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APPENDICES

Appendix A Yields of Pyrolysis Products

Table A1 Yield of products obtained from pyrolysis

| Catalyst | Sample | Yield (wt.%) | | | |
|---------------|--------------|--------------|--------|-------|------|
| | | Gas | Liquid | Solid | Coke |
| Non-catalyst | Non-catalyst | 11.6 | 46.0 | 42.4 | 0.00 |
| Zeolite | HMOR | 11.9 | 43.8 | 41.6 | 2.60 |
| | KL | 12.2 | 43.5 | 41.5 | 2.79 |
| | HBeta | 9.62 | 43.3 | 41.6 | 5.41 |
| | HZSM-5 | 13.2 | 43.1 | 41.7 | 1.90 |
| Metal loading | 5%Co/HMOR | 11.4 | 43.8 | 41.8 | 3.01 |
| | 5%Co/KL | 12.7 | 41.4 | 42.5 | 3.37 |
| | 5%Co/HBeta | 12.9 | 40.3 | 41.6 | 5.20 |
| | 5%Co/HZSM-5 | 14.2 | 40.1 | 41.8 | 3.95 |
| | 5%Fe/HMOR | 13.3 | 42.4 | 42.4 | 1.89 |
| | 5%Fe/KL | 12.3 | 43.1 | 42.6 | 1.98 |
| | 5%Fe/HBeta | 11.4 | 43.1 | 42.1 | 3.44 |
| | 5%Fe/HZSM-5 | 16.4 | 38.8 | 41.9 | 2.94 |

Appendix B Gas Products

Table B1 Yield of gas components obtained from waste tire pyrolysis

| Catalyst | Methane | Ethylene | Ethane | Propylene | Propane | Mixed-C4 | Mixed-C5 |
|--------------|---------|----------|--------|-----------|---------|----------|----------|
| Non-catalyst | 20.3 | 9.38 | 15.9 | 12.2 | 9.06 | 19.6 | 13.5 |
| HMOR | 18.2 | 4.73 | 14.9 | 10.6 | 16.7 | 19.4 | 15.5 |
| KL | 19.5 | 6.70 | 15.9 | 12.4 | 9.13 | 19.9 | 16.4 |
| HBeta | 14.8 | 6.31 | 11.0 | 11.9 | 8.98 | 29.2 | 17.8 |
| HZSM-5 | 13.6 | 5.20 | 10.7 | 10.5 | 19.7 | 26.5 | 13.7 |
| 5%Co/HMOR | 21.0 | 7.38 | 16.3 | 11.5 | 10.2 | 19.5 | 14.2 |
| 5%Co/KL | 19.3 | 8.87 | 15.2 | 11.8 | 9.06 | 19.0 | 16.8 |
| 5%Co/HBeta | 16.5 | 8.08 | 13.2 | 12.6 | 8.52 | 25.1 | 16.1 |
| 5%Co/HZSM-5 | 15.8 | 7.09 | 12.5 | 15.5 | 11.6 | 24.2 | 13.4 |
| 5%Fe/HMOR | 20.7 | 7.59 | 16.7 | 11.3 | 11.1 | 18.0 | 14.5 |
| 5%Fe/KL | 20.4 | 9.34 | 16.1 | 12.4 | 9.11 | 19.1 | 13.5 |
| 5%Fe/HBeta | 19.53 | 9.02 | 15.2 | 12.3 | 8.62 | 20.1 | 15.3 |
| 5%Fe/HZSM-5 | 15.17 | 7.40 | 12.2 | 17.4 | 9.98 | 24.4 | 13.4 |

