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## APPENDICES

### Appendix A Raw Data

**Table A-1** The product distributions from tire pyrolysis with various heating rates

Sample	% Yield		
	Gas	Liquid	Solid
HT10 <sup>a</sup>	8.73	50.43	40.84
HT15	7.31	52.56	40.13
HT20	6.29	53.24	40
HT30	4.07	54.93	41

<sup>a</sup>heating rate

**Table A-2** The gas composition from tire pyrolysis with various heating rates shown in % volume

Gases	% Volume			
	HT10 <sup>a</sup>	HT15	HT20	HT30
Methane	34.70	24.62	25.03	21.90
Ethylene	5.63	5.29	6.64	5.46
Ethane	13.60	11.83	13.42	10.58
Propylene	5.52	4.96	5.69	5.03
Propane	6.76	5.99	6.30	5.38
C <sub>4</sub>	13.67	16.76	17.39	21.18
C <sub>5</sub>	11.82	17.21	12.22	17.84
C <sub>6</sub>	5.52	7.13	7.12	6.83
C <sub>7</sub>	1.57	2.81	2.76	2.44
C <sub>8</sub>	1.19	3.41	3.42	3.36

<sup>a</sup>heating rate

**Table A-3** Carbon number distribution in liquid products from co-pyrolysis of tire with various heating rates

Carbon number	Boiling Point	% Mass			
		HT10 <sup>a</sup>	HT15	HT20	HT30
6	69.9		3.40	0.20	
7	98.4		3.54	3.08	1.99
8	125.1	4.90	3.77	3.62	2.44
9	150.1	4.99	3.98	3.73	2.91
10	173.6	5.05	4.17	4.03	3.40
11	195.6	5.10	4.34	4.30	3.86
12	216.3	5.13	4.48	4.56	4.29
13	235.8	5.13	4.59	4.78	4.64
14	254.0	5.13	4.66	4.96	4.90
15	271.3	5.11	4.70	5.10	5.05
16	287.5	5.08	4.70	5.17	5.09
17	302.8	5.04	4.65	5.19	5.03
18	317.4	4.99	4.55	5.12	4.87
19	331.1	4.91	4.41	4.99	4.64
20	344.2	4.79	4.21	4.77	4.36
21	356.6	4.61	3.97	4.48	4.05
22	368.5	4.32	3.69	4.13	3.72
23	379.9	3.88	3.38	3.75	3.39
24	390.8	3.26	3.05	3.34	3.06
25	401.2	2.54	2.72	2.93	2.76
26	411.3	1.82	2.40	2.53	2.47
27	421.0	1.21	2.09	2.16	2.21
28	430.5	0.76	1.80	1.83	1.98
29	439.6	0.47	1.54	1.54	1.76
30	448.4	0.28	1.31	1.28	1.57
31	457.0	0.17	1.10	1.07	1.39
32	465.4	0.10	0.93	0.88	1.24
33	473.5	0.06	0.78	0.73	1.10
34	481.3	0.04	0.65	0.60	0.98
35	489.0	0.02	0.54	0.50	0.87
36	496.4	0.01	0.45	0.41	0.77
37	503.5	0.01	0.38	0.34	0.68
38	510.4	0.01	0.31	0.28	0.60
39	517.0	0.00	0.26	0.23	0.53
40	523.2	0.00	0.21	0.19	0.46
41	529.1	0.00	0.18	0.15	0.41
42	534.7	0.00	0.15	0.13	0.35
43	539.8	0.00	0.12	0.10	0.30
44	544.5	0.00	0.10	0.08	0.26
45	548.6	0.00	0.08	0.07	0.22
46	552.2	0.00	0.06	0.05	0.18
47	555.2	0.00	0.05	0.04	0.14
48	557.5	0.00	0.04	0.03	0.11
49	559.1	0.00	0.02	0.02	0.07

<sup>a</sup> heating rate

**Table A-4** Oil fractions from co-pyrolysis of tire with various heating rates shown in %Mass

Fraction	Boiling Point (°C)	% Mass			
		HT10 <sup>a</sup>	HT15	HT20	HT30
Gasoline	15.5-149	16.85	11.29	9.08	9.11
Kerosene	149-232	20.46	17.36	17.89	17.36
Gas oil	232-343	33.76	32.27	36.05	33.06
Fuel Oil	343-371	8.81	8.31	8.88	8.47
Heavy vacuum gas oil	371-559.1	20.12	30.78	28.09	31.45

