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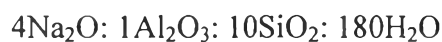
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APPENDICES

Appendix A Gel Batch Composition Calculations

As mentioned previously in Chapter 3, Na-Y zeolite was prepared by using the recipe $4\text{Na}_2\text{O} : 1\text{Al}_2\text{O}_3 : 10\text{SiO}_2 : 180\text{H}_2\text{O}$. The calculations to estimate the required weights of gel as follows:

The Composition of desired NaY Zeolite is



So

$$\frac{\text{SiO}_2}{\text{Al}_2\text{O}_3} \quad \text{molar ratio} = 10$$

$$\frac{\text{Na}_2\text{O}}{\text{SiO}_2} \quad \text{molar ratio} = 0.4$$

$$\frac{\text{H}_2\text{O}}{\text{SiO}_2} \quad \text{molar ratio} = 18$$

Basis; The initial mole of SiO_2 which I want to synthesis equal to 10 g or 0.1664 mole

$$\text{So; Ludox HS-40} = 0.1664 \text{ mole}$$

$$= 9.9992 \text{ g}$$

$$- 40\% \text{ Ludox} = 9.9992/0.4 = 24.9982 \text{ g} = \underline{19.2293 \text{ mL}}$$

$$- 40\% \text{ Ludox consist of water } 24.9982 \times 0.6 = 14.9989 \text{ g} = \underline{14.9989 \text{ mL}}$$

$$\underline{\text{Al Content:}} \quad \text{From} \quad \frac{\text{SiO}_2}{\text{Al}_2\text{O}_3} = 10$$

$$\text{So ; } \text{Al}_2\text{O}_3 = \text{mole of SiO}_2 / 10$$

$$= 0.1664/10 = 0.01664 \text{ mole}$$

Since NaAlO_2 is used for Al source, Mole of NaAlO_2 be used equal to 0.01664×2 mole

$$= 0.0333 \text{ mole}$$

$$= 0.0333 \times 81.97 = 2.729 \text{ g}$$

And NaAlO_2 consist of Al, Na equal to 53.5 and 45% respectively, So the real content of Al that will be used equal to $\underline{2.729/0.535 = 5.1 \text{ g}}$ and have a Na content equal to 2.2949

Na Content: From $\frac{\text{Na}_2\text{O}}{\text{SiO}_2} = 0.4$

So ; $\text{Na}_2\text{O} = \text{mole of SiO}_2 \times 0.4$
 $= 0.1664 \times 0.4 = 0.067 \text{mole}$

Since NaOH is used for Na source, Mole of NaOH be used equal to 0.067×2
 $= 0.13312 \text{ mole}$
 $= 0.13312 \times 39.997 = 5.3244 \text{ g}$

Since assay percentage of NaOH = 99.17%, the content of Na that will be used for synthesis equal to $5.3244/0.9917 = 5.369 \text{ g}$ and the content of Na in NaAlO₂ equal to 2.2949, So the real content of NaOH equal to $5.369 - 2.2949 = \underline{3.0741 \text{ g}}$

H₂O Content: From $\frac{\text{H}_2\text{O}}{\text{SiO}_2} = 18$

So ; Mole of H₂O = mole of SiO₂ × 18
 $= 0.1664 \times 18 = 2.9952 \text{ mole}$
 $= 53.9136 \text{ g or } \underline{53.9136 \text{ mL}}$

The real content of water that we want equal to $53.9136 - 14.9989 = 38.9147 \text{ ml}$ (14.9989 mL of water is found in Ludox).

Table A1 Molecular weight of each used chemical as follow in the table A1

Component	MW
40% Ludox	60.08
NaAlO ₂	81.97
SiO ₂	60.08
Al ₂ O ₃	101.9
NaOH	39.9
H ₂ O	18.01

