen of 20:80 %wt were used. Table 4.1 s hows the r esults of C 8-, C 12-, and C 16- monolithic c olumns pr epared using constant and different amounts (mmol) of the functional monomers (C8, C12 and C16 acrylate or methacrylate monomers) and the crosslinking monomer PETA. On the other hand, the optimum composition of the ternary por ogenic s olvent was determined by increasing the %wt of macroporogen EG while decreasing the %wt of microporogen c yclohexanol. These attempts r esulted in the monoliths with higher separation efficiency in CEC and higher permeability using a pressure driven flow. The optimal column efficiency and reasonable EOF were obtained with a porogen composed of 68.8 w t% cyclohexanol, 27.7 w t% EG, and 3.6 w t% water. The C8-, C12-, and C16- monoliths prepared from variable monomer composition are referred to as 1A, 2A, and 3A columns (the A columns series), respectively, the details are shown in Table 4.1. The amount of functional monomer for the A monoliths series was increased in the order C8 > C12 > C16, resulting in the slightly higher retention factor (k) of ABs on C8 and C12 than on C16. The longer alkyl chain length monolith yielded t he h igher s eparation e fficiency. Figure 4.5 a s hows t he E OF v elocity increased with increasing the macroporogen content (i.e. EG content) of the monolith most likely due to the reduction of the electric double layers overlap as a result of the increased macroporosity of the monoliths. As shown in Table 4.1 and Figure 4.5a, the shorter the alkyl chain length, the higher the EOF velocity. This indicates stronger mobile phase ions adsorption as the alkyl chain length decreases. As can be seen in Figure 4.5b, i ncreasing t he m acroporogen content i n t he pol ymerization m ixture increases the separation efficiency. This may be due to increasing the monolith pore size with higher m acroporogen c ontent t hat l eads t o r educing t he m ass t ransfer resistance and consequently increasing the separation efficiency. It should be noted that in the A columns series, the compositions of the monomers were adjusted to yield

a chromatographic retention of more or less the same order of magnitude, see Table 4.1.

Another s et o f t he C 8-, C 12-, a nd C 16- monoliths w as pr epared b y k eeping t he composition of the functional monomers and the crosslinker PETA constant, and the resulting monoliths are referred to as 1B, 2B, and 3B columns (the B columns series), respectively (see T able 4.1). In all cases, the p orogen w as composed o f 72.8 w t% cyclohexanol, 23.7 wt% EG, and 3.6 wt% water. The *k* values of ABs increased with increasing the alkyl ch ain length as in principle should be t he cas e. As shown in Table 4.1, the separation efficiency obtained on the monolithic columns with the same composition of the polymerization mixture (i.e. the B columns series) was lower than that of t he variable ones (i.e. the A columns series). In the B columns series, the column made with the shorter alkyl chain length yielded higher separation efficiency than the longer on e. This is d ue primarily to the f act th at a shorter analysis time would a llow less band s preading t hat a rises from longitudinal m olecular di ffusion assuming that everything else has remained the same.



Figure 4.4 Electrochromatograms of benzene and AB hom ologous series in (a) and some standard proteins in (b). C16 capillary column for which ni tric was us ed as initiator, 20 cm effective length, 27 cm to tal length \times 100 µm i.d.; mo bile p hase, 1.0 mM in (a) and 10 mM in (b) sodium phosphate monobasic, pH 7.0, at 65 % ACN (v/v) in (a) and 45% ACN (v/v) in (b), running voltage 15 kV in (a) and 10 kV in (b); EOF tracer, thiourea; electrokinetic i njection for 3 s at 10 kV . Solutes in (a): 1, benzene; 2, toluene; 3, e thylbenzene; 4, pr opylbenzene; 5, but ylbenzene; 6, pentylbenzene; 7, he xylbenzene; 8, he ptylbenzene. Solutes in (b): 1, l ysozyme; 2, cytochrome *C*; 3, ribonuclease A; 4, α -chymotrypsin.



Figure 4.5 Effect of w t% m acroporogen in the polymerization solution for three monolithic columns prepared from polymerization solution at different *n*-alkyl chain length on the apparent EOF velocity in (a) and the average plate number per meter in (b). 1A, 2A, and 3A capillary columns, 20 cm effective length, 27 cm total length \times 100 µm i.d.; mobile phase, 1.0 mM sodium phosphate monobasic, pH 7.0, a t 75 % ACN (v/v), running voltage 15 kV ; electrokinetic injection for 3 s at 10 kV. The average plate number per meter is the average taken for benzene and the first eight AB homologous series: benzene, toluene, ethylbenzene, propylbenzene, butylbenzene, pentylbenzene, hexylbenzene, and heptylbenzene. EOF tracer, thiourea.

4.3.1.2 Van Deemter plots

The A columns series i.e. 1A, 2A and 3A columns were further evaluated in terms of the plate height versus linear flow velocity by varying the operating voltage from 8 to 25 kV. F igure 4.6 shows the van Deemter plots obtained with benzene and the first seven ABs series on the three monolithic columns at varying alkyl chains length in their polymeric networks (i.e. columns 1A, 2A, and 3A). C olumns 1A, 2A and 3A were prepared from polymerization solutions at 0.58, 0.47, and 0.26 mmol functional monomers, respectively. T he curves show that the H_{min} value has nearly stabilized over the velocity range from ~1.0 to ~1.5 mm/s, which corresponds to 1 ittle or no variation in the separation efficiency over this linear flow velocity range. This may be an indication of an efficient solute mass transfer characteristic within the porous monoliths. The monolithic column 3A (C16 ligand) seems to be a good compromise as far as the efficiency and EOF velocity are concerned. T his column exhibited the highest s eparation efficiency r eaching a value of 209,000 pl ates/m at about 1.33 mm/s.