<sup>a</sup>heating rate

**Table A-5** The product distributions from tire pyrolysis with various oxides

Sample	% Yield		
	Gas	Liquid	Solid
Non-cat	8.73	50.43	40.84
4%Fe <sub>2</sub> O <sub>3</sub>	23.23	33.6	43.17
5%Fe <sub>2</sub> O <sub>3</sub>	19.89	36.9	43.21
CaO	19.11	41.56	39.33

**Table A-6** The gas compositions from tire pyrolysis with various oxides shown in % volume

Gases	% Volume			
	Non-cat	4%Fe2O3	5%Fe2O3	CaO
Methane	34.70	16.961	25.161	27.83
Ethylene	5.63	4.182	6.656	6.99
Ethane	13.60	8.273	11.957	13.98
Propylene	5.52	3.415	5.179	5.75
Propane	6.76	3.447	4.766	5.98
C <sub>4</sub>	13.67	29.349	29.284	20.75
C <sub>5</sub>	11.82	12.425	7.127	9.19
C <sub>6</sub>	5.52	11.008	6.692	7.32
C <sub>7</sub>	1.57	8.056	1.854	1.32
C <sub>8</sub>	1.19	2.884	1.325	0.91

**Table A-7** Carbon number distribution in liquid products from pyrolysis of tire with various oxides

Carbon number	Boiling Point (°C)	%Mass			
		Non-cat	4%Fe2O3	5%Fe2O3	CaO
6	69.9				0.85
7	98.4				2.30
8	125.1	4.90	8.16	7.79	2.97
9	150.1	4.99	2.23	2.01	3.74
10	173.6	5.05	2.80	2.49	4.57
11	195.6	5.10	3.42	3.00	5.42
12	216.3	5.13	4.07	3.54	6.21
13	235.8	5.13	4.70	4.07	6.86
14	254.0	5.13	5.26	4.57	7.27
15	271.3	5.11	5.69	5.00	7.38
16	287.5	5.08	5.95	5.32	7.16
17	302.8	5.04	6.01	5.50	6.67
18	317.4	4.99	5.87	5.54	5.97
19	331.1	4.91	5.55	5.42	5.17
20	344.2	4.79	5.10	5.17	4.36
21	356.6	4.61	4.58	4.81	3.60
22	368.5	4.32	4.02	4.39	2.94
23	379.9	3.88	3.47	3.93	2.37
24	390.8	3.26	2.96	3.47	1.90
25	401.2	2.54	2.50	3.02	1.52
26	411.3	1.82	2.10	2.61	1.22
27	421.0	1.21	1.76	2.24	0.98
28	430.5	0.76	1.47	1.91	0.79
29	439.6	0.47	1.22	1.62	0.64
30	448.4	0.28	1.02	1.38	0.51

Carbon number	Boiling Point (°C)	%Mass			
		Non-cat	4%Fe2O3	5%Fe2O3	CaO
31	457.0	0.17	0.85	1.16	0.42
32	465.4	0.10	0.71	0.98	0.34
33	473.5	0.06	0.59	0.83	0.28
34	481.3	0.04	0.50	0.70	0.23
35	489.0	0.02	0.41	0.59	0.19
36	496.4	0.01	0.35	0.50	0.16
37	503.5	0.01	0.29	0.42	0.13
38	510.4	0.01	0.24	0.36	0.11
39	517.0	0.00	0.20	0.30	0.09
40	523.2	0.00	0.17	0.25	0.07
41	529.1	0.00	0.14	0.21	0.06
42	534.7	0.00	0.12	0.18	0.05
43	539.8	0.00	0.10	0.15	0.04
44	544.5	0.00	0.08	0.12	0.03
45	548.6	0.00	0.07	0.10	0.03
46	552.2	0.00	0.05	0.08	0.02
47	555.2	0.00	0.04	0.06	0.02
48	557.5	0.00	0.03	0.05	0.01
49	559.1	0.00	0.02	0.03	0.01

**Table A-8** Oil fractions from tire co-pyrolysis with various oxides shown in %Mass

Fraction	Boiling Point (°C)	% Mass			
		Non-cat	4%Fe2O3	5%Fe2O3	CaO
Gasoline	15.5-149	16.85	7.85	5.98	8.19
Kerosene	149-232	20.46	18.71	10.02	24.08
Gas oil	232-343	33.76	39.19	22.92	43.77
Fuel Oil	343-371	8.81	10.13	5.28	8.15
Heavy vacuum gas oil	371-559.1	20.12	24.13	55.80	15.81

