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## APPENDICES

### Appendix A Source Code of MINLP Single Period Model

The following text is source code which is entered in GAMS for synthesizing HEN for single period.

#### SETS

```
I hot streams          /I1*I3/
J cold streams         /J1*J4/
K index of stage or location ^/K1*K4,KL/ //last number is no. of stages
```

```
//dynamic sets//
```

```
stage(k) all stages
;
stage(k) = yes; stage('KL') = no;
```

#### SCALARS

```
//Cost//
```

```
CA per unit cost of heat exchanger area($ per unit) /641.7/
B exponent for area cost(dimensionless) /1/
CF fixed cost of heat exchanger($ per unit) /8333.3/

CHU per unit cost of hot utility($ per kW) /115.2/
CCU fixed cost of heat exchanger($ per kW) /1.3/

AF annualisation factor /0.2/
```

```
//other//
```

```
EMAT exchanger minimum approach temperature(C) /5/

HHU heat transfer coefficient of hot utility(kW|(m2.C)) /2/
HCU heat transfer coefficient of cold utility(kW|(m2.C)) /1/
;
```

#### PARAMETERS

```
//Hot Streams//
```

```
THIN(i) inlet temperature of hot streams(C)
/ I1 406
I2 160
I3 362
/
THOUT(i) outlet temperature of hot streams(C)
/ I1 60
```

```

        I2  40
        I3  60
    /
//Cold Streams//
    TCIN(j) inlet temperature of cold streams(C)
    /    J1  72
        J2  62
        J3  220
        J4  250
    /
    TCOUT(j) outlet temperature of cold streams(C)
    /    J1  365
        J2  210
        J3  370
        J4  290
    /
//Heat Capacity Flowrates//
    FCPH(i) heat capacity flowrates fo hot streams(C)
    /    I1  205.0
        I2  198.8
        I3  136.4
    /
    FCPC(j) heat capacity flowrates fo cold streams(C)
    /    J1  210.3
        J2  141.0
        J3  175.4
        J4  318.7
    /
//Utility//
    THUIN(j) inlet temperature of hot utility(C)
    /    J1  400
        J2  400
        J3  400
        J4  400
    /
    THUOUT(j) outlet temperature of hot utility(C)
    /    J1  399
        J2  399
        J3  399
        J4  399
    /
    TCUIN(i) inlet temperature of cold utility(C)
    /    I1  15
        I2  15
        I3  15
    /
    TCUOUT(i) outlet temperature of cold utility(C)

```

```

/      I1  20
      I2  20
      I3  20
/
//Heat transfer coefficient//
HH(i)  heat capacity flowrates of hot streams(kW|(m2.C))
/      I1  2
      I2  2
      I3  2
/
HC(j)  heat capacity flowrates of cold streams(kW|(m2.C))
/      J1  1.5
      J2  1.5
      J3  2
      J4  2
/
//overall heat transfer coefficient//
U(i,j)      Overall heat transfer coefficient for match(i,j)
UHU(j)      Overall heat transfer coefficient for cold stream(j) and hot utility
UCU(i)      Overall heat transfer coefficient for hot stream(i) and cold utility

//upper bound for logical constraints//
GAMMA_HX(i,j,k)  upper bound heat load for match (i,j)
GAMMA_HU(j)      upper bound heat load for hot utility
GAMMA_CU(i)      upper bound heat load for cold utility

TAU_HX(i,j,k)   upper bound of temperature difference for heat exchanger
TAU_HUL(j)      upper bound of temperature difference for left side of hot
utility exchanger
TAU_HUR(j)      upper bound of temperature difference for right side of hot
utility exchanger
TAU_CUL(i)      upper bound of temperature difference for left side pf cold
utility exchanger
TAU_CUR(i)      upper bound of temperature difference for right side of cold
utility exchanger

//parameter for answer verification//
z1(i,j,k)       correct existence of match(i,j) at stage k
zhu1(j)         correct existence of hot utility for cold stream j
zcu1(i)         correct existence of cold utility for hot stream i

dt1(i,j,k)      correct temperature difference(C) for match(i,j) at location k
dthul1(j)       correct temperature difference(C) for left side of hot utility ex
changer
dthur1(j)       correct temperature difference(C) for right side of hot utility ex
changer

```

dtcul1(i) correct temperature difference(C) for left side of cold utility exchanger  
 dtcur1(i) correct temperature difference(C) for right side of cold utility exchanger  
  
 LMTD1(i,j,k) correct log mean temperature difference of match(i,j) at stage k  
 LMTDHU1(j) correct log mean temperature difference of hot utility exchanger for cold stream j  
 LMTDCU1(i) correct log mean temperature difference of cold utility exchanger for cold stream i  
  
 AREAHX1(i,j,k) correct area of heat exchanger of match(i,j) at stage k  
 AREAHU1(j) correct area of hot utility exchanger of cold stream j  
 AREACU1(i) correct area of cold utility exchanger of hot stream i  
  
 Cost\_fix1 correct fixed cost  
 Cost\_areal correct area cost  
 Cost\_utility1 correct utility cost  
  
 TAC1 correct total annualized cost  
  
 TOT\_AREA total area of heat exchangers including utility exchangers  
 TOT\_HU total hot utility  
 TOT\_CU total cold utility  
 ;

//Overall heat transfer coefficient calculations//

$U(i,j) = 1/(1/HH(i)+1/HC(j));$   
 $UHU(j) = 1/(1/HC(j)+1/HHU);$   
 $UCU(i) = 1/(1/HH(i)+1/HCU);$

VARIABLES

th(i,k) temperature(C) of hot streams i at location k  
 tc(j,k) temperature(C) of cold streams j at location k  
  
 q(i,j,k) heat load(kW) of match(i,j) at stage k  
 qhu(j) heat load(kW) of hot utility for cold stream j  
 qcu(i) heat load(kW) of cold utility for hot stream i  
  
 z(i,j,k) existence of match(i,j) at stage k  
 zhu(j) existence of hot utility for cold stream j  
 zcu(i) existence of cold utility for hot stream i  
  
 dt(i,j,k) temperature difference(C) for match(i,j) at location k  
 dthul(j) temperature difference(C) for left side of hot utility exchanger  
 dthur(j) temperature difference(C) for right side of hot utility exchanger  
 dtcul(i) temperature difference(C) for left side of cold utility exchanger



dcur(i) temperature difference(C) for right side of cold utility exchanger

LMTD(i,j,k) log mean temperature difference of match(i,j) at stage k

LMTDHU(j) log mean temperature difference of hot utility exchanger for cold stream j

LMTDCU(i) log mean temperature difference of cold utility exchanger for cold stream i

AREA(i,j,k) area of heat exchanger of match(i,j) at stage k

AREAHU(j) area of hot utility exchanger of cold stream j

AREACU(i) area of cold utility exchanger of hot stream i

Cost\_fix fixed cost

Cost\_area area cost

Cost\_utility utility cost

TAC total annualized cost

;

POSITIVE VARIABLES q(i,j,k), qhu(j), qcu(i),  
dt(i,j,k), dthul(j), dthur(j), dtcul(i), dcur(i),  
LMTD(i,j,k),LMTDHU(j),LMTDCU(i),  
AREA(i,j,k),AREAHU(j),AREACU(i)

;

BINARY VARIABLES z(i,j,k), zhu(j), zcu(i) ;

//variable bounding//

th.up(i,k) = THIN(i);

th.lo(i,k) = THOUT(i);

tc.up(j,k) = TCOUT(j);

tc.lo(j,k) = TCIN(j);

q.up(i,j,k)\$stage(k) = max(min( FCPH(i)\*(th.up(i,k)-  
max(th.lo(i,k+1),tc.lo(j,k+1)+EMAT)) , FCPC(j)\*(min(th.up(i,k)-  
EMAT,tc.up(j,k))-tc.lo(j,k+1)) ) , 0)\$ ( (th.up(i,k)-tc.lo(j,k) >= EMAT) and  
(th.up(i,k+1)-tc.lo(j,k+1) >= EMAT)) +0\$( (th.up(i,k)-tc.lo(j,k) < EMAT) or  
(th.up(i,k+1)-tc.lo(j,k+1) < EMAT)) ;

qhu.up(j) = max( FCPC(j)\*(min(THUIN(j)-EMAT,TCOUT(j))-  
tc.lo(j,'K1')) , 0)\$((THUIN(j)-TCOUT(j) >= EMAT) and (THUOUT(j)-  
tc.lo(j,'K1') >= EMAT)) +0\$( (THUIN(j)-TCOUT(j) < EMAT) or (THUOUT(j)-  
tc.lo(j,'K1') < EMAT)) ;

$qcu.up(i) = \max(FCPH(i)*(th.up(i,'KL') - \max(THOUT(i), TCUIN(i) + EMAT)), 0) * (th.up(i,'KL') - TCUOUT(i) \geq EMAT)$   
 $and (THOUT(i) - TCUIN(i) \geq EMAT) + 0 * (th.up(i,'KL') - TCUOUT(i) < EMAT) or$   
 $(THOUT(i) - TCUIN(i) < EMAT);$

$z.up(i,j,k) \$stage(k) = 0 * (q.up(i,j,k) = 0) + 1 * (q.up(i,j,k) \neq 0);$   
 $zhu.up(j) = 0 * (qhu.up(j) = 0) + 1 * (qhu.up(j) \neq 0);$   
 $zcu.up(i) = 0 * (qcu.up(i) = 0) + 1 * (qcu.up(i) \neq 0);$

$dt.up(i,j,k) = \max(EMAT, (th.up(i,k) - tc.lo(j,k)));$   
 $dt.lo(i,j,k) = EMAT;$   
 $dthul.up(j) = \max(EMAT, THUIN(j) - TCOUT(j));$   
 $dthul.lo(j) = EMAT;$   
 $dthur.up(j) = \max(EMAT, THUOUT(j) - tc.lo(j,'K1'));$   
 $dthur.lo(j) = EMAT;$   
 $dcul.up(i) = \max(EMAT, th.up(i,'KL') - TCUOUT(i));$   
 $dcul.lo(i) = EMAT;$   
 $dcur.up(i) = \max(EMAT, THOUT(i) - TCUIN(i));$   
 $dcur.lo(i) = EMAT;$

$LMTD.up(i,j,k) \$stage(k) =$   
 $(dt.up(i,j,k) * dt.up(i,j,k+1) * (dt.up(i,j,k) + dt.up(i,j,k+1)) / 2) ** (1/3);$   
 $LMTD.lo(i,j,k) \$stage(k) =$   
 $(dt.lo(i,j,k) * dt.lo(i,j,k+1) * (dt.lo(i,j,k) + dt.lo(i,j,k+1)) / 2) ** (1/3);$   
 $LMTDHU.up(j) =$   
 $(dthur.up(j) * dthul.up(j) * (dthur.up(j) + dthul.up(j)) / 2) ** (1/3);$   
 $LMTDHU.lo(j) =$   
 $(dthur.lo(j) * dthul.lo(j) * (dthur.lo(j) + dthul.lo(j)) / 2) ** (1/3);$   
 $LMTDCU.up(i) =$   
 $(dcul.up(i) * dcur.up(i) * (dcul.up(i) + dcur.up(i)) / 2) ** (1/3);$   
 $LMTDCU.lo(i) =$   
 $(dcul.lo(i) * dcur.lo(i) * (dcul.lo(i) + dcur.lo(i)) / 2) ** (1/3);$

$AREA.up(i,j,k) \$stage(k) = q.up(i,j,k) / LMTD.lo(i,j,k) / U(i,j);$   
 $AREAHU.up(j) = qhu.up(j) / LMTDHU.lo(j) / UHU(j);$   
 $AREACU.up(i) = qcu.up(i) / LMTDCU.lo(i) / UCU(i);$

//Assign bounding to pamaters in logical constraint//

$GAMMA\_HX(i,j,k) = q.up(i,j,k);$   
 $GAMMA\_HU(j) = qhu.up(j);$   
 $GAMMA\_CU(i) = qcu.up(i);$

$TAU\_HX(i,j,k) = -th.lo(i,k) + tc.up(j,k) + dt.lo(i,j,k);$   
 $TAU\_HUL(j) = -THUIN(j) + TCOUT(j) + dthul.lo(j);$   
 $TAU\_HUR(j) = -THUOUT(j) + tc.up(j,'K1') + dthur.lo(j);$   
 $TAU\_CUL(i) = -th.lo(i,'KL') + TCUOUT(i) + dcul.lo(i);$   
 $TAU\_CUR(i) = -THOUT(i) + TCUIN(i) + dcur.lo(i);$

```
//Last stage forcing bound//
q.fx(i,j,'KL') =0;
z.fx(i,j,'KL') =0;
LMTD.fx(i,j,'KL') =0;
AREA.fx(i,j,'KL') =0;
```

