

REFERENCES

- Ali, A-G.A., Ali, L.I., Aboul-Fotouh, S.M., and Aboul-Gheit, A.K. (2001) Hydroisomerization, hydrocracking and dehydrocyclization of n-pentane and n-hexane using mono- and bimetallic catalysts promoted with fluorine. Applied Catalysis A: General, 215, 161-173.
- Ali, L.I., Ali, A-G.A., Aboul-Fotouh, S.M., and Aboul-Gheit, A.K. (2001) Hydroconversion of *n*-paraffins in light naphtha using Pt/Al₂O₃ catalysts promoted with noble metals and/or chlorine. Applied Catalysis A: General, 205, 129-146.
- Baroutian, S., Aroua, M.K., Raman, A.A.A., Shafie, A., Ismail, R.A., and Hamdan, H. (2013) Blended aviation biofuel from esterified jatropha curcas and waste vegetable oils. Journal of the Taiwan Institute of Chemical Engineers, in press.
- Bezergianni, S. and Kalogianni, A. (2009) Hydrocracking of used cooking oil for biofuels production. Bioresource Technology, 100, 3927-3932.
- Calemma, V., Peratello, S., and Perego, C. (2000) Hydroisomerization and hydrocracking of long chain n-alkanes on Pt/amorphous SiO₂-Al₂O₃ catalyst. Applied Catalysis A: General, 190, 207-218.
- Charles, E. "Hydrogenation of Unsaturated Fats Trans Fat." Virtual Chem book. 2003. 25 Apr. 2013
<http://www.elmhurst.edu/~chm/vchembook/558hydrogenation.html>.
- Connor, R. and Adkins, H. (1932) Hydrogenolysis of oxygenated organic compounds. Journal of the American Chemical Society, 54(12), 4678-4690.
- Corma, A., Martinez, A., Pergher, S., Peratello, S., Perego, C., and Bellusi, G. (1997) Hydrocracking-hydroisomerization of n-decane on amorphous silica-alumina with uniform pore diameter. Applied Catalysis A: General, 152, 107-125.
- Debrabandere, B. and Froment, G.F. (1997) Influence of the hydrocarbon chain length on the kinetics of the hydroisomerization and hydrocracking of n-paraffins. Hydrotreatment and Hydrocracking of Oil Fractions, 106, 379-389.

- Denayer, J.M. and Baron, G.V. (1997) Adsorption of normal and branched paraffins in faujasite zeolites NaY, HY, Pt/NaY and USY. Adsorption, 3, 251-265.
- Fangrui, M. and Milford, A. (1999) Biodiesel production: a review. Bioresource Technology, 70, 1-15.
- Gerhard, K., Robert, O.D., and Marvin, O.B. (1997) Biodiesel: The use vegetable oils and their derivatives as alternative diesel fuels. Illinois: U.S. Department of Agriculture.
- Girgis, M.J. and Tsao, Y.P. (1996) Impact of catalyst metal-acid balance in n-hexadecane hydroisomerization and hydrocracking. Industrial & Engineering Chemistry Research, 35, 386-396.
- Gong, S., Chen, N., Nakayama, S., and Qian, E.W. (2013) Isomerization of n-alkanes derived from jatropha oil over bifunctional catalysts. Journal of Molecular Catalysis A: Chemical, 370, 14-21.
- Gong, S., Shinozaki, A., Shi, M., and Qian, E.W. (2012) Hydrotreating of jatropha oil over alumina based catalysts. Energy and Fuels, 26, 2394–2399.
- Gorring, R.L. (1973) Diffusion of normal paraffins in zeolite T occurrence of window effect. Journal of Catalysis, 31, 13-26.
- Gu, B. "Schematic diagram of the zeolite-Y" RSC Publishing. 2000. 3 May. 2013
<<http://www.rsc.org/ej/JM/2000/b002473m/b002473m-f1.gif>>.
- Htay, M.M. and Oo, M.M. (2008) Preparation of Zeolite Y Catalyst for Petroleum Cracking. World Academy of Science, Engineering and Technology, 48, 114-120.
- Huber, G.W. and Corma, A. (2007) Synergies between bio- and oil refineries for the production of fuels from biomass. Angewandte Chemie International Edition, 46, 7184-7201.
- Huber, G.W., O'Connor, P., and Corma, A. (2007) Processing biomass in conventional oil refineries: Production of high quality diesel by hydrotreating vegetable oils in heavy vacuum oil mixtures. Applied Catalysis A: General, 329, 120-129.
- Ikura, M., Stanciulescu, M., and Hogan, E. (2003) Emulsification of pyrolysis derived bio-oil in diesel fuel. Biomass and Bioenergy, 24, 221-232.

