

REFERENCES

- Argun, H., Kargi, F., Kapdan, I.K., and Oztekin, R. (2008). Biohydrogen production by dark fermentation of wheat powder solution: effects of C/N and C/P ratio on hydrogen yield and formation rate. International Journal of Hydrogen Energy, 33, 6109-6115.
- Bartacek, J., Zabranska, J., and Lens, P.N.L. (2007). Developments and constraints in fermentative hydrogen production. Biofuels, Bioproducts and Biorefining, 1, 201-214.
- Bashaar, Y.A. (2005). Treatment of olive mill wastewater using an anaerobic sequencing batch reactor. Desalination, 177, 157-165.
- Bhaskar, Y.V., Mohan, S.V., and Sarna, P.N. (2008) Effect of substrate loading rate of chemical wastewater on fermentative biohydrogen production in biofilm configured sequencing batch reactor. Bioresource Technology, 99, 6941-6948.
- Chong, M., Sabaratnam, V., Shirai, Y and Hassan, M. (2009). Biohydrogen production from biomass and industrial wastes by dark fermentation. International Journal of Hydrogen Energy, 34, 3277-3287.
- Das, D. and Veziroglu, T.N. (2001). Hydrogen production by biological processes: a survey of literature. International Journal of Hydrogen Energy, 26, 13-28.
- Deutschmann, O. and Schmidt, L. (1998). Two-dimensional modeling of partial oxidation of methane on rhodium in contact time reactor. The Combustion Institute, 2283-2291.
- Dugba, P.N. and Zhang, R. (1998). Treatment of dairy wastewater with two-stage anaerobic sequencing batch reactor systems - thermophilic versus mesophilic operations. Bioresource Technology, 68, 225-233
- Fan, Y.T., Zhang, G.S., Guo, X.Y., Xing, Y., and Fan, M.H. (2006). Biohydrogen-production from beer lees biomass by cow dung compost. Biomass and Bioenergy, 30, 493-496.

- Fascetti, E., D'Addario, E., Todini, O., and Robertiello, A. (1998). Photosynthetic hydrogen evolution with volatile organic acids from the fermentation of source selected municipal solid wastes. International Journal of Hydrogen Energy, 23(9), 753-760.
- Eaton, A.D., Clesceri, L.S., Rice, E.W., and Greenberg, A.E. (2005). Standard Methods for the Examination of Water and Wastewater. Washington, D.C.: American Public Health Association.
- Ginkel, S.W., Oh, S.E., and Logan, B.E. (2005). Biohydrogen gas production from food processing and domestic wastewater. International Journal of Hydrogen Energy, 30, 1535-1542.
- Hawkes, F.R., Dinsdale, R., Hawkes, D.L., and Hussy, I. (2002). Sustainable fermentative hydrogen production: challenges for process optimisation. International Journal of Hydrogen Energy, 27(11-12), 1339-1347.
- Kapdan, I.K. and Kargi, F. (2006). Bio-hydrogen production from waste materials. Enzyme and Microbial Technology, 38, 569-582.
- Kothari, R., Buddhi, D., and Sawnew, R.L. (2004). Sources and technology production: a review. International Journal of Global Energy Issues, 21, 154-178.
- Lee, K.S., Hsu, Y.F., Lo, Y.C., Lin, P.J., Lin, C.Y., and Chang, J.S. (2008). Exploring optimal environmental factors for fermentative hydrogen production from starch using mixed anaerobic microflora. International Journal of Hydrogen Energy, 33, 1565 – 1572.
- Lin, C. Y. and Chen, H. P. (2006). Sulfate effect on fermentative hydrogen production using anaerobic mixed microflora. International Journal of Hydrogen Energy, 31, 953-960.
- Luo, G., Xie, L., Zou, Z., Wang, W., and Zhou, Q. (2010) Exploring optimum conditions for thermophilic fermentative hydrogen production from cassava stillage. Chemical Engineering Journal, 35, 6161-6169.
- Manish, S. and Banerjee. R. (2007). Comparison of biohydrogen production processes. International Journal of Hydrogen Energy, 33, 279-286.