## EQUATIONS

```
OVERALL_H(i)    overall energy balance of hot stream i
OVERALL_C(j)    overall energy balance of cold stream j

EBAL_H(i,k)     energy balance of hot stream i in stage k
EBAL_C(j,k)     energy balance of cold stream j in stage k

TIN_H(i)        assignment inlet temperature of hot stream i
TIN_C(j)        assignment inlet temperature of cold stream j

MONOT_H(i,k)    monotonic in temperature of hot stream i at location k
MONOT_C(j,k)    monotonic in temperature of cold stream j at location k
MONOT_HU(j)     monotonic in outlet temperature of cold stream j
MONOT_CU(i)     monotonic in outlet temperature of hot stream i

EBAL_HU(j)      energy balance of hot utility of cold stream j
EBAL_CU(i)      energy balance of cold utility of hot stream i

LOGIC_HX(i,j,k) logical constraint to define z of match(i,j) at stage k
LOGIC_HU(j)     logical constraint to define zhu of cold stream j at stage k
LOGIC_CU(i)     logical constraint to define zcu of hot stream i at stage k

DTFEAS_HXL(i,j,k) temperature feasibility of heat exchanger of match(i,j)
                  at location k
DTFEAS_HXR(i,j,k) temperature feasibility of heat exchanger of match(i,j)
                  at location k+1
DTFEAS_HUL(j)   temperature feasibility of hot utility of outlet cold
                  stream j
DTFEAS_HUR(j)   temperature feasibility of hot utility of inlet cold stream j
DTFEAS_CUL(i)   temperature feasibility of cold utility of inlet hot stream i
DTFEAS_CUR(i)   temperature feasibility of cold utility of outlet hot stream i

LOGMTD(i,j,k)   log mean temperature of match(i,j) at stage k
LOGMTDHU(j)     log mean temperature of hot utility exchanger
LOGMTDCU(i)     log mean temperature of cold utility exchanger

A_HX(i,j,k)     area of heat exchanger of match(i,j) at stage k
A_HU(j)         area of hot utility exchanger of cold stream j
A_CU(i)         area of cold utility exchanger of hot stream i
```



```

LOGMTDHU(j)      .. LMTDHU(j) =e= (dthur(j) *dthul(j) *(dthur(j)
                  +dthul(j)) /2)**(1/3);
LOGMTDCU(i)      .. LMTDCU(i) =e= (dteul(i) *dteur(i) *(dteul(i)
                  +dteur(i)) /2)**(1/3);

A_HX(i,j,k)$stage(k) .. AREA(i,j,k) *LMTD(i,j,k)*U(i,j) =e= q(i,j,k);
A_HU(j)          .. AREAHU(j) *LMTDHU(j) *UHU(j) =e= qhu(j);
A_CU(i)          .. AREACU(i) *LMTDCU(i) *UCU(i) =e= qcu(i);

FIXCOST          .. cost_fix =e= AF*(sum((i,j,k)$stage(k),CF*z(i,j,k)) +
                  sum(j,CF*zhu(j)) + sum(i,CF*zcu(i)));
AREACOST         .. cost_area =e=
                  AF*(sum((i,j,k)$stage(k),CA*AREA(i,j,k)))
                  + AF*(sum(j,CA*AREAHU(j)))
                  + AF*(sum(i,CA*AREACU(i)));
UTILITYCOST      .. cost_utility =e= sum(j,CHU*qhu(j)) +
                  sum(i,CCU*qcu(i));

OBJ              .. TAC =e= cost_fix + cost_area + cost_utility;

model STAGEMODEL_SINGLEPERIOD /all/;

option iterlim=1e9;
option domlim=0;
option reslim=1e8;
STAGEMODEL_SINGLEPERIOD.optfile=0;

solve STAGEMODEL_SINGLEPERIOD using MINLP minimizing TAC;

display th.l,tc.l,
        z.l,zhu.l,zcu.l,
        q.l,qhu.l,qcu.l,
        AREA.l,AREAHU.l,AREACU.l,
        dt.l,dthur.l,dthul.l,dteul.l,dteur.l,
        LMTD.l,
        TAC.l,
        TAU_HX,
        q.up,q.lo,qhu.up,qhu.lo,qcu.up,qcu.lo,
        dt.up,dt.lo,dthul.lo,dthul.up, dthur.lo,dthur.up, dteul.lo,dteul.up,
        dteur.lo,dteur.up,
        cost_fix.l, cost_area.l, cost_utility.l;

```

## Appendix B Source Code of Models for HEN Adaptation

The following text is source code which is entered in GAMS for each model used in HEN adaptation step. Please note that this is just an example for only one case.

### B1 Model A

#### SETS

```

I hot streams          /I1*I3/
J cold streams         /J1*J4/
K index of stage or location /K1*K4,KL/ //last number is no. of stages

```

```

stage(k)              all stages
HEN(i,j,k)            define where HX exists
HEN_HOT(i,k)          define where HX exists 2 dimensions for hot streams
HEN_COLD(j,k)         define where HX exists 2 dimensions for cold streams
HU(j)                 define where HU exists
HUNEW_HU(j)           define where HU could have in cold stream
HUNEW_CU(j)           define where CU could have in cold stream
CU(i)                 define where CU exists
;

```

```
//dynamic set for stage pointer
```

```

stage(k) = yes;
stage('KL') = no;

```

```
//dynamic set for existing HEN// <---- To fix topology
```

```
HEN(i,j,k) = no;
```

```
TABLE Z_OLD(i,j,k) Existing HX from original HEN of each period
```

	K1	K2	K3	K4
I1.J1	1.000	1.000	1.000	
I1.J2			1.000	1.000
I1.J3		1.000		
I3.J1		1.000	1.000	
I3.J4	1.000			

```

;

```

```
loop((i,j,k)$(Z_OLD(i,j,k)=1), HEN(i,j,k) = yes);
```

```
//dynamic set for existing Utility exchanger// <---- To fix topology
```

```
//hot utility
```

```

HU(j) = no;
PARAMETER ZHU_OLD(j) Existing HU from original HEN of each period
/J3 1.000/;
loop(j$(ZHU_OLD(j)=1), HU(j) = yes);
HUNEW_HU('J1') = yes;
HUNEW_HU('J2') = yes;
HUNEW_CU('J4') = yes;
//cold utility
CU(i) = no;
PARAMETER ZCU_OLD(i) Existing CU from original HEN of each period
/I1 1.000, I2 1.000, I3 1.000/;
loop(i$(ZCU_OLD(i)=1), CU(i) = yes);

//define dynamic set for existing HEN but only 2 dimensions (for hot and cold)//
HEN_HOT(i,k) = no;
HEN_COLD(j,k) = no;
loop((i,j,k)$(HEN(i,j,k)), HEN_HOT(i,k) = yes);
loop((i,j,k)$(HEN(i,j,k)), HEN_COLD(j,k) = yes);

```

## SCALARS

```

//Cost//
CA      per unit cost of heat exchanger area($ per unit)  /641.7/
B       exponent for area cost(dimensionless)             /1/
CF      fixed cost of heat exchanger($ per unit)         /8333.3/

CHU     per unit cost of hot utility($ per kW)            /115.2/
CCU     fixed cost of heat exchanger($ per kW)           /1.3/

AF      annualisation factor                              /0.2/

//other//
EMAT    exchanger minimum approach temperature(C)        /5/

HHU     heat transfer coefficient of hot utility(kW|(m2.C)) /2/
HCU     heat transfer coefficient of cold utility(kW|(m2.C)) /1/

TAU     tau /500/
GAMMA   gamma /1e6/
;

```

## PARAMETERS

```

//Hot Streams//
THIN(i) inlet temperature of hot streams(C)
/ I1 393

```

```

        I2  160
        I3  354
    /
    THOUT(i) outlet temperature of hot streams(C)
    /
        I1  60
        I2  40
        I3  60
    /
//Cold Streams//
    TCIN(j) inlet temperature of cold streams(C)
    /
        J1  72
        J2  62
        J3  220
        J4  253
    /
    TCOUT(j) outlet temperature of cold streams(C)
    /
        J1  356
        J2  210
        J3  370
        J4  284
    /
//Heat Capacity Flowrates//
    FCPH(i) heat capacity flowrates fo hot streams(C)
    /
        I1  201.6
        I2  185.1
        I3  137.4
    /
    FCPC(j) heat capacity flowrates fo cold streams(C)
    /
        J1  209.4
        J2  141.6
        J3  176.4
        J4  294.4
    /
//Utility//
    THUIN(j) inlet temperature of hot utility(C)
    /
        J1  400
        J2  400
        J3  400
        J4  15
    /
    THUOUT(j) outlet temperature of hot utility(C)
    /
        J1  399
        J2  399
        J3  399
        J4  20
    /
    TCUIN(i) inlet temperature of cold utility(C)

```



```

/   I1  15
    I2  15
    I3  15
/

```

TCUOUT(i) outlet temperature of cold utility(C)

```

/   I1  20
    I2  20
    I3  20
/

```

//Heat transfer coefficient//

HH(i) heat capacity flowrates of hot streams(kW|(m2.C))

```

/   I1  2
    I2  2
    I3  2
/

```

HC(j) heat capacity flowrates of cold streams(kW|(m2.C))

```

/   J1  1.5
    J2  1.5
    J3  2
    J4  2
/

```

//overall heat transfer coefficient//

U(i,j) Overall heat transfer coefficient for match(i,j)  
 UHU(j) Overall heat transfer coefficient for cold stream(j) and hot utility  
 UCU(i) Overall heat transfer coefficient for hot stream(i) and cold utility

//upper bound for logical constraints//

GAMMA\_HX(i,j,k) upper bound heat load for match (i,j)  
 GAMMA\_HU(j) upper bound heat load for hot utility  
 GAMMA\_CU(i) upper bound heat load for cold utility

TAU\_HX(i,j,k) upper bound of temperature difference for heat exchanger  
 TAU\_HUL(j) upper bound of temperature difference for left side of hot utility exchanger  
 TAU\_HUR(j) upper bound of temperature difference for right side of hot utility exchanger  
 TAU\_CUL(i) upper bound of temperature difference for left side pf cold utility exchanger  
 TAU\_CUR(i) upper bound of temperature difference for right side of cold utility exchanger

//Old value of variables from original HEN//

//Area//

TABLE AREA\_OLD(i,j,k) old area from original HEN of each period

	K1	K2	K3	K4
I1.J1	680.055	166.126	751.970	
I1.J2		1290.040	132.794	
I1.J3		597.190		
I3.J1		356.123	1470.846	
I3.J4	324.859			

;

PARAMETERS

AREAHU\_OLD(j) old area of HU from original HEN

/J3 256.025/

AREACU\_OLD(i) old area of CU from original HEN

/I1 117.036, I2 541.396, I3 97.762/

;

//Temperature//

TABLE TH\_OLD(i,k) old hot temperature from original HEN

	K1	K2	K3	K4	KL
I1	406.000	293.498	231.178	88.555	79.812
I2	160.000	160.000	160.000	160.000	160.000
I3	362.000	268.540	234.038	86.252	86.252

;

TABLE TC\_OLD(j,k) old cold temperature from original HEN

	K1	K2	K3	K4	KL
J1	365.000	255.334	216.175	72.000	72.000
J2	210.000	210.000	210.000	74.710	62.000
J3	272.717	272.717	220.000	220.000	220.000
J4	290.000	250.000	250.000	250.000	250.000

;

//Heat load//

TABLE Q\_OLD(i,j,k) old heat load from original HEN

	K1	K2	K3	K4
I1.J1	23062.852	3528.959	10162.028	
I1.J2		19075.844	1792.156	
I1.J3		9246.623		
I3.J1		4706.050	20158.011	
I3.J4	12748.000			

;

## PARAMETERS

QHU\_OLD(j) old heat load of HU from original HEN

/J3 17063.377/

QCU\_OLD(i) old heat load of CU from original HEN

/I1 4061.538, I2 23856.000, I3 3580.739/

;

## //Temperature Difference//

TABLE DT\_OLD(i,j,k) old temperature differene from original HEN

K1 K2 K3 K4 KL

I1.J1 41.000 38.165 15.003 16.555

I1.J2 21.178 13.844 17.812

I1.J3 20.781 11.178

I3.J1 13.206 17.863 14.252

I3.J4 72.000 18.540

;

## PARAMETERS

DTHUL\_OLD(j) old left-side temperature differene of HU from original HEN

/J3 30.000/

DTHUR\_OLD(j) old right-side temperature differene of HU from original HEN

/J3 126.283/

DTCUL\_OLD(i) old left-side temperature differene of CU from original HEN

/I1 59.812, I2 140.000, I3 66.252/

DTCUR\_OLD(i) old right-side temperature differene of CU from original HEN

/I1 45.000, I2 25.000, I3 45.000/

;

## //Log Mean Temperature Difference//

TABLE LMTD\_OLD(i,j,k) old log mean temperature from original HEN

K1 K2 K3 K4

I1.J1 39.565 24.783 15.766

I1.J2 17.252 15.745

I1.J3 15.484

I3.J1 15.417 15.989

I3.J4 39.242

;

## PARAMETERS

LMTDHU\_OLD(j) old log mean temperature of HU from original HEN

/J3 66.647/

LMTDCU\_OLD(i) old log mean temperature of CU from original HEN

/I1 52.055, I2 66.096, I3 54.941/

;

//Overall heat transfer coefficient calculations//

$$U(i,j) = 1/(1/HH(i)+1/HC(j));$$

$$UHU(j) \$(HU(j) \text{ or } HUNEW\_HU(j)) = 1/(1/HC(j)+1/HHU);$$

$$UHU(j) \$(HUNEW\_CU(j) = 1/(1/HC(j)+1/HCU); \quad //\text{suppose it is cold utility}$$

$$UCU(i) = 1/(1/HH(i)+1/HCU);$$

#### VARIABLES

th(i,k) temperature(C) of hot streams i at location k

tc(j,k) temperature(C) of cold streams j at location k

q(i,j,k) heat load(kW) of match(i,j) at stage k

qhu(j) heat load(kW) of hot utility for cold stream j

qcu(i) heat load(kW) of cold utility for hot stream i

zhu(j) addition of hot utility

zcu(i) addition of cold utility

dt(i,j,k) temperature difference(C) for match(i,j) at location k

dthul(j) temperature difference(C) for left side of hot utility exchanger

dthur(j) temperature difference(C) for right side of hot utility exchanger

dtcu(i) temperature difference(C) for left side of cold utility exchanger

dtdcu(i) temperature difference(C) for right side of cold utility exchanger

lmt(i,j,k) log mean temperature difference of match(i,j) at stage k

lmtdhu(j) log mean temperature difference of hot utility exchanger for cold stream j

lmtd(i) log mean temperature difference of cold utility exchanger for cold stream i

area(i,j,k) area of heat exchanger of match(i,j) at stage k

areahu(j) area of hot utility exchanger of cold stream j

areacu(i) area of cold utility exchanger of hot stream i

areahu\_add(j) additional area of hot utility exchanger of cold stream j

areacu\_add(i) additional area of cold utility exchanger of hot stream i

Cost\_fix\_add additional fixed cost from new utility

Cost\_area\_add area cost

Cost\_utility utility cost

tot\_area\_add total additional cost

POSITIVE VARIABLES q(i,j,k), qcu(i), // qhu(j)

dt(i,j,k), dthul(j), dthur(j), dtcu(i), dtcu(i),

lmt(i,j,k), lmtdhu(j), lmtd(i),

areahu(j), areacu(i),

areahu\_add(j), areacu\_add(i);

BINARY VARIABLES    zhu(j), zcu(i);

//variable bounding//

th.up(i,k) = THIN(i);  
th.lo(i,k) = THOUT(i);  
tc.up(j,k)\$ (HU(j) or HUNEW\_HU(j)) = TCOUT(j);    //bound only exist HU  
tc.lo(j,k) = TCIN(j);

q.up(i,j,k)\$stage(k) = max(min( FCPH(i)\*(th.up(i,k)-  
max(th.lo(i,k+1),tc.lo(j,k+1)+EMAT)) , FCPC(j)\*(min(th.up(i,k)-  
EMAT,tc.up(j,k))-tc.lo(j,k+1)) ) , 0)\$ ( th.up(i,k)-tc.lo(j,k) >= EMAT) and  
(th.up(i,k+1)-tc.lo(j,k+1) >= EMAT))    +0\$( th.up(i,k)-tc.lo(j,k) < EMAT) or  
(th.up(i,k+1)-tc.lo(j,k+1) < EMAT)) ;

