

REFERENCES

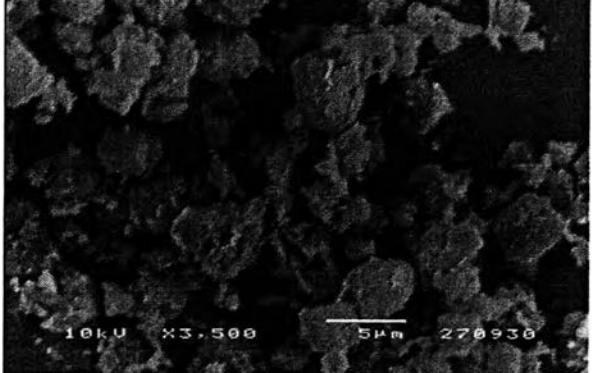
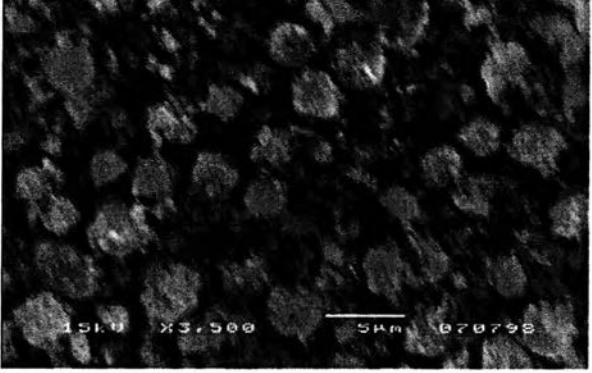
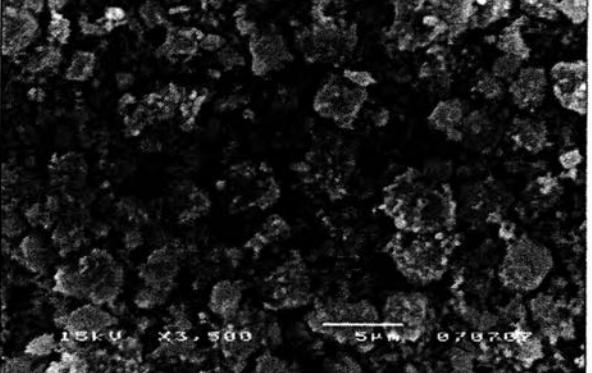
- Ali Khan, I., and Loughlin, K.F. (2003). Kinetics of sorption in deactivated zeolite crystal adsorbents. *Computers and Chemical Engineering*, 27, 689- 696.
- Berger Bill D., and Anderson Kenneth E. (1980). *Gas handling and field processing*. Tulsa, Okla. Pennwell.
- Campbell John M. (1984). *Gas conditioning and processing v.2: the equipment modules*. Norman, Okla. Campbell Petroleum Series.
- Chaikasetpaiboon, P. (2002). Experimental and mathematical modeling of a multibed gas adsorber. M.S. Thesis, The Petroleum and Petrochemical College, Chulalongkorn University.
- Fogler, H.S., (2006). *Elements of Chemical Reaction Engineering 4th edition*. New Jersy, Prentice-Hall Inc.
- Gandhidasan P., Al-Farayedhi Abdulghani A., Al-Mubarak Ali A.. (2001). Dehydration of natural gas using solid desiccants. *Energy*, 26, 855–868.
- Khaikham, W. (2007). Deactivation modeling for adsorption isotherm of deactivated adsorbents used in natural gas dehydration process. M.S. Thesis, The Petroleum and Petrochemical College, Chulalongkorn University.
- Kopac, T., and Kocabas, S. (2002). Adsorption equilibrium and breakthrough analysis for sulfur dioxide adsorption on silica gel. *Chemical Engineering and Processing*, 41, 223–230.
- Kopac, T., and Kocabas, S. (2004). Adsorption equilibrium and breakthrough analysis for sulfur dioxide adsorption on silica gel. *Advances in Environmental Research*, 8, 417–424.
- Murillo, R., García, T., Aylon, E., Callen, M.S., Navarro, M.V., Lopez, J.M., Mas- tral, A.M. (2004). Adsorption of phenanthrene on activated carbons: Breakthrough curve modeling. *Carbon*, 42, 2009–2017.
- Ruthven, D. M. (1984). *Principle of Adsorption and Adsorption Process*. New York: Wiley.
- Rojey, A., Jaffret, C., Cornot-Gadolphe, S., Durand, B., Jullian, S., and Valais, M. (1997). *Natural Gas: production processing transport*. France, Imprimerie Nouvelle.