**Table A-9** The product distributions from tire pyrolysis with various catalyst : tire ratios

Sample	% Yield		
	Gas	Liquid	Solid
Non-cat	8.73	50.43	40.84
0.10 <sup>a</sup> MOR	15.42	40.42	44.16
0.25MOR	17.33	39.71	42.96
0.50MOR	29.44	25.68	44.88

<sup>a</sup> ratio of catalyst to tire

**Table A-10** The gas composition from tire pyrolysis with various catalyst: tire ratio shown in %volume

Gases	% Volume			
	Non-cat	0.10 <sup>a</sup> MOR	0.25MOR	0.50MOR
Methane	34.70	23.62	17.51	10.17
Ethylene	5.63	8.90	11.58	12.66
Ethane	13.60	9.78	7.98	4.69
Propylene	5.52	6.38	8.69	10.43
Propane	6.76	8.92	12.22	16.97
C <sub>4</sub>	13.67	15.36	15.11	18.55
C <sub>5</sub>	11.82	14.00	12.27	10.85
C <sub>6</sub>	5.52	7.41	9.25	10.84
C <sub>7</sub>	1.57	2.21	2.87	2.60
C <sub>8</sub>	1.19	3.43	3.50	2.23

<sup>a</sup> ratio of catalyst to tire

**Table A-11** Carbon number distribution in liquid products from pyrolysis of tire with various catalyst : tire ratios

Carbon number	Boiling Point	% Mass			
		Non-cat	0.10 <sup>a</sup> MOR	0.25MOR	0.50MOR
6	69.9				3.00
7	98.4		3.25	3.16	3.20
8	125.1	4.90	3.88	3.54	3.95
9	150.1	4.99	4.05	3.86	4.59
10	173.6	5.05	4.20	4.16	5.06
11	195.6	5.10	4.33	4.43	5.36
12	216.3	5.13	4.43	4.65	5.47
13	235.8	5.13	4.52	4.82	5.44
14	254.0	5.13	4.58	4.93	5.29
15	271.3	5.11	4.62	4.98	5.06
16	287.5	5.08	4.63	4.96	4.77
17	302.8	5.04	4.62	4.88	4.46
18	317.4	4.99	4.58	4.75	4.14
19	331.1	4.91	4.50	4.57	3.82
20	344.2	4.79	4.38	4.35	3.52
21	356.6	4.61	4.23	4.10	3.23
22	368.5	4.32	4.04	3.83	2.96
23	379.9	3.88	3.81	3.55	2.72
24	390.8	3.26	3.54	3.27	2.50
25	401.2	2.54	3.24	3.00	2.30
26	411.3	1.82	2.93	2.73	2.12
27	421.0	1.21	2.61	2.48	1.95
28	430.5	0.76	2.29	2.24	1.81
29	439.6	0.47	1.98	2.02	1.67
30	448.4	0.28	1.70	1.81	1.55
31	457.0	0.17	1.44	1.63	1.43
32	465.4	0.10	1.21	1.45	1.33
33	473.5	0.06	1.01	1.30	1.23
34	481.3	0.04	0.83	1.16	1.15
35	489.0	0.02	0.69	1.03	1.06
36	496.4	0.01	0.56	0.91	0.98
37	503.5	0.01	0.46	0.81	0.91
38	510.4	0.01	0.38	0.71	0.84
39	517.0	0.00	0.31	0.63	0.77
40	523.2	0.00	0.25	0.55	0.70
41	529.1	0.00	0.21	0.48	0.64
42	534.7	0.00	0.17	0.42	0.58
43	539.8	0.00	0.13	0.36	0.52
44	544.5	0.00	0.11	0.31	0.46
45	548.6	0.00	0.09	0.26	0.40
46	552.2	0.00	0.07	0.21	0.33
47	555.2	0.00	0.05	0.17	0.27
48	557.5	0.00	0.04	0.12	0.21
49	559.1	0.00	0.02	0.08	0.14

<sup>a</sup> ratio of catalyst to tire

**Table A-12** Oil fractions from tire pyrolysis with various catalyst: tire ratios shown in %Mass

Fraction	Boiling Point (°C)	% Mass			
		Non-cat	0.10 <sup>a</sup> MOR	0.25MOR	0.50MOR
Gasoline	15.5-149	16.85	10.13	9.81	14.55
Kerosene	149-232	20.46	17.31	18.04	20.52
Gas oil	232-343	33.76	33.02	33.73	31.85
Fuel Oil	343-371	8.81	8.56	8.88	7.45
Heavy vacuum gas oil	371-559.1	20.12	30.98	29.54	25.64

