METHYL BROMIDE SYNTHESIS VIA OXIDATIVE BROMINATION OF METHANE

Varinee Sirijantarat

A Thesis Submitted in Partial Fulfilment of the Requirements
for the Degree of Master of Science

The Petroleum and Petrochemical College, Chulalongkorn University
in Academic Partnership with

The University of Michigan, The University of Oklahoma,
Case Western Reserve University and Institut Français du Pétrole
2014

Thesis Title:

Methyl Bromide Synthesis via Oxidative Bromination of

Methane

By:

Varinee Sirijantarat

Program:

Petrochemical Technology

Thesis Advisor:

Asst. Prof. Boonyarach Kitiyanan

Accepted by The Petroleum and Petrochemical College, Chulalongkorn University, in partial fulfilment of the requirements for the Degree of Master of Science.

College Dean

(Asst. Prof. Pomthong Malakul)

Thesis Committee:

B. Kitiyanan

Prawoel a.

(Asst. Prof. Boonyarach Kitiyanan)

(Assoc. Prof. Pramoch Rangsunvigit)

(Dr. Tanate Danuthai)

ABSTRACT

5571038063: Petrochemical Technology Program

Varinee Sirijantarat: Methyl Bromide Synthesis via Oxidative

Bromination of Methane.

Thesis Advisor: Asst. Prof. Boonyarach Kitiyanan, 77 pp.

Keywords: Oxidative bromination/ Methane / Methyl bromide / Rh/SiO₂

catalyst

The thermodynamic stability of methane is a critical factor for methane utilization. Oxidative bromination of methane (OBM) is one of the reaction pathways to transform methane into more reactive reactant, methyl bromide (CH₃Br), which can be used for the productions of higher hydrocarbons and/or other compounds. In the current study, methane was brominated with HBr/H₂O, with the flow of oxygen and nitrogen in a fixed-bed continuous-flow reactor at atmospheric pressure. The effect of various parameters including support materials, wt% Rh/SiO₂ catalyst, reaction temperature, and %O₂ were investigated. Before and after the reaction, the catalysts were also characterized by several techniques—BET, XRD, TPR, H₂ Chemisorption, and SEM. The results shows that under the same conditions (20 ml/min of CH₄, 5 ml/min of O₂, 5 ml/min of N₂, 6.5 ml/h of 48 wt% HBr/H₂O), high selectivity of CH₃Br (100%) could be achieved at reaction temperature of 400°C, while at higher temperature partial oxidation of methane to synthesis gas was instead dominant. Moreover, when adding Rh/SiO₂ catalyst, the methane conversion increased while the high selectivity to methyl bromide was preferable.

บทคัดย่อ

วาริณี ศิริจันทรัตน์ : การสังเคราะห์เมทิลโบรไมค์ค้วยปฏิกิริยาออกซิเคทีฟโบรมิเนชัน ของมีเทน (Methyl Bromide Synthesis via Oxidative Bromination of Methane) อาจารย์ ที่ปรึกษา : ผศ. คร. บุนยรัชต์ กิติยานันท์ 77 หน้า