- Jovanovic, D., Cupic, Z., Stankovic, M., Rozic, L., and Markovic, B. (2000) The influence of the isomerization reactions on the soybean oil hydrogenation process. Journal of Molecular Catalysis A: Chemical, 159, 353-357.
- Kritsanakun, C. (2013) Production of hydrotreated renewable jet fuel from hydrogenated biodiesel derived from jatropha oil over Pt/HY catalysts: effect of metal loadings. M.S. Thesis, The Petroleum and Petrochemical College, Chulalongkorn University, Bangkok, Thailand.
- Kuznetsov, P.N. (2003) Study of n-octane hydrocracking and hydroisomerization over Pt/H-Y zeolites using the reactors of different configurations. Journal of Catalysis, 218, 12-23.
- Li, X. and Hsing, I.M. (2006) The effect of the Pt deposition method and the support on Pt dispersion on carbon nanotubes. Electrochimica Acta, 51, 5250-5258.
- Mohammad, M., Hari, T.K., Yaakob, Z., Sharma, Y.C., and Sopian, K. (2013) Overview on the production of paraffin based-biofuels via catalytic hydrodeoxygenation. Renewable and Sustainable Energy Reviews, 22, 121-132.
- Nishimura, S. (Ed.). (2001) Handbook of Heterogeneous Catalyst Hydrogenation for Organic Synthesis. New York: John Wiley.
- Osrgard, D.J., Kustov, L., Poeppelmeier, K.R., and Sachtler, W.M.H. (1992) Comparison of Pt/KL catalysts prepared by ion exchange or incipient wetness impregnation. Journal of Catalysis, 133, 342-357.
- Park, K.C., and Ihm, S.K. (2000) Comparison of Pt/zeolite catalysts for n-hexadecane hydroisomerization. Applied Catalysis A: General, 203, 201-209.
- Pereira, C. and Gorte, R.J. (1992) Method for distinguishing brønsted-acid sites in mixtures of H-ZSM-5, H-Y and silica-alumina. Applied Catalysis A: General, 90, 145-157.
- Prado, C.M.R. and Filho, N.R.A. (2009) Production and characterization of the biofuels obtained by thermal cracking and thermal catalytic cracking of vegetable oils. Journal of Analytical and Applied Pyrolysis, 86, 338-347.