<sup>a</sup> ratio of catalyst to tire

**Table A-13** The product distributions from tire co- pyrolysis with various catalysts.

Sample	% Yield		
	Gas	Liquid	Solid
Non-cat	8.73	50.43	40.84
0.25 <sup>a</sup> MOR	17.33	39.71	42.96
0.25ITQ-21	12.48	43.11	44.41
0.25ITQ-24	14.86	40.44	44.71
0.50MOR	29.44	25.68	44.88
0.50ITQ-21	30.43	25.85	43.72
0.50ITQ-24	25.75	28.83	45.42

<sup>a</sup> ratio of catalyst to tire

**Table A-14** The gas composition from tire co-pyrolysis with various catalysts shown in %volume

Gases	% Volume						
	Non-cat	0.25 <sup>a</sup> MOR	0.25 ITQ-21	0.25 ITQ-24	0.50 MOR	0.50 ITQ-21	0.50 ITQ-24
Methane	34.7	17.51	19.65	17.12	10.17	11.42	13.23
Ethylene	5.63	11.58	10.54	9.08	12.66	14.96	9.36
Ethane	13.6	7.98	8.31	8.34	4.69	5.24	5.07
Propylene	5.52	8.69	7.21	7.63	10.43	8.56	8.97
Propane	6.76	12.22	12.56	14.83	16.97	17.00	17.34
C <sub>4</sub>	13.67	15.11	14.62	17.15	18.55	17.10	18.69
C <sub>5</sub>	11.82	12.27	12.98	12.35	10.85	9.89	10.40
C <sub>6</sub>	5.52	9.25	8.21	8.85	10.84	10.47	10.82
C <sub>7</sub>	1.57	2.87	2.67	2.37	2.6	2.79	3.00
C <sub>8</sub>	1.19	3.5	3.25	2.28	2.23	2.58	3.11

<sup>a</sup> ratio of catalyst to tire

**Table A-15** Carbon number distribution in liquid products from tire co-pyrolysis with various catalysts

Carbon number	Boiling Point	% Mass						
		Non-cat	0.25 <sup>a</sup> MOR	0.25 ITQ-21	0.25 ITQ-24	0.50 MOR	0.50 ITQ-21	0.50 ITQ-24
6	69.9					3		
7	98.4		3.16	4.30	7.01	3.2	2.15	2.85
8	125.1	4.9	3.54	3.53	3.91	3.95	2.91	3.23
9	150.1	4.99	3.86	3.78	3.97	4.59	3.35	3.96
10	173.6	5.05	4.16	3.99	4.02	5.06	3.77	4.57
11	195.6	5.1	4.43	4.16	4.05	5.36	4.17	5.02
12	216.3	5.13	4.65	4.27	4.07	5.47	4.52	5.28
13	235.8	5.13	4.82	4.33	4.07	5.44	4.80	5.38
14	254	5.13	4.93	4.35	4.05	5.29	5.00	5.35
15	271.3	5.11	4.98	4.32	4.03	5.06	5.11	5.22
16	287.5	5.08	4.96	4.26	3.99	4.77	5.12	5.01
17	302.8	5.04	4.88	4.16	3.93	4.46	5.04	4.75
18	317.4	4.99	4.75	4.05	3.87	4.14	4.88	4.47
19	331.1	4.91	4.57	3.91	3.79	3.82	4.65	4.19
20	344.2	4.79	4.35	3.77	3.70	3.52	4.37	3.90
21	356.6	4.61	4.1	3.61	3.59	3.23	4.06	3.62