- Rodrigues, E., LeVan, M., and Tondeur, D. (1989). Adsorption:Science and Technology. Natherlands, Kluwer
- Toth, J. (2002). Adsorption theory,modeling, and analysis. New york, Dekker.
- Uttamaroop, T. (2003). Sensitivity analysis and development of mathematical model for water breakthrough curves of a multi-layer adsorber. M.S. Thesis, The Petroleum and Petrochemical College, Chulalongkorn University.
- Yang, R.T. (1987) Gas Adsorption by Adsorption Process. London: Butterworths.
- Zhang, H., and Cheng, D. (2000). Mathematical model for a fixed bed adsorptive reactor. Carbon, 38, 877– 880.

APPENDICES

Appendix A: SEM Images of Molecular Sieve Zeolites

Table A1 SEM images of 1/8" molecular sieve

Number of batches	SEM images
Fresh	 <p>10kV X3,500 5μm 270930</p> <p>x 3500</p>
5 batches	 <p>15kV X3,500 5μm 070798</p> <p>x 3500</p>
15 batches	 <p>15kV X3,500 5μm 070707</p> <p>x 3500</p>

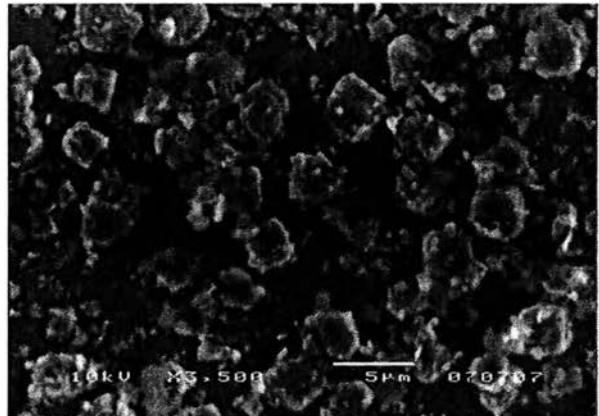
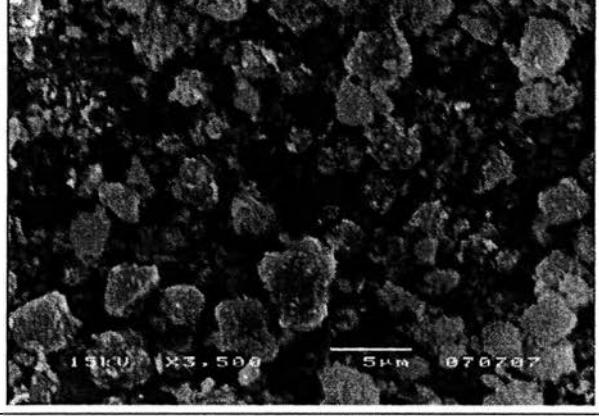
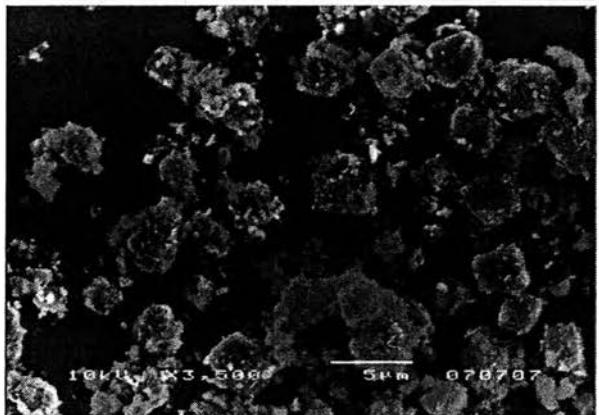
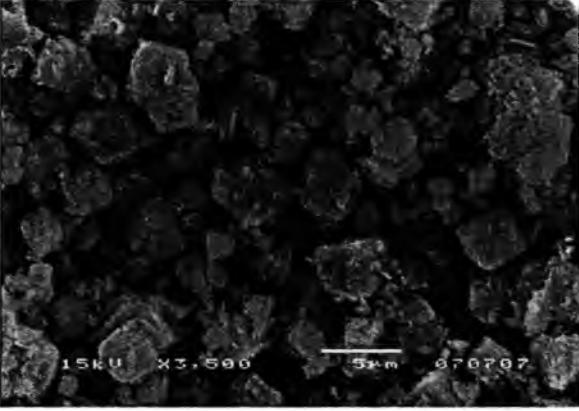
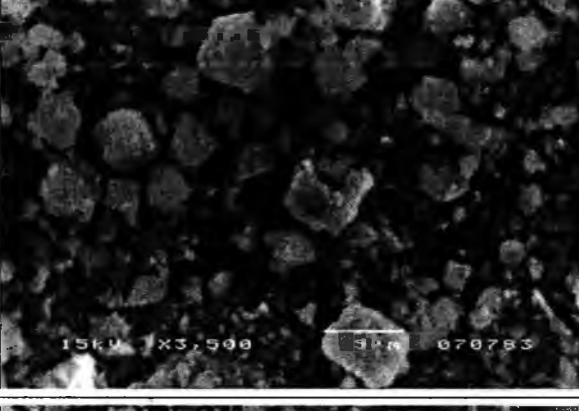
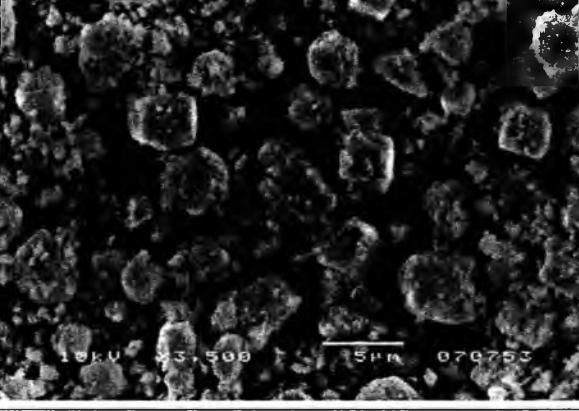
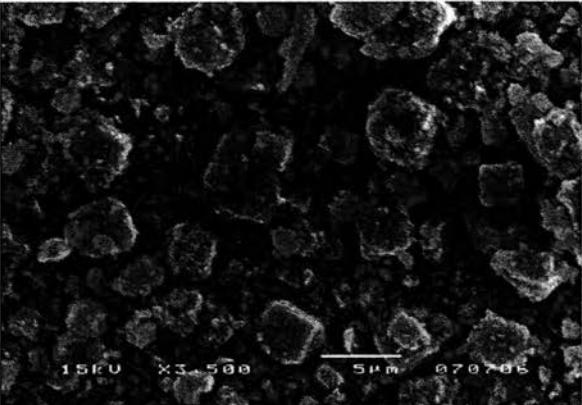
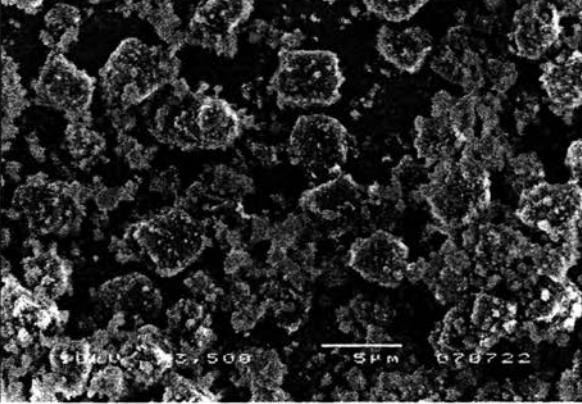