- Masse, D.I. and Masse, L. (2001). The effect of temperature on slaughterhouse wastewater treatment in anaerobic sequencing batch reactors. Bioresource Technology, 76, 91-98.
- Meyers, R. A. Ed. (2001). Solar thermochemical process technology. Encyclopedia of Physical Science & Technology. 15, 237-256.
- Mohan, S.V., Babu, V.L. and Sarma, P.N. (2007). Anaerobic biohydrogen production from dairy wastewater treatment in sequencing batch reactor (AnSBR): Effect of organic loading rate. Enzyme and Microbial Technology, 41, 506-515.
- Ni, M., Leung, D.Y.C., Leung, M.K.H., and Sumathy, K. (2006). An overview of hydrogen production from biomass. Fuel Processing Technology, 87, 461-472.
- Parkin, G.F., and Owen, W.F. (1986). Fundamentals of anaerobic digestion of wastewater sludge. Journal of Environmental Engineering, 5, 112.
- Ren, N., Li, J., Li, B., Wang, Y., and Liu, S. (2006) Biohydrogen production from molasses by anaerobic fermentation with pilot-scale bioreactor system. International Journal of Hydrogen Energy, 31, 2147-57.
- Searmsirimongkol, P. (2010). Biohydrogen Production from Alcohol Distillery Wastewater Using an Anaerobic Sequencing Batch Reactor. M.S. Thesis, The Petroleum and Petrochemical College, Chulalongkorn University.
- Sreethawong, T., Chatsiriwatana, S., Rungsunvigit, P., and Chavadej, S. (2010a). Hydrogen production from cassava wastewater using an anaerobic sequencing batch reactor: effects of operational parameters, COD:N ratio, and organic acid composition. International Journal of Hydrogen Energy, 35, 4092-4102.
- Sreethawong, T., Niyamapa, T., Neramitsuk, H., Rungsunvigit, P., Leethochwalit, M. and Chavadej, S. (2010b). Hydrogen production from glucose-containing wastewater using an anaerobic sequencing batch reactor: effect of COD loading rate, nitrogen content, and organic acid composition. Chemical Engineering Journal, 160, 322-332.

- Ueno, Y., Otsuka, S., and Morimoto, M. (1996). Hydrogen production from industrial wastewater by anaerobic microflora in chemostat culture. Journal of Fermentation and Bioengineering, 82(2), 194-197.
- Vijayaraghavan, K., Ahmad, D., and Ibrahim, M.K.B. (2005). Biohydrogen generation from jackfruit peel using anaerobic contact filter. International Journal of Hydrogen Energy, 31(5), 569-579.
- Vijayaraghavan, K., and Soom, M.A.M (2006). Trends in bio-hydrogen generation a review. Environmental Sciences, 3, 255-271.
- Yokoi, H., Maki, R., Hirose, J., and Hayashi, S. (2002). Microbial production of hydrogen from starch-manufacturing wastes. Biomass and Bioenergy, 22, 389-395.
- Yusoff, M.Z.M., Rahman, N.A.A., Aziz, S.A., Ling, C.M., Hassan, M.A., and Shirai, Y. (2010). The effect of hydraulic retention time and volatile fatty acids on biohydrogen production from palm oil mill effluent under non-sterile condition. Australian Journal of Basic and Applied Sciences, 4, 577-587.

APPENDICES

Appendix A Calibration Curves

Table A1 Calibration curve for hydrogen (H₂)

Volume of hydrogen (ml)	Peak area
0.02	16,313
0.04	58,770
0.08	180,674
0.1	226,743
0.2	427,198
0.4	778,509

