

## REFERENCES

- American Gas Association. Gas engineers handbook. New York : Industrial press., 1965.
- Bird, R. B.; Stewart, W. E.; and Lightfoot, E. N. Transport phenomena. New York : John Wiley & sons, 1960.
- Carleton, F. B. ; Kershenbaum, L. S. ; and Kakeham, W. A. Adsorption in non-isobaric fixed-beds. Chem. Eng. Sci. 33 (1978) : 1239-1246.
- Chen, Y. D. , and Yang, R. T. Predicting binary Fickian diffusivities from pure-component Fickian diffusivities for surface diffusion. Chem. Eng. Sci. 47 (1992) : 3895-3905.
- Chiang, A. S. ; Dixon, A. G. ; and Ma, Y. H. The determination of zeolite crystal diffusivity by gas chromatography. Chem. Eng. Sci. 39 (1984) : 1451-1468.
- Choudhary, V. R. and Srinivasan, K. R. Sorption of benzene in H-ZSM-5 at catalytic conditions using gas chromatographic sorption/desorption technique. Chem. Eng. Sci. 42 (1987) : 382-385.

Eic, M. and Ruthven, D. M. A new experimental technique for measuring intracrystalline diffusivities in zeolites. Zeolites 8 (1988) : 40

Gamba, G. ; Paludetto, R. ; Carra, S. ; and Morbidelli, M. Adsorption equilibria of nonideal multicomponent systems at saturation. AIChE J. 36 (1990) : 1736-1742.

Guo, C. J. ; Talu, O. ; and Hayhurst, D. T. Phase transition and structural heterogeneity ; benzene adsorption on zeolite. AIChE J. 35 (1989) : 573-578.

Haynes, H. W. and Sarma, P. N. Model for the application of gas chromatography to measurements of diffusion in bidisperse structured catalysts. AIChE J. 19 (1973) : 1043-1046.

Huften, J. R. and Danner, R. P. Chromatographic study of alkanes in silicalite. AIChE J. 39 (1993) : 954-974.

Humphrey, J. L. Separation processes : playing a critical role. Chem. Eng. Progress 91 (October, 1995) : 31-41.

Keller II, G. E. Adsorption : building upon a solid foundation. Chem. Eng. Progress 91 (November, 1995) : 56-67.

- Kershenbaum, L. S. and Kohler, M. A. Adsorption in non-isobaric fixed-bed-II : measurements of rates of adsorption. Chem. Eng. Sci. 39 (1984) : 1423-1426.
- Li, J. and Talu, O. Adsorption equilibrium of benzene-p-xylene vapor mixture on silicalite. Chem. Eng. Sci. 49 (1994) : 189-197.
- Mantell, C. L. Adsorption. New York : McGraw-Hill, 1951.
- Masuda, T. ; Fukada, K. ; Fujikata, Y. ; Ikeda, H. ; and Hashimoto, K. Measurement and prediction of the diffusivity of Y-type zeolite. Chem. Eng. Sci. 51 (1996) : 1879-1888.
- McCabe, W. L.; Smith, J. C.; and Harriott, P. Unit operations of chemical engineering. 4 th ed. Singapore : McGraw-Hill, 1985.
- McInnes, R. G. Explore new options for hazardous air pollutant control. Chem. Eng. Progress 91 (November, 1995) : 36-48.
- Paludetto, R. ; Storti, G. ; Gamba, G. ; Carra, S. ; and Morbidelli, M. On multicomponent adsorption equilibria of xylene mixtures on zeolites. Ind. Eng. Chem. Res. 26 (1987) : 2250-2258.
- Perry, R. T. Perry's engineers' handbook. 6 th ed. New York : McGraw-Hill, 1987.

Pope, C. G. Sorption of benzene, toluene and p-xylene on ZSM-5. J. Phys. Chem. 88 (1984) : 6312-6313.

Pope, C. G. Sorption of benzene, toluene and p-xylene on silicalite and H-ZSM-5. J. Phys. Chem. 90 (1986) : 835-837.