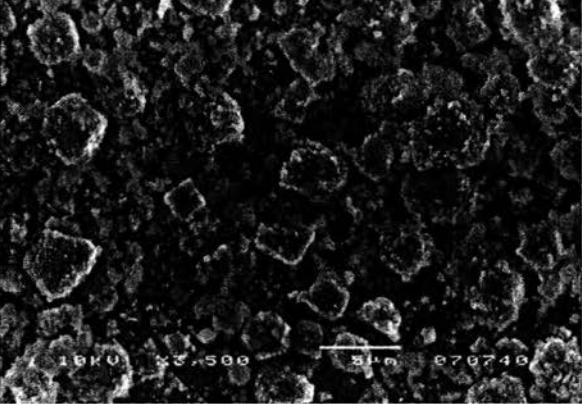
Number of batches	SEM images
25 batches	 A scanning electron micrograph showing a surface covered with numerous small, irregularly shaped particles. The particles appear to be clusters of smaller units. The background is dark. Technical data at the bottom left reads "10KV X3.500". A scale bar labeled "5μm" is located at the bottom right, with the number "878787" next to it. x 3500
35 batches	 A scanning electron micrograph showing a similar surface morphology to the 25 batches image, with a dense distribution of small particles. Technical data at the bottom left reads "10KV X3.500". A scale bar labeled "5μm" is located at the bottom right, with the number "878787" next to it. x 3500
45 batches	 A scanning electron micrograph showing a surface with a higher density of larger, more distinct clusters compared to the previous images. Technical data at the bottom left reads "10KV X3.500". A scale bar labeled "5μm" is located at the bottom right, with the number "878787" next to it. x 3500

Table A2 SEM images of 1/16" molecular sieve

Number of batches	SEM images
Fresh	 15kV x3,500 5μm 070707 x 3500
5 batches	 15kV x3,500 5μm 070783 x 3500
15 batches	 15kV x3,500 5μm 070753 x 3500