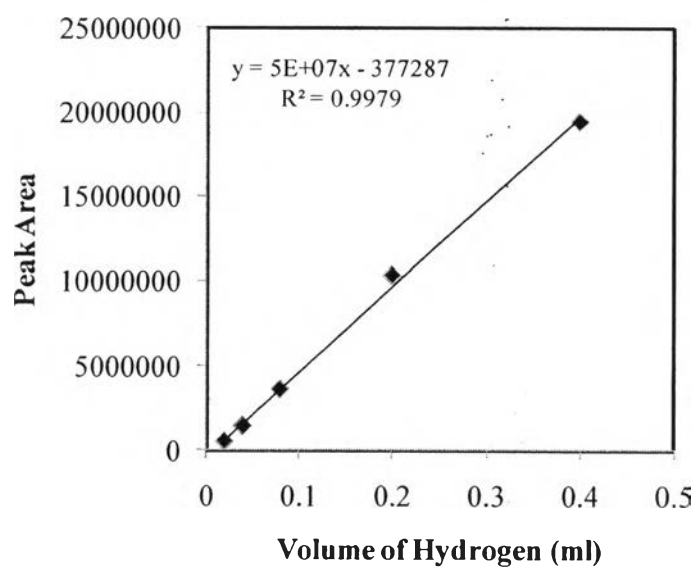


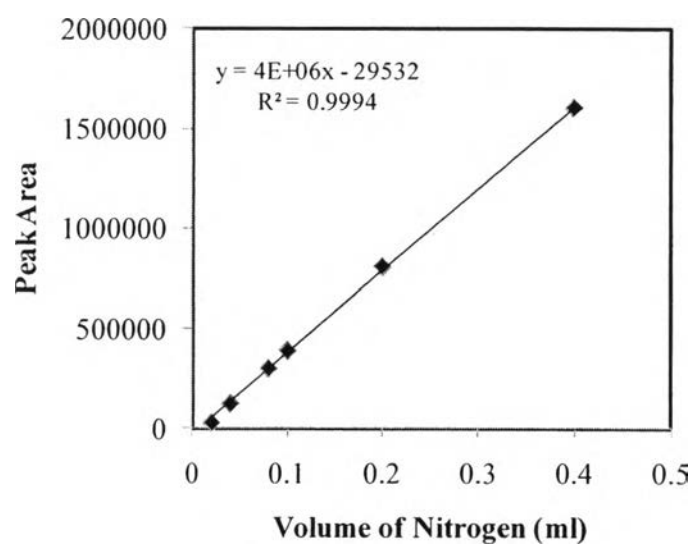
Figure A1 The relationship between volume of hydrogen (H₂) and peak area.

Equation

$$\text{Amount of hydrogen} = \frac{\text{Peak area} + 377287}{5 \times 10^7}$$

Table A2 Calibration curve for nitrogen

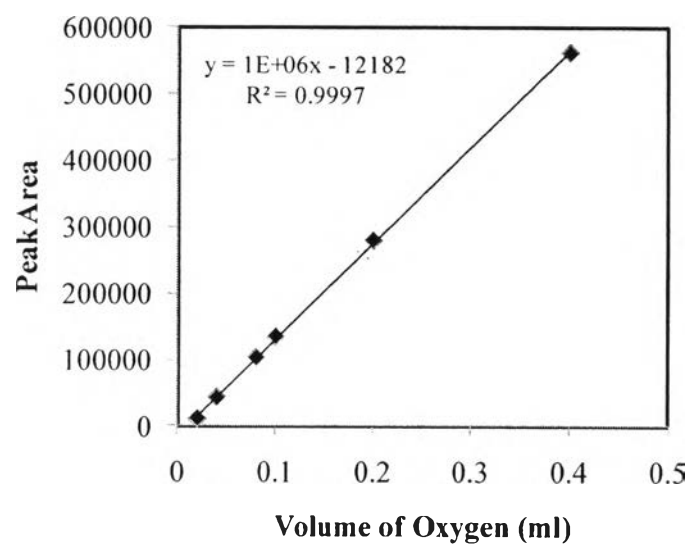
Volume of nitrogen (ml)	Peak area
0.02	34,210
0.04	128,767
0.08	305,287
0.1	393,916
0.2	809,433
0.4	1,602,475

**Figure A2** The relationship between volume of nitrogen (N₂) and peak area.**Equation**

$$\text{Amount of nitrogen} = \frac{\text{Peak area} + 29532}{4 \times 10^6}$$

Table A3 Calibration curve for oxygen

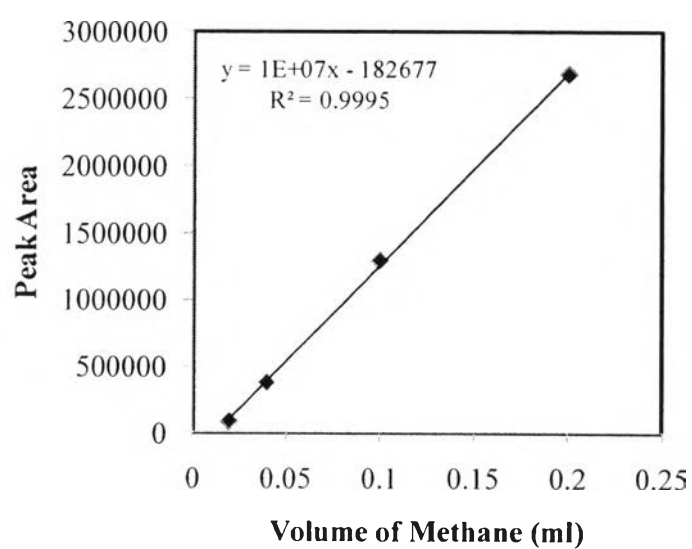
Volume of oxygen (ml)	Peak area
0.02	12,286
0.04	43,995
0.08	104,342
0.1	135,546
0.2	280,220
0.4	562,001