Rees, L. V. C. and Shen, D. Frequency-response measurements of diffusion of sorbates in zeolites. In E. G. Derouane, and et al. (eds.), Zeolite microporous solids : synthesis, structure and reactivity, pp. 151-166. Netherland : Kluwer Academic, 1992.

Rees, L. V. C. ; Hamson, J. ; and Bruckner, P. Sorption of single gases and their binary mixtures in zeolite. In E. G. Derouane, and et al. (eds.), Zeolite microporous solids : synthesis, structure and reactivity, pp. 133-149. Netherland : Kluwer Academic, 1992.

Ruthven, D. M. Principles of adsorption and adsorption processes. New York : John Wiley & sons, 1984.

Ruthven, D. M. and Kaul, B. K. Adsorption of aromatic hydrocarbons in NaX zeolite 1. equilibrium. Ind. Eng. Chem. Res. 32 (1993) : 2047-2052.

Schneider, P. and Smith, J. M. Adsorption rate constants from chromatography.

AICHE J. 14 (1968) : 762-771.

Schneider, P. and Smith, J. M. Chromatographic study of surface diffusion. AICHE J.

14 (1968) : 886-895.

Shah, D. B. ; Hayhurst, D. T. ; Evanina, G. ; and Guo, C. J. Sorption and diffusion of

benzene in HZSM-5 and silicalite crystals. AICHE J. 34 (1988) : 1713-1717.

Suzuki, M. and Smith, J. M. Axial dispersion in beds of small particles. Chem. Eng.

J. 3 (1972) : 256-264.

Xiao, J. and Wei, J. Diffusion mechanism of hydrocarbons in zeolites. Chem. Eng.

Sci. 47 (1992) : 1123-1159.

Yang, R. T. Gas separation by adsorption processes. London : Butterworths, 1987.

**APPENDIX**

## APPENDIX A

### CALCULATION

#### 1. CONCENTRATIONS OF TOLUENE AND O-XYLENE VAPORS

The concentrations of toluene and o-xylene vapors are calculated from the ratio of vapor pressure and total pressure of the system.

For toluene vapor,

vapor pressure of toluene at 30 °C (Perry,1987) = 50.72 cmH<sub>2</sub>O

total pressure of the system is the summation of the atmospheric

pressure and the difference level of manometer = 1037.50 cmH<sub>2</sub>O

then, the mole fraction of toluene is  $50.72/1037.50 = 0.0489$

$\approx 4.89 \text{ \%mol}$

For o-xylene vapor,

vapor pressure of o-xylene at 30 °C (Perry, 1987) = 5.60 cmH<sub>2</sub>O

total pressure of the system = 1033.50 cmH<sub>2</sub>O

then, the mole fraction of o-xylene is  $5.60/1033.50 = 0.0054$

$\approx 0.54$  %mol

## 2. CALCULATION OF ADSORPTION EQUILIBRIUM CONSTANT

From equation 2-19,

$$t_R = \frac{L}{v} \left( 1 + \left( \frac{1-\epsilon}{\epsilon} \right) K \right)$$

The plot of the  $t_R$  versus  $L/v$  provided the slope,  $1 + [(1-\epsilon)/\epsilon]K$  which was used adsorption equilibrium constant calculation.

An example of the plot between  $t_R$  and  $L/v$  are illustrated in Figure A-1.