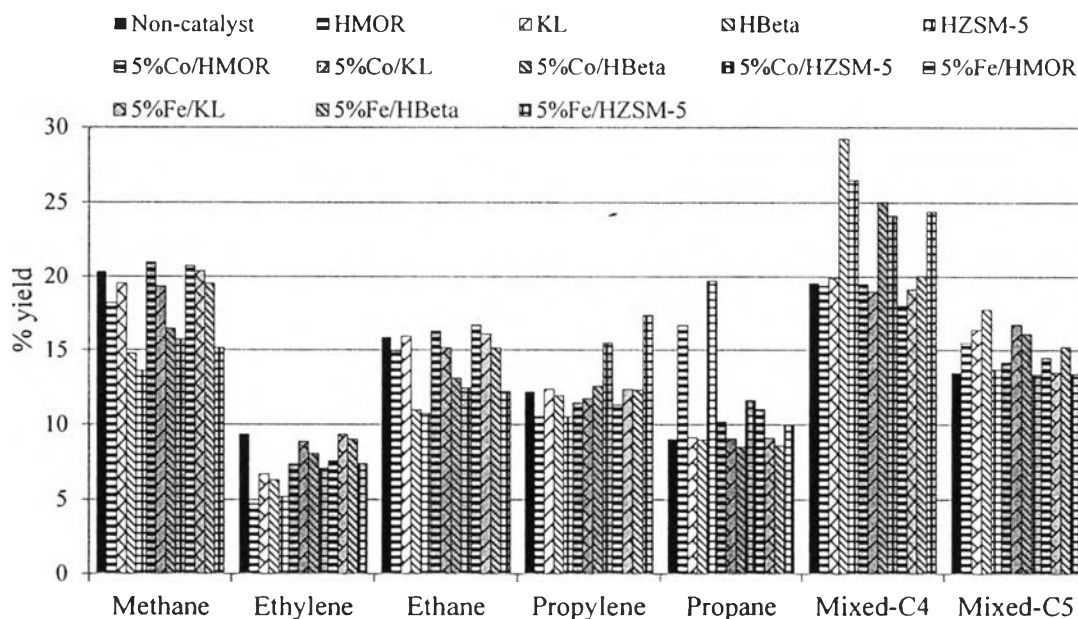


Figure B1 Distribution of gas components obtained from waste tire pyrolysis.

Appendix C Liquid Products

Table C1 Concentration of petroleum fractions in maltenes obtained from waste tire pyrolysis

| Catalysts | Fractions (wt.%) | | | | |
|--------------|--------------------|----------|---------------|---------------|--------------|
| | Full range naphtha | Kerosene | Light gas oil | Heavy gas oil | Long residue |
| Non-catalyst | 22.1 | 23.4 | 20.1 | 18.3 | 16.2 |
| HMOR | 31.7 | 21.5 | 16.9 | 17.5 | 12.5 |
| KL | 22.1 | 27.9 | 19.2 | 15.4 | 15.5 |
| HBeta | 38.6 | 22.0 | 19.1 | 10.1 | 10.4 |
| HZSM-5 | 28.2 | 21.5 | 17.3 | 18.8 | 14.3 |
| 5%Co/HMOR | 38.8 | 20.7 | 15.5 | 13.8 | 11.2 |
| 5%Co/KL | 44.6 | 19.5 | 12.5 | 11.0 | 12.3 |
| 5%Co/HBeta | 29.9 | 21.8 | 16.4 | 15.5 | 16.5 |
| 5%Co/HZSM5 | 37.5 | 23.1 | 16.2 | 14.1 | 9.11 |
| 5%Fe/HMOR | 42.8 | 19.4 | 14.3 | 12.6 | 10.9 |
| 5%Fe/KL | 44.7 | 19.7 | 13.6 | 15.6 | 6.36 |
| 5%Fe/HBeta | 32.8 | 20.7 | 16.5 | 15.5 | 14.6 |
| 5%Fe/HZSM5 | 46.4 | 21.1 | 12.3 | 11.1 | 9.11 |