Figure 4.6 van Deemter plots showing average height as a function of apparent EOF velocity for 1A, 2A, and 3A capillary columns, 20 c m effective length, 27 cm total length \times 100 µm i.d.; mobile phase, 1.0 mM sodium phosphate monobasic, pH 7.0, at 75 % A CN (v/v), electrokinetic injection for 3 s at 10 kV. The plate height is the average t aken f or t he f irst e ight A B hom ologous s eries: benzene, t oluene, ethylbenzene, pr opylbenzene, but ylbenzene, pe ntylbenzene, h exylbenzene, heptylbenzene. EOF tracer, thiourea.

4.3.1.3 Reproducibility of column fabrication

The reproducibility of c olumn production was assessed through the percent relative standard deviation (%RSD) for the retention time of EOF marker (t_0), retention factor (k) of heptylbenzene, and the separation efficiency (N) of benzene and the first seven of the ABs series using a mobile phase containing 75% v/v ACN in 1.0 mM sodium phase buffer, pH 7.0. Table 4.2 s hows the ov erall %RSD from c olumn-to-column (n=3) for the EOF velocity, retention factor, and separation efficiency on columns 1A, 2A, and 3A. These reproducibility data agree with those previously reported for other monoliths [Karenga, and El Rassi, 2010a, 2010b].

Table 4.2 The over all %RSD f rom c olumn-to-column (n = 3) of ve locity (t_0), retention factor (k), and separation efficiency (N) reproducibilities.

	RSD (%)					
Column	to	lr.	N			
	(min)	ĸ	(plates/m)			
1A (C8)	2.3	4.1	11			
2A (C12)	1.4	1.4	9.3			
3A (C16)	2.1	2.3	10			

4.3.1.4 The driving force of EOF

The A columns series a re void of fixed charges, and therefore, they have no z eta potential with respect to water. As can be seen in Figure 4.7, the magnitude of the EOF depends on the pH and the ACN content of the mobile phase. This is indicative of the a dsorption of e lectrolyte i ons of the mobile phase to the monolithic surface, which i mparts the monoliths with the z eta potential ne cessary to support the EOF. The ability of the monoliths to adsorb phosphate ions from the mobile phase can be traced to the presence of polar ester groups in the C8, C12, and C16 monomers and the crosslinker P ETA a s well as the hydroxyl group in P ETA. U nder the mobile phase conditions used, the direction of the EOF is from anode to cathode, indicating that the zeta potential is negative. Figure 4.7a shows the EOF is somewhat increased in the pH range 4.0 to 5.0 and then increased sharply at pH 5.0 to 7.0. In the pH range 5.0 to 7.0, the amount of the adsorbed phosphate ions are more ionized, carrying each

ion a double negative charge thus producing the sharp rise in EOF, while at pH 4.0 most of t he phos phate i ons ha ve a s ingle n egative c harge, t hus explaining t he relatively lower EOF. Good agreement was found between this observation and that reported earlier with C17, C18, and NMM neutral monoliths based on pentaerythritol diacrylate m onostearate, o ctadecyl acr ylate, and n aphthyl m ethacrylate m onomers, respectively [Okanda, and El Rassi, 2005; Karenga, and El Rassi, 2008, 2010b].

As can be seen from Figure 4.7b, the A columns series exhibited an increase in EOF velocity upon increasing the ACN content of the mobile phase due to an increases in phosphate i ons a dsorption to the monolithic surface. The shorter is the alkyl chain length the higher is the EOF velocity. This indicates stronger mobile phase i ons adsorption as the alkyl chain length decreases. Despite the fact that increasing the ACN content d ecreases the d ielectric constant of the mobile phase, which may diminish the ionization of the adsorbed phosphate i ons, the concomitant decrease in the viscosity of the mobile phase and increase in the amount of adsorbed phosphate ions to the monolithic surface would be the two major contributors to increasing the EOF velocity at high ACN concentration in the mobile phase. It is believed that the adsorption of the phosphate i ons to the monolith surface is of a polar type and the extent of which would increase with the ACN content of the mobile phase. This observation is similar to that previously reported with different ne utral monoliths. [Okanda, and El Rassi, 2005; Karenga, and El Rassi, 2008, 2010a, 2010b, 2010c]