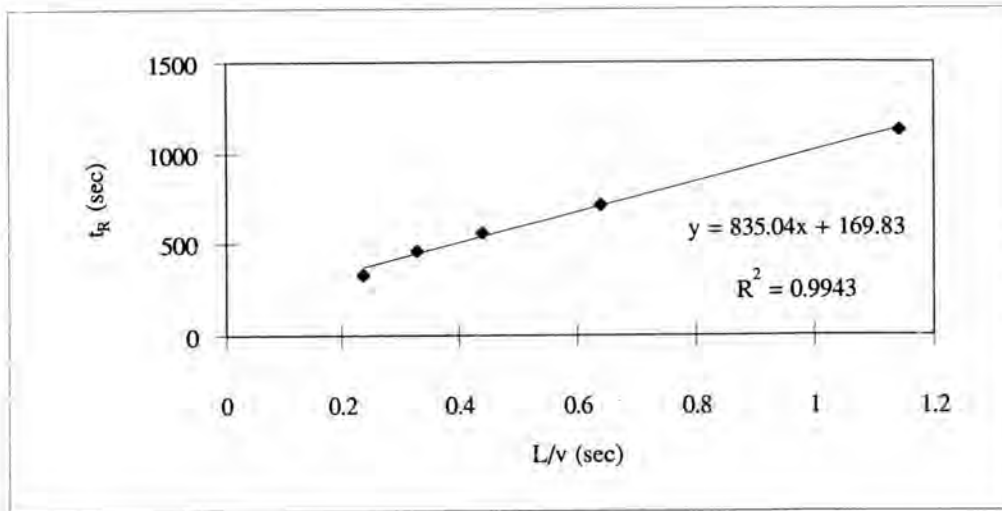


Figure A-1 First moment plot of adsorption of o-xylene on synthesized 4A at 80 °C

Therefore, the adsorption equilibrium constant could be obtained from :

$$K = \frac{\text{slope}}{1 + (1 - \varepsilon) / \varepsilon}$$

The bed porosity of synthesized the 4A is 0.461, the adsorption equilibrium constant of o-xylene on the synthesized 4A is

$$\begin{aligned} K &= \frac{835.04}{1 + (1 - 0.461) / 0.461} \\ &= 713.34 \end{aligned}$$

### 3. CALCULATION OF HEAT OF ADSORPTION

From the van't Hoff equation (Equation 2-3)

$$\frac{d \ln K}{dT} = \frac{\Delta H}{RT^2}$$

This equation could be integrated with an assumption of constant heat of adsorption ( $-\Delta H$ ) to yield

$$K = K_0 \exp(-\Delta H / RT)$$

or 
$$\ln K = \ln K_0 + (-\Delta H / RT)$$

Thus, the heat of adsorption could be obtained from the slope of the plot of  $\ln K$  with  $1/T$ , as illustrated in Figure A-2.

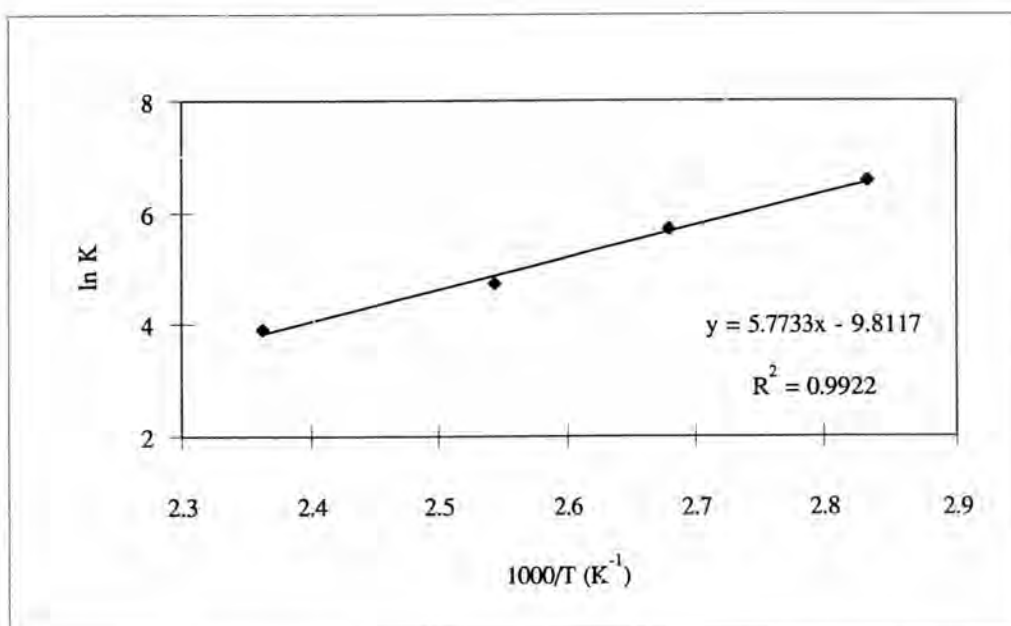


Figure A-2 Adsorption equilibrium constants of o-xylene on synthesized 4A

$$\begin{aligned} -\Delta H &= \text{slope} \times R \\ &= (5773.3 \text{ K}) \times (8.314 \text{ J/mol K}^{-1}) \\ &= 48.00 \text{ kJ/mol} \end{aligned}$$