- Rao T.V.M., Dupain, X., and Makkee, M. (2012) Fluid catalytic cracking: processing opportunities for fischer–tropsch waxes and vegetable oils to produce transportation fuels and light olefins. Microporous and Mesoporous Materials, 164, 148-163.
- Reaume, S.J. and Ellis, N. (2013) Use of isomerization and hydroisomerization reactions to improve the cold flow properties of vegetable oil based biodiesel. Energies, 6(2), 619-633.
- Regali, F., Boutonnet, M., and Järås, S. (2013) Hydrocracking of n-hexadecane on noble metal/silica–alumina catalysts. Catalysis Today, 214, 12-18.
- Rossettia, I., Gambarob, C., and Calemma, V. (2009) Hydrocracking of long chain linear paraffins. Chemical Engineering Journal, 154, 295-301.
- Sotelo, D.S., Yescas, R.M., Domínguez, E.M., Salomón, S.R., and López, M.A. (2004) Effect of hydrotreating FCC feedstock on product distribution. Catalysis Today, 98, 273-280.
- Sie, S.T. (1993) Acid-catalyzed cracking of paraffinic hydrocarbons. 3. evidence for the protonated cyclopropane mechanism from hydrocracking/hydroisomerization experiments. Industrial & Engineering Chemistry Research, 32, 403-408.
- Simacek, P. and Kubicka, D. (2010) Hydrocracking of petroleum vacuum distillate containing rapeseed oil:Evaluation of diesel fuel. Fuel, 89, 1508-1513.
- Snare, M. and Murzin, D.Y. (2006) Reply to “comment on ‘heterogeneous catalytic deoxygenation of stearic acid for production of biodiesel’ ”. Industrial & Engineering Chemistry Research, 45, 6875.
- Souverijns, W., Martens, J.A., Froment, G.F., and Jacobs, P.A. (1998) Hydrocracking of isoheptadecanes on Pt/H-ZSM-22: an example of pore mouth catalysis. Journal of Catalysis, 174, 177-184.
- Steijns, M., and Froment, G. F. (1981) Hydroisomerization and hydrocracking. 3. kinetic analysis of rate data for n-decane and n-dodecane. Industrial & Engineering Chemistry Product Research, 20, 660-668.
- Veriansyah, B., Han, J.Y., Kim, S.K., Hong, S.A., Kim, Y.J., Lim, J.S., Shu, Y.W., Ohc, S.G., and Kim, J. (2011) Production of renewable diesel by hydroprocessing of soybean oil: Effect of catalysts. Fuel, 94, 578-585.

- Voge, H.H. (1958) Catalytic cracking. In Emmett, P.H. (Ed.), Catalysis (pp 407-492). New York: Reinhold Publishing.
- Weitkamp, J. (1975) The influence of chain length in hydrocracking and hydroisomerization of n-alkanes. In Ward, J.W. and Qader, S.A. (Eds.), Hydrocracking and Hydrotreating (pp. 1-27). Washington, DC: American Chemical Society.
- Webb, T. "British Airways yet to gain official approval for bio-jet fuel from food scraps." guardian.co.uk. 15 Feb. 2010. 22 May. 2011
<<http://www.guardian.co.uk/business/2010/feb/15/british-airways-biojet-fuel-factory>>.
- Yun, S., Lee, E., Park, Y.K., Jeong, S.Y., Han, J., Jeong, B., and Jeon, J.K. (2011) Selecttive hydroisomerization of n-dodecane over platinum supported on zeolites. Research on Chemical Intermediates, 37, 1215-1223.
- Zhang, X., Guo, Q., Qin, B., Zhang, Z., Ling, F., Sun, W., and Li, R. (2010) Structural features of binary microporous zeolite composite Y-Beta and its hydrocracking performance. Catalysis Today, 149, 212-217.
- Zhijian, T., Dongbai, L., and Liwu, L. (2009) Research and development of hydroisomerization and hydrocracking catalysts in dalian institute of chemical physics. Chinese Journal of Catalysis, 30(8), 705-710.
- "Hydrocracking." Citizendium. (N/A). 3 May. 2013
<<http://en.citizendium.org/wiki/Hydrocracking>>.
- "Hydrogenolysis." Wikipedia. (N/A). 3 May. 2013
<<http://en.wikipedia.org/wiki/Hydrogenolysis>>.
- "Jet fuel." Wikipedia. (N/A). 20 Apr. 2011
<http://en.wikipedia.org/wiki/Jet_fuel>.

APPENDICES

Appendix A Products Obtained from Hydrocracking of Different Feedstock Chain Length (*n*-C₁₅, *n*-C₁₆, *n*-C₁₇, and *n*-C₁₈) over 0.1 wt% Pt/HY Catalysts Prepared by IWI and IE

Table A1 Conversion and product yield of different-carbon number (Reaction condition: 310 °C, 500 psig, LHSV of 1 h⁻¹, H₂/feed molar ratio of 30, and TOS of 6 h)