4.3.2 Evaluation of chromatographic retention

4.3.2.1 Neutral nonpolar solutes

The A columns series were evaluated for their performance with three homologous series i ncluding A Bs, A PKs, a nd N As, which a re t ypical model s olutes of high, moderate, a nd l ow h ydrophobic c haracter, r espectively. Figure 4.8 shows t ypical electrochromatograms for benzene and its alkyl derivatives which are the first seven ABs hom ologous s eries obt ained on t he three columns. Column 3A bearing the longest C 16 c hain on i ts surface yielded the highest theoretical plate count for the

separation of benzene and the first seven ABs series in less than 14 min. Under the same mobile phase composition and applied voltage, the magnitude of retention order was ABs > APKs > NAs, which is consistent with that of the hydrophobic order of the homologous ABs > APKs > NAs. In fact, whereas the rapid separation of ABsnecessitated the use of 75% (v/v) ACN in the mobile phase, that of APKs and NAs required 70 % (v/v) A CN and 35% (v/v) ACN in the mobile phase, r espectively. Under t hese c onditions, f or A PKs (up t o he ptanophenone) t he analysis t ime w as slightly less than 6.0 min on C16 column, and approximately 6.5 min on C8 and C12 columns while for NAs (up to nitrohexane) the analysis time was approximately 11.3 min on C16 column, approximately 11.5 min on C12 column and approximately 11.8 min on C 8 column. These observations, which are indicative of a typical reversed phase chromatographic retention mechanism, were further confirmed by the linearity of the p lots of logarithmic $k (\log k)$ versus % ACN in the mobile phase for A Bs, APKs, and N As over a wide range of A CN concentration on t he 3A monolithic column, the results are shown in Figure 4.9. Furthermore, the magnitude order of kvalues ABs > APKs > NAs were in accordance to their relative hydrophobicity order ABs > APKs > NAs. This is a nother indicative of a r eversed p hase r etention mechanism. The slopes of the lines in each set of solutes increased with increasing the s ize of t he s olute. These b ehaviors w ere a lso c onserved w ith 2 A a nd 1 A monoliths, results are shown in Figures 4.10 and 4.11, respectively. It should be noted that the amount of the functional monomers for the A series such as 1A, 2A, and 3A monoliths, increased in the order C8 > C12 > C16, and the shorter alkyl chain length the higher is the EOF velocity (see Figure 4.7). This explains the slightly higher k values or s lightly l onger s eparation t ime on C 8 and C 12 t han on C 16 monoliths. In short, a monolith with short alkyl chain (i.e. C8 or C12) at relatively high functional monomer content would a ccomplish as much retention as a longer alkyl chain length such as C16. But, this would be at the expense of lower separation efficiency. Therefore, and for difficult separations that would require high separation efficiency, one would consider a longer a lkyl chain monolith at optimal functional monomer content (i.e. C16) with slightly lower retention and faster analysis time.



Figure 4.7 Plots of the apparent EOF velocity versus the pH of the mobile phase in (a) and the % ACN (v/v) in the mobile phase in (b) for 1A, 2A, and 3A monolithic columns, 20 cm effective length, 27 cm total length \times 100 µm i.d.; mobile phase, 1.0 mM sodium phos phate monobasic at various pHs and 50 % ACN (v/v) in (a) and various % A CN (v/v) in 1.0 m M sodium pho sphate monobasic, pH 7.0, in (b); running voltage 25 kV, electrokinetic injection for 3 s at 10 kV. EOF tracer, thiourea.



Figure 4.8 Electrochromatograms of be nzene a nd A B hom ologous s eries us ing columns with different *n*-alkyl chain length, 20 cm effective length, 27 cm total length \times 100 µm i.d., 1A: C8 column in (a), 2A: C12 column in (b) and 3A: C16 column in (c); mobile phase, 1.0 mM sodium phosphate monobasic, pH 7.0, at 75 % ACN (v/v), running voltage 15 kV; electrokinetic injection for 3 s at 10 kV. EOF tracer, thiourea, solutes: 1, benzene; 2, toluene; 3, ethylbenzene; 4, propylbenzene; 5, butylbenzene; 6, pentylbenzene; 7, hexylbenzene; 8, heptylbenzene.



Figure 4.9 Plots of log *k* for (a) ABs, (b) APKs, and (c) NAs versus % ACN (v/v) in the mobile phase for 3A : C16 capillary column, 20 cm effective length, 27 cm total length × 100 µm i.d.; mobile phase, 1.0 m M sodium phos phate monobasic, pH 7.0, running voltage 25 kV, electrokinetic injection for 3 s at 10 kV. EOF tracer, thiourea. Solutes i n (a) 1, b enzene; 2, t oluene; 3, e thylbenzene; 4, pr opylbenzene; 5, butylbenzene; 6, pe ntylbenzene; 7, he xylbenzene; 8, he ptylbenzene; (b) 1, acetophenone; 2, pr opiophenone; 3, but yrophenone; 4, va lerophenone; 5, hexanophenone; 6, he ptanophenone; (c) 1, ni tromethane; 2, ni troethane; 3, nitropropane; 4, nitrobutane; 5, nitropentane; and 6, nitrohexane.



Figure 4.10 Plots of log *k* for (a) ABs, (b) APKs, and (c) NAs versus % ACN (v/v) in the mobile phase for 2A: C12 capillary column, 20 cm effective length, 27 cm total length \times 100 µm i.d.; mobile phase, 1.0 m M sodium phos phate monobasic, pH 7.0, running voltage 25 kV, electrokinetic injection for 3 s at 10 kV. EOF tracer, thiourea. Solutes i n (a) 1, b enzene; 2, t oluene; 3, e thylbenzene; 4, pr opylbenzene; 5, butylbenzene; 6, pe ntylbenzene; 7, he xylbenzene; 8, he ptylbenzene; (b) 1, acetophenone; 2, pr opiophenone; 3, bu tyrophenone; 4, va lerophenone; 5, hexanophenone; 6, he ptanophenone.; (c) 1, ni tromethane; 2, ni troethane; 3, nitropropane; 4, nitrobutane; 5, nitropentane; and 6, nitrohexane.