#### 4. CALCULATION OF OVERALL MASS TRANSFER COEFFICIENT

According to equation 2-20,

$$\frac{\sigma^2}{2t_R^2} = \frac{D_L}{vL} + \frac{v}{L} \left( \frac{\varepsilon}{1-\varepsilon} \right) \frac{1}{kK} \left( 1 + \frac{\varepsilon}{(1-\varepsilon)K} \right)^{-2}$$

The plots of  $(\sigma^2/2t_R^2)(L/v)$  versus  $1/v^2$  has yield a straight line providing 2 independent information, i.e. slope of the straight line and 0-intercept. The overall mass transfer coefficient could be determined from the intercept while the slope of the plot has provided useful information for the axial dispersion coefficient determination, as illustrated in Figure A-3.

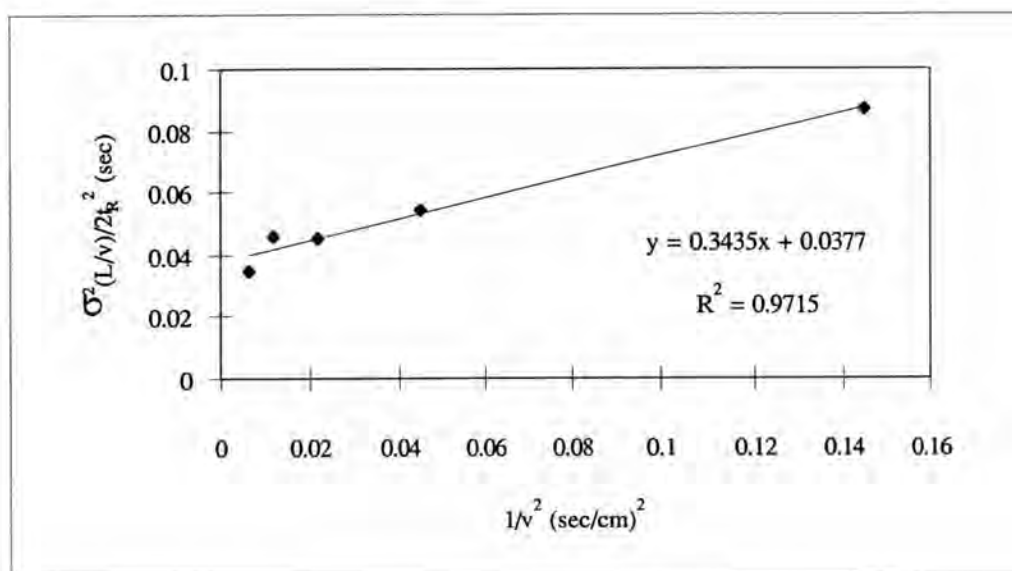


Figure A-3 The second moment plot of adsorption of o-xylene on synthesized 4A

$$\frac{\sigma^2}{2t_R^2} \frac{L}{v} = \frac{D_L}{v^2} + \left( \frac{\varepsilon}{1-\varepsilon} \right) \frac{1}{kK} \left( 1 + \frac{\varepsilon}{(1-\varepsilon)K} \right)^{-2}$$

$$\text{intercept} = \left( \frac{\varepsilon}{1-\varepsilon} \right) \frac{1}{kK} \left( 1 + \frac{\varepsilon}{(1-\varepsilon)K} \right)^{-2}$$

$$k = \frac{1}{\text{intercept}} \left( \frac{\varepsilon}{1-\varepsilon} \right) \frac{1}{K} \left( 1 + \frac{\varepsilon}{(1-\varepsilon)K} \right)^{-2}$$

