



REFERENCES

ศูนย์วิทยทรัพยากร
จุฬาลงกรณ์มหาวิทยาลัย

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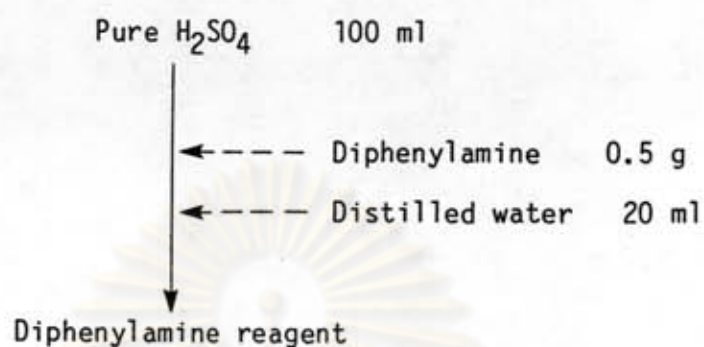
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APPENDIXS

ศูนย์วิทยทรัพยากร
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Appendix A : The Preparation of Diphenylamine Reagent.



This reagent is used to test the existence of NO_3^- in the test solution. Fill a few amount of this reagent into the tube and then slowly drop the test solution in the same tube. If NO_3^- exists in test solution, the layer between these two solutions turns to blue. This reagent can also test the existence of NO_2^- and ClO_3^- .

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Appendix B : The Preparation of Copper Nitrate Solution
for the Synthesis of Catalyst.

$$\begin{aligned} \text{Cu(NO}_3)_2 \cdot 3\text{H}_2\text{O} \text{ molecular weight} &= 241.6 \\ \text{CEC of Na-Laponite} &= 80 \text{ meq./100 g-cat.} \\ &= 0.8 \text{ mmol Na}^+/\text{1 g-cat.} \\ &= 4.0 \text{ mmol Na}^+/\text{5 g-cat.} \end{aligned}$$

Since 2 Na⁺ will be exchanged with Cu²⁺ then for 100% ion exchange,
the needed amount of Cu²⁺ = 2.0 mmol Na⁺/5 g-cat.
so, needed amount of Cu(NO₃)₂·3H₂O = (2.0 × 10⁻³)(241.6)
= 0.4832 g

For Cu²⁺ 0.01 N = 0.01 mol Cu²⁺/ 2000 ml H₂O

For various degrees of ion exchange, various concentrations of copper nitrate solution are prepared as follows :

Degree of ion exchange(%)	Amount of Cu ²⁺ (mol)	Weight of Cu(NO ₃) ₂ ·3H ₂ O (g)	H ₂ O (ml)
200	4.0 × 10 ⁻³	0.9664	800
150	3.0 × 10 ⁻³	0.7248	600
120	2.4 × 10 ⁻³	0.5798	480
100	2.0 × 10 ⁻³	0.4832	400
75	1.5 × 10 ⁻³	0.3624	300
50	1.0 × 10 ⁻³	0.2416	200

Appendix C : The Analysis Condition of Gas Chromatograph (GC)A. GC (12)

Analyzing column : stainless steel tube 3x4 mm o.d.
packed with porapac Q 2 m and porapac T 1 m