Figure 4.11 Plots of log *k* for (a) ABs, (b) APKs, and (c) NAs versus % ACN (v/v) in the mobile phase for 1A : C8 c apillary c olumn, 20 c m e ffective length, 27 c m total length \times 100 µm i.d.; mobile phase, 1.0 m M sodium phosphate monobasic, pH 7.0, running voltage 25 kV, electrokinetic injection for 3 s at 10 kV. EOF tracer, thiourea. Solutes i n (a) 1, b enzene; 2, t oluene; 3, e thylbenzene; 4, pr opylbenzene; 5, butylbenzene; 6, pe ntylbenzene; 7, he xylbenzene; 8, he ptylbenzene; (b) 1, acetophenone; 2, pr opiophenone; 3, but yrophenone; 4, va lerophenone; 5, hexanophenone; 6, he ptanophenone.; (c) 1, ni tromethane; 2, nitroethane; 3, nitropropane; 4, nitrobutane; 5, nitropentane; and 6, nitrohexane.

4.3.2.2 Slightly polar solutes

Figure 4.12 illustrates the separation of six phenols on the A columns series using a mobile phase at 50% v/v A CN for 1A column and 45% v/v A CN for 2A and 3A columns, and at pH 7.0 to bring about similar analysis time and base line resolution among the three columns. O ne of these phenols, na mely 2,4 -dichlorophenol (last eluting solute) with pK_a of 7.85, is very slightly ionized at the operating pH, while all other phenols under investigation with $pK_a \ge 8.5$ are largely undissociated and can be considered as neutral solutes. 2,4-Dichlorophenol seems to broaden (noticeably on the 1A column) m ay be due to its relatively higher m igration t ime, which would translate i nto i ncreased longitudinal m olecular di ffusion. The phenols investigated eluted in the or der of d ecreasing pol arity on the three columns, a behavior that is typical of RP-CEC. For instance, phenol and hydroxyphenol (i.e. quinol < phenol) are less retained than monochlorophenols (4-chlorophenol < 3-chlorophenol) and 2,4-dichlorophenol.

Another class of slightly polar solutes consisting of seven anilines including aniline $(pK_a = 4.70)$, 3 -methylaniline $(pK_a = 4.91)$, 4 -isopropylaniline $(pK_a = 5.0)$, 4-chloroaniline $(pK_a = 4.06)$, 4-bromoaniline $(pK_a = 3.86)$, 3-chloro-4-methylaniline $(pK_a = 4.05)$, a nd 3,4 -dichloroaniline $(pK_a = 3.33)$, w ere us ed t o e valuate t he retention pr operty of t he A c olumns s eries. The s even an ilines w ere b aseline separated in ca. 12 min on the 1A, 2A, and 3A columns (see Figure 4.13) at 45 % v/v ACN in the mobile phase affording a theoretical plate count of 96,000, 108,000, a nd 108,000 plates/m, respectively. The elution order of the anilines on 1A, 2A and, 3A columns w as the s ame, and in the order of increasing of nonpol ar character of the solutes. This retention behavior is typical to RP-CEC where halogenated anilines are more retained than methyl-substituted anilines.



Figure 4. 12 Electrochromatograms of s ome p henols f or t hree c olumns, 20 c m effective length, 27 cm total length \times 100 µm i.d., 1A: C8 column in (a), 2A: C12 column in (b) and 3A: C16 column in (c); hydro-organic mobile phase at 50 % ACN (v/v) in (a), 45 % ACN (v/v) in (b and c); 1.0 mM sodium phosphate, pH 7.0; running voltage 15 kV; electrokinetic injection for 3 s at 10 kV. Solutes: 1, quinol; 2, phenol; 3, 3,4-dimethylphenol; 4, 4-chlorophenol; 5,3-chlorophenol; 6, 2,4-dichlorophenol.



Figure 4. 13 Electrochromatograms of s ome a nilines f or t hree columns, 20 c m effective length, 27 cm total length \times 100 μ m i.d., 1A: C8 column in (a), 2A: C12 column in (b) and 3A: C16 column in (c); hydro-organic mobile phase at 45 % ACN (v/v), 1.0 m M sodium phos phate, pH 7.0; r unning vol tage 15 kV ;electrokinetic injection f or 3 s a t 10 kV. EOF t racer, t hiourea. Solutes: 1, a niline; 2, 3 - methylaniline; 3, 4-chloroaniline; 4, 4 -isopropylaniline; 5, 4-bromoaniline; 6, 3 - chloro-4-methylaniline; 7, 3,4-dichloroaniline.

