

REFERENCES

- Borer, A.L. and Prins, R. (1993) Temperature-Programmed Reduction and CO Hydrogenation of La₂O₃-Promoted Rh/SiO₂ Catalysts. Journal of Catalysis 144(2), 439-451.
- Lin, R., Ding, Y., Gong, L., Dong, W., Wang, J. , and Zhang, T. (2010) Efficient and stable silica-supported iron phosphate catalysts for oxidative bromination of methane. Journal of Catalysis 272(1), 65-73.
- Lin, R., Ding, Y., Gong, L., Li, J., Chen, W., Yan, L. , and Lu, Y. (2009) Oxidative bromination of methane on silica-supported non-noble metal oxide catalysts. Applied Catalysis A: General 353(1), 87-92.
- Liu, Z., Li, W. and Zhou, X. (2010) Product oriented oxidative bromination of methane over Rh/SiO₂ catalysts. Journal of Natural Gas Chemistry 19(5), 522-529.
- Moya, S.F., Martins, R.L., and Schmal, M. (2011) Monodispersed and nanostructured Ni/SiO₂ catalyst and its activity for non oxidative methane activation. Applied Catalysis A: General 396(1-2), 159-169.
- Reyes, P., Rodríguez, C., Pecchi, G., and Fierro, J.L.G. (2000) Promoting effect of Mo on the selective hydrogenation of cinnamaldehyde on Rh/SiO₂ catalysts. Catalysis Letters 69(1-2), 27-32.
- Wang, K.X., Xu, H.F., Li, W.S., Au, C.T., and Zhou, X.P. (2006) The synthesis of acetic acid from methane via oxidative bromination, carbonylation, and hydrolysis. Applied Catalysis A: General 304(0), 168-177.
- Wang, K.X., Xu, H.F., Li, W.S., and Zhou, X.P. (2005) Acetic acid synthesis from methane by non-synthesis gas process. Journal of Molecular Catalysis A: Chemical 225(1), 65-69.
- Xu, H., Wang, K., Li, W., and Zhou, X. (2005) Dimethyl ether synthesis from methane by non syngas process. Catalysis Letters 100(1-2), 53-57.
- Yang, F., Liu, Z., Li, W., Wu, T., and Zhou, X. (2008) The Oxidative Bromination of Methane Over Rh/SiO₂ Catalyst. Catalysis Letters 124(3-4), 226-232.
- Aboul-Gheit, A.K., Hanafy, S.A., Aboul-Enein, A.A., and Ghoneim, S.A. (2011) Para-xylene maximization: Part IX—Activation of toluene methylation catalysts with palladium. Journal of the Taiwan Institute of Chemical Engineers 42(5), 860-867.

- Albert E. Schweizer, M.E.J., and Daniel A. Hickman (2002) Oxidative Halogenation of C1 Hydrocarbons to Halogenated C1 Hydrocarbons and Integrated Process Related Thereto. USA, Dow Global Technologies. U.S. Patent 6,452,058.
- BP (2006) BP Statistical Review of World Energy. London : BP p.l.c.
- Chang, C.D. (1983) Hydrocarbons from Methanol. Catalysis Reviews 25(1), 1-118.
- Crabtree, R.H. (1995) Aspects of Methane Chemistry. Chemical Reviews 95(4), 987-1007.
- Degirmenci, V., Uner, D., and Yilmaz, A. (2005) Methane to higher hydrocarbons via halogenation. Catalysis Today 106(1-4), 252-255.
- Ding, K., Metiu, H., and Stucky, G.D. (2013) The Selective High-Yield Conversion of Methane Using Iodine-Catalyzed Methane Bromination. ACS Catalysis 3(3), 474-477.
- George A. Olah, B.G., Jeff D. Felberg, Wai M. Ip, Altaf Husain, Richard Karpeles, Koop Lammertsma, Ashok K. Melhotra, and Nirupam J. Trivedi (1985) Selective Monohalogenation of Methane over Supported Acid or Platinum Metal Catalysts and Hydrolysis of Methyl Halides over γ -Alumina-Supported Metal Oxide/Hydroxide Catalysts. A Feasible Path for the Oxidative Conversion of Methane to Methyl Alcohol/Dimethyl Ether. Journal of the American Chemical Society 107, 7097-7105.
- Hutchings, G.J. and Hunter, R. (1990) Hydrocarbon formation from methanol and dimethyl ether: a review of the experimental observations concerning the mechanism of formation of the primary products. Catalysis Today 6(3), 279-306.
- Lin, R., Ding, Y., Gong, L., Dong, W., Wang, J., and Zhang, T. (2010) Efficient and stable silica-supported iron phosphate catalysts for oxidative bromination of methane. Journal of Catalysis 272(1), 65-73.
- Lin, R., Ding, Y., Gong, L., Li, J., Chen, W., Yan, L., and Lu, Y. (2009) Oxidative bromination of methane on silica-supported non-noble metal oxide catalysts. Applied Catalysis A: General 353(1), 87-92.
- Liu, Z., Huang, L., Li, W.S., Yang, F., Au, C.T., and Zhou, X.P. (2007) Higher hydrocarbons from methane condensation mediated by HBr. Journal of Molecular Catalysis A: Chemical 273(1-2), 14-20.