Reference column : stainless steel tube 3x4 mm o.d.
packed with porapac Q 3 m

Analyzing temperature : 100 °C

Carrier gas : H₂

Carrier gas flow rate : 40 ml/min

Analyzing products : N₂ , CO , CO₂ , H₃COCH₃ , HCOOCH₃ and CH₃OH

B. GC (13)

Analyzing column : stainless steel tube 3x4 mm o.d.
packed with active carbon

Reference column : stainless steel tube 3x4 mm o.d.
packed with active carbon

Analyzing temperature : 100 °C

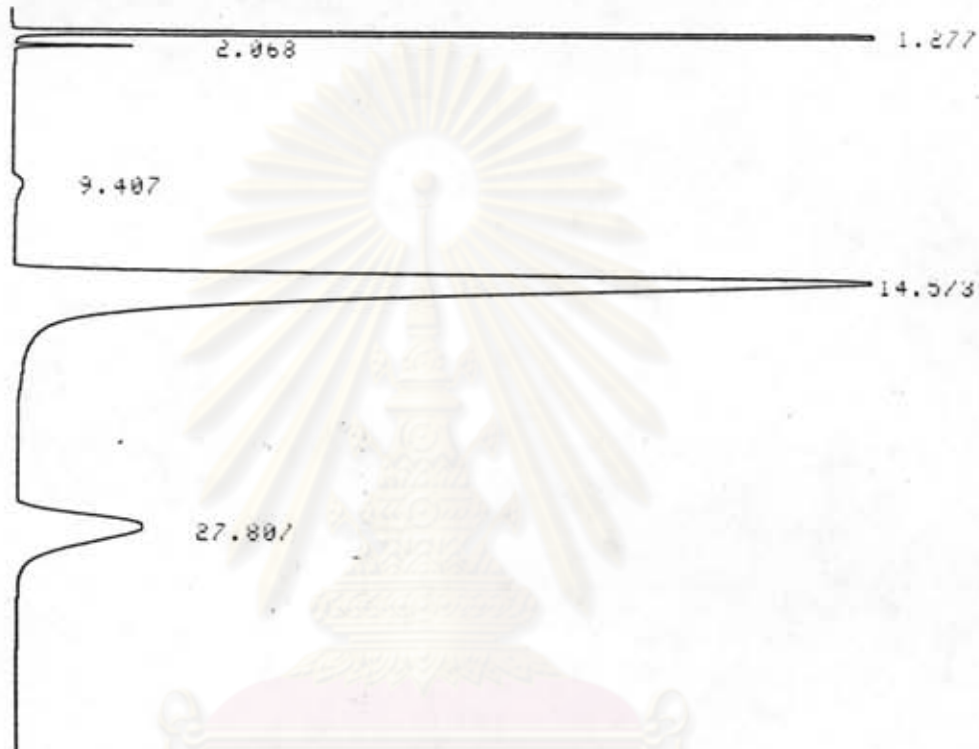
Carrier gas : Ar

Carrier gas flow rate : 40 ml/min

Analyzing products : H₂ , N₂ , CO , CO₂ and CH₄

Appendix D : Raw Data from GC , Data Sheet and the Calculation of Catalytic Activity and Selectivity

START 1



C-R2AX
CHANNEL 1
SAMPLE NO 0
REPORT NO 369

FILE 0
METHOD 41

PKNO	TIME	AREA	MK	IDNO	CONC	NAME
1	1.277	253050			56.8398	
2	2.068	1703			0.3825	
3	9.407	1131			0.254	
4	14.573	159331			35.7887	
5	27.807	29984			6.735	
TOTAL		445199			100	



DEHYDROGENATION OF METHANOL

DATE / / EXPT. NO.
 CATALYST (NO) WEIGHT OF CATALYST g.
 REACTION TEMP. °C TREATMENT TEMP. °C
 W/F g.cat-min/mol MeOH INPUT(x) mol/min
 $Y = 757778.6X + 148.5837$ (y=dial) DIAL
 $N_2 : MeOH = 5:2$ at 273 K N_2 FLOW RATE = mol/min
 (°C) = sec/10cc
 OUT GAS FLOW RATE sec/10 cc = cc/min at °C
 = mol/min at 273 K

	<u>PA</u>	<u>Z COMPOSITION</u>	<u>FLOW RATE (mol/min) at 273 K</u>
AIR	<u> </u>	<u> </u>	<u> </u>
H ₂	<u> </u>	<u> </u>	<u> </u>
N ₂	<u> </u>	<u> </u>	<u> </u>
CO	<u> </u>	<u> </u>	<u> </u>
CH ₄	<u> </u>	<u> </u>	<u> </u>
CO ₂	<u> </u>	<u> </u>	<u> </u>

	<u>PA</u>	<u>MF</u>	<u>PA'</u>	<u>PA' fraction</u>	<u>FLOW RATE</u>
N ₂ + CO	<u> </u>	<u> </u>	N ₂	<u> </u>	<u> </u>
CO ₂	<u> </u>	<u> </u>		<u> </u>	<u> </u>
H ₂ O	<u> </u>	<u> </u>		<u> </u>	<u> </u>
H ₃ COCH ₃	<u> </u>	<u> </u>		<u> </u>	<u> </u>
CH ₃ OH	<u> </u>	<u> </u>		<u> </u>	<u> </u>
HCOOCH ₃	<u> </u>	<u> </u>		<u> </u>	<u> </u>