//only for HU(j) that exist hot utility

qhu.up(j)\$ (HU(j) or HUNEW\_HU(j))    =  
max( FCPC(j)\*(min(THUIN(j)-EMAT,TCOUT(j))-tc.lo(j,'K1')) , 0)\$((THUIN(j)-  
TCOUT(j) >= EMAT) and (THUOUT(j)-tc.lo(j,'K1') >= EMAT)) +0\$( (THUIN(j)-  
TCOUT(j) < EMAT) or (THUOUT(j)-tc.lo(j,'K1') < EMAT)) ;

qhu.lo(j)\$ (HU(j) or HUNEW\_HU(j)) = 0;  
qcu.up(i)    = max( FCPH(i)\*(th.up(i,'KL')-  
max(THOUT(i),TCUIN(i)+EMAT)) , 0)\$ ( th.up(i,'KL')-TCUOUT(i) >= EMAT  
and (THOUT(i)-TCUIN(i) >= EMAT)) +0\$( th.up(i,'KL')-TCUOUT(i) < EMAT) or  
(THOUT(i)-TCUIN(i) < EMAT)) ;

qcu.lo(i) = 0;

dt.up(i,j,k) = max(EMAT,(th.up(i,k)-tc.lo(j,k)));  
dt.lo(i,j,k) = EMAT;  
dthul.up(j)\$ (HU(j) or HUNEW\_HU(j)) = max(EMAT,THUIN(j)-TCOUT(j));  
//bound only exist HU  
dthul.lo(j) = EMAT;  
dthur.up(j)\$ (HU(j) or HUNEW\_HU(j)) = max(EMAT,THUOUT(j)-  
tc.lo(j,'K1'));    //bound only exist HU  
dthur.lo(j) = EMAT;  
dteul.up(i) = max(EMAT,th.up(i,'KL')-TCUOUT(i));  
dteul.lo(i) = EMAT;  
dteur.up(i) = max(EMAT,THOUT(i)-TCUIN(i));  
dteur.lo(i) = EMAT;

lmtd.up(i,j,k)\$stage(k) =  
(dt.up(i,j,k)\*dt.up(i,j,k+1)\*(dt.up(i,j,k)+dt.up(i,j,k+1))/2)\*\*(1/3);  
lmtd.lo(i,j,k)\$stage(k) =  
(dt.lo(i,j,k)\*dt.lo(i,j,k+1)\*(dt.lo(i,j,k)+dt.lo(i,j,k+1))/2)\*\*(1/3);

```

lmtdhu.up(j)$ (HU(j) or HUNEW_HU(j)) =
(dthur.up(j)*dthul.up(j)*(dthur.up(j)+dthul.up(j))/2)**(1/3); //bound only exist HU
lmtdhu.lo(j) = (dthur.lo(j)*dthul.lo(j)*(dthur.lo(j)+dthul.lo(j))/2)**(1/3);
lmtdhu.up(i) = (dthul.up(i)*dthul.up(i)*(dthul.up(i)+dthul.up(i))/2)**(1/3);
lmtdhu.lo(i) = (dthul.lo(i)*dthul.lo(i)*(dthul.lo(i)+dthul.lo(i))/2)**(1/3);

area.up(i,j,k)$stage(k) = q.up(i,j,k)/lmtd.lo(i,j,k)/U(i,j);
areahu.up(j)$ (HU(j) or HUNEW_HU(j)) = qhu.up(j)/lmtdhu.lo(j)/UHU(j);
//bound only exist HU
areacu.up(i) = qcu.up(i)/lmtdhu.lo(i)/UCU(i);

//Assign bounding to pamaters in logical constraint//
GAMMA_HX(i,j,k) = q.up(i,j,k);
GAMMA_HU(j)$ (HU(j) or HUNEW_HU(j)) = qhu.up(j);
GAMMA_HU(j)$HUNEW_CU(j) = GAMMA;
GAMMA_CU(i) = qcu.up(i);

TAU_HX(i,j,k) = -th.lo(i,k)+tc.up(j,k)+dt.lo(i,j,k);
TAU_HUL(j)$ (HU(j) or HUNEW_HU(j)) = -THUIN(j)+TCOUT(j)
+dthul.lo(j); //bound only exist HU
TAU_HUL(j)$HUNEW_CU(j) = TAU; //Arbitrary create a value
TAU_HUR(j)$ (HU(j) or HUNEW_HU(j)) = -THUOUT(j)+tc.up(j,'K1')
+dthur.lo(j); //bound only exist HU
TAU_HUR(j)$HUNEW_CU(j) = TAU; //Arbitrary create a value
TAU_CUL(i) = -th.lo(i,'KL')+TCUOUT(i)+dthul.lo(i);
TAU_CUR(i) = -THOUT(i)+TCUIN(i)+dthul.lo(i);

//Last stage forcing bound//
q.fx(i,j,'KL') = 0;
lmtd.fx(i,j,'KL') = 0;
area.fx(i,j,'KL') = 0;

//To force no q, area change where there is no existing HX//
q.fx(i,j,k)$ (not HEN(i,j,k)) = 0;
area.fx(i,j,k)$ (not HEN(i,j,k)) = 0;

//Fix area in the process-process HX//
area.fx(i,j,k)$ (HEN(i,j,k)) = AREA_OLD(i,j,k); //and(not HEN('I3','J3','K1'))

//initial value for variables//
areahu.l(j) = AREA_HU_OLD(j);
areacu.l(i) = AREA_CU_OLD(i);

areahu_add.l(j) = 0;
areacu_add.l(i) = 0;

```

$th.l(i,k) = TH\_OLD(i,k);$   
 $tc.l(j,k) = TC\_OLD(j,k);$   
  
 $q.l(i,j,k) = Q\_OLD(i,j,k);$   
 $qhu.l(j) = QHU\_OLD(j);$   
 $qcu.l(i) = QCU\_OLD(i);$   
  
 $dt.l(i,j,k) = DT\_OLD(i,j,k);$   
 $dthul.l(j) = DTHUL\_OLD(j);$   
 $dthur.l(j) = DTHUR\_OLD(j);$   
 $dtcul.l(i) = DTCUL\_OLD(i);$   
 $dteur.l(i) = DTEUR\_OLD(i);$   
  
 $lmtl.l(i,j,k) = LMTD\_OLD(i,j,k);$   
 $lmtdhu.l(j) = LMTDHU\_OLD(j);$   
 $lmtdcu.l(i) = LMTDCU\_OLD(i);$   
  
 $zhu.l(j)\$(not HU(j)) = 0;$   
 $zcu.l(i)\$(not CU(i)) = 0;$

## EQUATIONS

OVERALL\_H(i) overall energy balance of hot stream i  
OVERALL\_C(j) overall energy balance of cold stream j  
  
EBAL\_H(i,k) energy balance of hot stream i in stage k  
EBAL\_C(j,k) energy balance of cold stream j in stage k  
  
TIN\_H(i) assignment inlet temperature of hot stream i  
TIN\_C(j) assignment inlet temperature of cold stream j  
  
MONOT\_H(i,k) monotonic in temperature of hot stream i at location k  
MONOT\_C(j,k) monotonic in temperature of cold stream j at location k  
MONOT\_HNOT(i,k) monotonic in temperature of hot stream i at location k  
if no HX  
MONOT\_CNOT(j,k) monotonic in temperature of cold stream j at  
location k if no HX  
  
MONOT\_HU(j) monotonic in outlet temperature of cold stream j  
MONOT\_CU(i) monotonic in outlet temperature of hot stream i  
  
EBAL\_HU(j) energy balance of hot utility of cold stream j  
EBAL\_CU(i) energy balance of cold utility of hot stream i  
EBAL\_HUNEW\_CU(j) energy balance of hot utility of cold stream j  
EBAL\_CUNOT(i) energy balance of cold utility of hot stream i  
  
LOGIC\_HUNEW\_HU(j) logical constraint to define zhu of cold stream j at  
stage k (hot utility)

LOGIC_HUNEW_CU(j)	logical constraint to define zhu of cold stream j at stage k (cold utility)
LOGIC_CU(i)	logical constraint to define zcu of hot stream i at stage k
DTFEAS_HXL(i,j,k)	temperature feasibility of heat exchanger of match(i,j) at location k
DTFEAS_HXR(i,j,k)	temperature feasibility of heat exchanger of match(i,j) at location k+1
DTFEAS_HUL(j)	temperature feasibility of hot utility of outlet cold stream j
DTFEAS_HUR(j)	temperature feasibility of hot utility of inlet cold stream j
DTFEAS_CUL(i)	temperature feasibility of cold utility of inlet hot stream i
DTFEAS_CUR(i)	temperature feasibility of cold utility of outlet hot stream i
DTFEAS_HUL_HUNEW_HU(j)	temperature feasibility of new hot utility of outlet cold stream j
DTFEAS_HUR_HUNEW_HU(j)	temperature feasibility of new hot utility of inlet cold stream j
DTFEAS_HUL_HUNEW_CU(j)	temperature feasibility of new cold utility of outlet cold stream j
DTFEAS_HUR_HUNEW_CU(j)	temperature feasibility of new cold utility of inlet cold stream j
DTFEAS_CULNOT(i)	temperature feasibility of cold utility of inlet hot stream i
DTFEAS_CURNOT(i)	temperature feasibility of cold utility of outlet hot stream i
LOGMTD(i,j,k)	log mean temperature of match(i,j) at stage k
LOGMTDHU(j)	log mean temperature of hot utility exchanger
LOGMTDCU(i)	log mean temperature of cold utility exchanger
ADDIAREA_HU1(j)	additional area needed for hot utility
ADDIAREA_HU2(j)	force ADDAREA_HU > 0
ADDIAREA_CU1(i)	additional area needed for cold utility
ADDIAREA_CU2(i)	force ADDAREA_CU > 0
A_HX(i,j,k)	area of heat exchanger of match(i,j) at stage k
A_HU(j)	area of hot utility exchanger of cold stream j
A_HUNOT(j)	area for cold utility for J1 J2
A_CU(i)	area of cold utility exchanger of hot stream i
OBJ	objective function (total additional area)
OVERALL_H(i)	.. (THIN(i) - THOUT(i)) * FCPH(i) = e = sum((j,k), q(i,j,k)) + qcu(i);



OVERALL\_C(j) .. (TCOUT(j)-TCIN(j)) \*FCPC(j) =e=  
sum((i,k),q(i,j,k))+qhu(j);

EBAL\_H(i,k)\$HEN\_HOT(i,k) .. (th(i,k)-th(i,k+1))\*FCPH(i) =e=  
sum(j,q(i,j,k)); //do only exist HEN

EBAL\_C(j,k)\$HEN\_COLD(j,k) .. (tc(j,k)-tc(j,k+1))\*FCPC(j) =e=  
um(i,q(i,j,k));

TIN\_H(i) .. THIN(i) =e= th(i,'K1');

TIN\_C(j) .. TCIN(j) =e= tc(j,'KL');

MONOT\_H(i,k)\$HEN\_HOT(i,k) .. th(i,k) =g= th(i,k+1); //if HX  
--> monotonic

MONOT\_C(j,k)\$HEN\_COLD(j,k) .. tc(j,k) =g= tc(j,k+1);

MONOT\_HNOT(i,k)\$((not HEN\_HOT(i,k)) and stage(k)) .. th(i,k) =e= th(i,k+1);  
//if no HX --> equal

MONOT\_CNQT(j,k)\$((not HEN\_COLD(j,k)) and stage(k)) .. tc(j,k) =e= tc(j,k+1);

MONOT\_HU(j)\$ (HU(j) or HUNEW\_HU(j)) .. TCOUT(j) =g= tc(j,'K1');  
//if HX --> monotonic

MONOT\_CU(i)\$CU(i) .. th(i,'KL') =g= THOUT(i);

EBAL\_HU(j)\$ (HU(j) or HUNEW\_HU(j)) .. (TCOUT(j) - tc(j,'K1'))\*FCPC(j)  
=e= qhu(j); //do only exist HEN

EBAL\_CU(i)\$CU(i) .. (th(i,'KL') - THOUT(i)) \*FCPH(i) =e= qcu(i);

EBAL\_HUNEW\_CU(j)\$HUNEW\_CU(j) .. (TCOUT(j) - tc(j,'K1'))\*FCPC(j)  
=e= qhu(j);

EBAL\_CUNOT(i)\$ (not CU(i)) .. (th(i,'KL') - THOUT(i)) \*FCPH(i) =e= qcu(i);

LOGIC\_HUNEW\_HU(j)\$HUNEW\_HU(j) .. qhu(j) - GAMMA\_HU(j)  
\*zhu(j) =l= 0;

LOGIC\_HUNEW\_CU(j)\$HUNEW\_CU(j) .. qhu(j) + GAMMA\_HU(j)  
\*zhu(j) =g= 0; //change - to + because qhu = -

LOGIC\_CU(i)\$ (not CU(i)) .. qcu(i) - GAMMA\_CU(i) \*zcu(i) =l= 0;

DTFEAS\_HXL(i,j,k)\$HEN(i,j,k) .. dt(i,j,k) =e= th(i,k) -tc(j,k) ;  
//if exist HEN --> equal

DTFEAS\_HXR(i,j,k)\$HEN(i,j,k) .. dt(i,j,k+1) =e= th(i,k+1) -tc(j,k+1);

DTFEAS\_HUL(j)\$HU(j) .. dthul(j) =e= THUIN(j) -TCOUT(j) ;

DTFEAS\_HUR(j)\$HU(j) .. dthur(j) =e= THUOUT(j) -tc(j,'K1');  
//if exist utility --> equal

DTFEAS\_CUL(i)\$CU(i) .. dtcul(i) =e= th(i,'KL')-TCUOUT(i) ;

DTFEAS\_CUR(i)\$CU(i) .. dtcur(i) =e= THOUT(i) -TCUIN(i) ;

DTFEAS\_HUL\_HUNEW\_HU(j)\$HUNEW\_HU(j) .. dthul(j) =l= THUIN(j) -  
TCOUT(j) +TAU\_HUL(j) \*(1-zhu(j)); //if no utility --> use TAU and binary

DTFEAS\_HUR\_HUNEW\_HU(j)\$HUNEW\_HU(j) .. dthur(j) =l= THUOUT(j)  
-tc(j,'K1')+TAU\_HUR(j) \*(1-zhu(j));

```

DTFEAS_HUL_HUNEW_CU(j)$HUNEW_CU(j) .. dthul(j) =|= TCOUT(j) -
THUIN(j) +TAU_HUL(j) *(1-zhu(j)); //if no utility --> use TAU and binary
DTFEAS_HUR_HUNEW_CU(j)$HUNEW_CU(j) .. dthur(j) =|= tc(j,'K1')
-THUOUT(j) +TAU_HUR(j) *(1-zhu(j));
DTFEAS_CULNOT(i)$ (not CU(i)) .. dtcul(i) =|= th(i,'KL')-TCUOUT(i)
+TAU_CUL(i) *(1-zcu(i));
DTFEAS_CURNOT(i)$ (not CU(i)) .. dtcur(i) =|= THOUT(i) -TCUIN(i)
+TAU_CUR(i) *(1-zcu(i));