Appendix B Atlas and Simulated XRD Power Patterns of Zeolite Structure Types

Framework Type: FAU

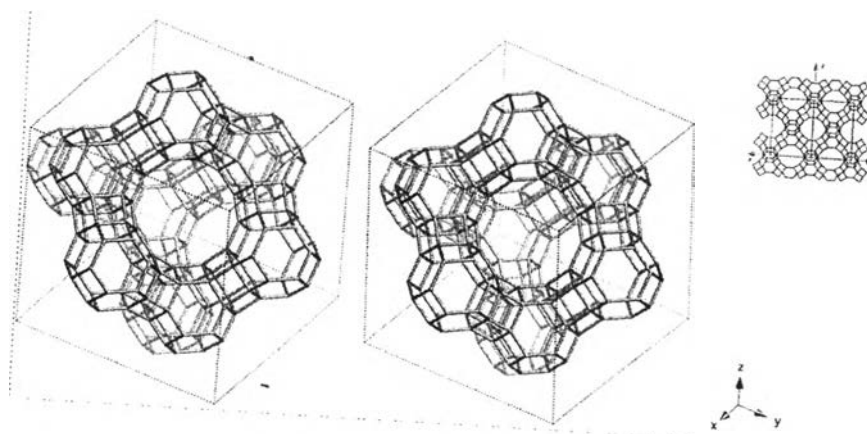


Figure B1 Framework viewed along [111] (upper right: projection down [110])

Cell Parameters:

$$a = 24.345 \text{ \AA} \quad b = 24.345 \text{ \AA} \quad c = 24.345 \text{ \AA}$$

$$\alpha = 90.000^\circ \quad \beta = 90.000^\circ \quad \gamma = 90.000^\circ$$

$$\text{Volume} = 14428.77 \text{ \AA}^3$$

$$R_{\text{DLS}} = 0.0009$$

Framework density
(FD_{Si}): 13.3 T/1000 \AA^3

Topological density: $\text{TD}_{10} = 579$ $\text{TD} = 0.476190$

Ring sizes (# T-atoms): 12 6 4

Channel system: 3-dimensional

Maximum diameter of a sphere:

that can be included 11.24 \AA

that can diffuse along

Figure B2 XRD power patterns of zeolite structure types.