$$\begin{aligned} \text{TOTAL C OUTPUT} &= \text{_____ mol/min} \\ \text{TOTAL C INPUT} &= \text{_____ mol/min} = \text{CH}_3\text{OH INPUT} = (\text{TOTAL H}_2 \text{ INPUT}) \\ \text{TOTAL H}_2 \text{ OUTPUT} &= \text{_____ mol/min} \end{aligned}$$

$$\text{C BALANCE} = \frac{(\text{total C output})}{(\text{total C input})} \times 100 = \text{_____} \times 100 = \text{_____} \%$$

$$\text{H}_2 \text{ BALANCE} = \frac{(\text{total H}_2 \text{ output})}{2(\text{total H}_2 \text{ input})} \times 100 = \text{_____} \times 100 = \text{_____} \%$$

C-MOLE BASIS

$$\text{CH}_3\text{OH INPUT} = \text{_____ mol/min} = \text{TOTAL C OUTPUT}$$

$$\text{CH}_3\text{OH OUTPUT} = \text{_____ mol/min}$$

$$\text{CH}_3\text{OH REACTED} = \text{_____ mol/min}$$

$$\% \text{ CONVERSION} = \frac{(\text{CH}_3\text{OH reacted})}{(\text{CH}_3\text{OH input})} \times 100 = \text{_____} \times 100 = \text{_____} \%$$

$$\% \text{ SEL. HCOOCH}_3 = \frac{2(\text{HCOOCH}_3)}{\text{CH}_3\text{OH reacted}} \times 100 = \text{_____} \times 100 = \text{_____} \%$$

$$\% \text{ SEL. CO} = \frac{\text{CO}}{\text{CH}_3\text{OH reacted}} \times 100 = \text{_____} \times 100 = \text{_____} \%$$

$$\% \text{ SEL. CO}_2 = \frac{(\text{CO}_2)}{\text{CH}_3\text{OH reacted}} \times 100 = \text{_____} \times 100 = \text{_____} \%$$

$$\% \text{ SEL. H}_3\text{COCH}_3 = \frac{2(\text{H}_3\text{COCH}_3)}{\text{CH}_3\text{OH reacted}} \times 100 = \text{_____} \times 100 = \text{_____} \%$$

Appendix E : Calculations of Surface Area

1. Calculation of amount of He introduce

$$\frac{(p/760) v_m}{273.15 + t} = \frac{(760/760) V_{He}}{273.15} \quad (1)$$

$$\bar{V}_{He} = \frac{273.15}{273.15 + t} \cdot \frac{p}{760} \cdot v_m \quad (2)$$

where p = the difference in the level of Hg in manometer (mmHg)

v_m = volume of mercury ball and glass line (ml)

t = room temperature ($^{\circ}\text{C}$)

2. Calculation of dead volume

$$\frac{(p/760)(\bar{V}_0 + v_m)}{273.15 + t} = \frac{(760/760) \bar{V}_{He}}{273.15} \quad (3)$$

$$\bar{V}_0 = \left[\frac{273.15 + t}{273.15} \cdot \frac{760}{p} \right] \cdot \bar{V}_{He} - v_m \quad (4)$$

3. Calculation of amount of N_2 introduce

$$\bar{V}_{\text{N}_2} = \frac{273.15}{273.15 + t} \cdot \frac{p}{760} \cdot v_m \quad (5)$$

4. Calculation of amount of N_2 adsorbed on catalyst

$$\frac{(p/760)(\bar{V}_0 + v_m)}{273.15 + t} = \frac{(760/760) \bar{V}}{273.15} \quad (6)$$

$$\bar{V} = \frac{273.15}{273.15 + t} \cdot \frac{p}{760} \cdot (\bar{V}_0 + v_m) \quad (7)$$

Since \bar{V} is the amount of N_2 free from adsorption

Therefore the amount of N_2 adsorption is calculated from

$$\text{amount of } N_2 \text{ adsorption} = \bar{V}_{N_2} - \bar{V} \quad (8)$$

5. Calculation of specific surface area

5.1 BET equation (multilayer adsorption)

$$\frac{p}{V(p_0 - p)} = \frac{1}{v_n \cdot c} + \frac{(c-1) \cdot p}{v_n \cdot c \cdot p_0} \quad (9)$$

where v_n = amount of N_2 adsorbed in multilayer

c = constant

p_0 = vapor pressure of adsorbed gas at adsorption temperature (760 mmHg)

p = adsorption equilibrium pressure (the difference of manometer in equation 7)

V = amount of N_2 free from adsorption (equation 7)

Then, the value of $[p/V(p_0 - p)]$ and p/p_0 are calculated and

Calculate the value of slope = $\frac{(c-1)}{v_n \cdot c}$ and

$$\text{y-intercept} = \frac{p}{V(p_0 - p)}$$

by using the method of linear regression analysis.