```

```

LOGMTD(i,j,k)$HEN(i,j,k) .. lmtd(i,j,k) =e=
(dt(i,j,k)*dt(i,j,k+1)*(dt(i,j,k)+dt(i,j,k+1))/2)**(1/3); //only HEN
LOGMTDHU(j) .. lmtdhu(j) =e= (dthur(j) *dthul(j) *(dthur(j)
+dthul(j)) /2)**(1/3);
LOGMTDCU(i) .. lmtdhu(i) =e= (dtcul(i) *dtcur(i) *(dtcul(i)
+dtcur(i)) /2)**(1/3);

```

```

A_HX(i,j,k)$HEN(i,j,k) .. area(i,j,k) *lmtd(i,j,k)*U(i,j) =e= q(i,j,k); //only HEN
A_HU(j)$ (HU(j) or HUNEW_HU(j)) .. areahu(j) *lmtdhu(j) *UHU(j) =e= qhu(j);
A_HUNOT(j)$HUNEW_CU(j) .. areahu(j) *lmtdhu(j) *UHU(j) =e= -qhu(j);
//qhu = -
A_CU(i) .. areacu(i) *lmtdhu(i) *UCU(i) =e= qcu(i);

```

```

ADDIAREA_HU1(j) .. areahu_add(j) =g= areahu(j) - AREA_HU_OLD(j);
ADDIAREA_HU2(j) .. areahu_add(j) =g= 0;
ADDIAREA_CU1(i) .. areacu_add(i) =g= areacu(i) - AREA_CU_OLD(i);
ADDIAREA_CU2(i) .. areacu_add(i) =g= 0;

```

//Only area penalty

```

OBJ .. TOT_AREA_ADD =e= sum(j,areahu_add(j)) +
sum(i,areacu_add(i));

```

```

model STAGEMODEL_SINGLEPERIOD /all/;

```

```

option iterlim=1e9;
option domlim=0;
option reslim=1e8;
STAGEMODEL_SINGLEPERIOD.optfile=0;

```

```

solve STAGEMODEL_SINGLEPERIOD using MINLP minimizing
TOT_AREA_ADD;

```

```
display th.l,tc.l,  
  q.l,qhu.l,qcu.l,  
  zhu.l, zcu.l,  
  area.l,areahu.l,areacu.l,  
  dt.l,dthul.l,dthur.l,dcul.l,dcur.l,  
  lmtl.l,lmtdhu.l,lmtdcu.l,  
  tot_area_add.l,  
  area.lo,area.up,areahu.lo,areahu.up,areacu.lo,areacu.up,  
  q.up,q.lo,qhu.up,qhu.lo,qcu.up,qcu.lo  
  dt.up,dt.lo,dthul.lo,dthul.up, dthur.lo,dthur.up, dcul.lo,dcul.up,  
  dcur.lo,dcur.up  
  ;
```

**B2 Model B**

## SETS

I hot streams /I1\*I3/  
 J cold streams /J1\*J4/  
 K index of stage or location /K1\*K4,KL/ //last number is no. of stages

stage(k) all stages  
 HEN(i,j,k) define where HX exists  
 HEN\_HOT(i,k) define where HX exists 2 dimensions for hot streams  
 HEN\_COLD(j,k) define where HX exists 2 dimensions for cold streams  
 HU(j) define where HU exists  
 CU(i) define where CU exists

//dynamic set for stage pointer

stage(k) = yes;  
 stage('KL') = no;

//dynamic set for existing HEN// <---- To fix topology

HEN(i,j,k) = no;

TABLE Z\_OLD(i,j,k) Existing HX from original HEN of each period

	K1	K2	K3	K4
I1.J1	1.000	1.000	1.000	
I1.J2			1.000	1.000
I1.J3		1.000		
I3.J1		1.000	1.000	
I3.J4	1.000			

loop((i,j,k)\$(Z\_OLD(i,j,k)=1), HEN(i,j,k) = yes);

//dynamic set for existing Utility exchanger// <---- To fix topology

//hot utility

HU(j) = no;  
 PARAMETER ZHU\_OLD(j) Existing HU from original HEN of each period  
 /J3 1.000/;  
 loop(j\$(ZHU\_OLD(j)=1), HU(j) = yes);

//cold utility

CU(i) = no;

```

PARAMETER ZCU_OLD(i) Existing CU from original HEN of each period
/11 1.000, I2 1.000, I3 1.000/;
loop(i$(ZCU_OLD(i)=1), CU(i) = yes);

```

```
//define dynamic set for existing HEN but only 2 dimensions (for hot and cold)//
```

```

HEN_HOT(i,k) = no;
HEN_COLD(j,k) = no;
loop((i,j,k)$(HEN(i,j,k)), HEN_HOT(i,k) = yes);
loop((i,j,k)$(HEN(i,j,k)), HEN_COLD(j,k) = yes);

```

## SCALARS

```
//Cost//
```

CA	per unit cost of heat exchanger area(\$ per unit)	/641.7/
B	exponent for area cost(dimensionless)	/1/
CF	fixed cost of heat exchanger(\$ per unit)	/8333.3/
CHU	per unit cost of hot utility(\$ per kW)	/115.2/
CCU	per unit cost of cold utility(\$ per kW)	/1.3/
AF	annualisation factor	/0.2/

```
//other//
```

EMAT	exchanger minimum approach temperature(C)	/5/
HHU	heat transfer coefficient of hot utility(kW (m2.C))	/2/
HCU	heat transfer coefficient of cold utility(kW (m2.C))	/1/

## PARAMETERS

```
//Hot Streams//
```

THIN(i)	inlet temperature of hot streams(C)
/ I1	393
I2	160
I3	354

```
/
```

THOUT(i)	outlet temperature of hot streams(C)
/ I1	60
I2	40
I3	60

```
/
```

```
//Cold Streams//
```

TCIN(j)	inlet temperature of cold streams(C)
/ J1	72

```

        J2  62
        J3  220
        J4  253
    /
    TCOUT(j) outlet temperature of cold streams(C)
    /
        J1  356
        J2  210
        J3  370
        J4  284
    /
//Heat Capacity Flowrates//
    FCPH(i) heat capacity flowrates fo hot streams(C)
    /
        I1  201.6
        I2  185.1
        I3  137.4
    /
    FCPC(j) heat capacity flowrates fo cold streams(C)
    /
        J1  209.4
        J2  141.6
        J3  176.4
        J4  294.4
    /
//Utility//
    THUIN(j) inlet temperature of hot utility(C)
    /
        J1  400
        J2  400
        J3  400
        J4  400
    /
    THUOUT(j) outlet temperature of hot utility(C)
    /
        J1  399
        J2  399
        J3  399
        J4  399
    /
    TCUIN(i) inlet temperature of cold utility(C)
    /
        I1  15
        I2  15
        I3  15
    /
    TCUOUT(i) outlet temperature of cold utility(C)
    /
        I1  20
        I2  20
        I3  20
    /
//Heat transfer coefficient//
    HH(i) heat capacity flowrates of hot streams(kW/(m2.C))

```

```

/      I1  2
      I2  2
      I3  2
/
HC(j) heat capacity flowrates of cold streams(kW/(m2.C))
/      J1  1.5
      J2  1.5
      J3  2
      J4  2
/
//overall heat transfer coefficient//
U(i,j)      Overall heat transfer coefficient for match(i,j)
UHU(j)      Overall heat transfer coefficient for cold stream(j) and hot utility
UCU(i)      Overall heat transfer coefficient for hot stream(i) and cold utility

//upper bound for logical constraints//
- GAMMA_HX(i,j,k)  upper bound heat load for match (i,j)
  GAMMA_HU(j)      upper bound heat load for hot utility
  GAMMA_CU(i)      upper bound heat load for cold utility

TAU_HX(i,j,k)  upper bound of temperature difference for heat exchanger
TAU_HUL(j)     upper bound of temperature difference for left side of hot
                utility exchanger
TAU_HUR(j)     upper bound of temperature difference for right side of hot
                utility exchanger
TAU_CUL(i)     upper bound of temperature difference for left side pf cold
                utility exchanger
TAU_CUR(i)     upper bound of temperature difference for right side of cold
                utility exchanger
;

//Old value of variables from original HEN//

//Area//
TABLE AREA_OLD(i,j,k) old area from original HEN of each period
      K1      K2      K3      K4

I1.J1  680.055  166.126  751.970
I1.J2           1290.040  132.794
I1.J3           597.190
I3.J1           356.123  1470.846
I3.J4  324.859
;

PARAMETERS
AREAHU_OLD(j) old area of HU from original HEN
/J3 256.025/

```

AREACU\_OLD(i) old area of CU from original HEN  
 /I1 117.036, I2 541.396, I3 97.762/  
 ;

//Temperature//

TABLE TH\_OLD(i,k) old hot temperature from original HEN  
 K1 K2 K3 K4 KL

I1	406.000	293.498	231.178	88.555	79.812
I2	160.000	160.000	160.000	160.000	160.000
I3	362.000	268.540	234.038	86.252	86.252

TABLE TC\_OLD(j,k) old cold temperature from original HEN  
 K1 K2 K3 K4 KL

J1	365.000	255.334	216.175	72.000	72.000
J2	210.000	210.000	210.000	74.710	62.000
J3	272.717	272.717	220.000	220.000	220.000
J4	290.000	250.000	250.000	250.000	250.000

//Heat load//

TABLE Q\_OLD(i,j,k) old heat load from original HEN  
 K1 K2 K3 K4

I1.J1	23062.852	3528.959	10162.028	
I1.J2		19075.844	1792.156	
I1.J3		9246.623		
I3.J1		4706.050	20158.011	
I3.J4	12748.000			

PARAMETERS

QHU\_OLD(j) old heat load of HU from original HEN  
 /J3 17063.377/

QCU\_OLD(i) old heat load of CU from original HEN  
 /I1 4061.538, I2 23856.000, I3 3580.739/  
 ;

//Temperature Difference//

TABLE DT\_OLD(i,j,k) old temperature difference from original HEN  
 K1 K2 K3 K4 KL

I1.J1	41.000	38.165	15.003	16.555
I1.J2			21.178	13.844
I1.J3		20.781	11.178	
I3.J1		13.206	17.863	14.252



I3.J4 72.000 18.540

;

PARAMETERS

DTHUL\_OLD(j) old left-side temperature difference of HU from original HEN  
/J3 30.000/

DTHUR\_OLD(j) old right-side temperature difference of HU from original HEN  
/J3 126.283/

DTCUL\_OLD(i) old left-side temperature difference of CU from original HEN  
/I1 59.812, I2 140.000, I3 66.252/

DTCUR\_OLD(i) old right-side temperature difference of CU from original HEN  
/I1 45.000, I2 25.000, I3 45.000/

;

//Log Mean Temperature Difference//

TABLE LMTD\_OLD(i,j,k) old log mean temperature from original HEN  
K1 K2 K3 K4

I1.J1	39.565	24.783	15.766	
I1.J2			17.252	15.745
I1.J3		15.484		
I3.J1		15.417	15.989	
I3.J4	39.242			

;

PARAMETERS

LMTDHU\_OLD(j) old log mean temperature of HU from original HEN  
/J3 66.647/

LMTDCU\_OLD(i) old log mean temperature of CU from original HEN  
/I1 52.055, I2 66.096, I3 54.941/

;

//Overall heat transfer coefficient calculations//

$U(i,j) = 1/(1/HH(i)+1/HC(j));$

$UHU(j) = 1/(1/HC(j)+1/HHU);$

$UCU(i) = 1/(1/HH(i)+1/HCU);$

VARIABLES

th(i,k) temperature(C) of hot streams i at location k  
tc(j,k) temperature(C) of cold streams j at location k

q(i,j,k) heat load(kW) of match(i,j) at stage k  
qhu(j) heat load(kW) of hot utility for cold stream j  
qcu(i) heat load(kW) of cold utility for hot stream i

dt(i,j,k) temperature difference(C) for match(i,j) at location k

dthul(j)      temperature difference(C) for left side of hot utility exchanger  
 dthur(j)      temperature difference(C) for right side of hot utility exchanger  
 dtcul(i)      temperature difference(C) for left side of cold utility exchanger  
 dtcur(i)      temperature difference(C) for right side of cold utility exchanger  
  
 lmtld(i,j,k)    log mean temperature difference of match(i,j) at stage k  
 lmtldhu(j)     log mean temperature difference of hot utility exchanger for cold  
                   stream j  
 lmtldcu(i)     log mean temperature difference of cold utility exchanger for cold  
                   stream i  
  
 area(i,j,k)     area of heat exchanger of match(i,j) at stage k  
 areahu(j)      area of hot utility exchanger of cold stream j  
 areacu(i)      area of cold utility exchanger of hot stream i

tot\_lsqr\_error    total least square error

POSITIVE VARIABLES    q(i,j,k), qhu(j), qcu(i),  
                           dt(i,j,k), dthul(j), dthur(j), dtcul(i), dtcur(i),  
                           lmtld(i,j,k), lmtldhu(j), lmtldcu(i),  
                           area(i,j,k), areahu(j), areacu(i)  
                           area\_add(i,j,k), areahu\_add(j), areacu\_add(i);