Carbon number	Boiling Point	% Mass						
		Non-cat	0.25 <sup>a</sup> MOR	0.25 ITQ-21	0.25 ITQ-24	0.50 MOR	0.50 ITQ-21	0.50 ITQ-24
22	368.5	4.32	3.83	3.46	3.46	2.96	3.73	3.36
23	379.9	3.88	3.55	3.30	3.32	2.72	3.40	3.12
24	390.8	3.26	3.27	3.15	3.16	2.5	3.08	2.90
25	401.2	2.54	3	3.00	2.98	2.3	2.77	2.69
26	411.3	1.82	2.73	2.86	2.78	2.12	2.49	2.50
27	421	1.21	2.48	2.72	2.57	1.95	2.22	2.32
28	430.5	0.76	2.24	2.59	2.35	1.81	1.98	2.16
29	439.6	0.47	2.02	2.46	2.12	1.67	1.76	2.02
30	448.4	0.28	1.81	2.34	1.89	1.55	1.56	1.88
31	457	0.17	1.63	2.22	1.67	1.43	1.39	1.76
32	465.4	0.1	1.45	2.10	1.45	1.33	1.23	1.64
33	473.5	0.06	1.3	1.99	1.25	1.23	1.09	1.53
34	481.3	0.04	1.16	1.88	1.07	1.15	0.96	1.43
35	489	0.02	1.03	1.78	0.91	1.06	0.85	1.33
36	496.4	0.01	0.91	1.67	0.77	0.98	0.75	1.24
37	503.5	0.01	0.81	1.57	0.64	0.91	0.66	1.16
38	510.4	0.01	0.71	1.47	0.53	0.84	0.58	1.07
39	517	0	0.63	1.37	0.44	0.77	0.51	0.99
40	523.2	0	0.55	1.27	0.37	0.7	0.45	0.91
41	529.1	0	0.48	1.16	0.30	0.64	0.39	0.83
42	534.7	0	0.42	1.06	0.25	0.58	0.34	0.75
43	539.8	0	0.36	0.96	0.20	0.52	0.29	0.68
44	544.5	0	0.31	0.85	0.16	0.46	0.25	0.60
45	548.6	0	0.26	0.74	0.13	0.4	0.21	0.52
46	552.2	0	0.21	0.63	0.10	0.33	0.17	0.44
47	555.2	0	0.17	0.51	0.08	0.27	0.13	0.36
48	557.5	0	0.12	0.39	0.06	0.21	0.10	0.27
49	559.1	0	0.08	0.26	0.04	0.14	0.07	0.18

<sup>a</sup> ratio of catalyst to tire

**Table A-16** Oil fractions from tire co- pyrolysis with various catalysts shown in %Mass

Fraction	Boilin g Point (°C)	% Mass				0.50 MOR	0.50 ITQ-21	0.50 ITQ-24
		Non- cat	0.25 <sup>a</sup> MOR	0.25 ITQ-21	0.25 ITQ-24			
Gasoline	15.5- 149	16.85	9.81	11.04	14.03	14.55	7.43	9.78
Kerosene	149- 232	20.46	18.04	16.45	16.35	20.52	16.92	19.45
Gas oil	232- 343	33.76	33.73	29.36	28.12	31.85	33.64	33.15
Fuel Oil	343- 371	8.81	8.88	7.96	7.63	7.45	8.32	8.22
Heavy vacuum gas oil	371- 559.1	20.12	29.54	35.20	33.86	25.64	33.70	29.41

<sup>a</sup> ratio of catalyst to tire

**Table A-17** The product distributions from tire co-pyrolysis with various %Ge loaded on mordenite.

Sample	% Yield		
	Gas	Liquid	Solid
Non-cat	8.73	50.43	40.84
0.00%Ge	17.3	39.7	42.9
0.50%Ge	21.8	30.9	41.3
1%Ge	28.9	30.8	40.3
3%Ge	32.8	27.1	40.1
5%Ge	28.6	30.1	41.3

**Table A-18** The gas compositions from tire co- pyrolysis with various %Ge loaded on mordenite shown in %volume

Gases	% Volume					
	Non-cat	0.00%Ge	0.5%Ge	1%Ge	3%Ge	5%Ge
Methane	34.70	17.51	28.52	27.07	21.01	21.24
Ethylene	5.63	11.58	8.89	7.91	10.13	7.33
Ethane	13.60	7.98	11.88	10.56	10.49	10.52
Propylene	5.52	8.69	7.41	7.14	7.82	6.61
Propane	6.76	12.22	11.56	10.69	19.57	13.25
C <sub>4</sub>	13.67	15.11	13.55	15.13	15.77	15.49
C <sub>5</sub>	11.82	12.27	10.65	11.51	10.68	18.48
C <sub>6</sub>	5.52	9.25	5.50	6.87	3.99	5.56
C <sub>7</sub>	1.57	2.87	1.08	1.65	0.00	0.91
C <sub>8</sub>	1.19	3.5	0.95	1.45	0.55	0.60

**Table A-19** Carbon number distribution in liquid products from tire co-pyrolysis with various %Ge loaded on mordenite analyzed