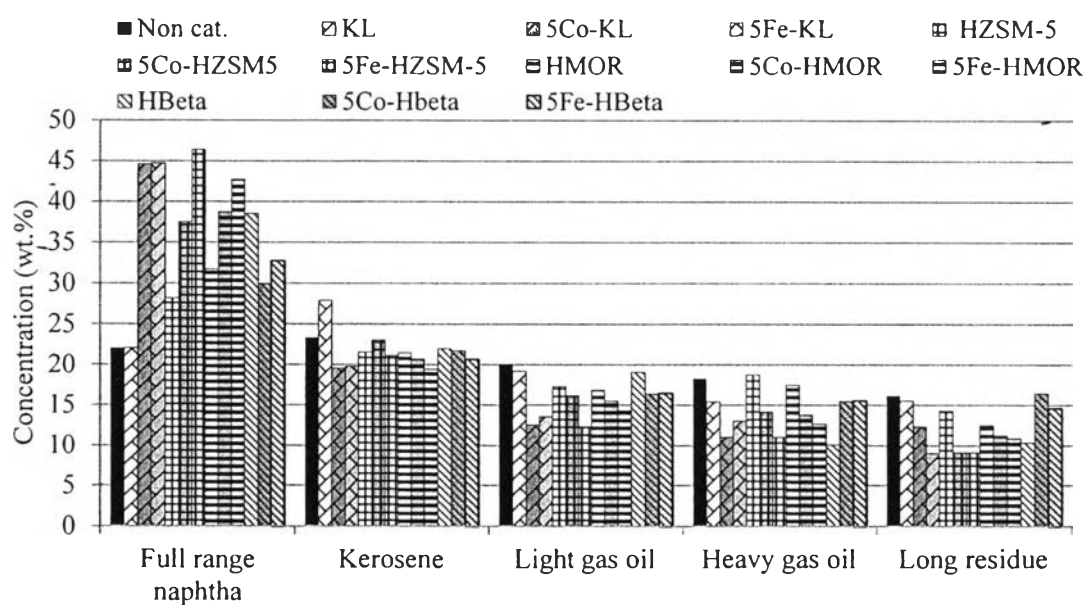


Figure C1 Concentration of petroleum fractions in maltenes obtained from using pure zeolites, 5%Co supported on zeolites, and 5%Fe-promoted catalysts.

Table C2 Concentration of chemical components in maltenes obtained from using pure zeolites (KL, HZSM-5, HMOR, and HBeta), 5%Co- and 5%Fe-promoted catalysts.

| Catalysts | Classification (wt.%) | | | |
|--------------|-----------------------|---------|------------|-----------|
| | Paraffins | Olefins | Naphthenes | Aromatics |
| Non-catalyst | 3.64 | 9.22 | 13.9 | 73.2 |
| KL | 3.81 | 10.3 | 11.7 | 74.2 |
| HZSM-5 | 1.77 | 16.9 | 14.7 | 66.6 |
| HBeta | 1.56 | 5.00 | 10.4 | 83.0 |
| HMOR | 2.90 | 8.50 | 11.7 | 76.9 |
| 5%Co/KL | 3.35 | 7.02 | 14.3 | 75.4 |
| 5%Co/HZSM-5 | 2.09 | 9.38 | 14.7 | 73.8 |
| 5%Co/HBeta | 2.99 | 9.03 | 12.0 | 76.0 |
| 5%Co/HMOR | 2.89 | 19.7 | 12.9 | 64.4 |
| 5%Fe/KL | 3.27 | 7.35 | 11.5 | 77.9 |
| 5%Fe/HZSM-5 | 1.69 | 12.27 | 14.1 | 72.0 |
| 5%Fe/HBeta | 3.66 | 3.58 | 8.79 | 84.0 |
| 5%Fe/HMOR | 4.53 | 2.96 | 12.3 | 80.2 |

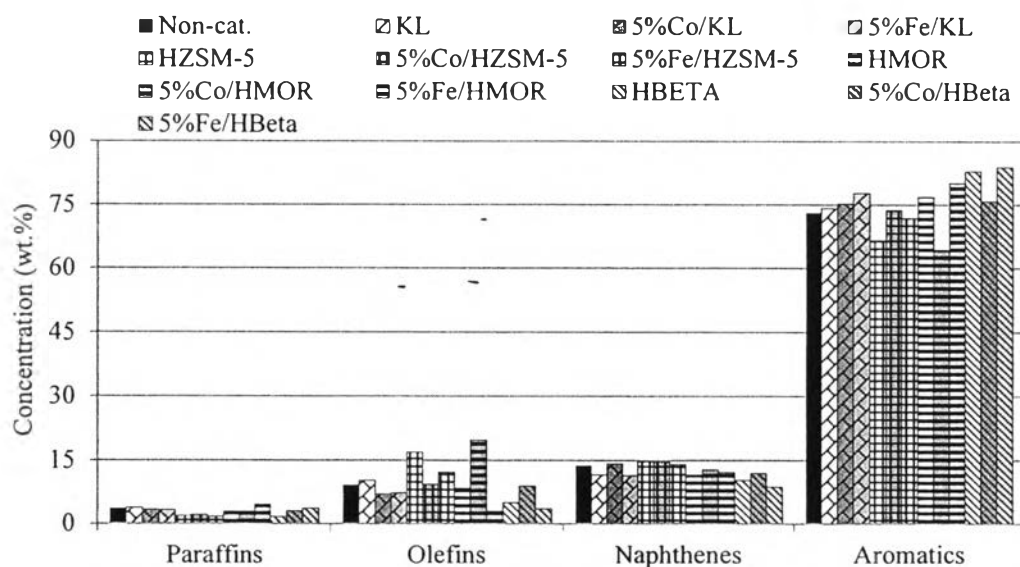


Figure C2 Concentration of chemical components in maltenes obtained from using pure zeolites (KL, HZSM-5, HMOR, and HBeta), 5%Co-, and 5% Fe-promoted catalysts.