Catalysts		IWI				IE
Feedstocks	<i>n</i> -C ₁₅	<i>n</i> -C ₁₆	<i>n</i> -C ₁₇	<i>n</i> -C ₁₈	<i>n</i> -C ₁₆	
Conversion (wt. %)	92.72	94.50	97.94	99.30	99.41	
Yield of gas products (wt. %)	C ₁	0.00	0.00	0.00	0.00	0.00
	C ₂	0.00	0.00	0.00	0.00	0.00
	C ₃	0.18	0.15	0.18	0.18	0.49
	iso-C ₄	0.45	0.41	0.59	0.49	1.31
	C ₄	0.48	0.38	0.41	0.39	0.98
	iso-C ₅	1.88	1.26	1.21	1.25	2.39
	C ₅	1.26	0.87	1.16	0.76	1.71
	iso-C ₆	0.96	0.98	0.95	1.32	1.70
	C ₆	0.91	0.87	0.91	0.85	1.05
	iso-C ₇	2.44	2.30	2.20	2.16	2.34
	C ₇	1.36	1.22	1.28	1.15	0.93
	iso-C ₈	3.70	3.45	3.33	3.87	2.10
	C ₈	1.77	1.82	1.56	1.21	0.73
	iso-C ₉	1.34	1.24	0.88	0.42	0.67
	C ₉	0.43	0.38	0.43	0.00	0.00
Yield of liquid Products (wt. %)	iso-C ₅	0.07	0.51	0.57	0.71	0.81
	n-C ₅	0.25	0.23	0.26	0.29	0.41
	iso-C ₆	1.94	2.34	2.67	2.47	3.67
	n-C ₆	1.17	0.89	1.34	1.73	1.89
	iso-C ₇	1.89	2.66	4.16	5.55	5.89
	n-C ₇	1.17	1.30	1.53	2.58	2.57
	iso-C ₈	5.19	5.65	6.71	11.70	11.70
	n-C ₈	1.33	1.44	1.64	2.75	2.51
	iso-C ₉	6.06	6.65	9.04	12.37	12.49
	n-C ₉	1.21	1.37	1.54	2.20	1.97

Table A1 (Cont.) Conversion and product yield of different carbon number
 (Reaction condition: 310 °C, 500 psig, LHSV of 1 h⁻¹, H₂/feed molar ratio of 30, and
 TOS of 6 h)

Catalysts		IWI				IE
Feedstocks		<i>n</i> -C ₁₅	<i>n</i> -C ₁₆	<i>n</i> -C ₁₇	<i>n</i> -C ₁₈	<i>n</i> -C ₁₆
Conversion (wt. %)		92.72	94.50	97.94	99.30	99.41
Yield of liquid Products (wt. %)	iso-C ₁₀	6.72	7.20	9.05	11.38	11.54
	<i>n</i> -C ₁₀	0.95	1.08	1.22	1.43	1.27
	iso-C ₁₁	5.46	6.66	8.44	9.05	9.78
	<i>n</i> -C ₁₁	0.61	0.93	1.07	0.97	0.83
	iso-C ₁₂	1.14	5.01	7.62	6.11	4.39
	<i>n</i> -C ₁₂	0.05	0.54	0.88	0.61	0.67
	iso-C ₁₃	0.29	0.87	4.76	3.91	0.17
	<i>n</i> -C ₁₃	0.27	0.00	0.34	0.32	0.00
	iso-C ₁₄	0.39	0.24	0.69	0.81	0.00
	<i>n</i> -C ₁₄	0.37	0.11	0.12	0.09	0.00
	iso-C ₁₅	39.10	0.36	0.30	0.34	0.21
	<i>n</i> -C ₁₅	7.23	0.32	0.22	0.22	0.12
	iso-C ₁₆	0.00	32.70	0.59	0.17	10.14
	<i>n</i> -C ₁₆	0.00	5.61	0.36	0.29	0.59
	iso-C ₁₇	0.00	0.00	18.13	0.00	0.00
	<i>n</i> -C ₁₇	0.00	0.00	1.64	0.22	0.00
	iso-C ₁₈	0.00	0.00	0.00	7.25	0.00
	<i>n</i> -C ₁₈	0.00	0.00	0.00	0.42	0.00