Since, the total surface area (S) = $(t \times 10^{-20}) \cdot v_n \cdot (6.02 \times 10^{23})$
 $\frac{22400}{}$

$$S = 0.269 \ t \ v_n$$

where t = space of one molecular adsorption

at $-195.8 \text{ }^\circ\text{C}$ $t = 16.2 / A^{0.2}$

Then $S = 4.35 \ v_n$

Since $S_{\text{silica wool}} = 6.27 \text{ m}^2/\text{g}$

Finally, specific surface area of catalyst : S_0 is calculated

$$S_0 = \frac{S - 6.27(\text{wt. of silica wool})}{\text{wt. of catalyst}}$$

If the adsorption is in monolayer form, the Langmuir equation is used.

5.2 Langmuir equation (monolayer adsorption)

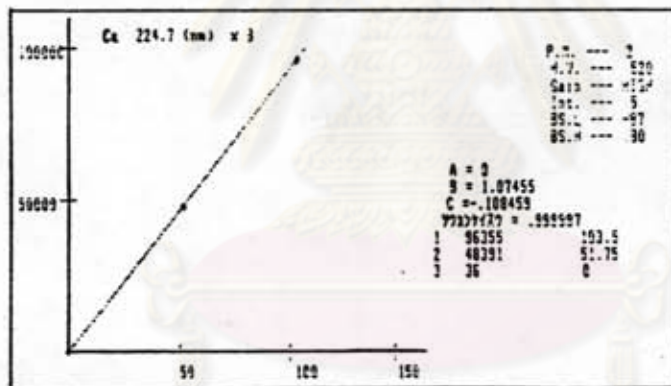
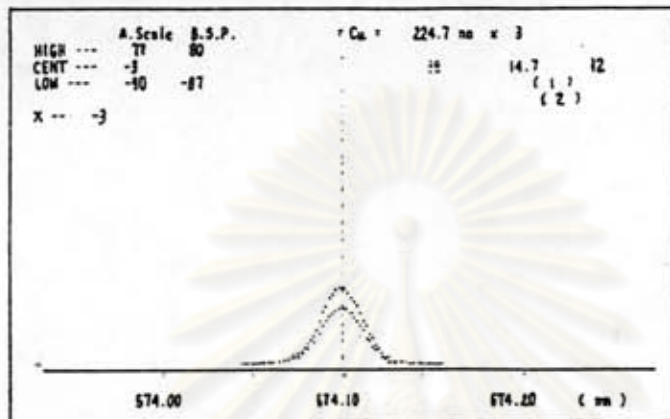
$$\frac{P}{V} = \frac{1}{a \cdot b} + \frac{1}{b} \cdot P$$

where P = adsorption equilibrium pressure (the difference in manometer from equation 7)

V = amount of N_2 free from adsorption

a, b = constant

Appendix F : Data of ICP Measurements



Command (I,2,M,P,K,R,F,C,+) : ?

LAPONITE-1

No.	Lower	Center	Higher	Conc	Conc (ppm)
1	136	141	133	6.56287	-101407
2	134	140	132	7.04192	-100893

平均: 6.8024
 標準偏差: 0.2395
 變動係數%: 3.521
 試料濃度 = <0 ppm 試料採放量 = .2015 校核量 = 100 奇次率 = 495.278

CU-LAPONITE

No.	Lower	Center	Higher	Conc	Conc (ppm)
1	783	74344	795	73554.7	78.3217
2	784	73846	791	73058.3	78.1953

平均: 73306.6
 標準偏差: 248.2
 變動係數%: 0.3386
 試料濃度 = 3.852% 試料採放量 = .2042 校核量 = 100 奇次率 = 489.716