Number of batches	SEM images
25 batches	 <p>15KV X3,500 5µm 070705</p> <p>x 3500</p>
35 batches	 <p>15KV X3,500 5µm 070722</p> <p>x 3500</p>
45 batches	 <p>15KV X3,500 5µm 070748</p> <p>x 3500</p>

Appendix B: Data of Crystal Size Distribution from SEM

Table B1 Data of crystal size distribution of 1/8" molecular sieve

Number of Batches Crystal size range (micron)	%quantity					
	fresh	5 batches	15 batches	25 batches	35 batches	45 batches
0.00-0.49	0	0	0	0	0	0
0.50-0.99	0	0	0	4	2	4
1.00-1.49	0	1	7	26	19	21
1.50-1.99	0	2	24	21	29	35
2.00-2.49	4	22	44	30	35	40
2.50-2.99	47	40	22	15	15	0
3.00-3.49	45	30	3	4	0	0
3.50-3.99	4	4	0	0	0	0
4.00-4.49	0	1	0	0	0	0
Average crystal size (micron)	2.99	2.805	2.195	1.96	1.955	1.8

Table B2 Data of crystal size distribution of 1/16" molecular sieve

Number of batches Crystal size range (micron)	%quantity					
	fresh	5 batches	15 batches	25 batches	35 batches	45 batches
0.00-0.49	0	0	0	0	0	0
0.50-0.99	0	0	2	4	2	2
1.00-1.49	0	3	15	14	20	32
1.50-1.99	5	7	23	30	32	39
2.00-2.49	9	17	42	34	25	17
2.50-2.99	35	33	18	18	20	10
3.00-3.49	33	26	0	0	1	0
3.50-3.99	16	13	0	0	0	0
4.00-4.49	2	1	0	0	0	0
Average crystal size (micron)	3.000	2.82	2.04	1.985	1.965	1.75

Appendix C: Bed Void Fraction

The bed void fraction of both fresh and deactivated adsorbents can be obtained from Figure A1.

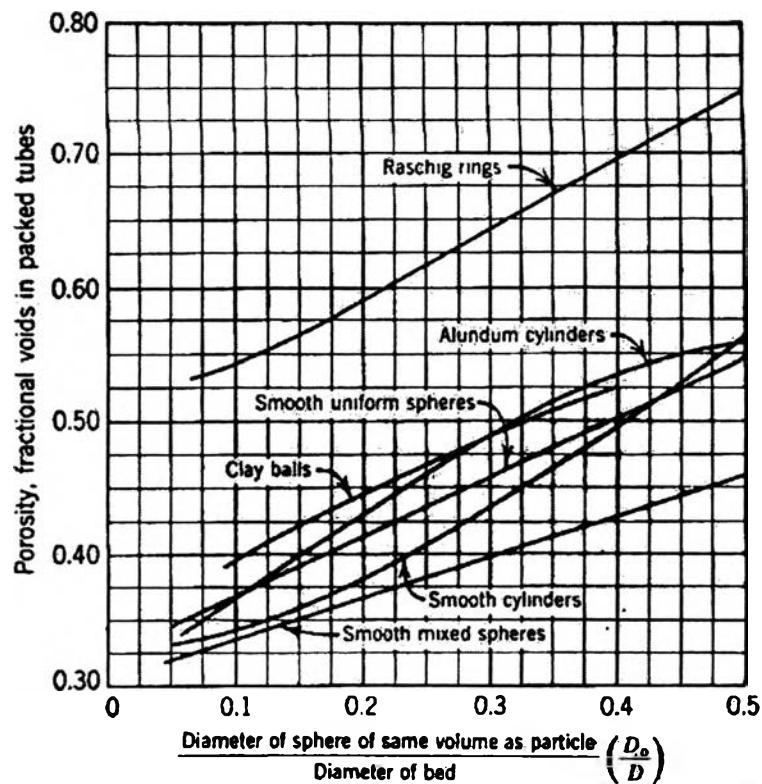


Figure C Porosity as a function of the ration of particle diameter to bed diameter (Leva, 1947).

Appendix D: Mass Transfer Coefficient

The mass transfer coefficient, k , of both fresh and deactivated adsorbents can be calculated by following equation (Murillo *et al.*, 2004).

$$\frac{1}{k} = \frac{R_p}{3k_f} K + \frac{R_p^2}{15\varepsilon_p D_e} K \quad (D1)$$

where

k	=	mass transfer coefficient (1/sec)
k_f	=	fluid mass transfer coefficient (m/s)
R_p	=	radius of pellet (m)
K	=	equilibrium constant
ε_p	=	porosity of particle
D_e	=	effective diffusivity (m^2/s)

The effective diffusivity (D_e), which was used in equation D1, is related to Knudsen diffusivity (D_k) and molecular diffusivity (D_m), as follows.