ความเสถียรทางเทอร์โมไคนามิกส์ของมีเทนเป็นอุปสรรคที่สำคัญต่อการนำมีเทนไปใช้ ในทางอุตสาหกรรมต่างๆ ปฏิกิริยาออกซิเคทีฟโบรมิเนชันของมีเทนเป็นอีกทางเลือกหนึ่งในการ เปลี่ยนสารตั้งต้นมีเทนไปเป็นรูปที่ว่องไวต่อการเกิดปฏิกิริยามากยิ่งขึ้น เมทิลโบรไมด์ซึ่งเป็น ผลิตภัณฑ์หลักที่ได้จากปฏิกิริยาดังกล่าว สามารถนำไปเป็นสารตั้งต้นในการผลิตสารประกอบ ใฮโครคาร์บอนมวลโมเลกุลสูง หรือสารประกอบอื่นๆอีกมากมาย ในการทคลองนี้มีเทนจะทำ ปฏิกิริยากับแก๊สออกซิเจนและกรคไฮโครโบรมิกโคยมีแก๊สในโตรเจนเป็นตัวพา สารตั้งค้น ทั้งหมคจะถูกป้อนสู่เตาปฏิกรณ์แบบต่อเนื่องและทำปฏิกิริยาที่ความคันบรรยากาศ นอกจากนี้แล้ว ในการทคลองยังมีการหาสภาวะที่เหมาะสมของตัวแปรต่างๆ อันได้แก่ ชนิดของตัวรองรับ อุณหภูมิที่ใช้ในการทำปฏิกิริยา ปริมาณโลหะโรเคียม และปริมาณออกซิเจนที่ใช้ โคยก่อนและ หลังการทำปฏิกิริยา ตัวเร่งปฏิกิริยาจะถูกวิเคราะห์ด้วยเทคนิคต่างๆ เพื่อหาพื้นที่ผิว ความเป็นผลึก รูปไอออนของโลหะ การกระจายตัวของโลหะและโครงสร้างระคับพื้นผิว จากผลการทคลอง พบว่าที่สภาวะการทคลองเคียวกัน (20 มิลลิลิตรต่อนาทีของมีเทน, 5 มิลลิลิตรต่อนาทีของ ออกซิเจน, 5 มิลลิลิตรต่อนาทีของในโตรเจน และ6.5 มิลลิลิตรต่อชั่วโมงของกรคไฮโครโบรมิก) ค่าการเลือกเกิดของเมทิลโบรไมด์ที่เท่ากับ 100% สามารถทำได้โดยใช้อุณหภูมิการทำปฏิกิริยา เท่ากับ 400 องศาเซลเซียส และพบว่ายิ่งอุณหภูมิการทำปฏิกิริยาสูงขึ้น จะไปสนับสนุนให้ เกิดปฏิกิริยาออกซิเคชันของมีเทนเพื่อเปลี่ยนไปเป็นแก๊สสังเคราะห์แทน การนำตัวเร่งปฏิกิริยา ของโลหะโรเคียมบนตัวรองรับซิลิกามาใช้จะช่วยปรับปรุงค่าการแปลงผันของมีเทนให้เพิ่มขึ้น โดยที่ค่าการเลือกเกิดของเมทิลโบรไมด์ยังอยู่ในเกณฑ์ที่น่าพอใจ

ACKNOWLEDGEMENTS

This research project would not have been possible without the support of many people. First, the author wishes to express my profound gratitude and deep regards to my advisor, Asst. Prof. Boonyarach Kitiyanan who is abundantly helpful and offered invaluable assistance, support and guidance. Deepest gratitude is also due to the members of the supervisory committee, Assoc. Prof. Pramoch Rangsunvigit and Dr. Tanate Danuthai. If the author is without whose knowledge and assistance, this study will not have been successful.

In addition, the author would also like to convey thanks to The Petroleum and Petrochemical College Chulalongkorn University, The Center of Excellence on Petrochemical and Materials Technology, and PTT Global Chemical Public Company Limited for providing the fund and laboratory facilities. Special thanks also to Mr. Thani Jermwongratanachai and all my PPC friends for creative suggestions and encouragement.

Last, the author wishes to express my love and gratitude to my families for their understanding and cheerfulness, through the duration of my studies.

TABLE OF CONTENTS

| | | | PAGE |
|----|--------|-----------------------------------------------------------|------|
| | Title | Page | i |
| | Abstr | act (in English) | iii |
| | Abstr | act (in Thai) | iv |
| | Ackn | owledgements - | v |
| | Table | of Contents | vi |
| | List o | f Tables | viii |
| | List o | f Figures | xi |
| CH | HAPTEF | R | |
| | I | INTRODUCTION | 1 |
| | II | LITERATURE REVIEW | 3 |
| | | 2.1 Methane Activation | 3 |
| | | 2.2 Halogenation of Methane | 4 |
| | | 2.3 Oxidative Bromination of Methane (OBM) | 7 |
| | | 2.4 Related Articles of Oxidative Bromination of Methane | 8 |
| | | 2.5 Related Articles of Methylation with Alkylating Agent | 13 |
| | III | METHODOLOGY | 18 |
| | | 3.1 Materials | 18- |
| | | 3.1.1 Chemicals | 18 |
| | | 3.1.2 Gases | 18 |
| | | 3.1.3 Equipments | 18 |
| | | 3.2 Experimental Procedures | 19 |
| | | 3.2.1 Catalyst Preparation | 19 |
| | | 3.2.2 Catalyst Characterization | 20 |
| | | 3.2.3 Catalytic Activity Testing | 22 |
| | | | |