Therefore, the overall mass transfer coefficient of adsorption of o-xylene on synthesized 4A is

$$k = \frac{1}{0.0377} \left( \frac{0.461}{1-0.461} \right) \frac{1}{713.34} \left( 1 + \frac{0.461}{(1-0.461)713.34} \right)^{-2}$$

$$k = 3.17 \times 10^{-2} \text{ sec}^{-1}$$

The axial dispersion coefficient is

$$D_L = \text{slope}$$

$$= 3.44 \times 10^{-1} \text{ cm}^2/\text{sec}$$

## APPENDIX B

### EXPERIMENT DATA

Table B-1 The retention times and variances of toluene on commercial 4A

Temperature	v (cm/sec)	t <sub>R</sub> (sec)	σ <sup>2</sup> (sec <sup>2</sup> )
80 °C	2.36	681.14	230,064.36
	5.38	281.29	42,415.98
	8.39	198.40	24,991.05
	11.45	190.15	26,195.01
	14.58	196.53	30,843.94
100 °C	1.39	364.16	68,213.64
	3.02	216.87	22,130.84
	5.81	138.51	12,987.71
	9.07	113.38	8,642.35
	12.24	112.44	12,637.39
	16.15	99.32	9,266.97

Table B-1 (continued)

Temperature	v (cm/sec)	t <sub>R</sub> (sec)	σ <sup>2</sup> (sec <sup>2</sup> )
120 °C	2.18	138.49	9,187.23
	5.40	59.53	2,318.48
	8.44	45.40	1,918.57
	11.45	37.96	1,294.25
	14.77	36.53	1,014.05
150 °C	2.17	96.35	3,649.18
	4.09	56.87	1,444.45
	6.28	41.852	795.68
	9.01	28.77	507.45
	12.00	24.73	326.15

Table B-2 The retention times and variances of toluene on synthesized 4A

Temperature	v (cm/sec)	t <sub>R</sub> (sec)	σ <sup>2</sup> (sec <sup>2</sup> )
80 °C	2.14	385.23	50,361.97
	3.78	258.29	32,153.99
	6.17	184.17	21,557.07
	9.30	140.34	13,235.89
	12.99	97.63	6,199.45

Table B-2 (continued)

Temperature	v (cm/sec)	t <sub>R</sub> (sec)	$\sigma^2$ (sec <sup>2</sup> )
100 °C	2.22	214.36	27,571.80
	3.51	161.10	15,933.85
	5.49	101.46	9,978.23
	7.92	81.13	8,608.46
	11.48	55.67	3,915.77
120 °C	1.82	98.97	6,065.98
	3.78	51.17	2,484.25
	5.63	37.37	1,363.22
	8.77	23.84	524.39
	11.93	19.77	342.80
150 °C	2.04	36.85	508.32
	3.79	24.16	247.69
	5.88	15.47	109.86
	8.26	8.21	50.809
	11.88	7.10	22.425

Table B-3 The retention times and variances of toluene on NaZSM-5

Temperature	v (cm/sec)	t <sub>R</sub> (sec)	$\sigma^2$ (sec <sup>2</sup> )
80 °C	5.33	505.68	282,574.75
	6.61	404.65	203,478.24
	8.12	298.05	111,250.43
	9.91	226.04	80,433.92
100 °C	4.30	492.41	228,263.06
	5.20	393.22	175,260.39
	6.91	285.20	119,710.19
	9.23	213.18	85,809.82
120 °C	5.06	242.94	79,688.05
	6.31	228.21	75,540.15
	8.16	196.23	72,897.31
	9.60	185.66	56,332.42



Table B-4 The retention times and variances of toluene on NH<sub>4</sub>ZSM-5

Temperature	v (cm/sec)	t <sub>R</sub> (sec)	σ <sup>2</sup> (sec <sup>2</sup> )
150 °C	7.74	726.35	486,442.83
	11.81	572.17	318,489.37
	15.26	498.29	252,463.913
	17.64	430.54	188,143.63
	21.80	391.87	151,000.26
175 °C	8.69	412.68	167,670.64
	10.95	341.43	139,148.94
	13.29	312.49	113,123.15
	16.25	260.50	90,654.97
	19.79	224.61	75,170.57
200 °C	7.57	247.35	92,820.68
	11.55	182.51	63,171.09
	13.84	168.76	56,733.43
	17.87	123.48	32,310.11
	21.04	109.57	25,870.85