- Liu, Z., Li, W., and Zhou, X. (2010) Product oriented oxidative bromination of methane over Rh/SiO₂ catalysts. *Journal of Natural Gas Chemistry* 19(5), 522-529.
- Lorkovic, I.M., Sun, S., Gadewar, S., Breed, A., Macala, G.S., Sardar, A., Cross, S.E., Sherman, J.H., Stucky, G.D., and Ford, P.C. (2006) Alkane Bromination Revisited: “Reproportionation” in Gas-Phase Methane Bromination Leads to Higher Selectivity for CH₃Br at Moderate Temperatures. *The Journal of Physical Chemistry A* 110(28), 8695-8700.
- Olah, G.A. (1987) Electrophilic methane conversion. *Accounts of Chemical Research* 20(11), 422-428.
- Otsuka, K. and Hatano, M. (1987) The catalysts for the synthesis of formaldehyde by partial oxidation of methane. *Journal of Catalysis* 108(1), 252-255.
- Reid, R.C., Prausnitz, J.M., and Sherwood, T.K. (1977) The properties of gases and liquids: McGraw-Hill.
- Stocker, M. (1999) Methanol-to-hydrocarbons: catalytic materials and their behavior. *Microporous and Mesoporous Materials* 29(1), 3-48.
- Wang, K.X., Xu, H.F., Li, W.S., Au, C.T., and Zhou, X.P. (2006) The synthesis of acetic acid from methane via oxidative bromination, carbonylation, and hydrolysis. *Applied Catalysis A: General* 304(0), 168-177.
- Wang, K.X., Xu, H.F., Li, W.S., and Zhou, X.P. (2005) Acetic acid synthesis from methane by non-synthesis gas process. *Journal of Molecular Catalysis A: Chemical* 225(1), 65-69.
- WorldBank (2006) Reducing the Gas Burning. World Bank Weekly Update. Washington, DC : The World Bank.
- Xu, H., Wang, K., Li, W., and Zhou, X. (2005) Dimethyl ether synthesis from methane by non syngas process. *Catalysis Letters* 100(1-2), 53-57.
- Yang, F., Liu, Z., Li, W., Wu, T., and Zhou, X. (2008) The Oxidative Bromination of Methane Over Rh/SiO₂ Catalyst. *Catalysis Letters* 124(3-4), 226-232.
- Zhou, X.-P., Ouyang, Q., Yin, S.-F., Chen, L., and Au, C.-T. (2013) A new catalytic process for high-efficiency synthesis of p-xylene by methylation of toluene with CH₃Br. *AIChE Journal* 59(2), 532-540.
- Zhou, X.P., Yilmaz, A., Yilmaz, G.A., Lorkovic, I.M., Laverman, L.E., Weiss, M., Sherman, J.H., McFarland, E.W., Stucky, G.D., and Ford, P.C. (2003) An

integrated process for partial oxidation of alkanes. Chemical communications (Cambridge, England) (18), 2294-2295.

APPENDICES

Appendix A Calculation of Methane Conversion and Product Selectivity

A.1 %CH₄ Conversion

1. Definition of CH₄ Conversion

$$\% \text{CH}_4 \text{Conversion} = \frac{\text{Total mol of } \text{CH}_{4,\text{in}} - \text{Total mol of } \text{CH}_{4,\text{out}}}{\text{Total mol of } \text{CH}_{4,\text{in}}} \times 100 \quad (1)$$

2. *Total mol of CH_{4,in}* can be replaced by the term *Total C* since the source of total carbon are derived from only methane and *Total C in CH_{4,out}* can be replaced by *C in unreacted CH₄*.

Therefore, the eq. (1) becomes;

$$\% \text{CH}_4 \text{Conversion} = \frac{\text{Total C} - \text{C in unreacted } \text{CH}_4}{\text{Total C}} \times 100 \quad (2)$$

3. Carbon balance with no coke formation:

Total C = Total C_{in} = Total C_{out} (obtained from all carbon in outlet stream)

Hence, *Total C – C in unreacted CH₄* in eq. (2) can be replaced by *Total C in all Products*

Thus eq. (2) becomes;

$$\% \text{CH}_4 \text{Conversion} = \frac{\text{Total C in all Products}}{\text{Total C}} \times 100 \quad (3)$$

Example; for the reaction in case of the blank tube

1. The resulting peak area from online GC of all chemicals in the exhaust stream listed below:

Table A1 Peak area of exhaust stream

FID					TCD
CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
11808.5	0	38.8	1126.4	79.7	932.7

2. Change area to mol by multiplying with response factor of each substance.

Table A2 Response factor (obtained from Calibration Data)

Substance	Response factor(mol/area)
CH ₄	4.5969E-10
C ₂ H ₆	3.4581E-10
C ₂ H ₄	3.4151E-10
CH ₃ Br	1.0000E-09
CH ₂ Br ₂	5.0000E-10
CO	5.6853E-10

Table A3 Mol of each chemical species in the exhaust stream

Mol					
CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
5.42827E-06	0	1.32506E-08	1.1264E-06	3.985E-08	5.30274E-07

3. Total mol of C was calculated by

$$= \text{mol of } C_{CH_4} + 2(\text{mol of } C_{C_2H_6}) + 2(\text{mol of } C_{C_2H_4}) + \text{mol of } C_{CH_3Br} + \text{mol of } C_{CH_2Br_2} + \text{mol of } C_{CO}$$

C in product was calculated by

$$= 2(\text{mol of } C_{C_2H_6}) + 2(\text{mol of } C_{C_2H_4}) + \text{mol of } C_{CH_3Br} + \text{mol of } C_{CH_2Br_2} + \text{mol of } C_{CO}$$

Accordingly, the methane conversion calculated from eq. (3) was shown in the below table

Table A4 Methane conversion

Total mol of C	C in product	% CH ₄ Conversion
7.15129E-06	1.72302E-06	24.0939

A.2 %CH₃Br Selectivity

$$\% \text{CH}_3\text{Br Selectivity} = \frac{\text{mol of } \text{CH}_3\text{Br}}{\text{Total mol of Product}} \times 100$$

Example;

1. Mol of CH₃Br (shown in Table A3)

$$= 1.1264\text{E-06 mol}$$

2. Total mol of Product was calculated by

$$= \text{mol of C}_2\text{H}_6 + \text{mol of C}_2\text{H}_4 + \text{mol of C}_{\text{CH}_3\text{Br}} + \text{mol of}$$

$$\text{C}_{\text{CH}_2\text{Br}_2} + \text{mol of CO}$$

Table A5 Total mol of Product

Mol					Total mol of product
C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO	
0	1.32506E-08	1.1264E-06	3.985E-08	5.30274E-07	1.70977E-06

$$\% \text{CH}_3\text{Br Selectivity} = \frac{1.1264\text{E-06}}{1.70977\text{E-06}} \times 100 = 65.88 \%$$

A.3 %CO Selectivity

*The conceptual calculation of %CO Selectivity is the same as %CH₃Br Selectivity.