| CHAPTER | | PAGE |
|---------|---------------------------------------------------------------------|------|
| IV | RESULTS AND DISCUSSION | 24 |
| | 4.1 Catalytic Activity Testing | 24 |
| | 4.1.1 Product Distribution for the OBM Reaction | |
| | (Blank Tube) | 24 |
| | 4.1.2 Screening of Different Material Supports for | |
| | the OBM Reaction | 25 |
| - | 4.1.3 Effect of Reaction Conditions for the OBM Reaction | 27 |
| | 4.1.4 Effect of Rh/SiO ₂ Catalyst for the OBM Reaction | 31 |
| | 4.1.5 Effect of Rh Loading on SiO ₂ for the OBM Reaction | 32 |
| | 4.1.6 Effect of Calcination Conditions of Rh/SiO ₂ | 34 |
| | 4.2 Catalyst Characterization | 38 |
| | 4.2.1 Surface Area Analysis (BET) | 38 |
| | 4.2.2 X-ray Diffraction (XRD) | 39 |
| | 4.2.3 Temperature Program Reduction (TPR) | 40 |
| | 4.2.4 H ₂ Chemisorption | 41 |
| | 4.2.5 Scanning Electron Microscopy and | |
| | Energy Dispersion X-ray Spectroscopy (SEM-EDX) | 42 |
| - V | CONCLUSIONS AND RECOMMENDATIONS | 46 |
| | 5.1 Conclusions | 46 |
| | 5.2 Recommendations | 47 |
| | 4 | |
| | REFERENCES | 48 |
| | APPENDICES | 52 |
| | Appendix A Calculation of Methane Conversion | |
| | and Product Selectivity | 52 |
| | Appendix B Calculation of Catalyst Composition | 55 |
| | Appendix C Calibration Data and Feed Flow Calibration | 57 |
| | Appendix D Raw Data of Reaction Results | 60 |
| | CURRICULUM VITAE . | 77 |

LIST OF TABLES

| TABLE | | PAGE |
|-------|----------------------------------------------------------------------------------------------|------|
| 2.1 | Enthalpy and free energy of formation of methane-halogen reactions | 5 |
| 2.2 | Product distribution of OBM reaction with different desired product | 9 |
| 2.3 | Catalyst performance for OBM reaction | 9 |
| 2.4 | OBM reaction on different supported metal oxide catalysts | 12 |
| 4.1 | Methyl bromide yield of the OBM-reaction | 37 |
| 4.2 | Specific surface area of different material supports | 38 |
| 4.3 | Specific surface area of 0.5 wt% Rh/SiO ₂ catalysts | |
| • | —different calcination conditions | 38 |
| 4.4 | Metal dispersion of 0.5 wt% Rh/SiO ₂ catalysts | |
| | —different calcination conditions | 41 |
| Al | Peak area of exhaust stream | 52 |
| A2 | Response factor (obtained from Calibration Data) | 53 |
| A3 | Mol of each chemical species in the exhaust stream | 53 |
| A4 | Methane conversion | 53 |
| A5 | Total mol of Product | 54 |
| B1 | The ingredients of prepared catalyst | 56 |
| C1 | The response factors calculated from the Single Point | |
| | External Standard | 57 |
| C2 | The response factors calculated from the Multiple Point | |
| | External Standard | 59 |
| D1 | The results of the reaction with 20 ml/min of CH ₄ , 5 ml/min of O ₂ , | |
| | 5 ml/min of N ₂ , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| | reaction temperature 660 °C, and 2 g of SiO ₂ | 60 |
| D2 | The results of the reaction with 20 ml/min of CH ₄ , 5 ml/min of O ₂ , | |
| | 5 ml/min of N ₂ , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| | reaction temperature 660 °C, and 2 g of Al ₂ O ₃ | 61 |
| D3 | The results of the reaction with 20 ml/min of CH ₄ , 5 ml/min of O ₂ , | |
| | 5 ml/min of N ₂ , 6.5 ml/h of 48 wt% HBr/H ₂ O, | 1.2 |