Carbon number	Boiling Point (°C)	%Mass					
		Non-cat	0.00%Ge	0.50%Ge	1%Ge	3%Ge	5%Ge
6	69.9					6.41	6.10
7	98.4		3.16	9.42	10.37	6.44	4.34
8	125.1	4.9	3.54	4.33	4.59	6.73	4.45
9	150.1	4.99	3.86	4.49	4.84	6.98	4.54
10	173.6	5.05	4.16	4.64	5.07	7.21	4.60
11	195.6	5.1	4.43	4.76	5.26	7.39	4.65
12	216.3	5.13	4.65	4.86	5.41	7.53	4.68
13	235.8	5.13	4.82	4.93	5.51	7.60	4.70
14	254	5.13	4.93	4.97	5.54	7.57	4.69
15	271.3	5.11	4.98	4.99	5.51	7.35	4.68
16	287.5	5.08	4.96	4.97	5.40	6.81	4.65
17	302.8	5.04	4.88	4.91	5.20	5.83	4.61
18	317.4	4.99	4.75	4.79	4.93	4.47	4.55
19	331.1	4.91	4.57	4.62	4.59	3.03	4.46
20	344.2	4.79	4.35	4.38	4.19	1.85	4.34
21	356.6	4.61	4.1	4.07	3.75	1.06	4.17
22	368.5	4.32	3.83	3.70	3.30	0.59	3.93
23	379.9	3.88	3.55	3.27	2.86	0.32	3.61
24	390.8	3.26	3.27	2.82	2.44	0.18	3.21

Carbon number	Boiling Point (°C)	%Mass					
		Non-cat	0.00%Ge	0.50%Ge	1%Ge	3%Ge	5%Ge
25	401.2	2.54	3	2.38	2.06	0.10	2.74
26	411.3	1.82	2.73	1.95	1.72	0.06	2.24
27	421	1.21	2.48	1.58	1.43	0.03	1.75
28	430.5	0.76	2.24	1.25	1.18	0.02	1.32
29	439.6	0.47	2.02	0.98	0.97	0.01	0.97
30	448.4	0.28	1.81	0.76	0.80	0.01	0.69
31	457	0.17	1.63	0.59	0.66	0.00	0.49
32	465.4	0.1	1.45	0.46	0.54	0.00	0.34
33	473.5	0.06	1.3	0.35	0.44	0.00	0.24
34	481.3	0.04	1.16	0.27	0.36	0.00	0.17
35	489	0.02	1.03	0.21	0.30	0.00	0.12
36	496.4	0.01	0.91	0.16	0.25	0.00	0.08
37	503.5	0.01	0.81	0.13	0.20	0.00	0.06
38	510.4	0.01	0.71	0.10	0.17	0.00	0.04
39	517	0	0.63	0.08	0.14	0.00	0.03
40	523.2	0	0.55	0.06	0.11	0.00	0.02
41	529.1	0	0.48	0.05	0.09	0.00	0.02
42	534.7	0	0.42	0.04	0.08	0.00	0.01
43	539.8	0	0.36	0.03	0.06	0.00	0.01
44	544.5	0	0.31	0.02	0.05	0.00	0.01
45	548.6	0	0.26	0.02	0.04	0.00	0.00
46	552.2	0	0.21	0.01	0.03	0.00	0.00
47	555.2	0	0.17	0.01	0.03	0.00	0.00
48	557.5	0	0.12	0.01	0.02	0.00	0.00
49	559.1	0	0.08	0.00	0.01	0.00	0.00

**Table A-20** Oil fractions from tire co-pyrolysis with %Ge loaded on mordenite shown in %Mass

Fraction	Boiling Point (°C)	% Mass					
		Non-cat	0.0%Ge	0.5%Ge	1%Ge	3%Ge	5%Ge
Gasoline	69.6-149	16.85	9.81	16.20	18.86	25.00	17.76
Kerosene	149-232	20.46	18.04	20.55	21.77	31.77	19.91
Gas oil	232-343	33.76	33.73	32.27	34.52	36.56	31.86
Fuel Oil	343-371	8.81	8.88	7.28	8.47	4.09	7.77
Heavy vacuum gas oil	371-559	20.12	29.54	23.71	16.39	2.58	22.69

**Table A-21** The curve fitting and equation of % CUT-OFF: Effect of heating rate.

$y = y_o + \frac{a}{\left[1 + e^{-\left(\frac{x-x_o}{b}\right)}\right]^c}$	Parameter	Coefficient	$R^2$
HT10 <sup>a</sup>	a	143.914	0.9983837
	b	17.0373	
	c	0.054422	
	x <sub>o</sub>	399.541	
	y <sub>o</sub>	-46.9545	
HT15	a	118.772	0.9982683
	b	42.5707	
	c	0.197548	
	x <sub>o</sub>	405.092	
	y <sub>o</sub>	-21.6696	
HT20	a	114.63	0.99846841
	b	41.1657	
	c	0.24196	
	x <sub>o</sub>	394.077	
	y <sub>o</sub>	-16.8721	
HT30	a	104.173	0.99907948
	b	68.7858	
	c	0.715779	
	x <sub>o</sub>	344.307	
	y <sub>o</sub>	-2.44037	