4.3.2.3 Peptides and proteins

The B monolithic columns series were further evaluated in the separation of polyionic solutes such as proteins and tryptic peptide mapping whose retention is based on their electrophoretic migration and chromatographic partitioning. F igure 4.14 shows the separation of four s tandard pr oteins of v arious s izes a nd c harges (i.e. i soelectric points, p*I*s), namely lysozyme (p*I* = 11.1), cytochrome C (p*I* = 10.2), ribonuclease A (pI = 9.3), and ovalbumin (pI = 4.7) obtained on the B columns series, using a hydroorganic mobile phase consisting of 10 m M sodium phosphate, pH 7.0 at 45% (v/v) ACN. A s can b e s een i n F igure 4.14a-c, t he pr oteins m igrated i n t he or der of decreasing pI values with the most acidic protein (ovalbumin) eluting last while the most basic protein (lysozyme) eluted first. On the 1B column, the four proteins were eluted in 14.8 min with an average theoretical plate count of 332,000 plates/m, while on 2B and 3B columns, the four proteins were eluted at about 18 min with an average theoretical plate count of 236,000 and 225,000 plates/m, respectively. The observed cathodal EOF velocity under the condition used was about 0.39, 0.34, and 0.32 mm/s on 1B, 2B, and 3B, respectively. The slight decrease in the EOF velocity when going from C8 to C16 corroborates with the slight increase in the analysis time in the order $C16 \ge C12 > C8$. In comparison with 2B and 3B monoliths, the 1B monolith seems to be the best column for the separation of the four standard proteins under investigation with the highest separation efficiency and the shortest analysis time (see Kinetically s peaking, for l arge m olecules s uch a s p roteins, Figure 4.14a). energetically "softer" surfaces such as C8 would allow faster sorption kinetics and in turn improved efficiency. Thus, a short alkyl chain monolith such as C8 at sufficient surface ligand density (i.e. 1B column) is preferred for protein separation.

In addition, the monoliths prepared from polymerization mixtures at the same amount of f unctional m onomer (i.e. t he B m onoliths series) pe rformed be tter i n pr otein separation than the A monolithic series. The A columns series gave broad peaks and much l onger analysis t ime (results not s hown). This m ay b e du e t o t he por e morphology. In another s et of experiments, a complex p eptide mix ture consisting of the tryptic digest of cytochrome C was separated on the B columns series. Figure 4.15 shows the tryptic peptide map of cytochrome C obtained on the B columns series using a hydroorganic m obile pha se c ontaining 35% (v/v) A CN i n 10 m M s odium phos phate concentration, pH 6.0. Increasing t he phos phate i on c oncentration i n t he m obile phase to 15 m M and 20 m M did not improve the peptide m ap profile in terms of resolution among the various peaks but resulted in decreasing substantially the EOF velocity and consequently increasing the analysis time, results are shown in Figure 4.16. This behavior is due to the decrease in the thickness of the electric double layer at the liquid-solid interface as the ionic strength is increased. For instance, the EOF velocity decreased from 0.16 mm/s at 10 m M sodium phosphate to 0.13 mm/s at 15 mM, and to 0.12 mm/s at 20 mM on the C16 column (i.e. 3B column). Increasing the % ACN in the mobile phase from 35% to 45% (v/v) increased the EOF velocity by a factor of approximately 1.2, 1.5 and 1.3 on C 8, C 12 and C 16, respectively, but resulted in decreasing the overall resolution of the CEC systems, results are shown in Figure 4.17. As can be seen in Figure 4.18, keeping the ACN content of the mobile phase at 35% (v/v) and that of the sodium phosphate at 10 mM, but decreasing the pH of the mobile phase from 6.0 t o 4.0 de creased the analysis time by more than 50%. Although de creasing t he pH of t he m obile p hase de creased t he E OF ve locity substantially, the fact that decreasing the pH of the mobile phase increases the amount of positive charges on the peptide fragments resulted in decreasing the peptide map retention.

Although, t he obs erved c athodal E OF unde r a ll c onditions us ed f or pr oteins a nd peptide mapping separation is very small and not strong, proteins and peptides eluted from t he B c olumns series i n a few m inutes. This m ay in dicate th at th e chromatographic partitioning contribution to proteins and peptides migration is much less i n m agnitude t han t he e lectrophoretic contribution. Figure 4.1 9a s hows t he separation of tryptic peptide mapping of cytochrome C on 3B column using a hydroorganic m obile ph ase c ontaining 10 m M s odium phos phate, pH 6.0 a t 35% (v/v) ACN, and a running voltage of 10 k V, the peptide fragments were eluted in 23 m in. The remaining p eptide fragments were completely el uted in 7 m in (Figure 4.1 9b)

using reversed polarity at the same mobile phase compositions. Using the same CEC conditions as Figure 4.19, the separation of cytochrome C tryptic map on 3A column was examined, resulting in the peptide fragments eluted in 30 m in and the remaining peptide fragments eluted in 6 min using reversed polarity as shown in Figure 4.20. The 3A m onolith, which prepared f rom p olymerization mix tures a t the o ptimal amount of f unctional monomer (Figure 4.20) performed be tter i n c ytochrome C tryptic m ap s eparation than those at the same a mount of f unctional monomer, 3B monolith (Figure 4.19).

Furthermore, t he A co lumns s eries w ere al so ev aluated i n t he s eparation o f cytochrome C tryptic digest using the same elution conditions as in Figure 4.15. As can be seen in Figure 4.21a-c, the shorter th e a lkyl c hain length of the functional monomer, the higher is the EOF velocity. In comparison with 1A and 2A monoliths, the 3A monolith s eems to be the best c olumn for the s eparation of c ytochrome C tryptic digest (see Figure 4.21c). In short, while an energetically soft surface (C8-monolith) is optimal for protein s eparation, an energetically "harder" surface (C16-monolith) is more favorable for the separation of smaller size solutes such as peptides.