| TABLE | | PAGE |
|-------|----------------------------------------------------------------------------------------------|------|
| | reaction temperature 660 °C, and 2 g of ZSM-5 | 62 |
| D4 | The results of the reaction with 20 ml/min of CH ₄ , 5 ml/min of O ₂ , | |
| | 5 ml/min of N ₂ , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| | reaction temperature 660 °C, and 2 g of Activated carbon | 63 |
| D5 | The results of the reaction with 20 ml/min of CH ₄ , 5 ml/min of O ₂ , | |
| | 5 ml/min of N ₂ , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| 19 | reaction temperature 400 °C | 64 |
| D6 | The results of the reaction with 20 ml/min of CH ₄ , 5 ml/min of O ₂ , | |
| | 5 ml/min of N ₂ , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| | reaction temperature 500 °C | 65 |
| D7 | The results of the reaction with 20 ml/min of CH ₄ , 5 ml/min of O ₂ , | |
| | 5 ml/min of N ₂ , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| | reaction temperature 600 °C | 66 |
| D8 | The results of the reaction with 20 ml/min of $\mathrm{CH_4}$, 5 ml/min of $\mathrm{O_2}$, | |
| | 5 ml/min of N ₂ , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| | reaction temperature 660 °C | 67 |
| D9 | The results of the reaction with 20 ml/min of CH_4 , 5 ml/min of O_2 , | |
| | 5 ml/min of N ₂ , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| | reaction temperature 700 °C | 68 |
| D10 | The results of the reaction with 20 ml/min of CH ₄ , | |
| | 10 ml/min of N_2 , 6.5 ml/h of 48 wt% HBr/ H_2O , | |
| | reaction temperature 400 °C, and | |
| | 2 g of 0.5 wt% Rh/SiO ₂ -calcined at 450 °C 6 h | 69 |
| D11 | The results of the reaction with 20 ml/min of CH ₄ , | |
| | 3.5 ml/min of O_2 , 7.5 ml/min of N_2 , | |
| | 6.5 ml/h of 48 wt% HBr/H ₂ O, reaction temperature 400 °C, | |
| | and 2 g of 0.5 wt% Rh/SiO ₂ -calcined at 450 °C 6 h | 70 |

| TABL | TABLE | |
|------|----------------------------------------------------------------------------------------|----|
| D12 | The results of the reaction with 20 ml/min of CH ₄ , | |
| | 5 ml/min of O ₂ , 5 ml/min of N ₂ , | |
| | 6.5 ml/h of 48 wt% HBr/ H_2O , reaction temperature 400 °C, | |
| | and 2 g of 0.5 wt% Rh/SiO ₂ -calcined at 450 °C 6 h | 71 |
| D13 | The results of the reaction with 20 ml/min of CH ₄ , | |
| | 6 ml/min of O_2 , 4 ml/min of N_2 , 6.5 ml/h of 48 wt% HBr/H_2O , | |
| | reaction temperature 400 $^{\circ}\text{C}$, and 2 g of 0.5 wt% Rh/SiO ₂ | - |
| | -calcined at 450 °C 6 h | 72 |
| D14 | The results of the reaction with 20 ml/min of CH ₄ , | |
| | 5 ml/min of O_2 , 5 ml/min of N_2 , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| | reaction temperature 400 $^{\circ}\text{C}$, and 2 g of 0.3 wt% Rh/SiO ₂ | |
| | -calcined at 450 °C 6 h | 73 |
| D15 | The results of the reaction with 20 ml/min of CH ₄ , | |
| | 5 ml/min of O_2 , 5 ml/min of N_2 , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| | reaction temperature 400 $^{\circ}\mathrm{C}$, and 2 g of 0.3 wt% Rh/SiO ₂ | |
| | -calcined at 900 °C 10 h | 74 |
| D16 | The results of the reaction with 20 ml/min of CH ₄ , | |
| | 5 ml/min of O_2 , 5 ml/min of N_2 , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| | reaction temperature 400 $^{\circ}\text{C}$, and 0.5 wt% Rh/SiO ₂ | |
| | -calcined at 900 °C 10 h | 75 |
| D17 | The results of the reaction with 20 ml/min of CH ₄ , | |
| | 5 ml/min of O_2 , 5 ml/min of N_2 , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| | reaction temperature 400 $^{\circ}\text{C}$, and 2 g of SiO_2 | 76 |