$$\frac{1}{D_e} = \frac{\tau}{\varepsilon_p} \left(\frac{1}{D_m} + \frac{1}{D_k} \right) \quad (\text{D2})$$

Also, the Knudsen diffusivity (D_k) and molecular diffusivity (D_m) can be obtained from equations D3 and D4, respectively.

$$D_k = 9.7 \times 10^3 r_p \left(\frac{T}{M} \right)^{1/2} \quad (\text{D3})$$

$$D_m = \frac{0.0018583 T^{3/2} (1/M_A + 1/M_B)^{1/2}}{P * \sigma_{AB}^2 \Omega_{AB}} \quad (\text{D4})$$

r_p	=	mean pore radius (cm)
T	=	absolute temperature (K); and
M	=	molecular weight of diffusing species
M_A	=	average molecular weight of bulk species
M_B	=	molecular weight of adsorbate species
P	=	total pressure
σ_{AB}	=	collision diameter from Lennard-Jones potential; and
Ω_{AB}	=	collision integral

Appendix E: Breakthrough Curve Prediction Program

This program can be used for predict the breakthrough curve by input the degree of deactivation because the parameters in mass balance equation and the adsorption isotherm were written as a function of the degree of deactivation.

```

IMPLICIT NONE
DOUBLE PRECISION RHR,Velo,Alu,Bmol,Smol,DA,Db,Ds
DOUBLE PRECISION C0,C,q,dt,KC,Kq,time,Csat,RH
DOUBLE PRECISION v1,v,e_A,e_B,e_C
INTEGER i,j,imax,jmax,n
PARAMETER(imax=90,jmax=5000)
DIMENSION C(imax,jmax),q(imax,jmax),v(imax,jmax)
DIMENSION KC(4,imax,jmax),Kq(4,imax,jmax)

c .....INITIAL CONDITION.....
dt = 0.008
time=0
j=1           !at time = 0
Csat=1.2794E-03
C(1,j)=C0

OPEN(9,file='breakthrough.txt') !open file to receive input values
READ(9,*)Alu,Bmol,Smol,RHR,Velo
RH = RHR
C0 = RH*Csat/100    !inlet concentration (mol/l)
v1= Velo            ! Superficial velocity
DA = Alu
Db    = Bmol
Ds    = Smol
e_A=-0.0000002834*DA**2-0.00001597 *DA+0.3698157 !void fraction as
a function of degree of deactivation
e_B=-0.00000003348 *Db**2-0.000004606*Db+0.3448013
If(Ds.LE.62.38) then
  e_C=-0.0004604*Ds**0.028037+0.329731
Else
  e_C=0.3691822-0.001106*Ds+7.44E-06*Ds**2
END if
v(1,j)=v1/e_A

WRITE(*,*)"Input Values' ! show input values
WRITE(*,*)%deactivation of alumina=',DA
WRITE(*,*)%deactivation of 1/8"4A Molsiv=',Db
WRITE(*,*)%deactivation of 1/16"4A Molsiv=',Ds

```

```

      WRITE(*,*)"Relative Humidity='RH'
      WRITE(*,*)"Superficial Velocity='v1,'(cm/s)'
      WRITE(*,*)'-----'
      WRITE(*,*)" Running Program   '
      WRITE(*,*)" Please Wait   '
      WRITE(*,*)'-----'
OPEN(5,file='velocity.dat')

DO i=2,imax

      C(i,j)=0
      q(i,j)=0

END DO

OPEN(1,file='data1.dat')

DO i=1,imax
      WRITE(1,101)time,i,j,C(i,j),q(i,j),v(i,j)
END DO

Call RK4(j,C,q,v,imax,jmax,KC,Kq,dt,v1,DA,Db,Ds)

GOTO 20

10   OPEN(2,FILE='DATA2.DAT')

      DO i=2,imax

            READ(2,102)time,C(i,1),q(i,1),v(i,1),(KC(n,i,1),n=1,4)
            1 ,(Kq(n,i,1),n=1,4)

      END DO

20   DO j=2,jmax

            DO i=2,imax

                  v(1,j)=v1/e_A
                  C(1,j)=C0

                  C(i,j)=C(i,j-1)+(dt/6)*(KC(1,i,j-1)+2*KC(2,i,j-1)
1                      +2*KC(3,i,j-1)+KC(4,i,j-1))

                  q(i,j)=q(i,j-1)+(dt/6)*(Kq(1,i,j-1)+2*Kq(2,i,j-1)
1                      +2*Kq(3,i,j-1)+Kq(4,i,j-1))

            END DO
      END DO

```

```

    END DO

    Call RK4(j,C,q,v,imax,jmax,KC,Kq,dt,v1,DA,Db,Ds)

    END DO