<sup>a</sup> heating rate

**Table A-15** The curve fitting and equation of % CUT-OFF of tire co-pyrolysis with various oxides.

$y = y_o + \frac{a}{\left[1 + e^{-\left(\frac{x-x_o}{b}\right)}\right]^c}$	Parameter	Coefficient	$R^2$
Non-cat	a	143.914	0.9983837
	b	17.0373	
	c	0.054422	
	$x_o$	399.541	
	$y_o$	-46.9545	
4%Fe <sub>2</sub> O <sub>3</sub>	a	93.3814	0.9965000
	b	48.3515	
	c	0.615117	
	$x_o$	339.696	
	$y_o$	2.11324	
5%Fe <sub>2</sub> O <sub>3</sub>	a	94.9773	0.9959000
	b	49.2674	
	c	0.582196	
	$x_o$	359.504	
	$y_o$	1.86882	
CaO	a	100.733	0.99909924
	b	45.5165	
	c	0.543988	
	$x_o$	309.584	
	$y_o$	-4.87751	

**Table A-16** The curve fitting and equation of % CUT-OFF of tire co-pyrolysis with various catalysts to tire ratios.

$y = y_0 + \frac{a}{\left[1 + e^{-\left(\frac{x-x_0}{b}\right)}\right]} c$	Parameter	Coefficient	$R^2$
Non-cat	a	143.914	0.9983837
	b	17.0373	
	c	0.054422	
	$x_0$	399.541	
	$y_0$	-46.9545	
0.10 <sup>a</sup> MOR	a	129.215	0.9985982
	b	37.4462	
	c	0.156029	
	$x_0$	426.314	
	$y_0$	-29.7028	
0.25MOR	a	123.89	0.99963226
	b	64.3239	
	c	0.399807	
	$x_0$	392.034	
	$y_0$	-16.7286	
0.50MOR	a	119.456	0.9994826
	b	130.051	
	c	3.31015	
	$x_0$	115.805	
	$y_0$	-3.38011	

<sup>a</sup> ratio of catalyst to tire

**Table A-17** The curve fitting and equation of % CUT-OFF of tire co-pyrolysis with various catalysts to tire ratios.

$y = y_o + \frac{a}{\left[1 + e^{-\left(\frac{x-x_o}{b}\right)}\right]^c}$	Parameter	Coefficient	$R^2$
Non-cat	a	143.914	0.9983837
	b	17.0373	
	c	0.054422	
	$x_o$	399.541	
	$y_o$	-46.9545	
0.25 <sup>a</sup> MOR	a	123.89	0.99963226
	b	64.3239	
	c	0.399807	
	$x_o$	392.034	
	$y_o$	-16.7286	
0.25ITQ-21	a	150.816	0.9996199
	b	120.67	
	c	0.807657	
	$x_o$	389.947	
	$y_o$	-15.6911	
0.25ITQ-24	a	135.412	0.99942476
	b	37.6647	
	c	0.11888	
	$x_o$	451.477	
	$y_o$	-37.4132	
0.50MOR	a	119.456	0.9994826
	b	130.051	
	c	3.31015	
	$x_o$	115.805	
	$y_o$	-3.38011	
0.50ITQ-21	a	109.655	0.999752
	b	65.7194	
	c	0.561979	
	$x_o$	359.392	
	$y_o$	-9.49625	
0.50ITQ-24	a	128.57	0.99906661
	b	140.279	
	c	5.61777	
	$x_o$	52.0613	
	$y_o$	-3.27977	

<sup>a</sup> ratio of catalyst to tire

**Table A-18** The curve fitting and equation of % CUT-OFF of tire co-pyrolysis with various %Ge loaded on mordenite.

$y = y_o + \frac{a}{\left[1 + e^{-\left(\frac{x-x_o}{b}\right)}\right]}^c$	Parameter	Coefficient	$R^2$
Non-cat	a	143.914	0.9983837
	b	17.0373	
	c	0.054422	
	$x_o$	399.541	
	$y_o$	-46.9545	
0.00%Ge	a	123.89	0.99963226
	b	64.3239	
	c	0.399807	
	$x_o$	392.034	
	$y_o$	-16.7286	
0.5%Ge	a	125.867	0.9978671
	b	31.5519	
	c	0.124918	
	$x_o$	395.529	
	$y_o$	-29.3922	
1%Ge	a	124.843	0.9990228
	b	42.8746	
	c	0.201499	
	$x_o$	372.735	
	$y_o$	-24.0008	
3%Ge	a	143.349	0.9975179
	b	19.4622	
	c	0.0767277	
	$x_o$	316.787	
	$y_o$	-47.7435	
5%Ge	a	134.812	0.9975559
	b	22.7872	
	c	0.074224	
	$x_o$	409.475	
	$y_o$	-38.5028	