Table C3 Concentration of chemical components in maltenes obtained from using pure zeolites, 5%Co- and 5%Fe-promoted catalysts

| Catalysts | Classification (wt.%) | | | | | | |
|------------|-----------------------|---------|------------|----------|--------|----------|-----------|
| | Paraffins | Olefins | Naphthenes | Mono-ar. | Di-ar. | Poly-ar. | Polar-ar. |
| Non-cat. | 3.64 | 9.22 | 13.9 | 34.9 | 10.2 | 15.4 | 7.74 |
| KL | 3.81 | 10.33 | 11.7 | 43.4 | 10.6 | 13.7 | 6.52 |
| HZSM-5 | 1.77 | 16.93 | 14.7 | 33.1 | 16.6 | 11.2 | 5.71 |
| HBeta | 1.56 | 5.00 | 10.4 | 45.2 | 18.3 | 12.9 | 6.53 |
| HMOR | 2.90 | 8.50 | 11.7 | 46.1 | 10.4 | 11.4 | 9.08 |
| 5%Co/KL | 3.35 | 7.02 | 14.3 | 51.8 | 8.81 | 8.03 | 6.70 |
| 5%Co/HZSM5 | 2.09 | 9.38 | 14.7 | 43.5 | 12.8 | 10.3 | 7.23 |
| 5%Co/HBeta | 2.99 | 9.03 | 12.0 | 42.0 | 13.3 | 12.1 | 8.56 |
| 5%Co/HMOR | 2.90 | 19.8 | 12.9 | 37.0 | 10.3 | 10.4 | 6.67 |
| 5%Fe/KL | 3.27 | 7.35 | 11.5 | 52.2 | 10.1 | 8.58 | 6.97 |
| 5%Fe/HZSM5 | 1.69 | 12.3 | 14.1 | 45.4 | 11.9 | 8.50 | 6.22 |
| 5%Fe/HBeta | 3.66 | 3.58 | 8.79 | 48.3 | 11.3 | 15.5 | 8.92 |
| 5%Fe/HMOR | 4.53 | 2.96 | 12.3 | 54.7 | 7.36 | 10.4 | 7.76 |

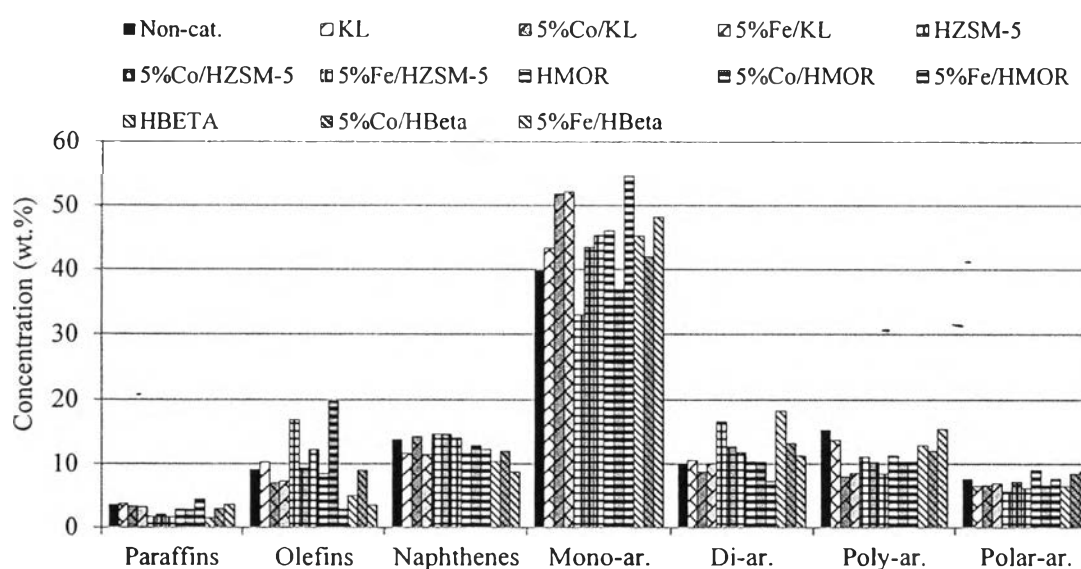


Figure C3 Concentration of chemical components in maltenes obtained from using pure zeolites, 5%Co-, and 5%Fe-promoted catalysts.