Table A2 Overall mass balance of hydrocracking over 0.1 wt.% Pt/HY (Reaction condition: 310 °C, 500 psig, LHSV of 1 h⁻¹, H₂/feed molar ratio of 30, and TOS of 6 h)

Catalysts	IWI				IE
Feedstocks	<i>n</i> -C ₁₅	<i>n</i> -C ₁₆	<i>n</i> -C ₁₇	<i>n</i> -C ₁₈	<i>n</i> -C ₁₆
HC feed flow rate (g/h)	2.31	2.32	2.33	2.33	2.32
H ₂ feed flow rate (g/h)	0.71	0.67	0.63	0.60	0.67
Gas Product (g/h)	0.37	0.35	0.33	0.33	0.35
Light Products (<C5) (g/h)	0.03	0.02-	0.03	0.02	0.07
Liquid Products (g/h)	1.71	1.79	1.93	1.91	1.79
Gasoline Products (C5-C8) (g/h)	0.71	0.63	0.72	0.98	0.99
Jet Products (C9-C14) (g/h)	0.51	0.73	0.96	1.05	0.87
Diesel Products (C15-C18) (g/h)	0.84	0.75	0.54	0.19	0.21
Remaining Feed (RF) (g/h)	0.15	0.13	0.05	0.01	0.01
Liquid Product + RF (g/h)	1.87	1.91	1.97	1.92	1.80
Gas + Liquid Products (g/h)	2.08	2.13	2.26	2.24	2.14
Total Products + RF (g/h)	2.24	2.26	2.31	2.26	2.15
Remaining H ₂ (RH) (g/h)	0.73	0.68	0.65	0.66	0.69
Total Products + RF + RH (g/h)	2.97	2.94	2.96	2.91	2.84

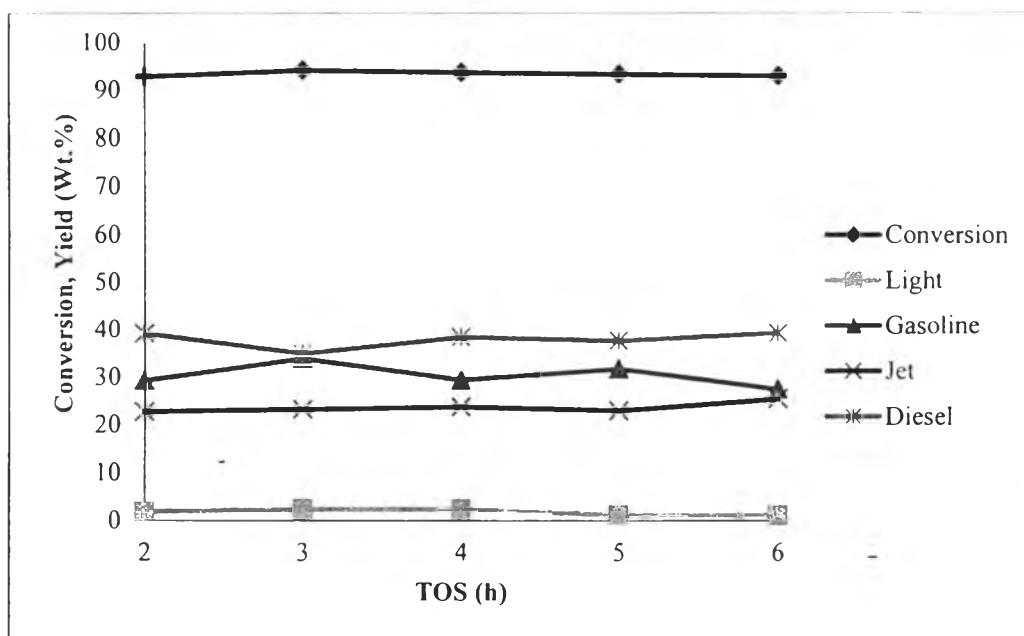


Figure A1 Conversion and yield of products obtained from hydrocracking of $n\text{-C}_{15}$ over 0.1 wt.% Pt/HY prepared by IWI (Reaction condition: 310 °C, 500 psig, LHSV of 1.0 h^{-1} , H_2/feed molar ratio of 30).