Figure 4.14 Electrochromatograms of s ome s tandard pr oteins f or t hree m onolithic capillary c olumns pr epared f rom pol ymerization s olution a t di fferent *n*-alkyl ch ain length, 20 c m effective length, 27 c m total length \times 100 µm i.d., 1B: C8 c olumn in (a), 2B: C12 column in (b) and 3B: C16 column in (c); mobile phase, 10 mM sodium phosphate m onobasic, pH 7.0, at 45% A CN (v/v), r unning vol tage 10 k V, electrokinetic injection for 3 s at 10 kV; EOF tracer, thiourea; solutes: 1, lysozyme; 2, cytochrome *C*; 3, ribonuclease A; 4, ovalbumin.



Figure 4.15 Electrochromatograms of the tryptic digest of cytochrome *C*. 1B: C 8 column in (a), 2B: C 12 column in (b) and 3B: C 16 column in (c), 20 c m effective length, 27 cm total length \times 100 µm i.d.; hydro-organic mobile phase, 35 % A CN (v/v), 10 m M i n s odium phos phate m onobasic, pH 6.0, r unning vol tage 10 kV ; electrokinetic injection for 5 s at 10 kV.



Figure 4.1 6 Electropherograms of t he t ryptic digest of c ytochrome *C*. 3 B: C 16 capillary c olumn, 20 cm effective length, 27 cm total length \times 100 μ m i.d.; hydroorganic mobile phase, 35 % ACN (v/v), 10 mM in (a), 15 mM in (b), and 20 mM in (c) s odium phos phate monobasic, pH 6.0, running vol tage 10 kV, electrokinetic injection for 5 s at 10 kV.



Figure 4.1 7 Electropherograms of t he t ryptic digest o f c ytochrome *C* for t hree monolithic c apillary c olumns pr epared f rom p olymerization s olution a t di fferent *n*-alkyl chain length, 20 cm effective length, 27 cm total length × 100 μ m i.d., 1B: C8 column in (a and b), 2B: C12 column in (c and d) and 3B: C16 column in (e and f); hydro-organic mobile phase at 35 % ACN (v/v) in (a, c, and e) and 45 % ACN (v/v) in (b, d, a nd f), 10 mM s odium phos phate, pH 6.0, r unning vol tage 10 kV , electrokinetic injection for 5 s at 10 kV.



Figure 4.17 Continued. Electropherograms of the tryptic digest of cytochrome *C* for 2B: C12 monolithic column, 20 cm effective length, 27 cm total length \times 100 µm i.d.; hydro-organic mobile phase at 35 % ACN (v/v) in (c) and 45 % ACN (v/v) in (d), 10 mM sodium phosphate, pH 6.0, running voltage 10 kV, electrokinetic injection for 5 s at 10 kV.



Figure 4.17 Continued. Electropherograms of the tryptic digest of cytochrome *C* for 3B: C16 monolithic column, 20 cm effective length, 27 cm total length × 100 μ m i.d.; hydro-organic mobile phase at 35 % ACN (v/v) in (e) and 45 % ACN (v/v) in (f), 10 mM sodium phosphate, pH 6.0, running voltage 10 kV, electrokinetic injection for 5 s at 10 kV.



Figure 4.18 Electrochromatograms of the tryptic digest of c ytochrome *C*. 3B : C 16 capillary c olumn, 20 cm effective length, 27 cm total length \times 100 μ m i.d.; hydroorganic mobile phase, 35 % ACN (v/v), 10 mM sodium phosphate monobasic, pH 4.0 in (a), pH 5.0 in (b) and pH 6.0 in (c), running voltage 10 kV, electrokinetic injection for 5 s at 10 kV.



Figure 4.19 Electrochromatograms of the tryptic digest of c ytochrome *C*. 3B: C 16 capillary c olumn, 20 cm effective length, 27 cm to tal length \times 100 µm i.d.; hydroorganic mobile phase, 35 % A CN (v/v), 10 m M s odium phosphate monobasic, pH 6.0, running voltage 10 kV, electrokinetic injection for 5 s at 10 kV in (a) and running voltage -10 kV, electrokinetic injection for 5 s at -10 kV in (b).



Figure 4.20 Electrochromatograms of the tryptic digest of c ytochrome *C*. 3A : C 16 capillary c olumn, 20 c m effective length, 27 c m total length \times 100 µm i.d.; hydroorganic mobile phase, 35 % A CN (v/v), 10 m M s odium phosphate m onobasic, pH 6.0, running voltage 10 kV, electrokinetic injection for 5 s at 10 kV in (a) and running voltage -10 kV, electrokinetic injection for 5 s at -10 kV in (b).



Figure 4 .21 Electrochromatograms of the tryptic d igest of c ytochrome *C* using columns with different *n*-alkyl chain length, 20 cm effective length, 27 cm total length \times 100 µm i.d., 1A: C8 column in (a), 2A: C12 column in (b) and 3A: C16 column in (c); hy dro-organic m obile phase, 35 % A CN (v/v), 10 m M sodium phos phate monobasic, pH 6.0, running voltage 10 kV, electrokinetic injection for 5 s at 10 kV.