Table B-5 The retention times and variances of toluene on HZSM-5

Temperature	v (cm/sec)	t <sub>R</sub> (sec)	σ <sup>2</sup> (sec <sup>2</sup> )
150 °C	9.99	591.90	271,505.59
	13.30	440.01	209,854.01
	19.72	370.97	149,158.86
	23.07	316.37	118,123.55
175 °C	6.59	386.83	208,913.78
	8.85	366.26	168,417.77
	11.57	284.18	110,991.07
	15.95	235.83	79,058.95
	19.16	191.86	50,436.558
200 °C	7.45	167.12	53,124.22
	9.74	125.73	33,613.86
	12.88	99.09	19,001.32
	16.65	87.20	12,805.99
	19.85	66.97	7,980.59

Table B-6 The retention times and variances of toluene on 13X

Temperature	v (cm/sec)	t <sub>R</sub> (sec)	$\sigma^2$ (sec <sup>2</sup> )
175 °C	7.09	1,696.14	1,215,206.11
	10.43	1,296.16	685,255.68
	12.46	1,220.72	620,280.44
	18.45	1,010.00	452,791.17
200 °C	7.16	1,201.06	758,345.68
	9.60	1,119.11	513,001.02
	13.41	889.99	356,781.79
	17.85	781.78	280,578.65
225 °C	5.77	778.74	306,295.06
	9.77	580.93	173,766.42
	13.48	453.60	110,726.87
	17.66	353.11	70,777.99

Table B-7 The retention times and variances of o-xylene on commercial 4A

Temperature	v (cm/sec)	t <sub>R</sub> (sec)	σ <sup>2</sup> (sec <sup>2</sup> )
80 °C	5.94	1,462.34	775,944.94
	6.89	1,343.30	629,820.24
	9.21	1,010.43	370,782.82
	12.08	791.70	287,571.44
100 °C	5.09	600.31	170,393.70
	7.44	453.47	105,847.65
	9.29	355.16	68,108.48
	12.33	312.77	62,581.91
120 °C	5.02	312.69	61,397.68
	6.57	272.78	49,887.79
	8.68	208.72	31,828.12
	11.83	177.51	26,956.88
150 °C	2.64	84.11	3,817.25
	3.99	56.53	2,117.95
	6.07	42.66	1,474.20
	8.00	32.63	968.45
	10.70	23.48	488.14

Table B-7 (continued)

Temperature	v (cm/sec)	t <sub>R</sub> (sec)	σ <sup>2</sup> (sec <sup>2</sup> )
175 °C	2.50	60.78	2,062.06
	4.13	39.35	1,042.60
	6.28	27.32	526.19
	8.35	23.42	346.96
	11.26	14.56	196.67

Table B-8 The retention times and variances of o-xylene on synthesized 4A

Temperature	v (cm/sec)	t <sub>R</sub> (sec)	σ <sup>2</sup> (sec <sup>2</sup> )
80 °C	2.63	1,114.81	189,190.02
	4.69	710.19	86,009.31
	6.82	555.23	63,517.61
	9.16	462.59	60,053.78
	12.63	333.15	32,452.66
100 °C	2.78	429.69	45,348.95
	4.69	296.48	26,584.22
	6.87	220.20	17,983.87
	9.43	172.33	12,219.91
	12.46	131.29	8,699.86

Table B-8 (continued)

Temperature	v (cm/sec)	t <sub>R</sub> (sec)	σ <sup>2</sup> (sec <sup>2</sup> )
120 °C	3.10	147.29	13,660.23
	4.32	105.42	7,701.30
	6.58	77.61	5,529.08
	8.57	68.46	4,786.56
	11.86	48.04	2,806.02
150 °C	2.79	64.12	3,817.25
	4.65	40.41	2,117.95
	6.31	29.56	1,474.20
	8.46	24.90	968.45
	10.68	14.46	488.14