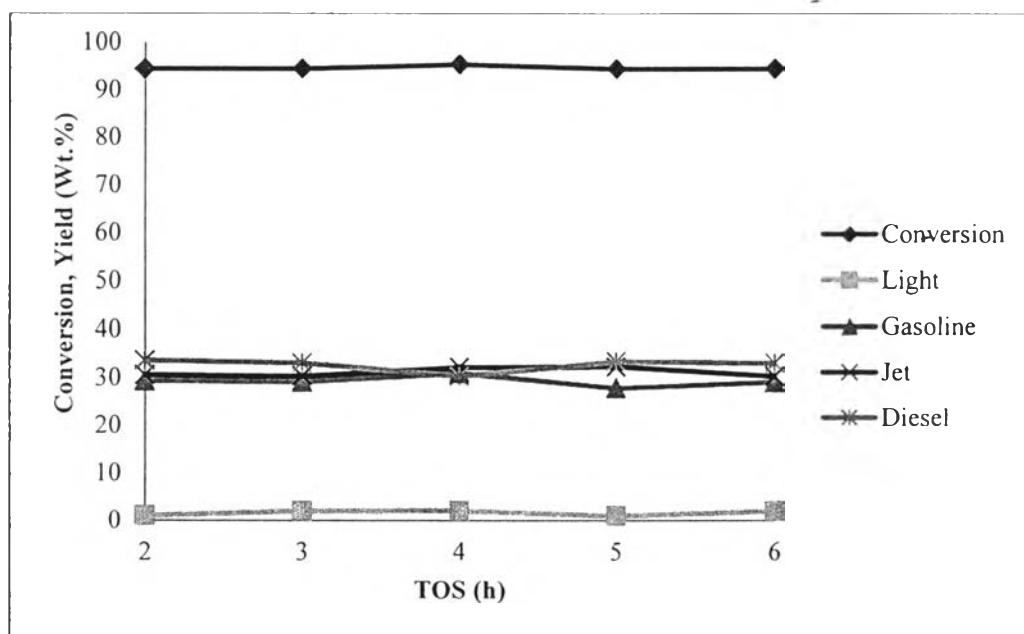


Figure A2 Conversion and yield of products obtained from hydrocracking of $n\text{-C}_{16}$ over 0.1 wt.% Pt/HY prepared by IWI (Reaction condition: 310 °C, 500 psig, LHSV of 1.0 h^{-1} , H_2/feed molar ratio of 30).