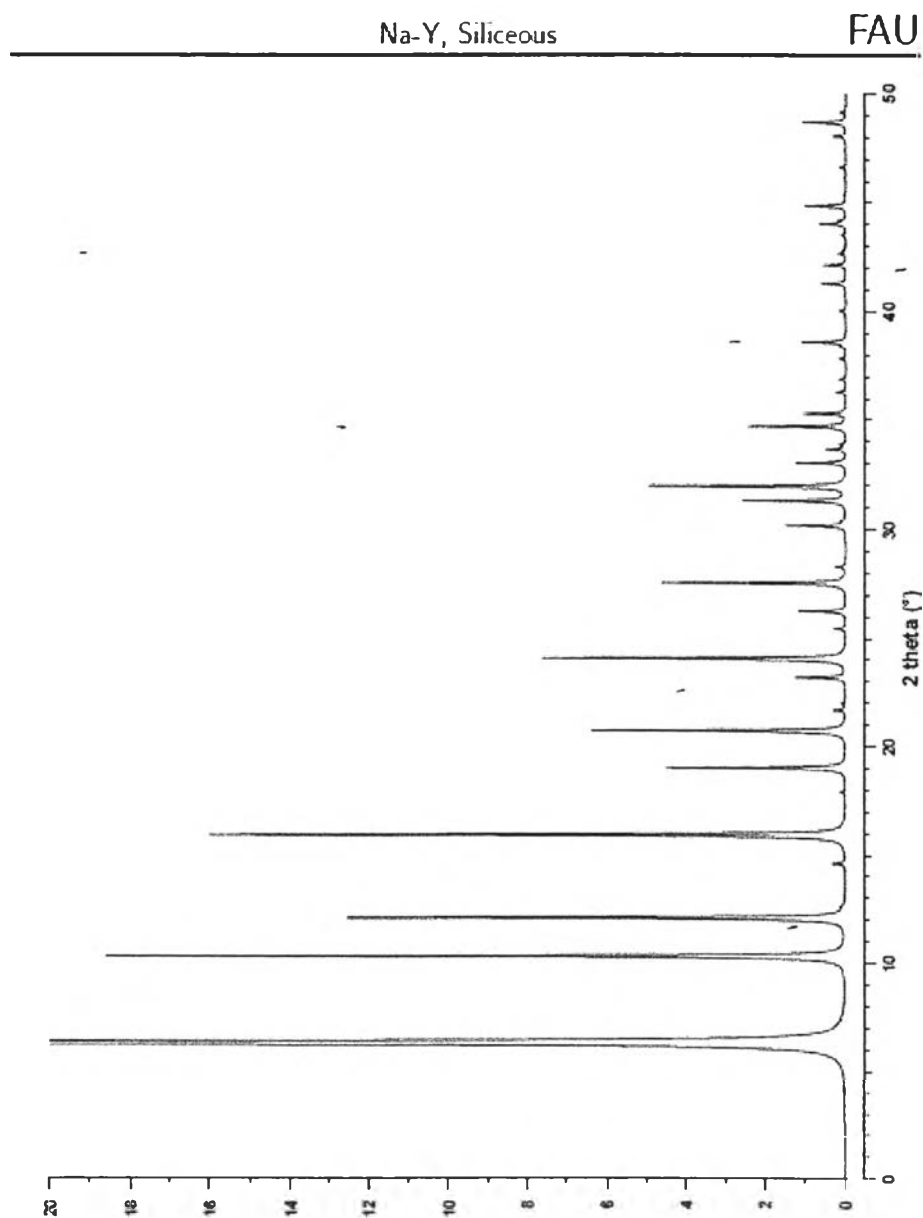


Table B1 Physical and chemical properties of commercial HY zeolite

Zeolite	Surface area (m ² /g)	Crystal size (μm)	Na ₂ O (%)	SiO ₂ /Al ₂ O ₃
Commercial HY	696.7	1.1	0.203	103.94

Appendix C Products Obtained over Tested Catalyst in Different Crystallite Sizes

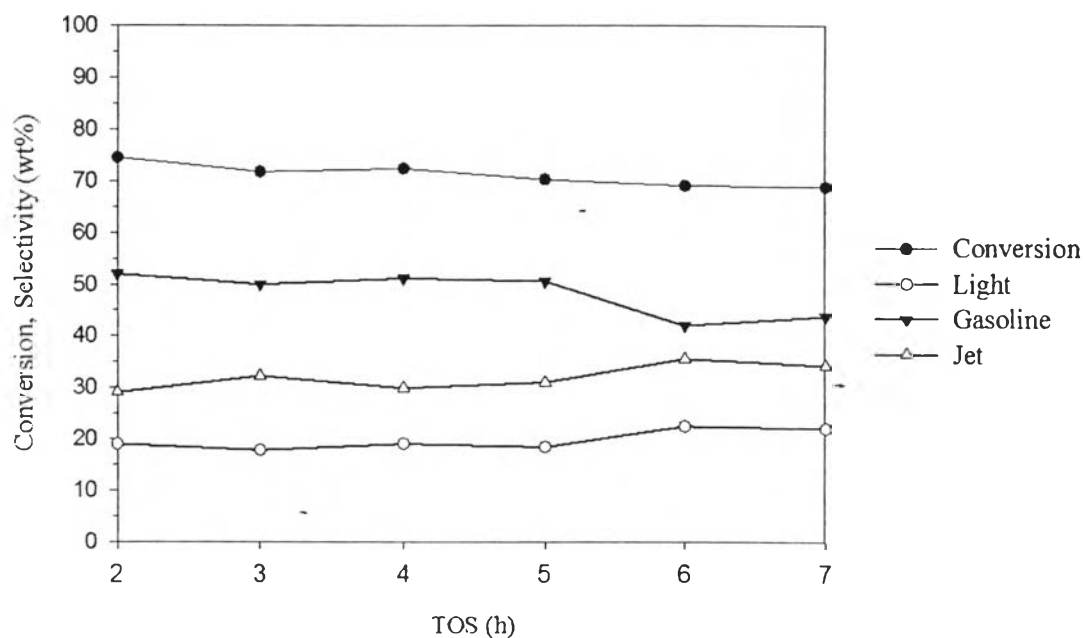


Figure C1 Conversion and selectivity of products obtained over Y-100A3 sample (Reaction condition: 450 °C, 500 psig, LHSV of 1.0 h⁻¹, H₂/ feed molar ratio of 30).