Table C3 Yield of chemical components in maltenes obtained from waste tire pyrolysis

| Catalysts | wt.% in maltenes | | | | | | | | |
|--------------|------------------|---------|--------------|------------------|------------------|------------------|---------|-------------|--------|
| | Benzene | Toluene | Ethylbenzene | <i>m</i> -xylene | <i>o</i> -xylene | <i>p</i> -xylene | Styrene | Cyclohexane | Cumene |
| Non-catalyst | 0.430 | 0.0274 | 0.833 | - | - | - | 0.189 | 0.0239 | 0.0660 |
| HMOR | 0.124 | 0.184 | 0.408 | 0.185 | - | - | 1.31 | - | 0.105 |
| HBeta | 4.81 | 0.917 | 3.31 | - | 0.161 | 0.129 | 0.320 | 1.05 | 0.0771 |
| HZSM-5 | - | 0.196 | 0.258 | 0.0981 | - | 0.0304 | 0.207 | 3.46 | 0.035 |
| KL | 0.265 | 0.00497 | 0.102 | - | - | - | 0.125 | - | 0.0827 |
| 5%Co/HMOR | - | 0.197 | 0.280 | - | - | 0.0831 | 0.396 | 3.78 | 0.280 |
| 5%Co/HBeta | 0.284 | 0.00540 | 0.00352 | - | - | - | - | 0.0394 | - |
| 5%Co/HZSM5 | 4.21 | 0.108 | 0.132 | - | 0.123 | 0.451 | 0.313 | 0.972 | 0.144 |
| 5%Co/KL | 9.99 | 3.79 | 0.311 | 0.994 | - | - | 0.891 | 2.43 | 0.717 |
| 5%Fe/HMOR | 14.0 | 0.053 | 0.833 | - | - | 0.284 | - | 7.17 | 0.882 |
| 5%Fe/HBeta | - | 0.0945 | 0.867 | - | 0.234 | 0.253 | 0.464 | 4.12 | 0.506 |
| 5%Fe/HZSM5 | 3.41 | 0.652 | 0.403 | 0.835 | 0.0105 | 0.044 | 0.602 | 4.11 | 1.09 |
| 5%Fe/KL | 12.7 | 1.19 | - | 0.392 | - | 0.210 | 0.464 | 3.28 | 0.682 |

Appendix D Sulfur Contents in Pyrolysis Products

| | Sulfur in oil (wt.%) | | | |
|--------------|----------------------|------|------|------|
| | Spent catalyst | Char | Oil | Gas |
| Non-catalyst | - | 45.4 | 23.9 | 30.7 |
| KL | 2.77 | 46.8 | 19.7 | 30.7 |
| HZSM-5 | 2.99 | 46.4 | 20.7 | 29.9 |
| HBeta | 4.55 | 45.0 | 21.2 | 29.3 |
| HMOR | 2.00 | 42.0 | 21.0 | 35.0 |
| 5%Co/KL | 8.13 | 43.8 | 15.7 | 32.3 |
| 5%Co/HZSM-5 | 12.3 | 42.9 | 15.3 | 29.5 |
| 5%Co/HBeta | 11.3 | 42.5 | 15.6 | 30.6 |
| 5%Co/HMOR | 8.16 | 43.1 | 19.3 | 29.5 |
| 5%Fe/KL | 10.3 | 43.0 | 17.6 | 29.2 |
| 5%Fe/HZSM-5 | 13.7 | 44.5 | 12.5 | 29.3 |
| 5%Fe/HBeta | 11.03 | 46.1 | 19.0 | 23.9 |
| 5%Fe/HMOR | 10.6 | 43.2 | 17.1 | 29.1 |