Appendix B Calculation of Catalyst Composition

The Rh/SiO₂ catalyst was prepared by incipient wetness impregnation method which means support containing the same pore volume as the volume of the solution that was added.

Example 2 g of 0.5 wt% Rh/SiO₂ catalyst

= 2 g (Rh₂O₃ + SiO₂) of 0.5 % (Rh⁰ w/w to Rh₂O₃ + SiO₂)

Rh₂O₃ form must be involved in this case due to small amount of catalyst prepared.

Step 1: wt. Rh⁰

wt. of Rh ⁰	0.0100	g
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Step 2: wt. Rh₂O₃

MW of Rh ⁰	102.9100	g/mol
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MW of Rh ₂ O ₃	253.8200	g/mol
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wt. of Rh ₂ O ₃	0.0123	g
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Step 3: wt SiO₂

wt. of Support (SiO ₂)	1.9877	g
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Step 4: wt RhCl₃*3H₂O

MW of RhCl ₃ *3H ₂ O	263.3103	g/mol
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g of RhCl ₃ *3H ₂ O	0.0256	g
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(assay \geq 99.9% trace metal basis)

Corrected weight	0.0258	g
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Step 5: Lattice water

Lattice water	0.0052	ml
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(negligible)

Step 6: Volume of SiO₂

From BET surface analysis, total pore volume of SiO₂ is

2.1606 ml/g

Volume of SiO ₂	4.2925	ml
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Step 7: Water required

Impregnation volume (100% pore volume)

Water required for RhCl ₃ *3H ₂ O	4.2925	ml
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Table B1 The ingredients of prepared catalyst

Loading (wt%)	SiO ₂ (g)	RhCl ₃ *3H ₂ O (g)	Required water (ml)
0.1	2	0.0052	4.3160
0.3	2	0.0258	4.2925
0.5	2	0.0155	4.3052

Appendix C Calibration Data and Feed Flow Calibration

The response factors of methane (CH_4) ethane (C_2H_6) ethylene (C_2H_4), and carbon monoxide (CO) were determined by using the Single Point External Standard assuming analyte response to be linear over a range of concentrations. This method requires a known amount of analytes and record the peak area. The peak area of each substrate was calculated from average areas. The volume of each online injection equals to 2.5 ml which subsequently converted to mol bases on an ideal gas. Then calculate a response factor using an equation below.

$$\text{Response Factor} = \frac{\text{mol}}{\text{area}}$$

Table C1 The response factors calculated from the Single Point External Standard

No./ Retention time	Methane	Ethane	Ethylene	Carbon monoxide
	3.49	4.46	5.02	9.34
1	22225.7	295.6	299.1	180.7
2	22315.9	294.3	297.9	180.5
3	22222.5	297.2	301.1	178.2
4		296.3	300.2	180.4
Area	22254.7	295.85	299.575	179.95
Volume(l)	0.00025	0.0000025	0.0000025	0.0000025
Mol	1.023E-05	1.023E-07	1.023E-07	1.023E-07
Response factor (mol/area)	4.5969E-10	3.4581E-10	3.4151E-10	5.6853E-10

For methyl bromide (CH_3Br) and dibromomethane (CH_2Br_2), the response factors were determined by using the Multiple Point External Standard. The samples used in this method cover the expected analyte concentration range. Use a line fitting algorithm such as point to point, linear least squares, or quadratic least squares to produce a calibration curve. The response factor used for calculation the

products amount were derived from the reciprocal of slope of calibration curve as shown in Figure C1 and Figure C2.

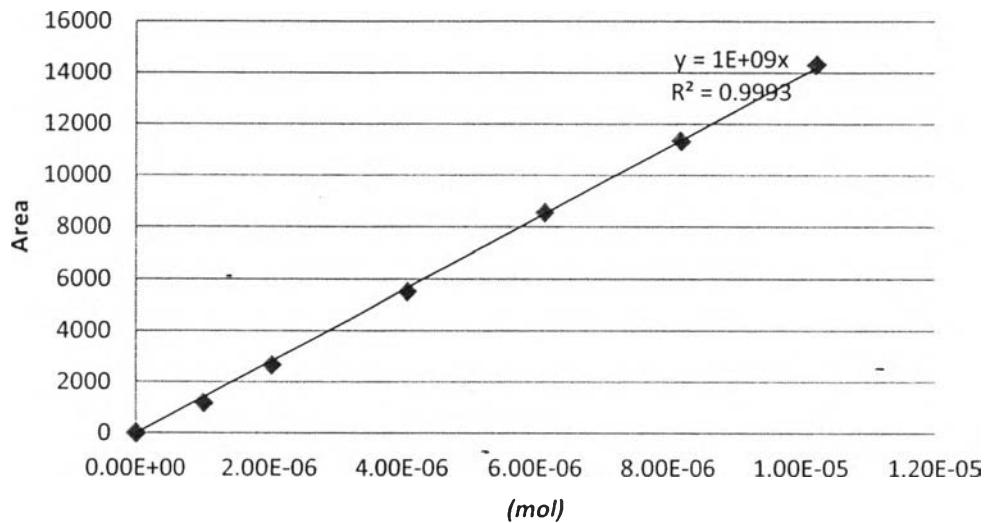


Figure C1 Response factors from GC FID as a function of injection volume of methyl bromide.