**Figure A3** The relationship between volume of oxygen (O₂) and peak area.**Equation**

$$\text{Amount of oxygen} = \frac{\text{Peak area} + 12182}{1 \times 10^6}$$

Table A4 Calibration curve for methane (CH₄)

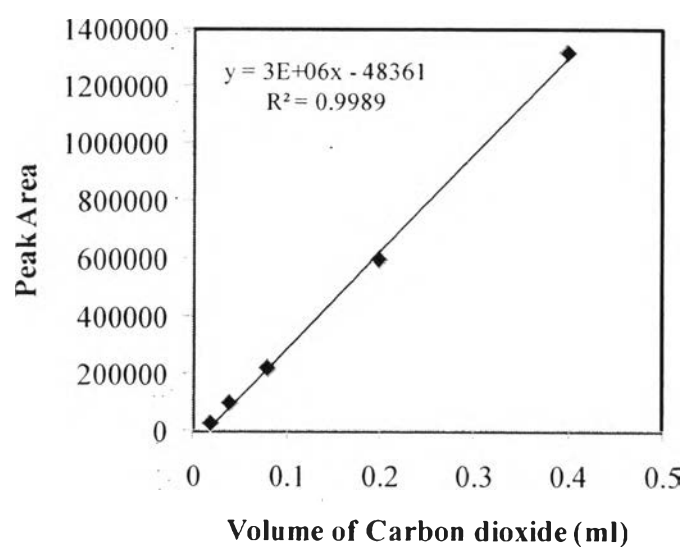
Volume of methane (ml)	Peak area
0.02	92,517
0.04	381,106
0.1	1,293,552
0.2	2,674,654

**Figure A4** The relationship between volume of methane (CH₄) and peak area.**Equation**

$$\text{Amount of methane} = \frac{\text{Peak area} + 182677}{1 \times 10^7}$$

Table A5 Calibration curve for carbon dioxide (CO₂)

Volume of carbon dioxide (ml)	Peak area
0.02	26,118
0.04	97,539
0.08	220,122
0.2	596,414
0.4	1,315,885

**Figure A5** The relationship between volume of carbon dioxide (CO₂) and peak area.**Equation**

$$\text{Amount of carbon dioxide} = \frac{\text{Peak area} + 48361}{3 \times 10^6}$$

Appendix B Preparation of 5 wt./vol.% NaOH Solution for pH-Controlled System

Preparation of NaOH at concentration of 5 wt./vol.%

$$= \frac{5 \text{ g}}{100 \text{ ml}} = 50 \frac{\text{g}}{\text{l}}$$

Appendix C Volatile Fatty Acids (VFA) Quantification by Distillation Method

C 1. Acetic Acids Stock Solution Preparation for Recovery Factor (f) Determination

Concentration of fresh acetic acid (liquid)	=	99.7%
Density of acetic acid	=	1.07 g/ml
Molecular weight of acetic acid	=	60

Determination of fresh acetic acids concentration in term of molar

$$= \frac{0.997 \text{ L of acetic acid}}{\text{L of solution}} \times \frac{1.07 \text{ g of acetic acid}}{\text{mL of acetic acid}} \times \frac{1 \text{ mol of acetic acid}}{60 \text{ g of acetic acid}}$$

$$= 17.78 \text{ M}$$

Preparation of acetic acid at concentration of 2,000 mg/L

$$= 2,000 \frac{\text{mg of acetic acid}}{\text{L of solution}} \times \frac{1 \text{ mole of acetic acid}}{60 \text{ g of acetic acid}}$$