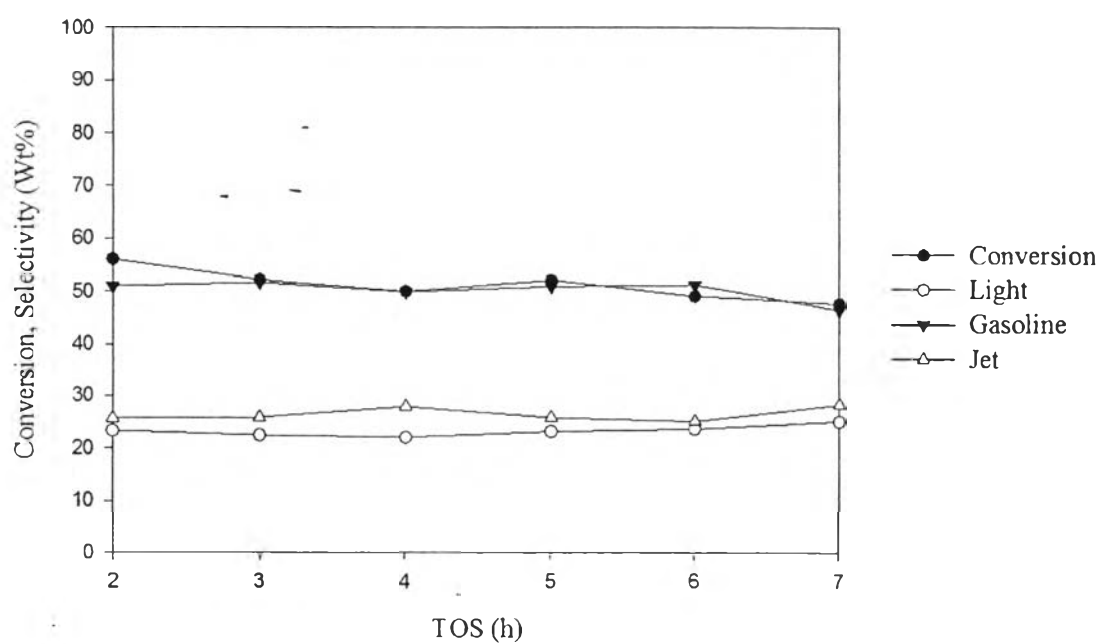


Figure C2 Conversion and selectivity of products obtained over Y-110A2 sample (Reaction condition: 450 °C, 500 psig, LHSV of 1.0 h⁻¹, H₂/ feed molar ratio of 30).

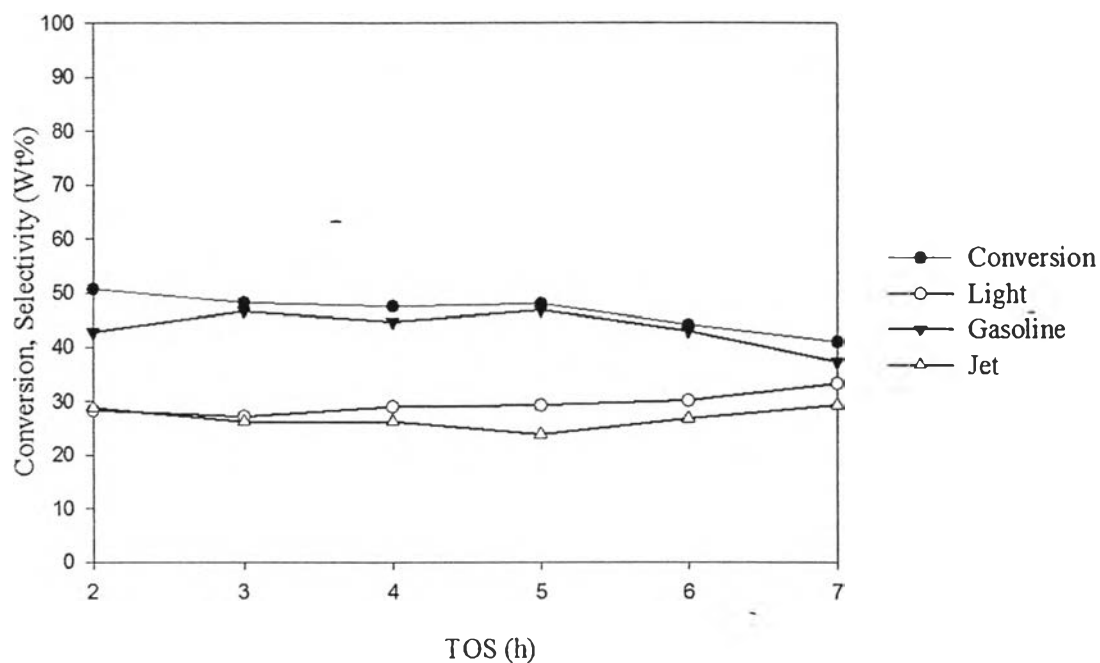


Figure C3 Conversion and selectivity of products obtained over Y-110A1 sample (Reaction condition: 450 °C, 500 psig, LHSV of 1.0 h⁻¹, H₂/ feed molar ratio of 30).