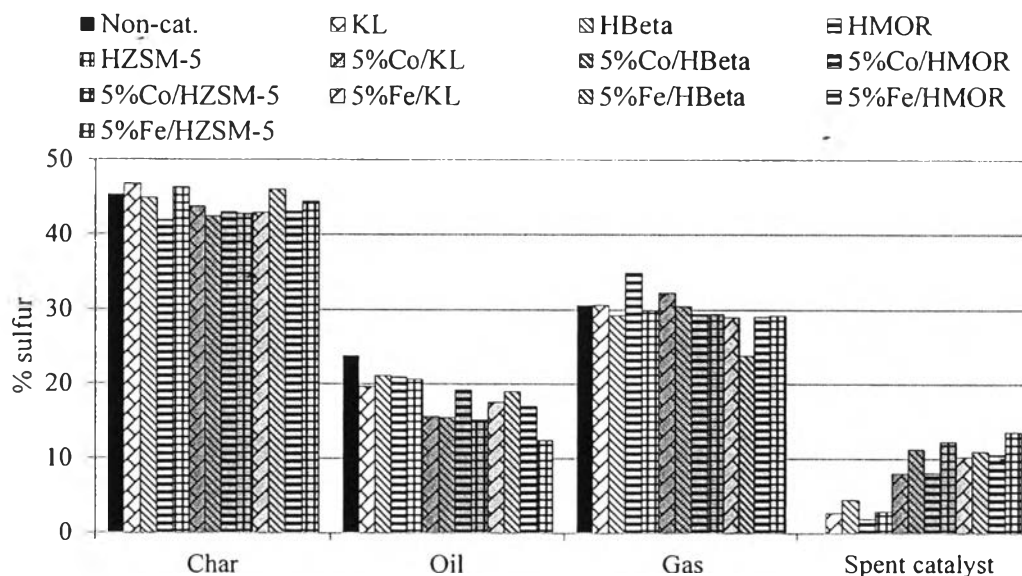


Figure D1 Distribution of sulfur in pyrolysis products obtained from using, pure zeolites (KL, HZSM-5, HMOR, and HBeta), 5%Co-, and 5%Fe-promoted catalysts.

Appendix E Surface Area and Pore Volume of Catalysts

Table E1 Catalyst properties obtained from surface area analyzer

| Catalyst | Surface area (m²/g) | Pore volume (cm³/g) | Maximum pore width (Å) | Median pore width (Å) |
|--------------------|---|--|---------------------------------------|--------------------------------------|
| HBeta | 539.3 | 0.2570 | 8.148 | 8.351 |
| HMOR | 394.3 | 0.1990 | 8.392 | 8.422 |
| HZSM-5 | 366.3 | 0.1780 | 7.774 | 7.443 |
| KL | 218.0 | 0.1130 | 6.954 | 7.078 |
| 5%Co/HBeta | 434.2 | 0.2422 | 7.137 | 7.277 |
| 5%Co/HMOR | 361.8 | 0.1821 | 7.553 | 7.421 |
| 5%Co/HZSM-5 | 310.3 | 0.2245 | 5.907 | 6.188 |
| 5%Co/KL | 114.1 | 0.0570 | 6.426 | 6.275 |
| 5%Fe/HBeta | 405.8 | 0.2339 | 6.589 | 8.112 |
| 5%Fe/HMOR | 351.7 | 0.1764 | 6.498 | 6.942 |
| 5%Fe/HZSM-5 | 265.0 | 0.1309 | 6.815 | 6.956 |
| 5%Fe/KL | 98.82 | 0.04700 | 6.618 | 7.006 |

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Proceedings:

1. Muenpol, S.; and Jitkarnka, S. Effect of Zeolitic Support Properties on Sulfur Species and Distribution in Tire-derived Products. Proceedings of The 5th Research Symposium on Petroleum, Petrochemicals, and Advanced Materials and the 20th PPC Symposium on Petroleum, Petrochemicals, and Polymers, Bangkok, Thailand.
2. Muenpol S.; and Jitkarnka S. (2014, August 23 - 27) Impact of Zeolite Channel Structure on Structure of Hydrocarbon Compounds and Petrochemicals in Waste Tyre-derived Oils. The 17th Conference Process Integration, Modelling and Optimisation for Energy Saving and Pollution Reduction (PRES 2014), Prague, Czech Republic.

Presentation:

1. Muenpol, S.; and Jitkarnka, S. (2014, April 22) Effect of Zeolitic Support Properties on Sulfur Species and Distribution in Tire-derived Products. Paper presented at The 5th Research Symposium on Petroleum, Petrochemicals, and Advanced Materials and the 20th PPC Symposium on Petroleum, Petrochemicals, and Polymers, Bangkok, Thailand.