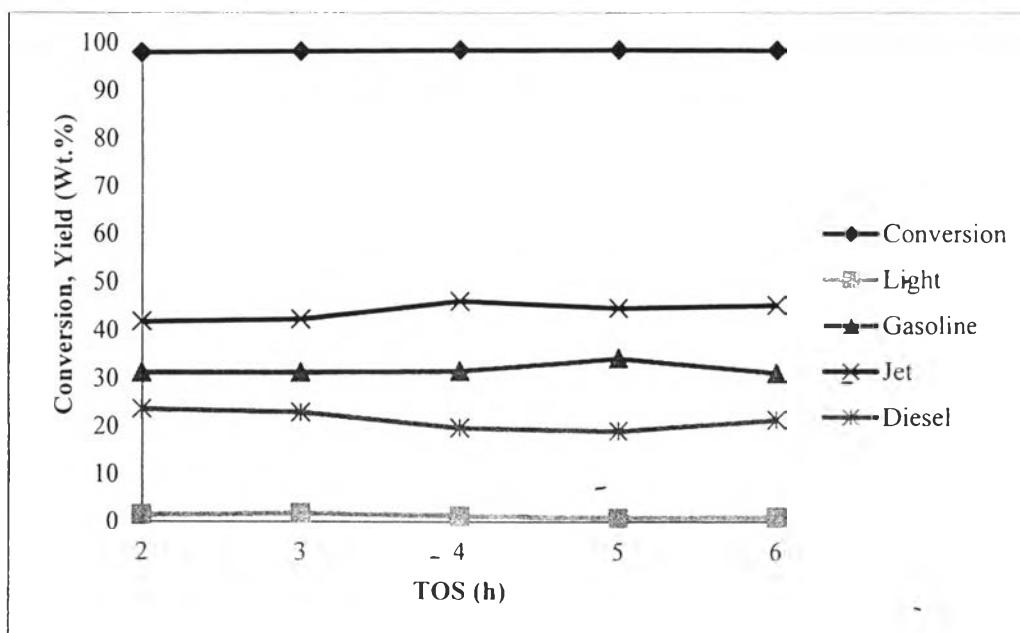


Figure A3 Conversion and yield of products obtained from hydrocracking of $n\text{-C}_{17}$ over 0.1 wt.% Pt/HY prepared by IWI (Reaction condition: 310 °C, 500 psig, LHSV of 1.0 h^{-1} , H_2/feed molar ratio of 30).

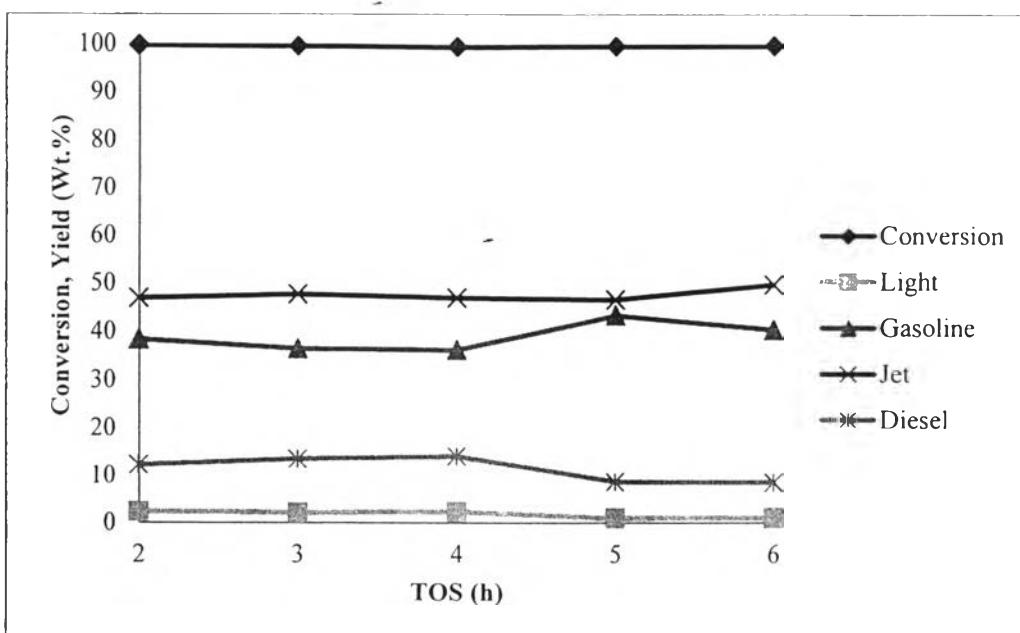


Figure A4 Conversion and yield of products obtained from hydrocracking of $n\text{-C}_{18}$ over 0.1 wt.% Pt/HY prepared by IWI (Reaction condition: 310 °C, 500 psig, LHSV of 1.0 h^{-1} , H_2/feed molar ratio of 30).