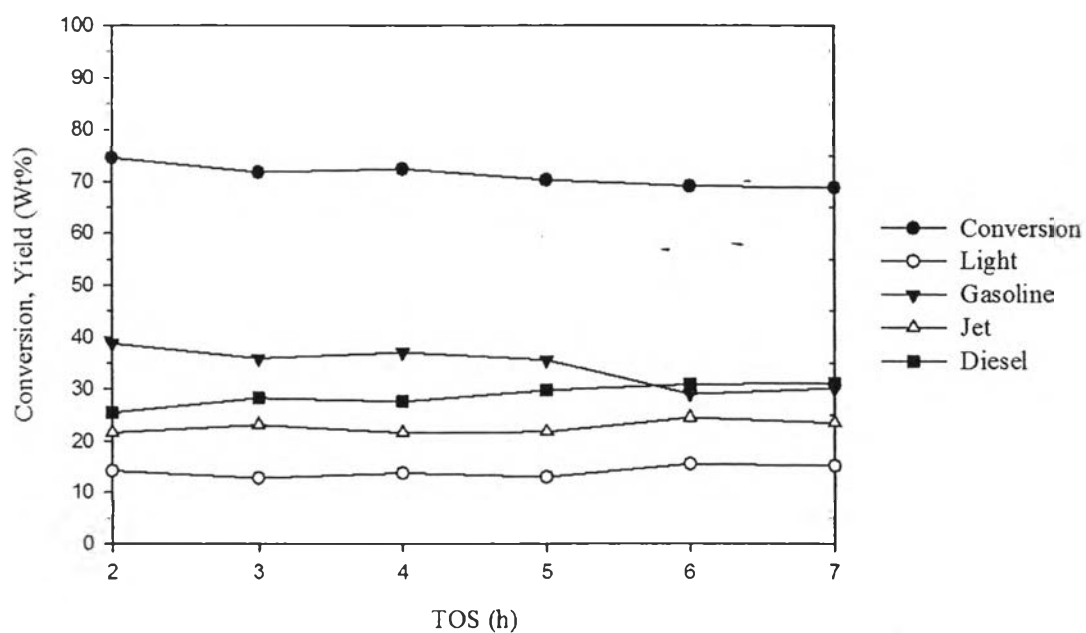


Figure C4 Conversion and yield of products obtained over Y-100A3 sample (Reaction condition: 450 °C, 500 psig, LHSV of 1.0 h⁻¹, H₂/ feed molar ratio of 30).