LIST OF FIGURES

| FIGUR | FIGURE | |
|-------|----------------------------------------------------------------------------------------------------|----|
| 2.1 | Halogenation of methane follow by hydrolysis to obtain methyl | |
| | alcohol and dimethyl ether. | 6 |
| 2.2 | Partial oxidation of alkanes via bromination followed by the reaction | |
| | with solid metal oxide mixtures. | 6 |
| 2.3 | Possible reaction pathways for the OBM reaction : gas phase and | |
| | the surface of the catalyst reaction. | 11 |
| 2.4 | Possible reaction pathways for the OBM reaction : | |
| | monobromomethane (main product), polybromomethanes, and | |
| | another byproducts. | 11 |
| 2.5 | The product distribution of the OBM reaction with different | |
| | calcination conditions. | 13 |
| 2.6 | Mechanism of toluene alkylation with methanol using H-zeolite. | 14 |
| 2.7 | Process for preparation of para-xylene from the alkylation of toluene | |
| | with CH ₃ Br. | 14 |
| 2.8 | Catalytic performance comparison of P/HZSM-5, Si/HZSM-5 and | |
| | Si-P/HZSM-5. | 15 |
| 2.9 | Possible reaction mechanism over Si-P/HZSM-5 catalyst. | 16 |
| 3.1 | Catalysts preparation flow scheme. | 19 |
| 3.2 | Procedure flow scheme for oxidative bromination of methane | |
| | reaction. | 22 |
| 3.3 | Experimental setup for oxidative bromination of methane reaction. | 23 |
| 4.1 | Methane conversion and product distributions as a function of | |
| | time on stream. Reaction Conditions: 20 ml/min of CH ₄ , | |
| | 5 ml/min of O ₂ , 5 ml/min of N ₂ , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| | reaction temperature 660 °C. | 25 |
| 4.2 | Methane conversion as a function of time on stream at various | |
| | material supports. Reaction Conditions: 20 ml/min of CH ₄ , | |
| | 5 ml/min of O ₂ , 5 ml/min of N ₂ , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |

| FIGU | GURE | |
|------|----------------------------------------------------------------------------------------------------|----|
| | reaction temperature 660 °C. | 26 |
| 4.3 | Methyl bromide selectivity as a function of time on stream at | |
| | various material supports. Reaction Conditions: 20 ml/min of CH ₄ , | |
| | 5 ml/min of O ₂ , 5 ml/min of N ₂ , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| | reaction temperature 660 °C. | 26 |
| 4.4 | Methane conversion as a function of time on stream at different | |
| | reaction temperature. Reaction Conditions: 20 ml/min of CH ₄ , | |
| | 5 ml/min of O ₂ , 5 ml/min of N ₂ , 6.5 ml/h of 48 wt% HBr/H ₂ O. | 28 |
| 4.5 | Methyl bromide selectivity as a function of time on stream at | |
| | different reaction temperature. Reaction Conditions: | |
| | 20 ml/min of CH ₄ , 5 ml/min of O ₂ , 5 ml/min of N ₂ , | |
| | 6.5 ml/h of 48 wt% HBr/H ₂ O. | 28 |
| 4.6 | Methane conversion as a function of time on stream at different | |
| | %O ₂ . Reaction Conditions: 20 ml/min of CH ₄ , | |
| | 6.5 ml/h of 48 wt% HBr/H ₂ O, reaction temperature 400 °C, | |
| | 0.5 wt% Rh/SiO ₂ (calcined at 450 °C 6 h). | 30 |
| 4.7 | Methyl bromide selectivity as a function of time on stream at | |
| | different %O ₂ . Reaction Conditions: 20 ml/min of CH ₄ , | |
| | 6.5 ml/h of 48 wt% HBr/H ₂ O, reaction temperature 400 °C, | |
| | 0.5 wt% Rh/SiO ₂ (calcined at 450 °C 6 h). | 30 |
| 4.8 | Methane conversion as a function of time on stream at various | |
| | materials. Reaction Conditions: 20 ml/min of CH ₄ , | |
| | 5 ml/min of O ₂ , 5 ml/min of N ₂ , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| | reaction temperature 400 °C. | 31 |
| 4.9 | Methyl bromide selectivity as a function of time on stream at | |
| | various materials. Reaction Conditions: 20 ml/min of CH ₄ , | |
| | 5 ml/min of O_2 , 5 ml/min of N_2 , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| | reaction temperature 400 °C | 32 |