$$= 0.0333 \text{ M}$$

Dilution of acetic acid

$$N_1 V_1 = N_2 V_2$$

$$V_1 = \frac{N_2 V_2}{N_1}$$

$$= \frac{(0.0333 \times 1)}{17.78}$$

$$= 1.873 \times 10^{-3} \text{ L}$$

C 2. Standard Sodium Hydroxide (0.1 M) Preparation

Concentration of fresh NaOH (solid)	=	99%
Molecular weight of acetic acid	=	40

Preparation of acetic acid at concentration of 0.1 M

$$= \frac{0.1 \text{ mol}}{1 \text{ L}} \times \frac{40 \text{ g}}{1 \text{ mol}} \times \frac{100}{99}$$

$$= 4.04 \text{ g}$$

C 3. Recovery Factor (f) Determination

Distill 150 ml of 0.0333 M of acetic acid in distillation apparatus

Calculate the recovery factor

$$f = \frac{a}{b}$$

where

a = volatile acid concentration recovered in distillate, mg/L

b = volatile acid concentration in standard solution used, mg/L

Find volatile acid concentration recovered in distillate by titration with 0.1 M of NaOH (MW of acetic acid = 60.5)

1) Distillate	50 ml	NaOH	11.7 ml	
Used NaOH		=		$11.7 \times 10^{-3} \times 0.1$
		=		$1.17 \times 10^{-3} \text{ mol}$
Acetic acid in distillate		=		$1.17 \times 10^{-3} \text{ mol}$
		=		$1.17 \times 10^{-3} \times 60.5$
		=		0.07 g
Concentration of acetic acid in distillate		=		0.07/50
		=		$1.405 \times 10^{-3} \text{ g/ml}$
		=		1,405 mg/l
2) Distillate	25 ml	NaOH	5.7 ml	
Used NaOH		=		$5.7 \times 10^{-3} \times 0.1$
		=		$5.7 \times 10^{-4} \text{ mol}$
Acetic acid in distillate		=		$5.7 \times 10^{-4} \text{ mol}$
		=		$5.7 \times 10^{-4} \times 60.5$
		=		0.034 g

Concentration of acetic acid in distillate

	=	0.034/25
	=	1.368×10^{-3} g/ml
	=	1,368 mg/l
Average	=	1,387 mg/l
Recovery factor (f)	=	$1,387/2,000$
	=	0.6935

Appendix D Raw Data of Effect of COD Loading Rate

D 1. COD loading rate = 30 kg/ m³d pH = 5.5 Temperature = 55°C

Days	Amount of each component (mL)			Total amount (mL)	Produced gas composition (%)		
	H ₂	CO ₂	CH ₄		H ₂	CO ₂	CH ₄
1	0.0202	0.3199	0.0184	0.3585	5.63	89.23	5.13
2	0.0448	0.277	0.0184	0.3402	13.17	81.42	5.41
3	0.0783	0.3182	0.0184	0.4149	18.87	76.69	4.43
4	0.0772	0.2661	0.0186	0.3619	21.33	73.53	5.14
5	0.0725	0.3011	0.0184	0.392	18.49	76.81	4.69
6	0.086	0.3181	0.0184	0.4225	20.36	75.29	4.36
7	0.0558	0.1967	0.0183	0.2708	20.61	72.64	6.76
8	0.0751	0.2489	0.0184	0.3424	21.93	72.69	5.37
9	0.0906	0.2977	0.0184	0.4067	22.28	73.2	4.52
10	0.0768	0.2638	0.0187	0.3593	21.37	73.42	5.2
11	0.0691	0.2592	0.0225	0.3508	19.7	73.89	6.41
12	0.0573	0.2899	0.0184	0.3656	15.67	79.29	5.03
13	0.0465	0.265	0.0188	0.3303	14.08	80.23	5.69
Avg.	0.0654	0.2786	0.01876	0.3628	17.96	76.8	5.24

Gas production rate	=	0.42	l/h
Hydrogen production rate	=	0.08	l/h
Specific hydrogen production rate	=	62.32	ml H ₂ /g MLVSS d
VFA Concentration	=	4,354.7	mg/l as acetic acid
Hydrogen yield	=	82.09	ml H ₂ /g COD removed
COD removal efficiency	=	17.42	%
MLVSS	=	7,262	mg/l
TSS	=	1,616	mg/l