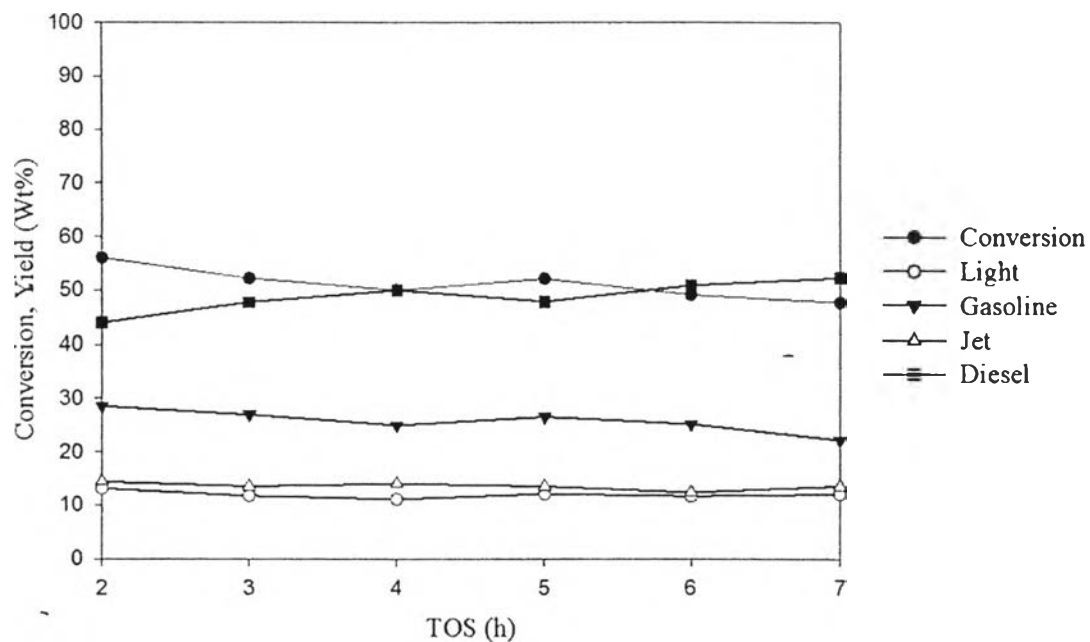


Figure C5 Conversion and yield of products obtained over Y-110A2 sample (Reaction condition: 450 °C, 500 psig, LHSV of 1.0 h⁻¹, H₂/ feed molar ratio of 30).

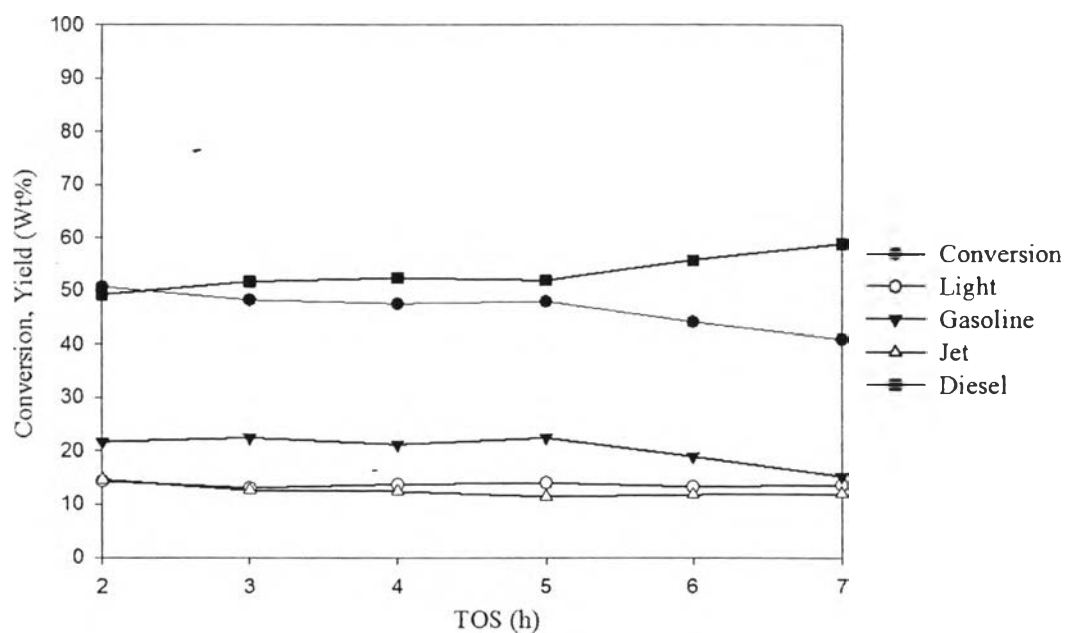


Figure C6 Conversion and yield of products obtained over Y-110A1 sample (Reaction condition: 450 °C, 500 psig, LHSV of 1.0 h⁻¹, H₂/ feed molar ratio of 30).

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Presentations:

1. Jadpon, N.; Hengsawad, T.; Jongpatiwut, S.; Chareonpanich M., and Butnark, S. (2014, March 10-12) Production of Biojet from Hydrogenated Biodiesel over Pt/HY Catalysts: Effect of Zeolite Crystals Size. Paper presented at NCCC XVth: Netherlands' Catalysis and Chemistry Conference 2014, Noordwijkerhout, Netherlands.
2. Jadpon, N.; Hengsawad, T.; Jongpatiwut, S.; Chareonpanich M., and Butnark, S. (2014, April 22) Microwave Hydrothermal (M-H) Synthesis of Small Crystal Sizes of Y Zeolite for Producing Hydrotreated Renewable Jet Fuel from Hydrogenated Biodiesel. Paper presented at The 5th Research Symposium on Petrochemical and Materials Technology and The 20th PPC Symposium on Petroleum, Petrochemicals, and Polymers, Bangkok, Thailand.