//variable bounding//

th.up(i,k) = THIN(i);  
 th.lo(i,k) = THOUT(i);  
 tc.up(j,k) = TCOUT(j);  
 tc.lo(j,k) = TCIN(j);

$$q.up(i,j,k)\$stage(k) = \max(\min(FCPH(i)*(th.up(i,k) - \max(th.lo(i,k+1), tc.lo(j,k+1) + EMAT)), FCPC(j)*( \min(th.up(i,k) - EMAT, tc.up(j,k)) - tc.lo(j,k+1) ) ), 0) \$ ( (th.up(i,k) - tc.lo(j,k) \geq EMAT) \text{ and } (th.up(i,k+1) - tc.lo(j,k+1) \geq EMAT) ) + 0 \$ ( (th.up(i,k) - tc.lo(j,k) < EMAT) \text{ or } (th.up(i,k+1) - tc.lo(j,k+1) < EMAT) );$$

$$qhu.up(j) = \max(FCPC(j)*( \min(THUIN(j) - EMAT, TCOUT(j)) - tc.lo(j, 'K1') ), 0) \$ ( (THUIN(j) - TCOUT(j) \geq EMAT) \text{ and } (THUOUT(j) - tc.lo(j, 'K1') \geq EMAT) ) + 0 \$ ( (THUIN(j) - TCOUT(j) < EMAT) \text{ or } (THUOUT(j) - tc.lo(j, 'K1') < EMAT) );$$

$$qcu.up(i) = \max(FCPH(i)*(th.up(i, 'KL') - \max(THOUT(i), TCUIN(i) + EMAT)), 0) \$ ( (th.up(i, 'KL') - TCUOUT(i) \geq EMAT) \text{ and } (THOUT(i) - TCUIN(i) \geq EMAT) ) + 0 \$ ( (th.up(i, 'KL') - TCUOUT(i) < EMAT) \text{ or } (THOUT(i) - TCUIN(i) < EMAT) );$$

```

dt.up(i,j,k) = max(EMAT,(th.up(i,k)-tc.lo(j,k)));
dt.lo(i,j,k) = EMAT;
dthul.up(j) = max(EMAT,THUIN(j)-TCOUT(j));
dthul.lo(j) = EMAT;
dthur.up(j) = max(EMAT,THUOUT(j)-tc.lo(j,'K1'));
dthur.lo(j) = EMAT;
dteul.up(i) = max(EMAT,th.up(i,'KL')-TCUOUT(i));
dteul.lo(i) = EMAT;
dteur.up(i) = max(EMAT,THOUT(i)-TCUIN(i));
dteur.lo(i) = EMAT;

lmtd.up(i,j,k)$stage(k) =
    (dt.up(i,j,k)*dt.up(i,j,k+1)*(dt.up(i,j,k)+dt.up(i,j,k+1))/2)**(1/3);
lmtd.lo(i,j,k)$stage(k) =
    (dt.lo(i,j,k)*dt.lo(i,j,k+1)*(dt.lo(i,j,k)+dt.lo(i,j,k+1))/2)**(1/3);
lmtdhu.up(j) = (dthur.up(j)*dthul.up(j)*(dthur.up(j)+dthul.up(j))/2)**(1/3);
lmtdhu.lo(j) = (dthur.lo(j)*dthul.lo(j)*(dthur.lo(j)+dthul.lo(j))/2)**(1/3);
lmtdteu.up(i) = (dteul.up(i)*dteur.up(i)*(dteul.up(i)+dteur.up(i))/2)**(1/3);
lmtdteu.lo(i) = (dteul.lo(i)*dteur.lo(i)*(dteul.lo(i)+dteur.lo(i))/2)**(1/3);

area.up(i,j,k)$stage(k) = q.up(i,j,k)/lmtd.lo(i,j,k)/U(i,j);
areahu.up(j) = qhu.up(j)/lmtdhu.lo(j)/UHU(j);
areacu.up(i) = qcu.up(i)/lmtdteu.lo(i)/UCU(i);

//Assign bounding to parameters in logical constraint//
GAMMA_HX(i,j,k) = q.up(i,j,k);
GAMMA_HU(j) = qhu.up(j);
GAMMA_CU(i) = qcu.up(i);

TAU_HX(i,j,k) = -th.lo(i,k)+tc.up(j,k)+dt.lo(i,j,k);
TAU_HUL(j) = -THUIN(j)+TCOUT(j)+dthul.lo(j);
TAU_HUR(j) = -THUOUT(j)+tc.up(j,'K1')+dthur.lo(j);
TAU_CUL(i) = -th.lo(i,'KL')+TCUOUT(i)+dteul.lo(i);
TAU_CUR(i) = -THOUT(i)+TCUIN(i)+dteur.lo(i);

//Last stage forcing bound//
q.fx(i,j,'KL') = 0;
lmtd.fx(i,j,'KL') = 0;
area.fx(i,j,'KL') = 0;
area_add.fx(i,j,'KL') = 0;

//To force no q, area change where there is no existing HX//
q.fx(i,j,k)$ (not HEN(i,j,k)) = 0;
area_add.fx(i,j,k)$ (not HEN(i,j,k)) = 0;

```

//initial value for variables//

area.l(i,j,k) = AREA\_OLD(i,j,k);  
 areahu.l(j) = AREAHU\_OLD(j);  
 areacu.l(i) = AREACU\_OLD(i);

th.l(i,k) = TH\_OLD(i,k);  
 tc.l(j,k) = TC\_OLD(j,k);

q.l(i,j,k) = Q\_OLD(i,j,k);  
 qhu.l(j) = QHU\_OLD(j);  
 qcu.l(i) = QCU\_OLD(i);

dt.l(i,j,k) = DT\_OLD(i,j,k);  
 dthul.l(j) = DTHUL\_OLD(j);  
 dthur.l(j) = DTHUR\_OLD(j);  
 dtcul.l(i) = DTCUL\_OLD(i);  
 dtcur.l(i) = DTCUR\_OLD(i);

lmtl.l(i,j,k) = LMTD\_OLD(i,j,k);  
 lmtdhu.l(j) = LMTDHU\_OLD(j);  
 lmtdcu.l(i) = LMTDCU\_OLD(i);

## EQUATIONS

OVERALL\_H(i) overall energy balance of hot stream i  
 OVERALL\_C(j) overall energy balance of cold stream j

EBAL\_H(i,k) energy balance of hot stream i in stage k  
 EBAL\_C(j,k) energy balance of cold stream j in stage k

TIN\_H(i) assignment inlet temperature of hot stream i  
 TIN\_C(j) assignment inlet temperature of cold stream j

MONOT\_H(i,k) monotonic in temperature of hot stream i at location k  
 MONOT\_C(j,k) monotonic in temperature of cold stream j at location k  
 MONOT\_HNOT(i,k) monotonic in temperature of hot stream i at location k  
 if no HX  
 MONOT\_CNOT(j,k) monotonic in temperature of cold stream j at location  
 k if no HX

MONOT\_HU(j) monotonic in outlet temperature of cold stream j  
 MONOT\_CU(i) monotonic in outlet temperature of hot stream i  
 MONOT\_HUNOT(j) monotonic in outlet temperature of cold stream j if no HX  
 MONOT\_CUNOT(i) monotonic in outlet temperature of hot stream i if no HX

EBAL\_HU(j) energy balance of hot utility of cold stream j  
 EBAL\_CU(i) energy balance of cold utility of hot stream i

DTFEAS\_HXL(i,j,k) temperature feasibility of heat exchanger of match(i,j)  
 at location k  
 DTFEAS\_HXR(i,j,k) temperature feasibility of heat exchanger of match(i,j)  
 at location k+1  
 DTFEAS\_HUL(j) temperature feasibility of hot utility of outlet cold  
 stream j  
 DTFEAS\_HUR(j) temperature feasibility of hot utility of inlet cold stream j  
 DTFEAS\_CUL(i) temperature feasibility of cold utility of inlet hot stream i  
 DTFEAS\_CUR(i) temperature feasibility of cold utility of outlet hot stream i

LOGMTD(i,j,k) log mean temperature of match(i,j) at stage k  
 LOGMTDHU(j) log mean temperature of hot utility exchanger  
 LOGMTDCU(i) log mean temperature of cold utility exchanger

A\_HX(i,j,k) - area of heat exchanger of match(i,j) at stage k  
 A\_HU(j) area of hot utility exchanger of cold stream j  
 A\_CU(i) area of cold utility exchanger of hot stream i

OBJ objective function (total additional area)

;

OVERALL\_H(i) .. (THIN(i) - THOUT(i)) \* FCPH(i) =e=  
 sum((j,k), q(i,j,k)) + qcu(i);  
 OVERALL\_C(j) .. (TCOUT(j) - TCIN(j)) \* FCPC(j) =e=  
 sum((i,k), q(i,j,k)) + qhu(j);

EBAL\_H(i,k) \$HEN\_HOT(i,k) .. (th(i,k) - th(i,k+1)) \* FCPH(i) =e=  
 sum(j, q(i,j,k)); //do only exist HEN  
 EBAL\_C(j,k) \$HEN\_COLD(j,k) .. (tc(j,k) - tc(j,k+1)) \* FCPC(j) =e=  
 sum(i, q(i,j,k));

TIN\_H(i) .. THIN(i) =e= th(i, 'K1');  
 TIN\_C(j) .. TCIN(j) =e= tc(j, 'KL');

MONOT\_H(i,k) \$HEN\_HOT(i,k) .. th(i,k) =g= th(i,k+1);  
 //if HX --> monotonic  
 MONOT\_C(j,k) \$HEN\_COLD(j,k) .. tc(j,k) =g= tc(j,k+1);  
 MONOT\_HNOT(i,k) \$((not HEN\_HOT(i,k)) and stage(k)) .. th(i,k) =e= th(i,k+1);  
 //if no HX --> equal  
 MONOT\_CNOT(j,k) \$((not HEN\_COLD(j,k)) and stage(k)) .. tc(j,k) =e= tc(j,k+1);

MONOT\_HU(j) \$HU(j) .. TCOUT(j) =g= tc(j, 'K1'); //if HX --> monotonic  
 MONOT\_CU(i) \$CU(i) .. th(i, 'KL') =g= THOUT(i);  
 MONOT\_HUNOT(j) \$(not HU(j)) .. TCOUT(j) =e= tc(j, 'K1'); //if no HX --> equal  
 MONOT\_CUNOT(i) \$(not CU(i)) .. th(i, 'KL') =e= THOUT(i);

```

EBAL_HU(j)$HU(j)      .. (TCOUT(j) - tc(j,'K1'))*FCPC(j) =e= qhu(j);
                                                                //do only exist HEN
EBAL_CU(i)$CU(i)      .. (th(i,'KL') - THOUT(i)) *FCPH(i) =e= qcu(i);

DTFEAS_HXL(i,j,k)$HEN(i,j,k) .. dt(i,j,k) =e= th(i,k) -tc(j,k) ;
DTFEAS_HXR(i,j,k)$HEN(i,j,k) .. dt(i,j,k+1) =e= th(i,k+1) -tc(j,k+1);
DTFEAS_HUL(j)$HU(j)      .. dthul(j) =e= THUIN(j) -TCOUT(j) ;
DTFEAS_HUR(j)$HU(j)      .. dthur(j) =e= THUOUT(j) -tc(j,'K1');
                                                                //if exist HEN and no TAU
DTFEAS_CUL(i)$CU(i)      .. dtcul(i) =e= th(i,'KL')-TCUOUT(i) ;
DTFEAS_CUR(i)$CU(i)      .. dtcur(i) =e= THOUT(i) -TCUIN(i) ;

LOGMTD(i,j,k)$HEN(i,j,k) .. lmtd(i,j,k) =e=
(dt(i,j,k)*dt(i,j,k+1)*(dt(i,j,k)+dt(i,j,k+1))/2)**(1/3); //only HEN
LOGMTDHU(j)$HU(j)      .. lmtdhu(j) =e= (dthur(j) *dthul(j) *(dthur(j)
+dthul(j)) /2)**(1/3);
LOGMTDCU(i)$CU(i)      .. lmtdcu(i) =e= (dtcul(i) *dtcur(i)
*(dtcul(i) +dtcur(i)) /2)**(1/3);

A_HX(i,j,k)$HEN(i,j,k)      .. area(i,j,k) *lmtd(i,j,k)*U(i,j) =e= q(i,j,k);
                                                                //only HEN
A_HU(j)$HU(j)      .. areahu(j) *lmtdhu(j) *UHU(j) =e= qhu(j);
A_CU(i)$CU(i)      .. areacu(i) *lmtdcu(i) *UCU(i) =e= qcu(i);

//least square error
OBJ      .. TOT_LSQR_ERROR =e=
sum((i,j,k)$HEN(i,j,k),power(area(i,j,k)-AREA_OLD(i,j,k),2))
+ sum(j$HU(j),power(areahu(j)-AREAHU_OLD(j),2))
+ sum(i$CU(i),power(areacu(i)-AREACU_OLD(i),2)));

model STAGEMODEL_SINGLEPERIOD /all/;

option iterlim=1e9;
option domlim=0;
option reslim=1e8;
STAGEMODEL_SINGLEPERIOD.optfile=0;

solve STAGEMODEL_SINGLEPERIOD using NLP minimizing
TOT_LSQR_ERROR;

```

```
display th.l,tc.l,  
q.l,qhu.l,qcu.l,  
area.l,areahu.l,areacu.l,  
dt.l,dthul.l,dthur.l,dtcu.l,dtcu.l,  
lmtd.l,lmtdhu.l,lmtdcu.l,  
tot_lsqr_error.l  
;
```

**B3 Model C**

## SETS

I hot streams /I1\*I3/  
 J cold streams /J1\*J4/  
 K index of stage or location /K1\*K4,KL/ //last number is no. of stages

stage(k) all stages  
 HEN(i,j,k) define where HX exists  
 HEN\_HOT(i,k) define where HX exists 2 dimensions for hot streams  
 HEN\_COLD(j,k) define where HX exists 2 dimensions for cold streams  
 HU(j) define where HU exists  
 CU(i) define where CU exists

;

//dynamic set for stage pointer

stage(k) = yes;  
 stage('KL') = no;

//dynamic set for existing HEN// &lt;---- To fix topology

HEN(i,j,k) = no;

TABLE Z\_OLD(i,j,k) Existing HX from original HEN of each period

	K1	K2	K3	K4
I1.J1	1.000	1.000	1.000	
I1.J2			1.000	1.000
I1.J3		1.000		
I3.J1		1.000	1.000	
I3.J4	1.000			

;

loop((i,j,k)\$(Z\_OLD(i,j,k)=1), HEN(i,j,k) = yes);

//dynamic set for existing Utility exchanger// &lt;---- To fix topology

//hot utility

HU(j) = no;  
 PARAMETER ZHU\_OLD(j) Existing HU from original HEN of each period  
 /J3 1.000/;  
 loop(j\$(ZHU\_OLD(j)=1), HU(j) = yes);

//cold utility

CU(i) = no;  
 PARAMETER ZCU\_OLD(i) Existing CU from original HEN of each period  
 /I1 1.000, I2 1.000, I3 1.000/;  
 loop(i\$(ZCU\_OLD(i)=1), CU(i) = yes);



```
//define dynamic set for existing HEN but only 2 dimensions (for hot and cold)//
```

```
HEN_HOT(i,k) = no;
HEN_COLD(j,k) = no;
loop((i,j,k)$ (HEN(i,j,k)), HEN_HOT(i,k) = yes);
loop((i,j,k)$ (HEN(i,j,k)), HEN_COLD(j,k) = yes);
```