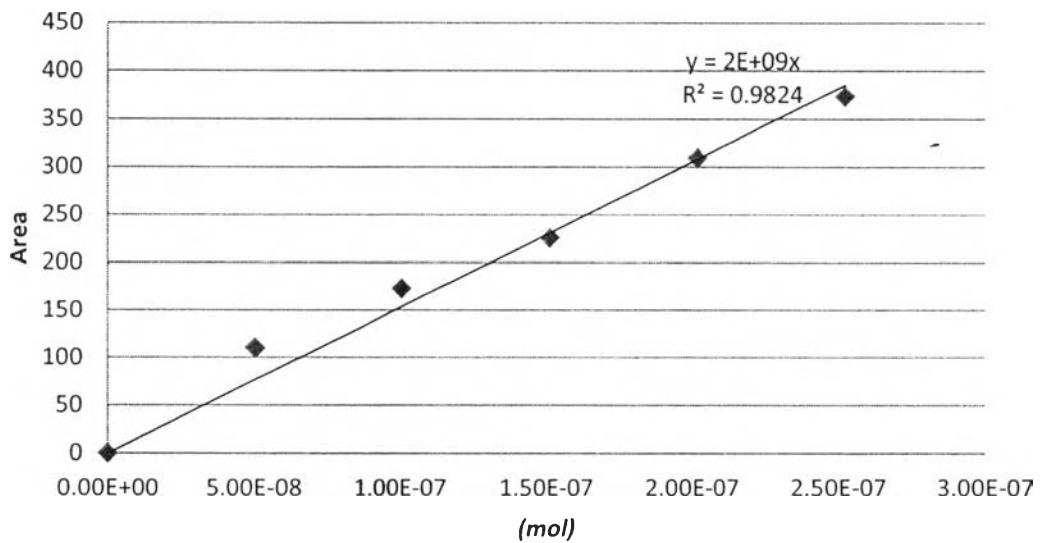


Figure C2 Response factors from GC FID as a function of injection volume of dibromomethanes.

Table C2 The response factors calculated from the Multiple Point External Standard

Chemicals	Retention time	Slope (area/mol)	Response factor (mol/area)
Methyl bromide	12.50	1E+09	1E-09
Dibromomethanes	21.03	2E+09	5E-10

Appendix D Raw Data of Reaction Results

The reaction results as a raw data of GC FID and TCD peak area and calculated data are shown below.

Table D1 The results of the reaction with 20 ml/min of CH₄, 5 ml/min of O₂, 5 ml/min of N₂, 6.5 ml/h of 48 wt% HBr/H₂O, reaction temperature 660 °C, and 2 g of SiO₂

TOS		FID					TCD	%CH ₄ Conversion	% Selectivity				
min	h	CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO		C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
30	0.5	13352.9	0	9.8	315.5	0	2398.6	21.55	0	0.20	18.75	0	81.05
64	1.1	12641.3	0	9.8	683.6	13.5	2316.2	25.74	0	0.17	34.00	0.34	65.50
98	1.6	12912.3	0	9.2	816.1	19.6	2113.3	25.52	0	0.15	40.19	0.48	59.17
132	2.2	12341.9	0	9.9	791.8	18.1	2152.1	26.36	0	0.17	39.05	0.45	60.34
166	2.8	12123.2	0	11.9	889.5	27.2	2217.6	28.04	0	0.19	41.03	0.63	58.16
200	3.3	12120.9	0	11.7	930.4	29.5	2106.8	27.85	0	0.19	43.34	0.69	55.79
234	3.9	11968	0	12.5	986.8	31.8	2079.2	28.50	0	0.20	45.08	0.73	54.00
268	4.5	12667.5	0	9.7	991	30.3	1723	25.49	0	0.17	49.82	0.76	49.25
302	5.0	11898.2	0	11.5	1017.7	33.5	2020	28.60	0	0.18	46.54	0.77	52.52
336	5.6	12240.6	0	10.2	964.3	32.9	1897.8	26.86	0	0.17	46.74	0.80	52.30
370	6.2	12114.9	0	9.8	962.2	30	1807.6	26.54	0	0.17	47.91	0.75	51.17
404	6.7	12070.2	0	7.8	993	31.9	1700.1	26.31	0	0.13	50.20	0.81	48.86
438	7.3	12511.4	0	6.6	891.5	26.3	1733.5	24.78	0	0.12	47.11	0.69	52.08

Table D2 The results of the reaction with 20 ml/min of CH₄, 5 ml/min of O₂, 5 ml/min of N₂, 6.5 ml/h of 48 wt% HBr/H₂O, reaction temperature 660 °C, and 2 g of Al₂O₃

TOS		FID					TCD	%CH ₄ Conversion	% Selectivity				
min	h	CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO		C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
30	0.5	12722	0	15.1	40.7	0	2226.8	18.38	0	0.39	3.10	0	96.50
64	1.1	12509.5	0	18.3	35.6	0	2667.6	21.39	0	0.40	2.28	0	97.31
98	1.6	12979.8	0	14.1	29.2	0	2488.9	19.59	0	0.33	2.02	0	97.65
132	2.2	12406.8	0	22	20.3	0	2713.5	21.67	0	0.48	1.29	0	98.23
166	2.8	12599.9	0	20.1	18	0	2700	21.29	0	0.44	1.15	0	98.41
200	3.3	12544.3	0	19	14	0	2830.3	22.10	0	0.40	0.86	0	98.74
234	3.9	12683.9	0	23.1	0	0	2994.5	22.76	0	0.46	0.00	0	99.54
268	4.5	13425.4	0	16.1	12.8	0	2685.9	20.08	0	0.36	0.83	0	98.82
302	5.0	13824.5	0	20.1	0	0	2621.9	19.14	0	0.46	0	0	99.54
336	5.6	13872.3	0	17.4	0	0	2606.3	18.98	0	0.40	0	0	99.60
370	6.2	13428	0	21.9	0	0	2776.4	20.52	0	0.47	0	0	99.53
404	6.7	13838.2	0	19.8	0	0	2761.7	19.93	0	0.43	0	0	99.57
438	7.3	13763	0	20.4	0	0	2693.1	19.63	0	0.45	0	0	99.55

Table D3 The results of the reaction with 20 ml/min of CH₄, 5 ml/min of O₂, 5 ml/min of N₂, 6.5 ml/h of 48 wt% HBr/H₂O, reaction temperature 660 °C, and 2 g of ZSM-5