Appendix G : The Calculations of Average Electronegativity

The Sanderson Electronegativity Principle ^{a)}

Electronegativity is usually defined as the power of an atom to attract electrons independently of the chemical composition of the compound to which the atom belongs. In a molecule with atoms of different electronegativity, the electrons will be redistributed such that they will be equally attracted to the nuclei in the bond. This constitutes Sanderson's electronegativity equalization principle. This intermediate electronegativity (S) is postulated to be the geometric mean of the compound atoms of the molecule under consideration. Using the Sanderson electronegativity scale, the partial charge on the atoms of a chemical compound can be calculated as well as its average electronegativity. For a compound $X_xY_yZ_z$, this intermediate electronegativity is

$$S = (S_X^x S_Y^y S_Z^z)^{1/(x+y+z)} \quad (1)$$

Calculations of Average Electronegativity

A. Laponite

The chemical formula of Laponite is $\text{Na}_x\text{Mg}_{6-x}\text{Li}_x(\text{Si}_8\text{O}_{20})(\text{OH})_4$

The amount of Na ions in Laponite = 1.1639 mmol/g-cat. ^{b)}
= 0.0268 g/g-cat.

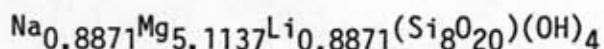
equal to

$$\frac{x\text{Na}}{x\text{Na} + (6-x)\text{Mg} + x\text{Li} + 8\text{Si} + 20(\text{O}) + 4(\text{OH})} = 0.0268$$

substitution with molecular weight : Na = 23 , Al = 27 , Mg = 24,
Si = 28 , O = 16 , OH = 17 and Li = 7

Thus, $x = 0.8871$

then, the chemical formula of Laponite is



Substitution this formula with electronegativity of each element :

$$H^+ = 2.1, Al = 1.5, Mg = 1.2, Si = 1.8, O = 3.5 \text{ and } Li = 1.0$$

Then, calculation of average electronegativity of Laponite using (1)

$$S = 2.50$$

B. Montmorillonite

The chemical formula of Montmorillonite is $\text{Na}_x\text{Al}_{4-x}\text{Mg}_x(\text{Si}_8\text{O}_{20})(\text{OH})_4$

$$\begin{aligned} \text{The amount of Na ions in Montmorillonite} &= 1.4538 \text{ mmol/g-cat. } ^b) \\ &= 0.0334 \text{ g/g-cat.} \end{aligned}$$

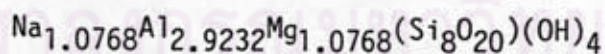
equal to

$$\frac{x\text{Na}}{x\text{Na} + (4-x)\text{Al} + x\text{Mg} + 8\text{Si} + 20(\text{O}) + 4(\text{OH})} = 0.0334$$

substitution with molecular weight

Thus, $x = 1.0768$

then, the chemical formular of Montmorillonite is



Substitution this formula with electronegativity of each element

Then, calculation of average electronegativity of Montmorillonite by using (1)

Then, $S = 2.64$

a) Catalytic Reviews : Science and Engineering, Vol.24, No.3, 1982:418

b) Data from ICP measurements.

Appendix H : Data of Thermal Gravimetric (TG) Analysis

Table 4-8 Amount of H₂O desorped from various degrees of ion exchanged of Cu-Lapo at treatment temperature of 800°C

Catalyst	Amount of H ₂ O desorped (g/g-cat.)
Cu-Lapo 200	0.1577
Cu-Lapo 150	0.1446
Cu-Lapo 120	0.1498
Cu-Lapo 100	0.1774
Cu-Lapo 50	0.1426
Na-Laponite	0.1543