| FIGUI | IGURE | |
|-------|----------------------------------------------------------------------------------------------------|----|
| 4.10 | Methane conversion as a function of time on stream at different | |
| | Rh loading on SiO ₂ . Reaction Conditions: 20 ml/min of CH ₄ , | |
| | 5 ml/min of O ₂ , 5 ml/min of N ₂ , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| | reaction temperature 400 °C. | 33 |
| 4.11 | Methyl bromide selectivity as a function of time on stream at | |
| | different Rh loading on SiO ₂ . Reaction Conditions: | |
| | 20 ml/min of CH ₄ , 5 ml/min of O ₂ , 5 ml/min of N ₂ , | |
| | 6.5 ml/h of 48 wt% HBr/H ₂ O, reaction temperature 400 °C. | 33 |
| 4.12 | Methane conversion as a function of time on stream at different | |
| | calcination conditions. Reaction Conditions: 20 ml/min of CH ₄ , | |
| | 5 ml/min of O ₂ , 5 ml/min of N ₂ , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| | reaction temperature 400 °C, 0.3 wt% Rh/SiO ₂ . | 35 |
| 4.13 | Methane conversion as a function of time on stream at different | |
| | calcination conditions. Reaction Conditions: 20 ml/min of CH ₄ , | |
| | 5 ml/min of O ₂ , 5 ml/min of N ₂ , 6.5 ml/h of 48 wt% HBr/H ₂ O, | |
| | reaction temperature 400 °C, 0.5 wt% Rh/SiO ₂ . | 35 |
| 4.14 | Methyl bromide selectivity as a function of time on stream | |
| | at different calcination conditions. Reaction Conditions: | |
| | 20 ml/min of CH ₄ , 5 ml/min of O ₂ , 5 ml/min of N ₂ , | |
| | 6.5 ml/h of 48 wt% HBr/H ₂ O, reaction temperature 400 °C, | |
| | 0.3 wt% Rh/SiO ₂ . | 36 |
| 4.15 | Methyl bromide selectivity as a function of time on stream | |
| | at different calcination conditions. Reaction Conditions: | |
| | 20 ml/min of CH ₄ , 5 ml/min of O ₂ , 5 ml/min of N ₂ , | |
| | 6.5 ml/h of 48 wt% HBr/H ₂ O, reaction temperature 400 °C, | |
| | 0.5 wt% Rh/SiO ₂ . | 36 |
| 4.16 | X-ray diffraction patterns of SiO ₂ and 0.5 wt% Rh/SiO ₂ catalysts | |
| | different calcination conditions | 30 |

| FIGURE | | PAGE |
|--------|--------------------------------------------------------------|------|
| 4.17 | TPR profiles of 0.5 wt% Rh/SiO ₂ catalysts | |
| | —differentt calcination conditions. | 40 |
| 4.18 | SEM image of SiO ₂ in the magnification 250x. | 42 |
| 4.19 | EDX image of SiO ₂ in the magnification 9000x. | 43 |
| 4.20 | SEM image of Rh/SiO ₂ in the magnification 250x . | 44 |
| 4.21 | EDX image of Rh/SiO ₂ in the magnification 9000x. | 45 |
| C1 | Response factors from GC FID as a function of injection | |
| | volume of methyl bromide. | 58 |
| C2 | Response factors from GC FID as a function of injection | |
| | volume of dibromomethanes. | 58 |