Table B-9 The retention times and variances of o-xylene on NaZSM-5

Temperature	v (cm/sec)	t <sub>R</sub> (sec)	σ <sup>2</sup> (sec <sup>2</sup> )
80 °C	6.80	326.33	177,0833.40
	9.44	229.16	108,428.70
	11.42	182.90	83,820.05
	12.99	166.896	61,313.80
100 °C	4.17	294.60	147,264.60
	6.64	233.38	106,986.30
	11.08	138.02	56,343.72
	12.26	129.58	42,035.98
120 °C	2.56	307.49	126,111.30
	5.20	167.40	57,647.79
	8.68	123.61	37,851.09
	12.30	62.34	13,682.73

Table B-10 The retention times and variances of o-xylene on NH<sub>4</sub>ZSM-5

Temperature	v (cm/sec)	t <sub>R</sub> (sec)	σ <sup>2</sup> (sec <sup>2</sup> )
120 °C	6.25	763.11	614,267.04
	7.75	586.28	407,369.31
	9.95	439.28	251,637.43
	13.51	309.93	140,558.57
	16.51	257.67	98,697.96
150 °C	5.72	639.40	399,522.78
	7.51	558.76	359,278.16
	9.76	416.99	211,119.60
	11.42	340.67	150,687.01
	14.30	274.56	101,032.11
175 °C	5.66	468.72	213,212.23
	7.16	312.12	120,637.38
	9.66	316.61	140,299.02
	11.88	231.63	93,100.02
	14.55	201.46	57,654.33
200 °C	4.84	227.53	67,012.91
	6.78	187.54	50,727.65
	8.51	128.20	31,667.04
	10.53	101.87	20,106.78
	12.97	65.13	9,099.88



Table B-11 The retention times and variances of o-xylene on HZSM-5

Temperature	v (cm/sec)	t <sub>R</sub> (sec)	σ <sup>2</sup> (sec <sup>2</sup> )
120 °C	6.95	594.38	313,504.14
	10.20	411.56	161,958.70
	12.76	336.00	127,276.77
	16.08	222.45	64,082.47
150 °C	7.16	495.21	218,720.63
	10.70	378.89	157,826.65
	14.16	275.73	99,903.82
	17.57	203.01	63,838.37
175 °C	5.46	346.24	132,581.85
	9.01	201.20	60,254.81
	12.53	156.79	43,274.15
	14.94	113.51	25,488.55
	19.21	82.59	14,786.03
200 °C	6.29	187.82	60,469.29
	7.92	134.87	38,100.69
	10.02	91.95	21,017.10
	13.50	60.57	11,232.48
	17.33	38.93	5,238.44

Table B-12 The retention times and variances of o-xylene on 13X

Temperature	v (cm/sec)	t <sub>R</sub> (sec)	$\sigma^2$ (sec <sup>2</sup> )
100 °C	1.99	212.32	50,156.67
	3.43	142.97	24,042.62
	5.97	81.28	9,589.41
	8.14	59.18	6,047.41
	11.39	43.03	2,542.82
120 °C	1.65	150.70	23,803.87
	3.75	80.50	7,800.31
	5.80	50.66	2,744.81
	7.66	34.02	1,595.45
	11.01	23.92	672.53
150 °C	2.06	80.94	8,926.55
	3.46	51.05	4,028.11
	5.74	33.04	2,083.12
	7.18	27.36	1,414.21
	9.44	23.21	1,047.26
175 °C	2.35	56.11	2,957.65
	3.77	35.54	1,227.241
	5.67	23.07	709.95
	7.52	20.13	553.17
	10.31	16.87	347.81

Table B-12 (continued)

Temperature	v (cm/sec)	t <sub>R</sub> (sec)	σ <sup>2</sup> (sec <sup>2</sup> )
200 °C	2.66	33.98	1,005.01
	4.17	23.86	493.90
	6.20	16.46	296.73
	7.73	14.31	199.27
	9.78	11.56	103.47

## VITA

Miss Rungrawee Yingyuad was born in August, 1971 in Nakhon Nayok. She graduated high school from Nakhon Nayok Wittayakhom School in 1990. She received Bachelor's Degree of Engineering in Chemical Engineering from Kasetsart University in 1994. Subsequently, she completed the requirements for Master's Degree in Chemical Engineering at the Department of Chemical Engineering, Faculty of Engineering, Chulalongkorn University in 1997.