## SCALARS

```
//Cost//
```

CA	per unit cost of heat exchanger area(\$ per unit)	/641.7/
B	exponent for area cost(dimensionless)	/1/
CF	fixed cost of heat exchanger(\$ per unit)	/8333.3/
CHU	per unit cost of hot utility(\$ per kW)	/115.2/
CCU	fixed cost of heat exchanger(\$ per kW)	/1.3/
AF	annualisation factor	/0.2/

```
//other//
```

EMAT	exchanger minimum approach temperature(C)	/5/
HHU	heat transfer coefficient of hot utility(kW (m2.C))	/2/
HCU	heat transfer coefficient of cold utility(kW (m2.C))	/1/

## PARAMETERS

```
//Hot Streams//
```

```
THIN(i) inlet temperature of hot streams(C)
/   I1  393
    I2  160
    I3  354
/
```

```
THOUT(i) outlet temperature of hot streams(C)
/   I1  60
    I2  40
    I3  60
/
```

```
//Cold Streams//
```

```
TCIN(j) inlet temperature of cold streams(C)
/   J1  72
    J2  62
    J3  220
    J4  253
/
```

```
TCOUT(j) outlet temperature of cold streams(C)
```

```

/      J1  356
      J2  210
      J3  370
      J4  284
/
//Heat Capacity Flowrates//
FCPH(i) heat capaity flowrates fo hot streams(C)
/      I1  201.6
      I2  185.1
      I3  137.4
/
FCPC(j) heat capaity flowrates fo cold streams(C)
/      J1  209.4
      J2  141.6
      J3  176.4
      J4  294.4
/
//Utility//
THUIN(j) inlet temperature of hot utility(C)
/      J1  400
      J2  400
      J3  400
      J4  400
/
THUOUT(j) outlet temperature of hot utility(C)
/      J1  399
      J2  399
      J3  399
      J4  399
/
TCUIN(i) inlet temperature of cold utility(C)
/      I1  15
      I2  15
      I3  15
/
TCUOUT(i) outlet temperature of cold utility(C)
/      I1  20
      I2  20
      I3  20
/
//Heat transfer coefficient//
HH(i) heat capaity flowrates of hot streams(kW|(m2.C))
/      I1  2
      I2  2
      I3  2
/
HC(j) heat capaity flowrates of cold streams(kW|(m2.C))

```

```

/      J1  1.5
      J2  1.5
      J3  2
      J4  2
/
//overall heat transfer coefficient//
U(i,j)      Overall heat transfer coefficient for match(i,j)
UHU(j)      Overall heat transfer coefficient for cold stream(j) and hot utility
UCU(i)      Overall heat transfer coefficient for hot stream(i) and cold utility

//upper bound for logical constraints//
GAMMA_HX(i,j,k)  upper bound heat load for match (i,j)
GAMMA_HU(j)      upper bound heat load for hot utility
GAMMA_CU(i)      upper bound heat load for cold utility

TAU_HX(i,j,k)   upper bound of temperature difference for heat exchanger
TAU_HUL(j)      upper bound of temperature difference for left side of hot
                 utility exchanger
TAU_HUR(j)      upper bound of temperature difference for right side of hot
                 utility exchanger
TAU_CUL(i)      upper bound of temperature difference for left side pf cold
                 utility exchanger
TAU_CUR(i)      upper bound of temperature difference for right side of cold
                 utility exchanger
;

//Old value of variables from original HEN//

//Area//
TABLE AREA_OLD(i,j,k) old area from original HEN of each period
      K1      K2      K3      K4

11.J1  680.055  166.126  751.970
11.J2           1290.040  132.794
11.J3           597.190
13.J1           356.123  1470.846
13.J4  324.859
;

PARAMETERS
AREAHU_OLD(j) old area of HU from original HEN
/J3 256.025/
AREACU_OLD(i) old area of CU from original HEN
/I1 117.036, I2 541.396, I3 97.762/
;

```

//Temperature//

TABLE TH\_OLD(i,k) old hot temperature from original HEN

	K1	K2	K3	K4	KL
I1	406.000	293.498	231.178	88.555	79.812
I2	160.000	160.000	160.000	160.000	160.000
I3	362.000	268.540	234.038	86.252	86.252

;

TABLE TC\_OLD(j,k) old cold temperature from original HEN

	K1	K2	K3	K4	KL
J1	365.000	255.334	216.175	72.000	72.000
J2	210.000	210.000	210.000	74.710	62.000
J3	272.717	272.717	220.000	220.000	220.000
J4	290.000	250.000	250.000	250.000	250.000

;

//Heat load//

TABLE Q\_OLD(i,j,k) old heat load from original HEN

	K1	K2	K3	K4
I1.J1	23062.852	3528.959	10162.028	
I1.J2		19075.844	1792.156	
I1.J3		9246.623		
I3.J1		4706.050	20158.011	
I3.J4	12748.000			

;

PARAMETERS

QHU\_OLD(j) old heat load of HU from original HEN

/J3 17063.377/

QCU\_OLD(i) old heat load of CU from original HEN

/I1 4061.538, I2 23856.000, I3 3580.739/

;

//Temperature Difference//

TABLE DT\_OLD(i,j,k) old temperature difference from original HEN

	K1	K2	K3	K4	KL
I1.J1	41.000	38.165	15.003	16.555	
I1.J2		21.178	13.844	17.812	
I1.J3		20.781	11.178		
I3.J1		13.206	17.863	14.252	
I3.J4	72.000	18.540			

;

## PARAMETERS

DTHUL\_OLD(j) old left-side temperature difference of HU from original HEN  
/J3 30.000/

DTHUR\_OLD(j) old right-side temperature difference of HU from original HEN  
/J3 126.283/

DTCUL\_OLD(i) old left-side temperature difference of CU from original HEN  
/I1 59.812, I2 140.000, I3 66.252/

DTCUR\_OLD(i) old right-side temperature difference of CU from original HEN  
/I1 45.000, I2 25.000, I3 45.000/

;

//Log Mean Temperature Difference//

TABLE LMTD\_OLD(i,j,k) old log mean temperature from original HEN  
K1 K2 K3 K4

I1.J1	39.565	24.783	15.766	
I1.J2			17.252	15.745
I1.J3		15.484		
I3.J1		15.417	15.989	
I3.J4	39.242			

;

## PARAMETERS

LMTDHU\_OLD(j) old log mean temperature of HU from original HEN  
/J3 66.647/

LMTDCU\_OLD(i) old log mean temperature of CU from original HEN  
/I1 52.055, I2 66.096, I3 54.941/

;

//Overall heat transfer coefficient calculations//

$U(i,j) = 1/(1/HH(i)+1/HC(j));$   
 $UHU(j) = 1/(1/HC(j)+1/HHU);$   
 $UCU(i) = 1/(1/HH(i)+1/HCU);$

## VARIABLES

th(i,k) temperature(C) of hot streams i at location k  
tc(j,k) temperature(C) of cold streams j at location k

q(i,j,k) heat load(kW) of match(i,j) at stage k  
qhu(j) heat load(kW) of hot utility for cold stream j  
qcu(i) heat load(kW) of cold utility for hot stream i

dt(i,j,k) temperature difference(C) for match(i,j) at location k  
dthul(j) temperature difference(C) for left side of hot utility exchanger  
dthur(j) temperature difference(C) for right side of hot utility exchanger  
dteul(i) temperature difference(C) for left side of cold utility exchanger

dtcur(i)      temperature difference(C) for right side of cold utility exchanger  
  
 lmtd(i,j,k)    log mean temperature difference of match(i,j) at stage k  
 lmtdhu(j)      log mean temperature difference of hot utility exchanger for cold  
                   stream j  
 lmtdcu(i)      log mean temperature difference of cold utility exchanger for cold  
                   stream i  
  
 area(i,j,k)    area of heat exchanger of match(i,j) at stage k  
 areahu(j)      area of hot utility exchanger of cold stream j  
 areacu(i)      area of cold utility exchanger of hot stream i  
  
 area\_add(i,j,k) additional area of heat exchanger of match(i,j) at stage k  
 areahu\_add(j) additional area of hot utility exchanger of cold stream j  
 areacu\_add(i) additional area of cold utility exchanger of hot stream i  
  
 tot\_area\_add   total additional area needed

POSITIVE VARIABLES    q(i,j,k), qhu(j), qcu(i),  
                           dt(i,j,k), dthul(j), dthur(j), dtcul(i), dtcur(i),  
                           lmtd(i,j,k),lmtdhu(j),lmtdcu(i),  
                           area(i,j,k),areahu(j),areacu(i)  
                           area\_add(i,j,k), areahu\_add(j), areacu\_add(i);

//variable bounding//

th.up(i,k) = THIN(i);  
 th.lo(i,k) = THOUT(i);  
 tc.up(j,k) = TCOUT(j);  
 tc.lo(j,k) = TCIN(j);

$$q.up(i,j,k)\$stage(k) = \max(\min(FCPH(i)*(th.up(i,k) - \max(th.lo(i,k+1), tc.lo(j,k+1)) + EMAT)), FCPC(j)*(\min(th.up(i,k) - EMAT, tc.up(j,k)) - tc.lo(j,k+1))), 0)\$( (th.up(i,k) - tc.lo(j,k) \geq EMAT) \text{ and } (th.up(i,k+1) - tc.lo(j,k+1) \geq EMAT)) + 0\$( (th.up(i,k) - tc.lo(j,k) < EMAT) \text{ or } (th.up(i,k+1) - tc.lo(j,k+1) < EMAT));$$

$$qhu.up(j) = \max(FCPC(j)*(\min(THUIN(j) - EMAT, TCOUT(j)) - tc.lo(j, 'K1')), 0)\$( (THUIN(j) - TCOUT(j) \geq EMAT) \text{ and } (THUOUT(j) - tc.lo(j, 'K1') \geq EMAT)) + 0\$( (THUIN(j) - TCOUT(j) < EMAT) \text{ or } (THUOUT(j) - tc.lo(j, 'K1') < EMAT));$$

$$qcu.up(i) = \max(FCPH(i)*(th.up(i, 'KL') - \max(THOUT(i), TCUIN(i)) + EMAT), 0)\$( (th.up(i, 'KL') - TCUOUT(i) \geq EMAT) \text{ and } (THOUT(i) - TCUIN(i) \geq EMAT)) + 0\$( (th.up(i, 'KL') - TCUOUT(i) < EMAT) \text{ or } (THOUT(i) - TCUIN(i) < EMAT));$$

```

dt.up(i,j,k) = max(EMAT,(th.up(i,k)-tc.lo(j,k)));
dt.lo(i,j,k) = EMAT;
dthul.up(j) = max(EMAT,THUIN(j)-TCOUT(j));
dthul.lo(j) = EMAT;
dthur.up(j) = max(EMAT,THUOUT(j)-tc.lo(j,'K1'));
dthur.lo(j) = EMAT;
dteul.up(i) = max(EMAT,th.up(i,'KL')-TCUOUT(i));
dteul.lo(i) = EMAT;
dteur.up(i) = max(EMAT,THOUT(i)-TCUIN(i));
dteur.lo(i) = EMAT;

```

```

lmtd.up(i,j,k)$stage(k) =
(dt.up(i,j,k)*dt.up(i,j,k+1)*(dt.up(i,j,k)+dt.up(i,j,k+1))/2)**(1/3);
lmtd.lo(i,j,k)$stage(k) =
(dt.lo(i,j,k)*dt.lo(i,j,k+1)*(dt.lo(i,j,k)+dt.lo(i,j,k+1))/2)**(1/3);
lmtdhu.up(j) =
(dthur.up(j)*dthul.up(j)*(dthur.up(j)+dthul.up(j))/2)**(1/3);
lmtdhu.lo(j) = (dthur.lo(j)*dthul.lo(j)*(dthur.lo(j)+dthul.lo(j))/2)**(1/3);
lmtdteu.up(i) =
(dteul.up(i)*dteur.up(i)*(dteul.up(i)+dteur.up(i))/2)**(1/3);
lmtdteu.lo(i) = (dteul.lo(i)*dteur.lo(i)*(dteul.lo(i)+dteur.lo(i))/2)**(1/3);

```

```

area.up(i,j,k)$stage(k) = q.up(i,j,k)/lmtd.lo(i,j,k)/U(i,j);
areahu.up(j) = qhu.up(j)/lmtdhu.lo(j)/UHU(j);
areacu.up(i) = qcu.up(i)/lmtdteu.lo(i)/UCU(i);

```

```
//Assign bounding to parameters in logical constraint//
```

```

GAMMA_HX(i,j,k) = q.up(i,j,k);
GAMMA_HU(j) = qhu.up(j);
GAMMA_CU(i) = qcu.up(i);

```

```

TAU_HX(i,j,k) = -th.lo(i,k)+tc.up(j,k)+dt.lo(i,j,k);
TAU_HUL(j) = -THUIN(j)+TCOUT(j)+dthul.lo(j);
TAU_HUR(j) = -THUOUT(j)+tc.up(j,'K1')+dthur.lo(j);
TAU_CUL(i) = -th.lo(i,'KL')+TCUOUT(i)+dteul.lo(i);
TAU_CUR(i) = -THOUT(i)+TCUIN(i)+dteur.lo(i);

```

```
//Last stage forcing bound//
```

```

q.fx(i,j,'KL') = 0;
lmtd.fx(i,j,'KL') = 0;
area.fx(i,j,'KL') = 0;
area_add.fx(i,j,'KL') = 0;

```

```
//To force no q, area change where there is no existing HX//
```

```

q.fx(i,j,k)$ (not HEN(i,j,k)) = 0;
area_add.fx(i,j,k)$ (not HEN(i,j,k)) = 0;

```

//initial value for variables//

area.l(i,j,k) = AREA\_OLD(i,j,k);  
 areahu.l(j) = AREAHU\_OLD(j);  
 areacu.l(i) = AREACU\_OLD(i);

area\_add.l(i,j,k) = 0;  
 areahu\_add.l(j) = 0;  
 areacu\_add.l(i) = 0;

th.l(i,k) = TH\_OLD(i,k);  
 tc.l(j,k) = TC\_OLD(j,k);

q.l(i,j,k) = Q\_OLD(i,j,k);  
 qhu.l(j) = QHU\_OLD(j);  
 qcu.l(i) = QCU\_OLD(i);

dt.l(i,j,k) = DT\_OLD(i,j,k);  
 dthul.l(j) = DTHUL\_OLD(j);  
 dthur.l(j) = DTHUR\_OLD(j);  
 dtcul.l(i) = DTCUL\_OLD(i);  
 dtcur.l(i) = DTCUR\_OLD(i);

lmtl.l(i,j,k) = LMTD\_OLD(i,j,k);  
 lmtdhu.l(j) = LMTDHU\_OLD(j);  
 lmtdcu.l(i) = LMTDCU\_OLD(i);