```

CThe Results.....

```

DO j=1,jmax

    time=time+dt           !sec

    END DO

    CLOSE(2)
    OPEN(2,file='data2.dat')
    DO i=2,imax

        WRITE(2,102)time,C(i,jmax),q(i,jmax),v(i,jmax)
1      ,(KC(n,i,jmax),n=1,4),(Kq(n,i,jmax),n=1,4)

        WRITE(5,102)time,C(i,jmax),q(i,jmax),v(i,jmax)

        OPEN(3,file='RESULT.dat')
        IF(i.EQ.imax)THEN
            WRITE(3,102)time,C(i,jmax),q(i,jmax),v(i,jmax)

        ELSE
        END IF

    END DO

```

CCheck Running Loop.....

```

IF(time.LT.400000) THEN
GOTO 10
ELSE
GOTO 999
END IF

```

CFormat for Input and Output Statements.....

```

99  FORMAT(E15.9,E15.9,E15.9,E15.9,E15.9)
101 FORMAT(F13.3,I3,I6,2E15.9,8E15.9)
102 FORMAT(F13.3E15.9,8E15.9)

```

```

999 STOP
    CLOSE(3)
END

c
*****
***** SUBROUTINE RK4(j,C,q,v,imax,jmax,KC,Kq,dt,v1,DA,Db,Ds)

IMPLICIT NONE
DOUBLE PRECISION DA,Db,Ds,v1
DOUBLE PRECISION CC,qq,C,q,dC_dt,dq_dt,dt,KC,Kq,v
INTEGER i,j,imax,jmax
DIMENSION C(imax,jmax),q(imax,jmax),dC_dt(imax,jmax)
DIMENSION dq_dt(imax,jmax),KC(4,imax,jmax),Kq(4,imax,jmax)
DIMENSION CC(imax,jmax),qq(imax,jmax),v(imax,jmax)

c .....Define Parameter.....
!v1= Velo      ! Superficial velocity
!DA = Alu
!Db    = Bmol
!Ds    = Smol

DO i=1,imax
    CC(i,j)=C(i,j)
    qq(i,j)=q(i,j)
END DO

Call ODEs_EQ(j,imax,jmax,CC,qq,dC_dt,dq_dt,v,v1,DA,Db,Ds)

DO i=2,imax
    KC(1,i,j)=dC_dt(i,j)
    Kq(1,i,j)=dq_dt(i,j)
    CC(i,j)=CC(i,j)+(dt/2)*KC(1,i,j)
    qq(i,j)=qq(i,j)+(dt/2)*Kq(1,i,j)
END DO

Call ODEs_EQ(j,imax,jmax,CC,qq,dC_dt,dq_dt,v,v1,DA,Db,Ds)

DO i=2,imax

```

```

KC(2,i,j)=dC_dt(i,j)
Kq(2,i,j)=dq_dt(i,j)

CC(i,j)=CC(i,j)+(dt/2)*KC(2,i,j)
qq(i,j)=qq(i,j)+(dt/2)*Kq(2,i,j)

END DO

Call ODEs_EQ(j,imax,jmax,CC,qq,dC_dt,dq_dt,v,v1,DA,Db,Ds)

DO i=2,imax

KC(3,i,j)=dC_dt(i,j)
Kq(3,i,j)=dq_dt(i,j)

CC(i,j)=CC(i,j)+(dt)*KC(3,i,j)
qq(i,j)=qq(i,j)+(dt)*Kq(3,i,j)

END DO

Call ODEs_EQ(j,imax,jmax,CC,qq,dC_dt,dq_dt,v,v1,DA,Db,Ds)

DO i=2,imax

KC(4,i,j)=dC_dt(i,j)
Kq(4,i,j)=dq_dt(i,j)

END DO

Return

End

c
*****
*****
```

SUBROUTINE ODEs_EQ(j,imax,jmax,c,q,dC_dt,dq_dt,v,v1,DA,Db,Ds)

```

IMPLICIT NONE
DOUBLE PRECISION
c,q,dC_dt,dz,L,d2C_dz2,DL_A,v1,e_A,e_B,e_C,dq_dt
DOUBLE PRECISION k1,k2,k3
DOUBLE PRECISION
dC_dz,qstar,a1,a2,a3,b1,db_A,db_B,db_C,DL_B,DL_C
DOUBLE PRECISION Csat,b2,t1,d1,b3,t2,d2,RT,Pa,Psat,P0
DOUBLE PRECISION v,dv_dz,Ct
DOUBLE PRECISION rd_A,rd_B,rd_C
```

```

DOUBLE PRECISION DA,Db,Ds
INTEGER i,j,imax,jmax
DIMENSION C(imax,jmax),q(imax,jmax),dC_dt(imax,jmax)
DIMENSION d2C_dz2(imax,jmax),dC_dz(imax,jmax),qstar(imax,jmax)
DIMENSION dq_dt(imax,jmax),v(imax,jmax),dv_dz(imax,jmax)

!v1= Velo           ! Superficial velocity
!DA = Alu
!Db    = Bmol
!Ds    = Smol

```

cDefine Parameter.....