TOS		FID					TCD	%CH ₄ Conversion	% Selectivity				
min	h	CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO		C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
30	0.5	14386.4	0	19.3	0	0	1974.9	14.66	0	0.58	0	0	99.42
64	1.1	12348.1	0	33.8	18.4	0	3382.7	25.71	0	0.59	0.94	0	98.47
98	1.6	13795.2	0	32.2	20.5	0	2950.4	21.33	0	0.64	1.20	0	98.16
132	2.2	12625.8	0	40.6	17	0	3009.8	23.23	0	0.80	0.98	0	98.23
166	2.8	13556.6	0	33.3	22.4	0	2344.1	18.11	0	0.83	1.64	0	97.53
200	3.3	12695.6	0	50.3	20.8	0	2823.8	22.15	0	1.05	1.27	0	97.69
234	3.9	12772.8	0	56.3	21.7	0	2633.1	20.96	0	1.25	1.41	0	97.34
268	4.5	13157.8	0	53.8	20.4	0	2500	19.64	0	1.26	1.40	0	97.34
302	5.0	13557.1	0	55.8	23.5	0	2389.3	18.56	0	1.36	1.68	0	96.96
336	5.6	12495.9	0	62.2	24	0	2606.5	21.23	0	1.39	1.57	0	97.04
370	6.2	12385.9	0	60.8	24.2	0	2617.3	21.44	0	1.35	1.58	0	97.07
404	6.7	12512.8	0	60.9	27.4	0	2573.4	21.03	0	1.38	1.81	0	96.81
438	7.3	12802.3	0	61.3	28.7	0	2463.2	20.00	0	1.44	1.98	0	96.58

Table D4 The results of the reaction with 20 ml/min of CH₄, 5 ml/min of O₂, 5 ml/min of N₂, 6.5 ml/h of 48 wt% HBr/H₂O, reaction temperature 660 °C, and 2 g of Activated carbon

TOS		FID					TCD	%CH ₄ Conversion	% Selectivity				
min	h	CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO		C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
30	0.5	12457.4	0	0	0	0	1827.3	15.36	0	0	0	0	100
64	1.1	11355.6	0	0	0	0	2190.6	19.26	0	0	0	0	100
98	1.6	11136.7	0	0	0	0	2268.3	20.12	0	0	0	0	100
132	2.2	10878.8	0	0	0	0	2186.7	19.91	0	0	0	0	100
166	2.8	11676.7	0	0	0	0	2029.4	17.69	0	0	0	0	100
200	3.3	11412.2	0	0	0	0	2089.6	18.46	0	0	0	0	100
234	3.9	11547.1	0	0	0	0	2004.9	17.68	0	0	0	0	100
268	4.5	10876.1	0	0	0	0	2439	21.71	0	0	0	0	100
302	5.0	10961.2	0	0	0	0	2278.5	20.45	0	0	0	0	100
336	5.6	10990.6	0	0	0	0	2286.4	20.46	0	0	0	0	100
370	6.2	10255.4	0	0	0	0	2417.1	22.57	0	0	0	0	100
404	6.7	10559.8	0	0	0	0	2357.3	21.64	0	0	0	0	100
438	7.3	10869.7	0	0	0	0	2277.3	20.58	0	0	0	0	100

Table D5 The results of the reaction with 20 ml/min of CH₄, 5 ml/min of O₂, 5 ml/min of N₂, 6.5 ml/h of 48 wt% HBr/H₂O, reaction temperature 400 °C

TOS		FID					TCD	%CH ₄ Conversion	% Selectivity				
min	h	CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO		C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
30	0.5	14407.6	0	0	49.6	0	0	0.74	0	0	100	0	0
64	1.1	13885.5	0	0	19	0	0	0.30	0	0	100	0	0
98	1.6	14061.1	0	0	13.3	0	0	0.21	0	0	100	0	0
132	2.2	14630.7	0	0	10.2	0	0	0.15	0	0	100	0	0
166	2.8	14026.6	0	0	12.7	0	0	0.20	0	0	100	0	0
200	3.3	13343.5	0	0	17.2	0	0	0.28	0	0	100	0	0
234	3.9	13498.8	0	0	10.3	0	0	0.17	0	0	100	0	0
268	4.5	13613.5	0	0	12.2	0	0	0.19	0	0	100	0	0
302	5.0	13349.7	0	0	11.6	0	0	0.19	0	0	100	0	0
336	5.6	13486.7	0	0	11.5	0	0	0.19	0	0	100	0	0
370	6.2	13032.5	0	0	14	0	0	0.23	0	0	100	0	0
404	6.7	13108.6	0	0	17.6	0	0	0.29	0	0	100	0	0
438	7.3	13166.3	0	0	13.9	0	0	0.23	0	0	100	0	0

Table D6 The results of the reaction with 20 ml/min of CH₄, 5 ml/min of O₂, 5 ml/min of N₂, 6.5 ml/h of 48 wt% HBr/H₂O, reaction temperature 500 °C

TOS		FID					TCD	%CH ₄ Conversion	% Selectivity				
min	h	CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO		C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
30	0.5	14349.3	0	0	359.7	27.3	124.3	6.31	0	0	81.01	3.07	15.92
64	1.1	14214.5	0	0	269.3	22.8	88.6	4.82	0	0	81.34	3.44	15.21
98	1.6	14619.4	0	0	302.9	23.4	101.2	5.25	0	0	81.40	3.14	15.46
132	2.2	13774.4	0	0	346.6	31.3	135.9	6.49	0	0	78.86	3.56	17.58
166	2.8	13423.9	0	0	395.1	36	159.1	7.54	0	0	78.46	3.57	17.96
200	3.3	13223.2	0	0	410.8	42	177.5	8.06	0	0	77.11	3.94	18.94
234	3.9	13117.2	0	0	419.9	44.2	185.2	8.32	0	0	76.72	4.04	19.24
268	4.5	12820.1	0	0	380.2	38.7	158.3	7.67	0	0	77.66	3.95	18.38
302	5.0	13035.8	0	0	359.5	37.3	141.7	7.11	0	0	78.37	4.07	17.56
336	5.6	13355.4	0	0	346.5	33.3	134.2	6.68	0	0	78.85	3.79	17.36
370	6.2	13135	0	0	367.4	34.8	141.8	7.16	0	0	78.94	3.74	17.32
404	6.7	13073.8	0	0	383	39.1	148.4	7.49	0	0	78.66	4.02	17.33
438	7.3	13222.2	0	0	373.2	38.1	147	7.26	0	0	78.43	4.00	17.56