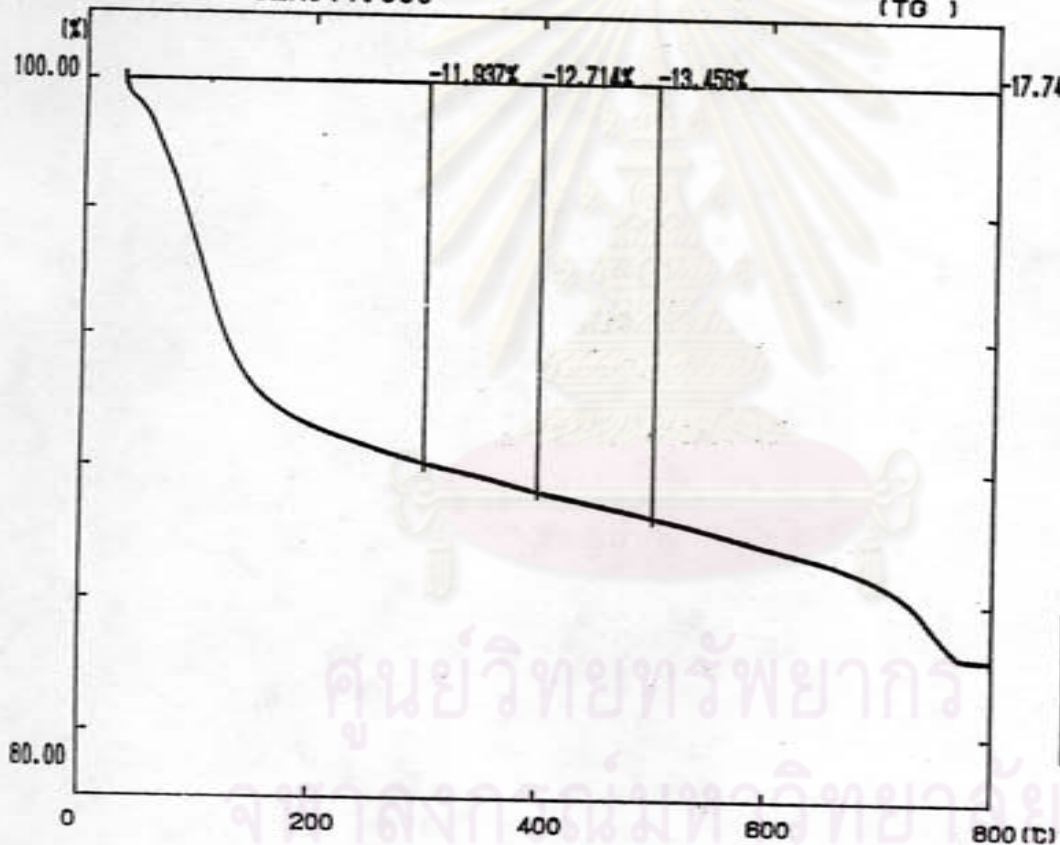
ศูนย์วิทยทรัพยากร
จุฬาลงกรณ์มหาวิทยาลัย

THERMAL ANALYSIS DATA

DATE 88/12/01

FILE NAME SEX011.000

(TG)



MEASURING CONDITIONS

SAMPLE NAME Cu/Inps100

SAMPLE SIZE 41.200mg

SAMPLING INT 1.000

ACQUIS DATE 88/12/01

HEATING PROGRAM

RATE	TEMP	TIME
1	10	800

COMMENT

MEMO

SHIMADZU CORP.

APPENDIX I : The details of calculation for amount of Na⁺ and Cu²⁺ ions base on dry catalyst.

Catalyst	Amount of H ₂ O ^{a)} desorption (g/g-cat.)	Amount of ions ^{b)}		Amount of ions ^{c)}	
		Cu ²⁺ (mmol/g-cat.)	Na ⁺ (mmol/g-cat.)	Cu ²⁺ (mmol/g-cat.)	Na ⁺ (mmol/g-cat.)
Cu-Lapo 200	0.1577	0.5921	0.0694	0.7030	0.0824
Cu-Lapo 150	0.1446	0.5188	0.0908	0.6065	0.1062
Cu-Lapo 120	0.1498	0.4563	0.1180	0.5367	0.1388
Cu-Lapo 100	0.1774	0.2907	0.2098	0.3534	0.2551
Cu-Lapo 50	0.1426	0.1984	0.4008	0.2314	0.4675
Na-Laponite	0.1543	-	0.9846	-	1.1643

a) data from TG measurements

b) data from ICP measurements

c) calculation base on dry catalyst.

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Miss Chatsuda Pantawong was born on December 20, 1964 in Bangkok, Thailand. In 1986, she received the Bachelor Degree of Science, major in Chemical Engineering from the Faculty of Science, Chulalongkorn University. After graduation, she continued her study for Master Degree in the field of Petrochemical Technology at The College of Petroleum and Petrochemistry, Chulalongkorn University. In 1987, she was one of the representatives from Thailand participated in The Ship for Southeast Asian Youth Program for about 2 months. Since September 1988, during her study for Master Degree, she got the scholarship from Waseda University, Japan as a research student there for 2 years. By the end of this year, after her graduation, she will get the industrial training in Japan for a period of time and in the near future she will go back to work in the Petrochemical Industry in Thailand.

ศูนย์วิทยทรัพยากร

March, 1990.

จุฬาลงกรณ์มหาวิทยาลัย