L =8.8	! Total bed length
dz = L/ (imax-2)	! Step size for length
Ct=0.040902639	! P/RT
RT=24.45388	! RT
Pa=1.0133E+08	! atmospheric pressure
P0=1.01325E+06	.

cParameter of Adsorber Zone-A (Activated Alumina).....

db_A =0.73743	! Bulk density of adsorbent
Zone-A	
DL_A=0.028249704	! Axial dispersion through Zone-A
e_A=-0.0000002834*DA**2-0.00001597*DA+0.3698157	!Void fraction ofZone-A
rd_A=(-0.0053*DA**2-0.1761*DA-195.93)/10	

cParameter of Adsorber Zone-B (UI-94 1/8").....

db_B=0.66529	! Bulk density of adsorbent Zone-B
DL_B=0.027733066	! Axial dispersion through Zone-B
e_B=-0.00000003348*Db**2-0.000004606*Db+0.3448013	!Void fraction of
C Zone-B	
rd_B=(-0.0026461*Db**2-0.0098614*Db-283.2747)/10	

cParameter of Adsorber Zone-C (UI-94 1/16").....

db_C =0.66529	! Bulk density of adsorbent
Zone-C	

```

DL_C=0.027170115          ! Axial dispersion through Zone-C
If(Ds.LE.62.38) then      ! Void fraction of Zone-C
  e_C=-0.0004604*Ds**0.028037+0.329731
  rd_C=(-53.02706*Ds**0.0287672-1167.399)/10

Else
  e_C=0.3691822-0.001106*Ds+7.44E-06*Ds**2
  rd_C=(3637.953-134.6133*Ds+0.9053535*Ds**2)/10
END if

c .....Adsorption Isotherm Constant Parameter.....
k1 =-0.000000001345*DA**2-0.0000003543*DA+0.00006169 ! Effective
overall mass transfer coeficient
k2 =-0.000000008449*Db**2-0.0000003555*Db+0.00004525
k3 =-0.000000007212*Ds**2-0.0000007993*Ds+0.0001557
j=j
c .....Zone-A (Silica gel).....
Csat=1.2794E-03
a1=1.197121-0.0290791*DA+0.0001773*DA**2 ! For Freundlich-
Isotherm
if(DA.LE.67.9) then
  b1= 2.09E-05*DA**2.510129+0.8289536
Else
  b1=-0.0005461*DA**2+0.0834425*DA-1.48687
END if
DO i=2,4

qstar(i,j)=a1*((100*C(i,j)/Csat)**b1)

dq_dt(i,j)=k1*(qstar(i,j)-q(i,j))

d2C_dz2(i,j)=(1/(dz**2))*(C(i+1,j)-2*C(i,j)+C(i-1,j))

dC_dz(i,j)=(1/(2*dz))*(C(i+1,j)-C(i-1,j))

dv_dz(i,j)=-(v1*rd_A)/(e_A*P0*((2*rd_A*(i-1)*dz/P0)+1)**1.5)

v(i,j)=dz*(dv_dz(i,j))+v(i-1,j)

dC_dt(i,j)=DL_A*d2C_dz2(i,j)-v(i,j)*dC_dz(i,j)
1 -((1-e_A)/e_A)*dq_dt(i,j)*db_A/1.8-C(i,j)*dv_dz(i,j)

END DO

c .....Zone-B (Mol Siv 1/8").....
Psat=3169904.00