Table D7 The results of the reaction with 20 ml/min of CH₄, 5 ml/min of O₂, 5 ml/min of N₂, 6.5 ml/h of 48 wt% HBr/H₂O, reaction temperature 600 °C

TOS		FID					TCD	%CH ₄ Conversion	% Selectivity				
min	h	CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO		C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
30	0.5	13706.7	0	11.2	1023.3	95.4	391.9	17.12	0	0.29	78.86	3.68	17.17
64	1.1	13409.2	0	7.7	938.9	87.1	372.2	16.29	0	0.22	78.46	3.64	17.68
98	1.6	13782.2	0	6.8	839.9	69.3	343.3	14.50	0	0.22	78.35	3.23	18.21
132	2.2	13618.2	0	0	847.1	70.4	336.3	14.64	0	0	78.91	3.28	17.81
166	2.8	13906	0	0	837.5	67.7	319.1	14.14	0	0	79.55	3.22	17.23
200	3.3	14116.1	0	0	786.5	60.7	296.5	13.18	0	0	79.81	3.08	17.11
234	3.9	14138.1	0	0	812.3	61.7	316.3	13.60	0	0	79.41	3.02	17.58
268	4.5	14311.7	0	0	785.7	58.9	285.2	12.93	0	0	80.40	3.01	16.59
302	5.0	13499.4	0	0	868.7	68.9	336.5	14.99	0	0	79.37	3.15	17.48
336	5.6	13625.1	0	0	848.1	66.2	354.4	14.74	0	0	78.33	3.06	18.61
370	6.2	13743.4	0	0	820.6	64.9	311.1	14.02	0	0	79.68	3.15	17.17
404	6.7	13773	0	0	798.7	62	297.4	13.63	0	0	79.97	3.10	16.93
438	7.3	12714.8	0	0	843.4	71.8	353.1	15.60	0	0	78.09	3.32	18.59

Table D8 The results of the reaction with 20 ml/min of CH₄, 5 ml/min of O₂, 5 ml/min of N₂, 6.5 ml/h of 48 wt% HBr/H₂O, reaction temperature 660 °C

TOS		FID					TCD	%CH ₄ Conversion	% Selectivity				
min	h	CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO		C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
30	0.5	11808.5	0	38.8	1126.4	79.7	932.7	24.09	0	0.77	65.88	2.33	31.01
64	1.1	11710.8	0	30	1518.3	145.9	886	28.21	0	0.49	72.12	3.47	23.93
98	1.6	11834.5	0	30.5	1447	133.2	840.9	27.00	0	0.52	72.27	3.33	23.88
132	2.2	11760.8	0	29.4	1387	124.7	794.6	26.22	0	0.53	72.57	3.26	23.64
166	2.8	11779.8	0	26.4	1362.4	116.5	791.2	25.86	0	0.48	72.49	3.10	23.93
200	3.3	12135.3	0	35.2	1284.4	104.8	801.8	24.57	0	0.67	71.17	2.90	25.26
234	3.9	11844.6	0	33.7	1292.3	103.8	810.4	25.13	0	0.63	71.14	2.86	25.36
268	4.5	11872.4	0	30.7	1294.2	100.6	790.5	24.96	0	0.58	71.72	2.79	24.91
302	5.0	12019.5	0	35.5	1240.9	93.8	810.5	24.29	0	0.69	70.48	2.66	26.17
336	5.6	12012.6	0	34.2	1298.4	97.3	834.7	25.04	0	0.64	70.82	2.65	25.89
370	6.2	12213.1	0	33.4	1256.1	92.9	811.8	24.14	0	0.64	70.75	2.62	25.99
404	6.7	12340.8	0	45.4	1261.8	92.6	879.2	24.48	0	0.85	69.20	2.54	27.41
438	7.3	11796.8	0	40.9	1143.4	84.8	805.3	23.56	0	0.84	68.98	2.56	27.62

Table D9 The results of the reaction with 20 ml/min of CH₄, 5 ml/min of O₂, 5 ml/min of N₂, 6.5 ml/h of 48 wt% HBr/H₂O, reaction temperature 700 °C

TOS		FID					TCD	%CH ₄ Conversion	% Selectivity				
min	h	CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO		C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
30	0.5	13577.5	16.1	217	1080.7	43.1	1085.7	23.23	0.31	4.11	59.90	1.19	34.21
64	1.1	12464.8	0	94.6	1361.9	84.6	1178.8	27.26	0	1.53	64.52	2.00	31.75
98	1.6	11991.3	0	78.1	1264.9	70.5	1067.6	26.30	0	1.38	65.30	1.82	31.34
132	2.2	11969.3	0	66.5	1368.2	71.8	1038.7	27.11	0	1.12	67.71	1.78	29.22
166	2.8	12360.9	0	76.8	1223.8	62.2	1016.8	24.97	0	1.41	65.72	1.67	31.05
200	3.3	12649	0	78.4	1224.5	57.6	1018.5	24.55	0	1.44	65.76	1.55	31.10
234	3.9	12081	0	69.2	1256	59.5	1046.8	25.83	0	1.24	65.84	1.56	31.20
268	4.5	12324.9	0	67.2	1297.4	59.2	980.8	25.47	0	1.20	67.91	1.55	29.19
302	5.0	11633.5	0	70.9	1221	62.8	1158.6	26.88	0	1.25	62.99	1.62	33.98
336	5.6	11799.8	0	72.2	1175.7	61.1	1080	25.69	0	1.33	63.63	1.65	33.23
370	6.2	11872.8	0	67.7	1244.5	61.1	1095.4	26.32	0	1.20	64.69	1.59	32.37
404	6.7	11953.7	0	62.7	1242.3	61.4	961	25.36	0	1.16	67.39	1.67	29.64
438	7.3	12138.7	0	70.1	1203.6	59	1029.9	25.12	0	1.30	65.22	1.60	31.73

Table D10 The results of the reaction with 20 ml/min of CH₄, 10 ml/min of N₂, 6.5 ml/h of 48 wt% HBr/H₂O, reaction temperature 400 °C, and 2 g of 0.5 wt% Rh/SiO₂-calcined at 450 °C 6 h