## EQUATIONS

OVERALL\_H(i) overall energy balance of hot stream i  
 OVERALL\_C(j) overall energy balance of cold stream j

EBAL\_H(i,k) energy balance of hot stream i in stage k  
 EBAL\_C(j,k) energy balance of cold stream j in stage k

TIN\_H(i) assignment inlet temperature of hot stream i  
 TIN\_C(j) assignment inlet temperature of cold stream j

MONOT\_H(i,k) monotonic in temperature of hot stream i at location k  
 MONOT\_C(j,k) monotonic in temperature of cold stream j at location k  
 MONOT\_HNOT(i,k) monotonic in temperature of hot stream i at location k  
 if no HX  
 MONOT\_CNOT(j,k) monotonic in temperature of cold stream j at location  
 k if no HX

MONOT\_HU(j) monotonic in outlet temperature of cold stream j  
 MONOT\_CU(i) monotonic in outlet temperature of hot stream i  
 MONOT\_HUNOT(j) monotonic in outlet temperature of cold stream j if no HX



MONOT\_CUNOT(i) monotonic in outlet temperature of hot stream i if no HX

EBAL\_HU(j) energy balance of hot utility of cold stream j  
 EBAL\_CU(i) energy balance of cold utility of hot stream i

DTFEAS\_HXL(i,j,k) temperature feasibility of heat exchanger of match(i,j)  
 at location k  
 DTFEAS\_HXR(i,j,k) temperature feasibility of heat exchanger of match(i,j)  
 at location k+1  
 DTFEAS\_HUL(j) temperature feasibility of hot utility of outlet cold  
 stream j  
 DTFEAS\_HUR(j) temperature feasibility of hot utility of inlet cold stream j  
 DTFEAS\_CUL(i) temperature feasibility of cold utility of inlet hot stream i  
 DTFEAS\_CUR(i) temperature feasibility of cold utility of outlet hot  
 stream i

LOGMTD(i,j,k) log mean temperature of match(i,j) at stage k  
 LOGMTDHU(j) log mean temperature of hot utility exchanger  
 LOGMTDCU(i) log mean temperature of cold utility exchanger

ADDIAREA\_HX1(i,j,k) additional area needed for heat exchanger  
 ADDIAREA\_HX2(i,j,k) force ADDAREA\_HX > 0  
 ADDIAREA\_HU1(j) additional area needed for hot utility  
 ADDIAREA\_HU2(j) force ADDAREA\_HU > 0  
 ADDIAREA\_CU1(i) additional area needed for cold utility  
 ADDIAREA\_CU2(i) force ADDAREA\_CU > 0

A\_HX(i,j,k) area of heat exchanger of match(i,j) at stage k  
 A\_HU(j) area of hot utility exchanger of cold stream j  
 A\_CU(i) area of cold utility exchanger of hot stream i

OBJ objective function (total additional area)

;

OVERALL\_H(i) .. (THIN(i) - THOUT(i)) \* FCPH(i) =e= sum((j,k), q(i,j,k)) + qcu(i);

OVERALL\_C(j) .. (TCOUT(j) - TCIN(j)) \* FCPC(j) =e= sum((i,k), q(i,j,k)) + qhu(j);

EBAL\_H(i,k)\$HEN\_HOT(i,k) .. (th(i,k) - th(i,k+1)) \* FCPH(i) =e= sum(j, q(i,j,k));  
 //do only exist HEN

EBAL\_C(j,k)\$HEN\_COLD(j,k) .. (tc(j,k) - tc(j,k+1)) \* FCPC(j) =e= sum(i, q(i,j,k));

TIN\_H(i) .. THIN(i) =e= th(i, 'K1');

TIN\_C(j) .. TCIN(j) =e= tc(j, 'KL');

```

MONOT_H(i,k)$HEN_HOT(i,k) .. th(i,k) =g= th(i,k+1);
                                //if HX --> monotonic
MONOT_C(j,k)$HEN_COLD(j,k) .. tc(j,k) =g= tc(j,k+1);
MONOT_HNOT(i,k)$((not HEN_HOT(i,k)) and stage(k)) .. th(i,k) =e= th(i,k+1);
                                //if no HX --> equal
MONOT_CNOT(j,k)$((not HEN_COLD(j,k)) and stage(k)) .. tc(j,k) =e= tc(j,k+1);

MONOT_HU(j)$HU(j) .. TCOUT(j) =g= tc(j,'K1'); //if HX --> monotonic
MONOT_CU(i)$CU(i) .. th(i,'KL') =g= THOUT(i);
MONOT_HUNOT(j)$((not HU(j)) .. OUT(j) =e= tc(j,'K1'); //if no HX --> equal
MONOT_CUNOT(i)$((not CU(i)) .. th(i,'KL') =e= THOUT(i);

EBAL_HU(j)$HU(j) .. (TCOUT(j) - tc(j,'K1'))*FCPC(j) =e= qhu(j);
                                //do only exist HEN
EBAL_CU(i)$CU(i) .. (th(i,'KL') - THOUT(i)) *FCPH(i) =e= qcu(i);

DTFEAS_HXL(i,j,k)$HEN(i,j,k) .. dt(i,j,k) =e= th(i,k) -tc(j,k) ;
DTFEAS_HXR(i,j,k)$HEN(i,j,k) .. dt(i,j,k+1) =e= th(i,k+1) -tc(j,k+1);
DTFEAS_HUL(j)$HU(j) .. dthul(j) =e= THUIN(j) -TCOUT(j) ;
DTFEAS_HUR(j)$HU(j) .. dthur(j) =e= THUOUT(j) -tc(j,'K1');
                                //if exist HEN and no TAU
DTFEAS_CUL(i)$CU(i) .. dtcul(i) =e= th(i,'KL')-TCUOUT(i) ;
DTFEAS_CUR(i)$CU(i) .. dtcur(i) =e= THOUT(i) -TCUIN(i) ;

LOGMTD(i,j,k)$HEN(i,j,k) .. lmtd(i,j,k) =e=
(dt(i,j,k)*dt(i,j,k+1)*(dt(i,j,k)+dt(i,j,k+1))/2)**(1/3);
                                //only HEN
LOGMTDHU(j)$HU(j) .. lmtdhu(j) =e= (dthur(j) *dthul(j) *(dthur(j)
+dthul(j)) /2)**(1/3);
LOGMTDCU(i)$CU(i) .. lmtdcu(i) =e= (dtcul(i) *dtcur(i) *(dtcul(i)
+dtcur(i)) /2)**(1/3);

A_HX(i,j,k)$HEN(i,j,k) .. area(i,j,k) *lmtd(i,j,k)*U(i,j) =e= q(i,j,k); //only HEN
A_HU(j)$HU(j) .. areahu(j) *lmtdhu(j) *UHU(j) =e= qhu(j);
A_CU(i)$CU(i) .. areacu(i) *lmtdcu(i) *UCU(i) =e= qcu(i);

ADDIAREA_HX1(i,j,k)$HEN(i,j,k) .. area_add(i,j,k) =g= area(i,j,k) -
AREA_OLD(i,j,k);
ADDIAREA_HX2(i,j,k)$HEN(i,j,k) .. area_add(i,j,k) =g= 0;
ADDIAREA_HU1(j)$HU(j) .. areahu_add(j) =g= areahu(j) - AREA_HU_OLD(j);
ADDIAREA_HU2(j)$HU(j) .. areahu_add(j) =g= 0;
ADDIAREA_CU1(i)$CU(i) .. areacu_add(i) =g= areacu(i) - AREACU_OLD(i);
ADDIAREA_CU2(i)$CU(i) .. areacu_add(i) =g= 0;

```

```
//least square
//OBJ      .. TAC =e=
           sum((i,j,k)$HEN(i,j,k) , power(AREAHX(i,j,k)-AREAOLD(i,j,k),2) )
           + sum(j$(HU(j)) , power(AREAHU(j)-AREAHUOLD(j),2) )
           + sum(i$(CU(i)) , power(AREACU(i)-AREACUOLD(i),2) );
```

```
//penalty only increased area
OBJ      .. TOT_AREA_ADD =e=
           sum((i,j,k)$HEN(i,j,k),area_add(i,j,k))
           + sum(j$(HU(j)),areahu_add(j))
           + sum(i$(CU(i)),areacu_add(i));
```

```
model STAGEMODEL_SINGLEPERIOD /all/;
```

```
option iterlim=1e9;
option domlim=0;
option reslim=1e8;
STAGEMODEL_SINGLEPERIOD.optfile=0;
```

```
solve STAGEMODEL_SINGLEPERIOD using NLP minimizing
TOT_AREA_ADD;
```

```
display th.l,tc.l,
       q.l,qhu.l,qcu.l,
       area.l,areahu.l,areacu.l,
       dt.l,dthul.l,dthur.l,dtcul.l,dtcu.l,
       lmt.l,lmtdhu.l,lmtdhu.l,
       tot_area_add.l,
       ;
```

## Appendix C Source Code of Simultaneous MINLP Multiperiod Model

The following text is source code which is entered in GAMS for synthesizing multi-period HEN by simultaneous approach.

### SETS

```

I hot streams           /I1*I3/
J cold streams         /J1*J4/
K index of stage or location /K1*K4,KL/ //last number is no. of stages
P period of operation  /P1*P3/

```

//dynamic sets//

```

stage(k) all stages
;
stage(k) = yes; stage('KL') = no;

```

### SCALARS

//Cost//

```

CA per unit cost of heat exchanger area($ per unit) /641.7/
CF fixed cost of heat exchanger($ per unit) /8333.3/

CHU per unit cost of hot utility($ per kW) /115.2/
CCU fixed cost of heat exchanger($ per kW) /1.3/

AF annualisation factor /0.2/

```

//other//

```

EMAT exchanger minimum approach temperature(C) /5/

HHU heat transfer coefficient of hot utility(kW|(m2.C)) /2/
HCU heat transfer coefficient of cold utility(kW|(m2.C)) /1/
;

```

//Hot Streams//

```

TABLE THIN(i,p) inlet temperatures of hot stream i in period p(C)
      P1      P2      P3
I1    393     406     420
I2    160     160     160
I3    354     362     360
;

```

```

TABLE THOUT(i,p) outlet temperatures of hot stream i in period p(C)
      P1      P2      P3
I1     60     60     60
I2     40     40     40
I3     60     60     60

```

//Cold Streams//

TABLE TCIN(j,p) inlet temperatures of cold stream j in period p(C)

	P1	P2	P3
J1	72	72	72
J2	62	62	62
J3	220	220	220
J4	253	250	249

TABLE TCOU(j,p) outlet temperatures of cold stream j in period p(kW|K)

	P1	P2	P3
J1	356	365	373
J2	210	210	210
J3	370	370	370
J4	284	290	286

//Heat Capacity Flowrates//

TABLE FCPH(i,p) heat capacity flowrates of hot stream i in period p(kW|K)

	P1	P2	P3
I1	201.6	205.0	208.5
I2	185.1	198.8	175.2
I3	137.4	136.4	134.1

TABLE FCPC(j,p) heat capacity flowrates of cold stream j in period p(kW|K)

	P1	P2	P3
J1	209.4	210.3	211.1
J2	141.6	141.0	140.5
J3	176.4	175.4	174.5
J4	294.4	318.7	271.2

//Utility//

TABLE THUIN(j,p) inlet temperature of hot utility for cold stream j in period p(C)

	P1	P2	P3
J1	400	400	400
J2	400	400	400
J3	400	400	400
J4	400	400	400

TABLE THUOUT(j,p) outlet temperature of hot utility for cold stream j in period p(C)

	P1	P2	P3
J1	399	399	399
J2	399	399	399
J3	399	399	399

J4 399 399 399

TABLE TCUIN(i,p) inlet temperature of cold utility for hot stream i in period p(C)

	P1	P2	P3
I1	15	15	15
I2	15	15	15
I3	15	15	15

TABLE TCUOUT(i,p) outlet temperature of cold utility for hot stream i in period p(C)

	P1	P2	P3
I1	20	20	20
I2	20	20	20
I3	20	20	20

#### PARAMETERS

//Heat transfer coefficient//

HH(i) heat capacity flowrates of hot streams(kW|(m2.C))

/	I1	2
	I2	2
	I3	2

/

HC(j) heat capacity flowrates of cold streams(kW|(m2.C))

/	J1	1.5
	J2	1.5
	J3	2
	J4	2

/

//Duration of each period//

DOP(p) duration of each period

/	P1	4
	P2	4
	P3	4

/

//Total duration//

TOP total duration of all period

//overall heat transfer coefficient//

U(i,j) Overall heat transfer coefficient for match(i,j)

UHU(j) Overall heat transfer coefficient for cold stream(j) and hot utility

UCU(i) Overall heat transfer coefficient for hot stream(i) and cold utility

//upper bound for logical constraints//

GAMMA\_HX(i,j,k,p) upper bound heat load for match (i,j) for period p  
 GAMMA\_HU(j,p) upper bound heat load for hot utility for period p  
 GAMMA\_CU(i,p) upper bound heat load for cold utility for period p  
  
 TAU\_HX(i,j,k,p) upper bound of temperature difference for heat exchanger  
 for period p  
 TAU\_HUL(j,p) upper bound of temperature difference for left side of hot  
 utility exchanger for period p  
 TAU\_HUR(j,p) upper bound of temperature difference for right side of hot  
 utility exchanger for period p  
 TAU\_CUL(i,p) upper bound of temperature difference for left side of cold  
 utility exchanger for period p  
 TAU\_CUR(i,p) upper bound of temperature difference for right side of cold  
 utility exchanger for period p

//Overall heat transfer coefficient calculations//

$U(i,j) = 1/(1/HH(i)+1/HC(j));$   
 $UHU(j) = 1/(1/HC(j)+1/HHU);$   
 $UCU(i) = 1/(1/HH(i)+1/HCU);$

//TOP calculation//

TOP = sum(p,DOP(p));

#### VARIABLES

th(i,k,p) temperature(C) of hot streams i at location k for period p  
 tc(j,k,p) temperature(C) of cold streams j at location k for period p  
  
 q(i,j,k,p) heat load(kW) of match(i,j) at stage k for period p  
 qhu(j,p) heat load(kW) of hot utility for cold stream j for period p  
 qcu(i,p) heat load(kW) of cold utility for hot stream i for period p  
  
 z(i,j,k) existence of match(i,j) at stage k  
 zhu(j) existence of hot utility for cold stream j  
 zcu(i) existence of cold utility for hot stream i  
  
 dt(i,j,k,p) temperature difference(C) for match(i,j) at location k for period p  
 dthul(j,p) temperature difference(C) for left side of hot utility exchanger  
 for period p  
 dthur(j,p) temperature difference(C) for right side of hot utility exchanger  
 for period p  
 dtcul(i,p) temperature difference(C) for left side of cold utility exchanger  
 for period p  
 dtcur(i,p) temperature difference(C) for right side of cold utility exchanger  
 for period p

