

## CHAPTER 1

### INTRODUCTION

#### 1.1 The Problem Considered.

The energy consumption rate of the world is so great that it is certain that the supply of the fossil fuels will be depleted within the next century. During the last few years, men have been searching to harness alternative sources of energy to be substituted for the fossil fuels. Among these, solar energy looks very promising since it is readily available in huge amount and has no known polluting effects upon the environment when converted into other forms for utilization.

Nowaday, refrigeration plays significant role in human society. It is used for preservation of food and medicine. It provides controlled temperature and humidity atmosphere for human comfort or for industrial processes. Absorption refrigeration cycle appears to be suitable for using solar radiation as heat source. There are two types of absorption refrigeration systems, namely the continuous and the intermittent cycle. The continuous one requires many mechanical components but gives continuous cooling effect while the intermittent machine gives periodic cooling. Its main advantages are the lack of mechanical component, simple system, low cost and long maintenance interval. These are the reasons for choosing the intermittent system for this study.

There are many published works on intermittent absorption unit. Trombe and Foex<sup>1</sup> reported some preliminary experiments with a pilot plant using the ammonia-water system. Williams, Chung, Lof Fester and Duffie<sup>2</sup> described a comprehensive investigation which included theoretical estimation of the performance of four different binary systems (methanol-silica gel, acetone-silica gel, ammonia-water and Freon 21-tetraethylene glycol dimethyl ether), and experimental study of two of these systems. In both the above investigations, the heat source was solar radiation focussed on to the generator by means of a reflector.

Eisenstadt, Flanigan and Farber<sup>3</sup> studied and reported on the ammonia-water system for solar cooling with solution concentration varying from 0.4 to 0.7 and with a maximum generator temperature ranges from 140 to 180 F.

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<sup>1</sup>Trombe, F. and Foex, M. Economic Balance Sheet of Ice Manufacture with an absorption machine utilizing the sun as the heat source Paper S/109 UN conference of New Sources of Energy (1961)

<sup>2</sup>Williams, D.A., Chung, R., Lof, G.O.G., Fester, D.A., and Duffie, J.A. Refrigerating Engineering, 66, 33 (Nov. 1958)

<sup>3</sup>Eisenstadt, m., Flannigan, F.M., and Farber, E.A. Solar airconditioning with an NH<sub>3</sub>-water absorption refrigeration system. Engineering Progress at University of Florida, Technical Progress Report, 14, No. 2, 22-28 (1960)

Chinnappa<sup>4</sup> reported about the efficiency of a refrigeration using both the ammonia-lithiumnitrate system and the ammonia-water system. The author gave detailed calculations of operations of both system, (without solar heating).

An ammonia-sodiumthiocyanate system was tested by Chung<sup>5</sup> et. al. for solar refrigeration in the laboratory. From a 20 pound steel cylinder containing 12 pounds of the solution of approximately 1:1 by weight of ammonia and sodiumthiocyanate, 9 pounds of ice were produced per cycle. The author did not give any detailed information describing the performance of his intermittent absorption.

Beckman<sup>6</sup> proposed a theoretical performance of an ammonia-sodiumthiocyanate intermittent absorption refrigeration cycle. Swartman<sup>7</sup> also studied the ammonia-sodiumthiocyanate refrigerator by using a flat plate collector as a generator-absorber. The author shows that the  $\text{NH}_3\text{-NaSCN}$  refrigerant-absorbent has better performance than  $\text{NH}_3\text{-H}_2\text{O}$  refrigerant.

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<sup>4</sup>Chinnappa, J.C.V. "Experimental Study of the Intermittent Vapour Absorption Refrigeration Cycle Employing the Refrigerant-Absorbent System of Ammonia-Water and Ammonia-Lithium Nitrate," J. Solar Energy Sci. and Eng. 5,1 (1961).

<sup>5</sup>Chung, r., and Duffie, J.A. "Cooling with Solar Energy," Paper S/82 presented at UN conference on New Sources of Energy (1961)

<sup>6</sup>Beckman, W.A. "Theoretical performance of an ammonia-sodiumthiocyanate intermittent absorption refrigeration cycle. Solar Energy 12, 137-146 (1968)

<sup>7</sup>Swartman, R.K., "Comparison of  $\text{NH}_3\text{-NaSCN}$ " J. Solar Energy, 17, (1975)

## 1.2 Purpose of the present investigation.

The purpose of the present investigation are:

- i) To study the performance of an intermittent absorption solar refrigeration system using  $\text{NH}_3\text{-NaSCN}$ .
- ii) To compare the actual cycle to the theoretical intermittent absorption cycle.
- iii) To compare the results with that of the existing data on  $\text{NH}_3\text{-LiNO}_3$  and  $\text{NH}_3\text{-H}_2\text{O}$  systems.
- iv) To determine the best practical concentration for intermittent refrigeration system ( $\text{NH}_3\text{-NaSCN}$ ).

## Notation

|          |   |
|----------|---|
| $c$      | specific heat of $\text{NH}_3$ -NaSCN solution  |
| $c_m$    | specific heat of $\text{NH}_3$ -NaSCN solutions over a temperature range                        |
| $H$      | enthalpy of solution  |
| $H_v$    | enthalpy of liquid ammonia  |
| $L_m$    | mean latent heat of ammonia   |
| $L_{dm}$ | mean differential heat of evaporation of ammonia  |
| $P$      | pressure  |
| $Q_c$    | effective cooling   |
| $Q_s$    | heat supplied to solution during regeneration   |
| $t$      | temperature of solution   |
| $W$      | mass of solution  |
| $X_a$    | concentration of solution, mass of absorbent per unit<br>mass of solution                       |
| $X_r$    | concentration of solution, mass of refrigerant per unit<br>mass of solution                     |
| $X_v$    | concentration of vapour, mass of refrigerant per unit<br>mass of vapour                         |
| $W$      | incremental change in solution mass   |
| $t_n$    | temperature rise of the solution during which the<br>incremental change in solution mass is $W$ |
| $C$      | concentration (light)   |
| COP      | coefficient of performance = $Q_c / Q_s$  |

$A_{nm}$  projected area of parabolic solar collector  
 $A_t$  surface area of target which receives the reflected light  
 $D$  diameter of collector  
 $d$  diameter of target  
 $n$  relative aperture  
 $f$  focus length  
 $\alpha$  angle