TOS		FID					TCD	%CH ₄ Conversion	% Selectivity				
min	h	CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO		C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
30	0.5	14280	0	0	0	0	0	0	0	0	0	0	0
64	1.1	14373.5	0	0	0	0	0	0	0	0	0	0	0
98	1.6	14293.2	0	0	0	0	0	0	0	0	0	0	0
132	2.2	15425.9	0	0	0	0	0	0	0	0	0	0	0
166	2.8	14940.5	0	0	0	0	0	0	0	0	0	0	0
200	3.3	15099.5	0	0	0	0	0	0	0	0	0	0	0
234	3.9	14621	0	0	0	0	0	0	0	0	0	0	0
268	4.5	14783.2	0	0	0	0	0	0	0	0	0	0	0
302	5.0	15310.6	0	0	0	0	0	0	0	0	0	0	0
336	5.6	15593.7	0	0	0	0	0	0	0	0	0	0	0
370	6.2	15549.6	0	0	0	0	0	0	0	0	0	0	0

Table D11 The results of the reaction with 20 ml/min of CH₄, 3.5 ml/min of O₂, 7.5 ml/min of N₂, 6.5 ml/h of 48 wt% HBr/H₂O, reaction temperature 400 °C, and 2 g of 0.5 wt% Rh/SiO₂-calcined at 450 °C 6 h

TOS		FID					TCD	%CH ₄ Conversion	% Selectivity				
min	h	CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO		C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
30	0.5	12113.2	0	0	98.9	0	71.1	2.44	0	0	70.99	0	29.01
64	1.1	12357.6	0	0	113.4	0	45.3	2.39	0	0	81.49	0	18.51
98	1.6	11700.9	0	0	103.1	0	39.1	2.28	0	0	82.26	0	17.74
132	2.2	11889.5	0	0	109.8	0	45.2	2.42	0	0	81.03	0	18.97
166	2.8	11850.3	0	0	109.5	0	44.4	2.41	0	0	81.27	0	18.73
200	3.3	11935.8	0	0	107.7	0	47.9	2.40	0	0	79.82	0	20.18
234	3.9	11848.5	0	0	101.8	0	35.5	2.19	0	0	83.45	0	16.55
268	4.5	11979.8	0	0	108.6	0	44	2.37	0	0	81.28	0	18.72
302	5.0	12245.3	0	0	113	0	43.5	2.39	0	0	82.04	0	17.96
336	5.6	12440.2	0	0	123.1	0	44.9	2.53	0	0	82.82	0	17.18
370	6.2	11616.7	0	0	125.9	0	48.9	2.80	0	0	81.91	0	18.09

Table D12 The results of the reaction with 20 ml/min of CH₄, 5 ml/min of O₂, 5 ml/min of N₂, 6.5 ml/h of 48 wt% HBr/H₂O, reaction temperature 400 °C , and 2 g of 0.5 wt% Rh/SiO₂-calcined at 450 °C 6 h

TOS		FID					TCD	%CH ₄ Conversion	% Selectivity				
min	h	CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO		C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
30	0.5	14919.2	0	0	249.6	0	80.3	4.13	0	0	84.54	0.00	15.46
64	1.1	14256.4	0	0	248.7	8.4	92.7	4.46	0	0	81.38	1.37	17.25
98	1.6	14624.3	0	0	277.8	12	72.4	4.61	0	0	85.49	1.85	12.67
132	2.2	14258.6	0	0	267.2	13	54.7	4.44	0	0	87.66	2.13	10.20
166	2.8	14157.2	0	0	266.1	13.2	52.7	4.44	0	0	87.92	2.18	9.90
200	3.3	14509	0	0	245.3	13.1	35.8	3.92	0	0	90.12	2.41	7.48
234	3.9	14593.9	0	0	256.6	13	38.3	4.07	0	0	90.07	2.28	7.64
268	4.5	14749.6	0	0	252.5	13.1	29.7	3.91	0	0	91.51	2.37	6.12
302	5.0	14777.2	0	0	246	12.9	22.1	3.75	0	0	92.83	2.43	4.74
336	5.6	13857.2	0	0	245.8	12.8	24.8	4.01	0	0	92.30	2.40	5.29
370	6.2	13999.4	0	0	245.6	12.4	20.6	3.93	0	0	93.20	2.35	4.44

Table D13 The results of the reaction with 20 ml/min of CH₄, 6 ml/min of O₂, 4 ml/min of N₂, 6.5 ml/h of 48 wt% HBr/H₂O, reaction temperature 400 °C , and 2 g of 0.5 wt% Rh/SiO₂-calcined at 450 °C 6 h

TOS		FID					TCD	%CH ₄ Conversion	% Selectivity				
min	h	CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO		C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
30	0.5	11798	0	0	120.6	0	177.3	3.92	0	0	54.47	0	45.53
64	1.1	11445.2	0	0	151.9	0	106.6	3.88	0	0	71.48	0	28.52
98	1.6	11298.5	0	0	145.4	0	106.9	3.82	0	0	70.52	0	29.48
132	2.2	11487.1	0	0	153	0	119.3	4.01	0	0	69.29	0	30.71
166	2.8	11775.9	0	0	154.1	0	103.9	3.79	0	0	72.29	0	27.71
200	3.3	12131.8	0	0	158.5	0	96.6	3.69	0	0	74.27	0	25.73
234	3.9	12220.4	0	0	167.9	0	111.1	3.95	0	0	72.66	0	27.34
268	4.5	11701.5	0	0	167.7	0	112.1	4.12	0	0	72.46	0	27.54
302	5.0	11727.8	0	0	168.6	0	105.8	4.07	0	0	73.70	0	26.30
336	5.6	11376.2	0	0	168.1	0	109.9	4.22	0	0	72.90	0	27.10
370	6.2	11590.7	0	0	175.6	6.5	107.8	4.31	0	0	73.12	1.35	25.52

Table D14 The results of the reaction with 20 ml/min of CH₄, 5 ml/min of O₂, 5 ml/min of N₂, 6.5 ml/h of 48 wt% HBr/H₂O, reaction temperature 400 °C , and 2 g of 0.3 wt% Rh/SiO₂-calcined at 450 °C 6 h