$lmtd(i,j,k,p)$  log mean temperature difference of match(i,j) at stage k for period p  
 $lmtdhu(j,p)$  log mean temperature difference of hot utility exchanger for cold stream j for period p  
 $lmtdcu(i,p)$  log mean temperature difference of cold utility exchanger for cold stream i for period p  
  
 $area(i,j,k,p)$  area of heat exchanger of match(i,j) at stage k for period p  
 $areahu(j,p)$  area of hot utility exchanger of cold stream j for period p  
 $areacu(i,p)$  area of cold utility exchanger of hot stream i for period p  
  
 $area\_max(i,j,k)$  maximum area of heat exchanger of match(i,j) at stage k for all period  
 $areahu\_max(j)$  maximum area of hot utility exchanger of cold stream j for all period  
 $areacu\_max(i)$  maximum area of cold utility exchanger of hot stream i for all period  
  
 $cost\_fix$  fixed cost  
 $cost\_area$  area cost  
 $cost\_utility$  utility cost  
  
 $TAC$  total annualized cost

POSITIVE VARIABLES  $q(i,j,k,p)$ ,  $qhu(j,p)$ ,  $qcu(i,p)$ ,  
 $dt(i,j,k,p)$ ,  $dthul(j,p)$ ,  $dthur(j,p)$ ,  $dcul(i,p)$ ,  $dcur(i,p)$ ,  
 $LMTD(i,j,k,p)$ ,  $LMTDHU(j,p)$ ,  $LMTDCU(i,p)$ ,  
 $AREAHX(i,j,k,p)$ ,  $AREAHU(j,p)$ ,  $AREACU(i,p)$   
 $AREAHX\_max(i,j,k)$ ,  $AREAHU\_max(j)$ ,  $AREACU\_max(i)$ ;

BINARY VARIABLES  $z(i,j,k)$ ,  $zhu(j)$ ,  $zcu(i)$  ;

//variable bounding//

$th.up(i,k,p) = THIN(i,p)$ ;  
 $th.lo(i,k,p) = THOUT(i,p)$ ;  
 $tc.up(j,k,p) = TCOU(j,p)$ ;  
 $tc.lo(j,k,p) = TCIN(j,p)$ ;

$q.up(i,j,k,p) \$stage(k) = \max(\min(FCPH(i,p)*(th.up(i,k,p) - \max(th.lo(i,k+1,p), tc.lo(j,k+1,p) + EMAT)), FCPC(j,p)*( \min(th.up(i,k,p) - EMAT, tc.up(j,k,p)) - tc.lo(j,k+1,p) ) , 0) \$ ( (th.up(i,k,p) - tc.lo(j,k,p) \geq EMAT) \text{ and } (th.up(i,k+1,p) - tc.lo(j,k+1,p) \geq EMAT)) + 0 \$ ( (th.up(i,k,p) - tc.lo(j,k,p) < EMAT) \text{ or } (th.up(i,k+1,p) - tc.lo(j,k+1,p) < EMAT)) ) ;$



$qhu.up(j,p) = \max(FCPC(j,p) * (\min(THUIN(j,p) - EMAT, TCOUT(j,p)) - tc.lo(j, 'K1', p)), 0) \$((THUIN(j,p) - TCOUT(j,p) \geq EMAT) \text{ and } (THUOUT(j,p) - tc.lo(j, 'K1', p) \geq EMAT)) + 0 \$((THUIN(j,p) - TCOUT(j,p) < EMAT) \text{ or } (THUOUT(j,p) - tc.lo(j, 'K1', p) < EMAT));$

$qcu.up(i,p) = \max(FCPH(i,p) * (th.up(i, 'KL', p) - \max(THOUT(i,p), TCUIN(i,p) + EMAT)), 0) \$((th.up(i, 'KL', p) - TCUOUT(i,p) \geq EMAT) \text{ and } (THOUT(i,p) - TCUIN(i,p) \geq EMAT)) + 0 \$((th.up(i, 'KL', p) - TCUOUT(i,p) < EMAT) \text{ or } (THOUT(i,p) - TCUIN(i,p) < EMAT));$

$z.up(i,j,k) \$stage(k) = 0 \$(\sum(p, q.up(i,j,k,p)) = 0) + 1 \$(\sum(p, q.up(i,j,k,p)) \neq 0);$   
 $zhu.up(j) = 0 \$(\sum(p, qhu.up(j,p)) = 0) + 1 \$(\sum(p, qhu.up(j,p)) \neq 0);$   
 $zcu.up(i) = 0 \$(\sum(p, qcu.up(i,p)) = 0) + 1 \$(\sum(p, qcu.up(i,p)) \neq 0);$

$dt.up(i,j,k,p) = \max(EMAT, (th.up(i,k,p) - tc.lo(j,k,p)));$   
 $dt.lo(i,j,k,p) = EMAT;$   
 $dthul.up(j,p) = \max(EMAT, THUIN(j,p) - TCOUT(j,p));$   
 $dthul.lo(j,p) = EMAT;$   
 $dthur.up(j,p) = \max(EMAT, THUOUT(j,p) - tc.lo(j, 'K1', p));$   
 $dthur.lo(j,p) = EMAT;$   
 $dtcul.up(i,p) = \max(EMAT, th.up(i, 'KL', p) - TCUOUT(i,p));$   
 $dtcul.lo(i,p) = EMAT;$   
 $dteur.up(i,p) = \max(EMAT, THOUT(i,p) - TCUIN(i,p));$   
 $dteur.lo(i,p) = EMAT;$

$lmt.d.up(i,j,k,p) \$stage(k) = (dt.up(i,j,k,p) * dt.up(i,j,k+1,p) * (dt.up(i,j,k,p) + dt.up(i,j,k+1,p)) / 2) ** (1/3);$   
 $lmt.d.lo(i,j,k,p) \$stage(k) = (dt.lo(i,j,k,p) * dt.lo(i,j,k+1,p) * (dt.lo(i,j,k,p) + dt.lo(i,j,k+1,p)) / 2) ** (1/3);$   
 $lmt.dhu.up(j,p) = (dthur.up(j,p) * dthul.up(j,p) * (dthur.up(j,p) + dthul.up(j,p)) / 2) ** (1/3);$   
 $lmt.dhu.lo(j,p) = (dthur.lo(j,p) * dthul.lo(j,p) * (dthur.lo(j,p) + dthul.lo(j,p)) / 2) ** (1/3);$   
 $lmt.dcu.up(i,p) = (dtcul.up(i,p) * dteur.up(i,p) * (dtcul.up(i,p) + dteur.up(i,p)) / 2) ** (1/3);$   
 $lmt.dcu.lo(i,p) = (dtcul.lo(i,p) * dteur.lo(i,p) * (dtcul.lo(i,p) + dteur.lo(i,p)) / 2) ** (1/3);$

$area.up(i,j,k,p) \$stage(k) = q.up(i,j,k,p) / LMTD.lo(i,j,k,p) / U(i,j);$   
 $areahu.up(j,p) = qhu.up(j,p) / LMTDHU.lo(j,p) / UHU(j);$   
 $areacu.up(i,p) = qcu.up(i,p) / LMTDCU.lo(i,p) / UCU(i);$

//Assign bounding to parameters in logical constraint//

$GAMMA\_HX(i,j,k,p) = q.up(i,j,k,p);$   
 $GAMMA\_HU(j,p) = qhu.up(j,p);$   
 $GAMMA\_CU(i,p) = qcu.up(i,p);$

$TAU\_HX(i,j,k,p) = -th.lo(i,k,p)+tc.up(j,k,p)+dt.lo(i,j,k,p);$   
 $TAU\_HUL(j,p) = -THUIN(j,p)+TCOUT(j,p)+dthul.lo(j,p);$   
 $TAU\_HUR(j,p) = -THUOUT(j,p)+tc.up(j,'K1',p)+dthur.lo(j,p);$   
 $TAU\_CUL(i,p) = -th.lo(i,'KL',p)+TCUOUT(i,p)+dteul.lo(i,p);$   
 $TAU\_CUR(i,p) = -THOUT(i,p)+TCUIN(i,p)+dteur.lo(i,p);$

//Last stage forcing bound//

$q.fx(i,j,'KL',p) = 0;$   
 $z.fx(i,j,'KL') = 0;$   
 $lmtd.fx(i,j,'KL',p) = 0;$   
 $area.fx(i,j,'KL',p) = 0;$

#### EQUATIONS

$OVERALL\_H(i,p)$  overall energy balance of hot stream i for period p  
 $OVERALL\_C(j,p)$  overall energy balance of cold stream j for period p  
  
 $EBAL\_H(i,k,p)$  energy balance of hot stream i in stage k for period p  
 $EBAL\_C(j,k,p)$  energy balance of cold stream j in stage k for period p  
  
 $TIN\_H(i,p)$  assignment inlet temperature of hot stream i for period p  
 $TIN\_C(j,p)$  assignment inlet temperature of cold stream j for period p  
  
 $MONOT\_H(i,k,p)$  monotonic in temperature of hot stream i at location k for period p  
 $MONOT\_C(j,k,p)$  monotonic in temperature of cold stream j at location k for period p  
 $MONOT\_HU(j,p)$  monotonic in outlet temperature of cold stream j for period p  
 $MONOT\_CU(i,p)$  monotonic in outlet temperature of hot stream i for period p  
  
 $EBAL\_HU(j,p)$  energy balance of hot utility of cold stream j for period p  
 $EBAL\_CU(i,p)$  energy balance of cold utility of hot stream i for period p  
  
 $LOGIC\_HX(i,j,k,p)$  logical constraint to define z of match(i,j) at stage k for period p  
 $LOGIC\_HU(j,p)$  logical constraint to define zhu of cold stream j at stage k for period p  
 $LOGIC\_CU(i,p)$  logical constraint to define zcu of hot stream i at stage k for period p  
  
 $DTFEAS\_HXL(i,j,k,p)$  temperature feasibility of heat exchanger of match(i,j) at location k for period p  
 $DTFEAS\_HXR(i,j,k,p)$  temperature feasibility of heat exchanger of match(i,j) at location k+1 for period p

DTFEAS_HUL(j,p)	temperature feasibility of hot utility of outlet cold stream j for period p
DTFEAS_HUR(j,p)	temperature feasibility of hot utility of inlet cold stream j for period p
DTFEAS_CUL(i,p)	temperature feasibility of cold utility of inlet hot stream i for period p
DTFEAS_CUR(i,p)	temperature feasibility of cold utility of outlet hot stream i for period p
LOGMTD(i,j,k,p)	log mean temperature of match(i,j) at stage k for period p
LOGMTDHU(j,p)	log mean temperature of hot utility exchanger for period p
LOGMTDCU(i,p)	log mean temperature of cold utility exchanger for period p
A_HX(i,j,k,p)	area of heat exchanger of match(i,j) at stage k for period p
A_HU(j,p)	area of hot utility exchanger of cold stream j for period p
A_CU(i,p)	area of cold utility exchanger of hot stream i for period p
AMAX_HX(i,j,k,p)	maximum area of heat exchanger of match(i,j) at stage k for all period
AMAX_HU(j,p)	maximum area of hot utility exchanger of cold stream j for all period
AMAX_CU(i,p)	maximum area of cold utility exchanger of hot stream i for all period
FIXCOST	fixed cost
AREACOST	area cost
UTILITYCOST	utility cost
OBJ	objective function (total annualized cost)
;	
OVERALL_H(i,p)	.. (THIN(i,p) - THOUT(i,p)) * FCPH(i,p) = e= sum((j,k), q(i,j,k,p)) + qcu(i,p);
OVERALL_C(j,p)	.. (TCOUT(j,p) - TCIN(j,p)) * FCPC(j,p) = e= sum((i,k), q(i,j,k,p)) + qhu(j,p);
EBAL_H(i,k,p)\$stage(k)	.. (th(i,k,p) - th(i,k+1,p)) * FCPH(i,p) = e= sum(j, q(i,j,k,p));
EBAL_C(j,k,p)\$stage(k)	.. (tc(j,k,p) - tc(j,k+1,p)) * FCPC(j,p) = e= sum(i, q(i,j,k,p));
TIN_H(i,p)	.. THIN(i,p) = e= th(i, 'K1', p);
TIN_C(j,p)	.. TCIN(j,p) = e= tc(j, 'KL', p);
MONOT_H(i,k,p)\$stage(k)	.. th(i,k,p) = g= th(i,k+1,p);



```

UTILITYCOST      .. cost_utility =e=
                   sum(p,DOP(p)/TOP*(sum(j,CHU*qhu(j,p))))
                   + sum(p,DOP(p)/TOP*(sum(i,CCU*qcu(i,p))));

OBJ              .. TAC =e= cost_fix + cost_area + cost_utility;

model STAGEMODEL_SINGLEPERIOD /all/;

option iterlim=1e9;
option domlim=0;
option reslim=1e8;
STAGEMODEL_SINGLEPERIOD.optfile=0;

solve STAGEMODEL_SINGLEPERIOD using MINLP minimizing TAC;

display th.l,tc.l,
        z.l,zhu.l,zcu.l,
        q.l,qhu.l,qcu.l,
        area.l,areahu.l,areacu.l,
        area_max.l,areahu_max.l,areacu_max.l,
        dt.l,dthur.l,dthul.l,dtcul.l,dtcu.l,
        lmtd.l, lmtdhu.l, lmtdhu.l,
        cost_fix.l, cost_area.l, cost_utility.l, TAC.l
;

```

## CURRICULUM VITAE

**Name:** Ms. Parawinee Tangnanthanakan

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**University Education:**

2007–2011 Bachelor Degree of Chemical Engineering, Faculty of Engineering, Mahidol University, Nakhon Pathom, Thailand

**Proceedings:**

1. Tangnanthanakan, P.; Siemanond, K. (2014, April 22) Sequential and simultaneous approaches for multiperiod heat exchanger network synthesis. Proceedings of The 5<sup>th</sup> Research Symposium on Petrochemical, and Materials Technology and The 20<sup>th</sup> PPC Symposium on Petroleum, Petrochemicals, and Polymers, Bangkok, Thailand.
2. Tangnanthanakan, P.; Siemanond, K. (2014, August 17-21) Comparison of sequential and simultaneous approaches for multiperiod heat exchanger network synthesis and application for crude preheat train. Proceedings of the 17<sup>th</sup> Conference on Process Integration, Modelling and Optimisation for Energy Saving and Pollution Reduction, Prague, Czech Republic.