Distillated sample 100 μ l + Internal standard (n-propanol 3,000 ppm) 100 μ l

VFA	Concentration (ppm)
Ethanol	251.73
Acetic acid	1,222.52
Propionic acid	1,553.41
Butyric acid	797
Valeric acid	856.8

D 2. COD loading rate = 45 kg/ m³d

pH = 5.5

Temperature = 55°C

Days	Amount of each component (mL)			Total amount (mL)	Produced gas composition (%)		
	H ₂	CO ₂	CH ₄		H ₂	CO ₂	CH ₄
1	0.0632	0.347824	0.0197	0.4307	14.67	80.75	4.57
2	0.0528	0.255108	0.0184	0.3263	16.18	78.18	5.64
3	0.0664	0.23436	0.0183	0.319	20.81	73.45	5.74
4	0.0426	0.211991	0.0209	0.2755	15.46	76.95	7.59
5	0.0486	0.20484	0.0193	0.2727	17.82	75.1	7.08
6	0.0494	0.221128	0.0186	0.2891	17.09	76.48	6.43
7	0.0478	0.163662	0.0183	0.2298	20.8	71.23	7.96
8	0.071	0.227719	0.0184	0.3171	22.39	71.81	5.8
9	0.0662	0.197982	0.0183	0.2825	23.44	70.07	6.48
10	0.0237	0.058898	0	0.0826	28.69	71.31	0
11	0.0437	0.135814	0.0183	0.1978	22.09	68.66	9.25
12	0.0505	0.157969	0	0.2085	24.22	75.78	0
13	0.123	0.3274	0.0184	0.4688	26.24	69.84	3.92
Avg.	0.0576	0.2111	0.0159	0.2847	19.72	73.87	6.41

Gas production rate	=	0.48	l/h
Hydrogen production rate	=	0.09	l/h
Specific hydrogen production rate	=	65.33	ml H ₂ /g MLVSS d
VFA concentration	=	3,677	mg/l as acetic acid
Hydrogen yield	=	56.08	ml H ₂ /g COD removed
COD removal efficiency	=	21.11	%
MLVSS	=	8,602	mg/l
TSS	=	916.67	mg/l

Distillated sample 100 μ l + Internal standard (n-propanol 3,000 ppm) 100 μ l

VFA	Concentration (ppm)
Ethanol	225.29
Acetic acid	1,183.56
Propionic acid	540.63
Butyric acid	1,333.56
Valeric acid	792.79

D 3. COD loading rate = 60 kg/ m³d

pH = 5.5

Temperature = 55 °C

Days	Amount of each component (mL)			Total amount (mL)	Produced gas composition (%)		
	H ₂	CO ₂	CH ₄		H ₂	CO ₂	CH ₄
1	0.0474	0.2351	0.0183	0.3008	15.76	78.16	6.08
2	0.0283	0.2004	0.0000	0.2287	12.37	87.63	0.00
3	0.0217	0.1904	0.0184	0.2305	9.41	82.60	7.98
4	0.0170	0.1776	0.0205	0.2151	7.90	82.56	9.54
5	0.0126	0.1793	0.0183	0.2102	5.99	85.29	8.72
6	0.0095	0.1540	0.0000	0.1635	5.81	94.19	0.00
7	0.0097	0.1665	0.0000	0.1762	5.51	94.49	0.00
8	0.0090	0.1515	0.0000	0.1605	5.61	94.39	0.00
9	0.0083	0.1436	0.0000	0.1519	5.47	94.53	0.00
10	0.0136	0.1770	0.0000	0.1906	7.13	92.87	0.00
11	0.0113	0.1123	0.0000	0.1236	9.14	90.86	0.00
12	0.0133	0.1731	0.0184	0.2047	6.50	84.53	8.97
13	0.0171	0.2189	0.0183	0.2543	6.73	86.06	7.21
14	0.0280	0.3189	0.0201	0.3670	7.63	86.89	5.48
15	0.0247	0.3098	0.0204	0.3549	6.96	87.28	5.76
16	0.0340	0.3510	0.0201	0.4051	8.39	86.66	4.95
17	0.0270	0.2667	0.0211	0.3148	8.58	84.71	6.71
18	0.0211	0.2972	0.0202	0.3385	6.23	87.79	5.97
19	0.0377	0.3200	0.0189	0.3766	10.01	84.96	5.03
Avg.	0.0206	0.2181	0.0123	0.2509	7.96	87.71	4.34