```

```

a2=-1.269777*Db**0.5740309+17.50962
b2=70.87607*Db**0.3887716+20.02354
t1=-1.038514*Db**0.1542384+2.902765
d1=0.0425293*Db**0.4721149+0.1048701
P0=P0*((2*rd_A*0.3/P0)+1)**0.5
DO i=5,60

    qstar(i,j)=(a2*b2*C(i,j)/Csat)/(((1+(b2*C(i,j)/ Csat)**t1)***(1/t1))*(1-c(i,j)/Csat)**d1)

    dq_dt(i,j)=k2*(qstar(i,j)-q(i,j))

    d2C_dz2(i,j)=(1/(dz**2))*(C(i+1,j)-2*C(i,j)+C(i-1,j))

    dC_dz(i,j)=(1/(2*dz))*(C(i+1,j)-C(i-1,j))

    dv_dz(i,j)=-(v(4,j)*rd_B)/(P0*((2*rd_B*(i-4)*dz/P0)+1)**1.5)

    v(i,j)=dz*(dv_dz(i,j))+v(i-1,j)

    v(5,j)=v(5,j)*e_A/e_B

    dC_dt(i,j)=DL_B*d2C_dz2(i,j)-v(i,j)*dC_dz(i,j)
    -((1-e_B)/e_B)*dq_dt(i,j)*db_B/1.8-C(i,j)*dv_dz(i,j)

END DO

c .....Zone-C (Mol Siv 1/16")
a3=-1.441778*Ds**0.5831572+18.0277
b3=15.51344*Ds**0.7242306+24.18842
t2=-1.740397*Ds**0.1264964+3.877282
d2=0.0262151*Ds**0.7678798+0.1262725
Psat=3169904.00
P0=P0*((2*rd_B*5.6/P0)+1)**0.5
DO i=61,89

    qstar(i,j)=(a3*b3*C(i,j)/Csat)/(((1+(b3*C(i,j)/ Csat)**t2)***(1/t2))*(1-c(i,j)/Csat)**d2)

    dq_dt(i,j)=k3*(qstar(i,j)-q(i,j))

    d2C_dz2(i,j)=(1/(dz**2))*(C(i+1,j)-2*C(i,j)+C(i-1,j))

    dC_dz(i,j)=(1/(2*dz))*(C(i+1,j)-C(i-1,j))

    dv_dz(i,j)=-(v(60,j)*rd_C)/(P0*((2*rd_C*(i-60)*dz/P0)+1)**1.5)

```

$$v(61,j) = v(61,j) * e_B / e_C$$

$$v(i,j) = dz * (dv_dz(i,j)) + v(i-1,j)$$

$$1 \quad dC_dt(i,j) = DL_C * d2C_dz2(i,j) - v(i,j) * dC_dz(i,j) \\ - ((1-e_C) / e_C) * dq_dt(i,j) * db_C / 1.8 - C(i,j) * dv_dz(i,j)$$

END DO

i=imax

$$qstar(imax,j) = qstar(imax-1,j)$$

$$dq_dt(imax,j) = dq_dt(imax-1,j)$$

$$d2C_dz2(imax,j) = 0$$

$$dC_dz(imax,j) = 0$$

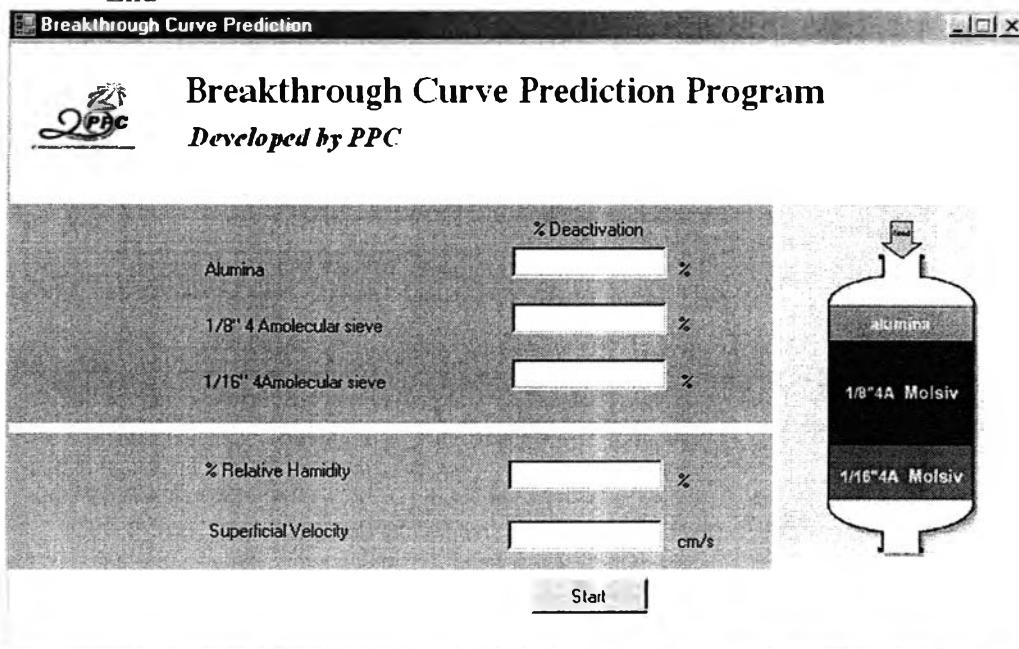
$$dC_dt(imax,j) = dC_dt(imax-1,j)$$

$$dv_dz(imax,j) = dv_dz(imax-1,j)$$

$$v(imax,j) = v(imax-1,j)$$

Return

End



CURRICULUM VITAE

Name: Mr. Satjatham Polsaen

Date of Birth: March 22, 1983

Nationality: Thai

University Education:

2002-2006 Bachelor Degree of Science (Department of Physics), Faculty of Science, Chulalongkorn University, Bangkok, Thailand.