4.4 Conclusion

In conclusions, this study has assessed the optimal *n*-alkyl chain length as well as the monomer c omposition f or t he p reparation o f ne utral m onoliths be st s uited f or t he reversed-phase capillary electrochromatography (RP-CEC) separation of peptides and proteins. In comparison with unstable monolithic columns obtained from the nitric acid initiator, the more stable monolithic columns obtained from the 2,2'azobisiobutylronitrile (AIBN) in itiator at the optimal composition of the monomers and the porogen provided comparable separation efficiency, up to 200,000 plates/m for a lkylbenzene, and therefore were chosen for further study. Using AIBN as a initiator, two different neutral nonpol ar monolithic columns series (designated as A and B c olumns s eries) each c onsisting of t hree c olumns at varying *n*-alkyl ch ain length w ere pr epared by the c opolymerization of t he f unctional m onomers C 8methacrylate, C 12-acrylate o r C 16-methacrylate w ith th e c rosslinking mo nomer pentaerythritol triacrylate in a ternary porogenic solvent composed of cyclohexanol, ethylene glycol, and water. The magnitude of the electroosmotic flow (EOF) of A columns series depends on the pH and the ACN content of the mobile phase. This is indicative of the adsorption of electrolyte ions of the mobile phase to the monolithic surface, which imparts the monoliths with the zeta potential necessary to support the EOF. The separation efficiency for ABs obtained on the monolithic columns with the same composition of the polymerization mixture (i.e. the B columns series) was lower than that of the variable ones (i.e. the A columns series). The C16-monolith of the A series (3A column) yielded better separation efficiency towards small solutes such as alkylbenzenes, alkyl phenyl ketones, nitroalkanes, phenols and anilines, but the A columns series were inadequate for protein separation by RP-CEC. However, the C8-monolith of the B series (1B column) provided better separation efficiency for proteins while for tryptic peptide mapping, the C 16-monolith of the A series (3A column) seems t o p rovide b etter separation. F or l arge p rotein m olecules, t he energetically "softer" C8 surface allowed faster sorption kinetics and in turn improved efficiency, while an energetically "harder" C16 surface favored better separation of the smaller size peptide solutes.

CHAPTER V

SUMMARY AND FUTURE WORK

5.1 Theoretical Mo dels o f Separation S electivity f or C harged C ompounds i n MEKC

The C ZE s eparation of charged an alytes c an b e p erformed b y the running buf fer, while t heir M EKC s eparation i s pe rformed b y the running buf fer c ontaining a surfactant as m icellar or p seudo-stationary p hase. T he s eparation s electivity or mobility s electivity in CZE (α_{CZE}) i s ba sed on t he di fference i n e lectrophoretic mobility of charged analytes, while the separation selectivity in MEKC (α_{MEKC}) arises from either the retention selectivity of the micellar phase (α_k) or α_{CZE} . In this work, equations and theoretical models for α_{MEKC} of two charged analytes were developed to predict a change in α_{MEKC} based on t he range of the mobility selectivity in CZE, retention selectivity in MEKC (α_k), selectivity ratio ($\rho = \alpha_k/\alpha_{CZE}$) and the order of the order of $|\mu|$ in CZE and k in MEKC. The proposed α_{MEKC} models were classified into four types: (I) $\rho > 1.0$, where $\alpha_k > \alpha_{CZE} \ge 1.0$; (II) $\rho \le 1.0$, where $\alpha_{CZE} \ge \alpha_k \ge$ 1.0; (III) $\rho > 1.0$, where $\alpha_k \ge 1.0 > \alpha_{CZE}$, (IV) $\rho = 1.0$, where $\alpha_k = \alpha_{CZE} = 1.0$.

In comparison with CZE, whether MEKC with normal elution mode will improve or reduce separation selectivity for two charged analytes depends on the model of α_{MEKC} and k value. Typically, better s eparation s electivity i n M EKC o ver C ZE can be obtained for the α_{MEKC} Type I ($\alpha_k > \alpha_{CZE}$), or T ype III models ($\alpha_k >> \alpha_{CZE}$, or $\alpha_k > 1/\alpha_{CZE}$) at appropriate values of k_1 , while those of Type II models result in worse of α_{MEKC} for two charged analytes. The α_{MEKC} Type IV with α_{CZE} of 1.0 and α_k of 1.0 ($\rho = 1.0$), no r esolution is obtained in either CZE or MEKC. It should be noted that for a theoretical value of α_{CZE} or $\alpha_{MEKC} < 1.0$, the practical separation selectivity is equal to $1/\alpha_{CZE}$ or $1/\alpha_{MEKC}$. Therefore, an increase in k_1 may result in a r eversed order of electrophoretic mobility for two charged analytes in MEKC. Type III model

starts f rom le ss th an 1 .0 $(1/\alpha_{MEKC} > 1.0)$ t o n ear 1 .0 (poorer s eparation) w ith increasing k_1 and then higher than 1.0 (better s eparation) at higher k_1 values. This indicates that reversed of $|\mu|$ in CZE and k in MEKC for two charged analytes. Using four alkylparabens as test analytes, such as IP, EP, PP and BP, excellent agreement was f ound be tween t he obs erved α_{MEKC} and t he proposed α_{MEKC} models of te st analytes in MEKC over a w ide range of [SDS] and values of k. It also should be noted t hat t he di rection of E OF ve locity and t otal ve locity do es not a ffect the electrophoretic mobility of analytes and micelles, and the retention factor of analytes in MEKC. Owing to independence of the values of α_m and α_k with the direction of these v elocities, t hese proposed s electivity m odels c an be us ed f or MEKC w ith normal, reversed and restricted modes.