Gas production rate	=	0.96	l/h
Hydrogen production rate	=	0.08	l/h
Specific hydrogen production rate	=	33.69	ml H ₂ /g MLVSS d
VFA concentration	=	4,297	mg/l as acetic acid
Hydrogen yield	=	31	ml H ₂ /g COD removed
COD removal efficiency	=	23.26	%
MLVSS	=	13,611	mg/l
TSS	=	1,359	mg/l

Distillated sample 100 μ l + Internal standard (n-propanol 3,000 ppm) 100 μ l

VFA	Concentration (ppm)
Ethanol	546.82
Acetic acid	827.66
Propionic acid	462.8
Butyric acid	1,372.25
Valeric acid	732.81

D4. COD loading rate = 75 kg/ m³d

pH = 5.5

Temperature = 55°C

Days	Amount of each component (mL)			Total amount (mL)	Produced gas composition (%)		
	H ₂	CO ₂	CH ₄		H ₂	CO ₂	CH ₄
1	0.0471	0.2898	0.0184	0.3554	13.25	81.56	5.19
2	0.0564	0.3001	0.0184	0.3749	15.04	80.05	4.91
3	0.0623	0.3123	0.0184	0.3929	15.85	79.47	4.68
4	0.0141	0.1641	0.0184	0.1965	7.16	83.50	9.34
5	0.0149	0.2039	0.0183	0.2371	6.28	86.00	7.72
6	0.0200	0.2373	0.0183	0.2756	7.27	86.08	6.65
7	0.0260	0.2764	0.0183	0.3207	8.11	86.18	5.72
8	0.0254	0.2752	0.0183	0.3190	7.97	86.28	5.75
9	0.0342	0.2950	0.0184	0.3476	9.84	84.88	5.28
10	0.0384	0.2977	0.0184	0.3545	10.83	83.98	5.19
11	0.0403	0.3008	0.0184	0.3595	11.22	83.67	5.11
12	0.0519	0.2987	0.0183	0.3690	14.08	80.96	4.96
13	0.0729	0.2884	0.0184	0.3797	19.21	75.95	4.84
14	0.0563	0.2959	0.0186	0.3708	15.18	79.80	5.02
15	0.0377	0.3050	0.0185	0.3611	10.43	84.44	5.13
16	0.0433	0.2924	0.0184	0.3541	12.24	82.57	5.19
17	0.0539	0.2711	0.0183	0.3433	15.70	78.97	5.33
18	0.0511	0.2888	0.0183	0.3582	14.26	80.63	5.12
19	0.0768	0.3186	0.0185	0.4139	18.56	76.98	4.46
Avg.	0.0433	0.2795	0.0184	0.3413	12.24	82.21	5.56

Gas production rate	=	0.95	l/h
Hydrogen production rate	=	0.12	l/h
Specific hydrogen production rate	=	68.56	ml H ₂ /g MLVSS d
VFA concentration	=	4,527.7	mg/l as acetic acid
Hydrogen yield	=	34.36	ml H ₂ /g COD removed
COD removal efficiency	=	25.6	%
MLVSS	=	10,198	mg/l
TSS	=	1,870	mg/l

Distillated sample 100 μ l + Internal standard (n-propanol 3,000 ppm) 100 μ l

VFA	Concentration (ppm)
Ethanol	1,231.91
Acetic acid	558.47
Propionic acid	579.69
Butyric acid	1,729.64
Valeric acid	686.49

CURRICULUM VITAE

Name: Ms. Aungsika Thungmanee

Date of Birth: June 11, 1987

Nationality: Thai

University Education:

2005-2008 Bachelor Degree of Science in Chemical Technology,
Faculty of Science, Chulalongkron University, Bangkok, Thailand

Work Experience:

2008 Position: Internship Student
Company name: Thairoil Public Company, Thailand

Proceedings:

1. Thungmanee, A., Rangsunvigit, P., Chavadej S., and Sreethawong, T. (2011, April 26) Hydrogen Production from Alcohol Distillery Wastewater Using an Anaerobic Sequencing Batch Reactor under Thermophilic Condition. Proceedings of The 2nd Research Symposium on Petroleum, Petrochemicals, and Advanced Materials and The 17th PPC Symposium on Petroleum, Petrochemicals, and Polymers, Bangkok, Thailand