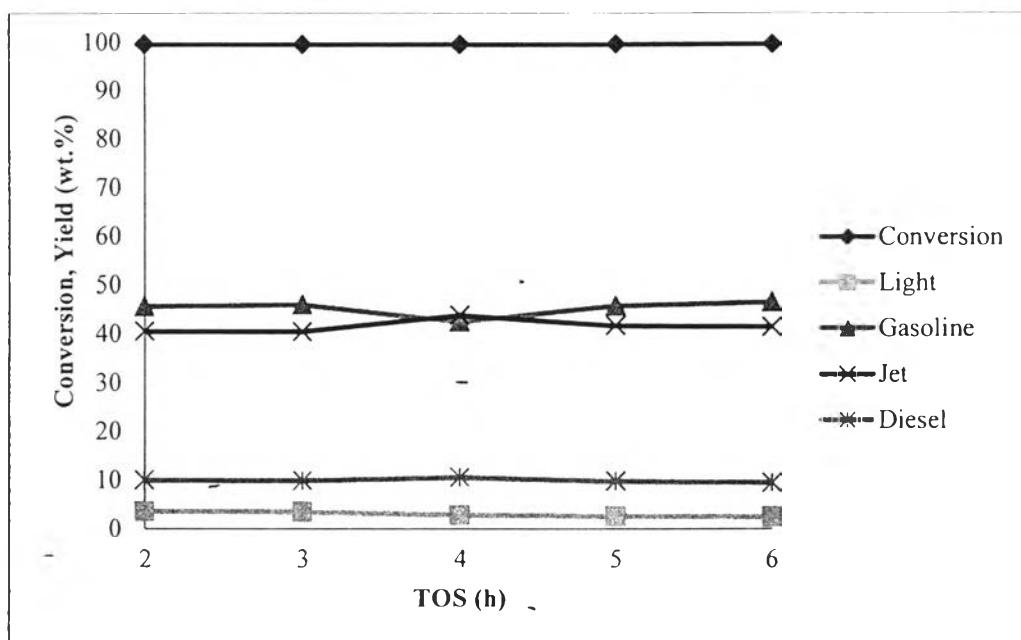


Figure A5 Conversion and yield of products obtained from hydrocracking of $n\text{-C}_{16}$ over 0.1 wt.% Pt/HY prepared by IE (Reaction condition: 310 °C, 500 psig, LHSV of 1.0 h^{-1} , H_2/feed molar ratio of 30).

Appendix B Products Obtained from Hydrocracking of *n*-C16 over 0.1 wt% Pt/HY Catalysts Prepared by IWI and IE at Different LHSV

Table B1 Yield of cracked and isomerized products at different contact time
(Reaction condition: 310 °C, 500 psig, LHSV of 0.5 – 2.5 h⁻¹, H₂/feed molar ratio of 30)

Catalysts		IWI			IE		
Contact time (h)	LHSV (h ⁻¹)	Cracked Product	Monobranch	multibranch	Cracked Product	Monobranch	multibranch
2.00	0.50	92.73	2.08	3.56	94.14	1.33	2.81
1.33	0.75	81.23	5.65	8.79	88.10	3.38	4.77
1.00	1.00	71.29	8.72	12.59	79.42	5.71	7.55
0.80	1.25	59.86	12.10	17.10	73.79	7.14	8.82
0.67	1.50	44.91	16.97	22.64	68.85	8.53	10.34
0.57	1.75	32.85	20.56	26.46	65.09	9.46	11.41
0.50	2.00	25.20	22.98	28.37	60.00	10.74	13.12
0.44	2.25	19.39	24.58	29.48	55.35	12.03	14.51
0.40	2.50	16.99	24.72	29.29	49.73	13.60	16.09

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Presentations:

1. Wijakkul, C.; Hengsawad, T.; Jongpatiwut, S.; and Butnark, S. (2014, March 10-12) Hydrocracking of C₁₅ - C₁₈ Hydrocarbons over Pt/HY Catalysts: Effect of Catalyst Preparation. Paper presented at NCCC XVth: Netherlands' Catalysis and Chemistry Conference 2014, Noordwijkerhout, Netherlands.
2. Wijakkul, C.; Hengsawad, T.; Jongpatiwut, S.; and Butnark, S. (2014, April 22) Hydrocracking of C₁₅ - C₁₈ Hydrocarbons over Pt/HY Catalysts for Hydrotreated Renewable Jet Fuel Production. Paper presented at The 5th Research Symposium on Petrochemical and Materials Technology and The 20th PPC Symposium on Petroleum, Petrochemicals, and Polymers, Bangkok, Thailand.