TOS		FID					TCD	%CH ₄ Conversion	% Selectivity				
min	h	CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO		C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
30	0.5	11844.5	0	0	122.7	27.4	81.1	3.24	0	0	67.23	7.51	25.26
64	1.1	13557.6	0	0	148.9	0	131.3	3.46	0	0	66.61	0	33.39
98	1.6	11609	0	0	126.2	0	59.5	2.91	0	0	78.86	0	21.14
132	2.2	12479	0	0	129.7	0	50.8	2.69	0	0	81.79	0	18.21
166	2.8	12276.5	0	0	115.7	0	34.4	2.34	0	0	85.54	0	14.46
200	3.3	13041.5	0	0	122.5	0	0	2.00	0	0	100	0	0
234	3.9	12864.1	0	0	119.6	0	0	1.98	0	0	100	0	0
268	4.5	12132.3	0	0	100.5	0	0	1.77	0	0	100	0	0
302	5.0	12140.6	0	0	102.5	0	0	1.80	0	0	100	0	0
336	5.6	11711	0	0	99.6	0	0	1.82	0	0	100	0	0
370	6.2	11592	0	0	103.9	0	0	1.91	0	0	100	0	0

Table D15 The results of the reaction with 20 ml/min of CH₄, 5 ml/min of O₂, 5 ml/min of N₂, 6.5 ml/h of 48 wt% HBr/H₂O, reaction temperature 400 °C , and 2 g of 0.3 wt% Rh/SiO₂-calcined at 900 °C 10 h

TOS		FID					TCD	%CH ₄ Conversion	% Selectivity				
min	h	CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO		C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
30	0.5	12510.7	0	0	38.5	0	0	0.66	0	0	100	0	0
64	1.1	12193.2	0	0	53.7	0	0	0.95	0	0	100	0	0
98	1.6	11643.9	0	0	43.6	0	0	0.81	0	0	100	0	0
132	2.2	11884	0	0	35.7	0	0	0.65	0	0	100	0	0
166	2.8	11605.1	0	0	44.5	0	0	0.83	0	0	100	0	0
200	3.3	11827.1	0	0	40.5	0	0	0.74	0	0	100	0	0
234	3.9	12069	0	0	43.3	0	0	0.77	0	0	100	0	0
268	4.5	11584.8	0	0	49.7	0	0	0.92	0	0	100	0	0
302	5.0	11840.5	0	0	42.4	0	0	0.77	0	0	100	0	0
336	5.6	12069	0	0	51.9	0	0	0.93	0	0	100	0	0
370	6.2	11863	0	0	48.9	0	0	0.89	0	0	100	0	0

Table D16 The results of the reaction with 20 ml/min of CH₄, 5 ml/min of O₂, 5 ml/min of N₂, 6.5 ml/h of 48 wt% HBr/H₂O, reaction temperature 400 °C , and 2 g of 0.5 wt% Rh/SiO₂-calcined at 900 °C 10 h

TOS		FID					TCD	%CH ₄ Conversion	% Selectivity				
min	h	CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO		C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
30	0.5	12697.1	0	0	35	0	50.7	1.08	0	0	54.84	0	45.16
64	1.1	12016.6	0	0	44.3	0	0	0.80	0	0	100	0	0
98	1.6	11789.8	0	0	35.9	0	0	0.66	0	0	100	0	0
132	2.2	11564.5	0	0	38.7	0	0	0.72	0	0	100	0	0
166	2.8	11757.2	0	0	41	0	0	0.75	0	0	100	0	0
200	3.3	11958.6	0	0	50.2	0	0	0.90	0	0	100	0	0
234	3.9	12146	0	0	45.3	0	0	0.80	0	0	100	0	0
268	4.5	12367.4	0	0	53	0	0	0.92	0	0	100	0	0
302	5.0	12521.7	0	0	45.8	0	0	0.79	0	0	100	0	0
336	5.6	12569.5	0	0	49.1	0	0	0.84	0	0	100	0	0
370	6.2	12024.1	0	0	57.8	0	0	1.03	0	0	100	0	0

Table D17 The results of the reaction with 20 ml/min of CH₄, 5 ml/min of O₂, 5 ml/min of N₂, 6.5 ml/h of 48 wt% HBr/H₂O, reaction temperature 400 °C , and 2 g of SiO₂

TOS		FID					TCD	%CH ₄ Conversion	% Selectivity				
min	h	CH ₄	C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO		C ₂ H ₆	C ₂ H ₄	CH ₃ Br	CH ₂ Br ₂	CO
30	0.5	15083.4	0	0	194.7	7.8	25.6	2.98	0	0	91.34	1.83	6.83
64	1.1	14822.8	0	0	161.7	7	41.1	2.69	0	0	85.75	1.86	12.39
98	1.6	14377.4	0	0	126.4	0	0	1.88	0	0	100	0	0
132	2.2	13460.6	0	0	102.3	0	0	1.63	0	0	100	0	0
166	2.8	13803.8	0	0	99.5	0	0	1.54	0	0	100	0	0
200	3.3	13922.4	0	0	103.4	0	0	1.59	0	0	100	0	0
234	3.9	14279	0	0	94.9	0	0	1.43	0	0	100	0	0
268	4.5	13355.4	0	0	93	0	0	1.49	0	0	100	0	0
302	5.0	13660.7	0	0	97	0	0	1.52	0	0	100	0	0
336	5.6	13766.7	0	0	93.2	0	0	1.45	0	0	100	0	0
370	6.2	13844.6	0	0	94.7	0	0	1.47	0	0	100	0	0

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Proceedings:

1. Sirijantarat, V.; Jermwongratanachai, T.; and Kitiyanan, B. (2014, April 22) Methyl Bromide Synthesis via Oxidative Bromination of Methane. Proceedings of The 5th Research Symposium on Petroleum, Petrochemicals, and Advanced Materials and The 20th PPC Symposium on Petroleum, Petrochemicals, and Polymers, Bangkok, Thailand.