## **Appendix B Standard for gas chromatography**

**Table B-1** Standard Refinery Gas Compositions for gas chromatography calibration

Approximate concentration % volume/volume

Compositions	% volume/volume
Hydrogen	15
Nitrogen	15
Carbon dioxide	5
Carbon monoxide	5
Methane	5
Ethane	1
Ethylene	10
Propane	1
Propylene	5
Iso-butane	10
N-butane	5
Butane	10
Trans-2-butene	5
Cis-2-butene	5
N-pentane	1
Iso-pentane	2

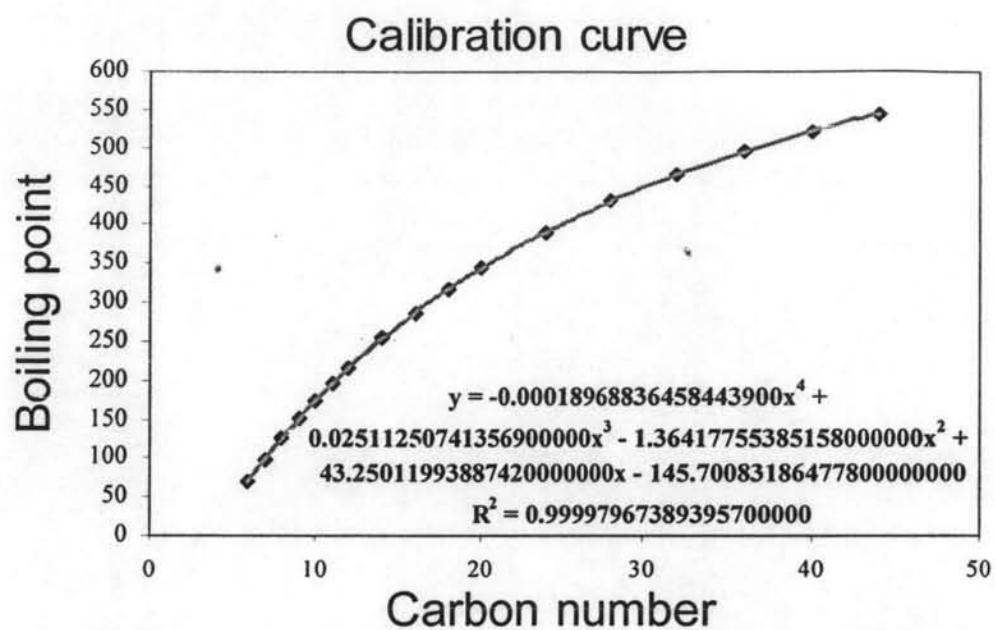
**Table B-2** Liquid for gas chromatography calibration

Liquid standard	Density @ 20°C
N-pentane	0.626
N-hexane	0.659
N-heptane	0.684
Iso-octane	0.6919

**Table B-3** ASTM Method D2887 Column Test Mixture

This ULTRA standard (TM) solution was gravimetrically prepared, and the analyte concentrations were verified using high resolution gas chromatography.

Components	Carbon number	% By weight
N-hexane	6	6.0
N-heptane	7	6.0
N-octane	8	8.0
N-nonane	9	8.0
N-decane	10	12.0
N-undecane	11	12.0
N-dodecane	12	12.0
N-tetradecane	14	12.0
N-hexadecane	16	10.0
N-octadecane	18	5.0
N-eicosane	20	2.0
N-tetracosane	24	2.0
N-octacosane	28	1.0
N-dotriacontane	32	1.0
N-hexatriacontane	36	1.0
N-tetracontane	40	1.0
N-tetratetracontane	44	1.0



**Figure B-1** GC calibration curve of ASTM D2887 Column Test Mixture with the equation of fitted curve.

## CURRICULUM VITAE

**Name:** Ms. Papaphan Surmanich

**Date of Birth:** September 9, 1981

**Nationality:** Thai

**University Education:**

2000-2004 Bachelor Degree of Science in Petrochemical, Faculty of Science, King Mongkut's Institute Technology of Ladkabang, Bangkok, Thailand