5.2 Investigation of Neutral Monolithic Capillary Columns with Varying *n*-alkyl Chain Lengths in CEC

Two di fferent ne utral n onpolar m onolithic c olumns series (designated as A and B columns series) each consisting of three columns at varying *n*-alkyl chain length were prepared by the copolymerization of the functional monomers C8-methacrylate, C12-acrylate or C 16-methacrylate w ith the c rosslinking m onomer P ETA t o yield monoliths with surface bound C8, C12 and C16 chains. A ternary porogenic solvent consisting of cyclohexanol and ethylene glycol in various ratios at constant 3.6 w t% water was used. AIBN (1.0 wt% with respect to monomers) was added to the solution as the free radical initiator. In the A columns series, the composition of the functional monomers a nd c rosslinker w as adjusted t o yield c omparable c hromatographic retention r egardless of t he a lkyl ch ain l ength. In the B c olumns s eries, t he composition of the functional monomers and c rosslinker was kept constant yielding chromatographic retention, which increased as expected in the order of increasing the *n*-alkyl chain length.

These two different neutral nonpolar monolithic columns were characterized over a wide range of mobile phase composition. The magnitude of the EOF of A columns

series depends on the pH and the ACN content of the mobile phase. This is indicative of the adsorption of electrolyte i ons of the mobile phase to the monolithic surface, which imparts the monoliths with the zeta potential necessary to support the EOF. The A columns series were evaluated for their performance by using ABs, APKs, and NAs, which a re t ypical m odel s olutes of high, m oderate, a nd l ow h ydrophobic character, r espectively. Under t he s ame m obile pha se c omposition a nd a pplied voltage, the magnitude order of k values was ABs > APKs > NAs, which is consistent with that of the hydrophobic order of the homologous ABs > APKs > NAs. This is indicative of a r eversed p hase r etention m echanism. It s hould be not ed t hat t he amount of t he f unctional m onomers for t he A s eries s uch as 1A, 2 A, a nd 3 A monoliths, increased in the order C8 > C12 > C16, the shorter is the alkyl chain length the higher is the EOF velocity. This explains the slightly higher k values or slightly longer separation time on C 8 and C 12 than on C16 monoliths. Therefore, and for difficult separations that would require high separation efficiency, one would consider a longer alkyl chain monolith at optimal functional monomer content (e.g. C16) with slightly lower retention and faster analysis time. In the case of B columns series, the k values of ABs increased with increasing the alkyl chain length as in principle should be the case. The separation efficiency for ABs obtained on the monolithic columns with the same composition of the polymerization mixture (i.e. the B columns series) was lower than that of the variable ones (i.e. the A columns series). In the B columns series, the column made with the shorter alkyl chain length yielded higher separation efficiency than the longer one. This is due primarily to the fact that a shorter analysis time w ould a llow le ss b and s preading th at arises f rom lo ngitudinal mo lecular diffusion assuming that everything else has remained the same.

In comparison with C8- and C12- monoliths, the C16-monolith of the A series yielded the highest separation efficiency towards small solutes, but the A columns series were inadequate f or pr otein s eparation b y R P-CEC. The C 8-monolith of t he B s eries provided the best separation efficiency for proteins while for tryptic peptide mapping, the C 16-monolith of t he A s eries s eems t o p rovide t he b est s eparation. For l arge protein m olecules, t he en ergetically "softer" C 8 s urface al lowed f aster s orption
kinetics and in turn improved efficiency, while an energetically "harder" C16 surface favored better separation of the smaller size peptide solutes.

5.3 Future Work

Work on MEKC separation selectivity for two negatively charged analytes in thesis has proved to be useful in explaining a change in α_{MEKC} through theoretical models of α_{MEKC} . In the future w ork, these theoretical models could be checked in charged compounds separation in MEKC using other MEKC modes such as reversed elution mode or restricted elution mode. It is also interesting to study the other negatively charged an alytes with normal elution mode or positively charged an alytes with reversed elution mode. The work on the investigation of neutral monolithic capillary columns with varying *n*-alkyl chain lengths in CEC has assessed the optimal *n*-alkyl chain l ength a s w ell a s t he monomer composition for t he preparation of neutral monoliths best suited for the RP-CEC separation of peptides and proteins. The work may be extended t o CEC c oupled with a mass s pectrometer i n or der t o i dentify peptides and proteins. It is also in teresting to investigate other c rosslinkers and initiator to prepare the neutral monolithic capillary columns.

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- C. Puangpila, T. Nhujak, Z. El Rassi "Investigation of neutral monolithic capillary columns with varying n-alkyl chain lengths in capillary electrochromatography" *Electrophoresis*, accepted. Impact factor = 3.569

International Presentations

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- 2) C. Puangpila, A. Petsom, T. Nhujak "Theoretical models of separation selectivity for ch arged co mpounds i n m icellar electrokinetic ch romatography" P oster presentation, 17 th International S ymposium o n Electro- and Liquid P haseseparation T echniques, 29 A ugust-1 S eptember, 2010, T reat M ont H otel, Baltimore, Maryland, USA.
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National Presentations

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