



REFERENCES

1. Gaugler, R.S. Heat transfer device. US Patent, 2350348, Appl. 21 December, 1942. Published 6 June, 1944.
2. Grover, G.M. Evaporation-condensation heat transfer device US. Patent 3229759, Appl. 2 Dec. 1963. Published 18 January, 1966.
3. Grover, G.M., Cotter, T.P. and Erikson, G.F. Structure of very high thermal conductance. J. Appl. 1964, 35(6), pp. 1990-1991
4. Leefer, B.I. Nuclear thermionic energy converter, 20th. Annual Power Source Conf. Atlantic City, N.J. 24-26 May, 1966. Proceeding, pp. 172-175, 1966
5. Judge, J.F. RCA test thermal energy pipe. Missiles and Rockets, Feb. 1966, pp. 36-38
6. Cotter, T.P. Theory of heat pipes, USAEC Report LA-3246. Contract W 7405-eng-36, Los Alamos Scientific Laboratory, University of California, 1965.
7. Cheung, H. A critical review of heat pipe theory and application UCRL-50453. July 15, 1968.
8. Anon. Proceedings of 2nd international heat pipe conference, Bologna, ESA Report SP-112, Vols 1&2, European Space Agency, 1976.
9. Van Andel, E. Heat pipe design theory. Euratom Center for Information and Documentation. Report Eur no. 4210 e,f, 1969.

10. Chisholm, D., The heat pipe, Mill & Boon Ltd., London, 1971
11. Cotter, T.P., Theory of heat pipe., Los Alamos Sci. Lab. Report,
No. LA -3246 - MS, 1965.

APPENDICES

APPENDIX A

WORKING FLUID PROPERTY

Properties listed: Latent heat of evaporation
 Liquid density
 Vapour density
 Liquid thermal conductivity
 Liquid dynamic viscosity
 Vapour dynamic viscosity
 Vapour pressure
 Vapour specific heat
 Liquid surface tension

WATER

Temp. °C	Latent Heat kJ/kg	Liquid Density kg/m ³	Vapour Density kg/m ³	Liquid Thermal Conduc- tivity W/m°C	Liquid Viscos. cP	Vapour Viscos. cP×10 ²	Vapour Press. Bar	Vapour Specific Heat kJ/kg°C	Liquid Surface Tension N/m×10 ²
20	2448	998.2	0.01	0.612	1.00	0.96	0.02	1.85	7.40
40	2402	992.3	0.05	0.630	0.65	1.04	0.07	1.86	6.96
60	2359	983.0	0.14	0.649	0.47	1.12	0.20	1.87	6.62
80	2309	972.0	0.29	0.668	0.36	1.19	0.47	1.88	6.26
100	2258	958.0	0.60	0.680	0.28	1.27	1.01	1.88	5.89
120	2200	945.0	1.12	0.682	0.23	1.34	2.02	1.89	5.50
140	2139	928.0	1.99	0.683	0.20	1.41	3.90	1.90	5.06
160	2074	909.0	3.27	0.679	0.17	1.49	6.44	1.91	4.66
180	2003	888.0	5.16	0.669	0.15	1.57	10.04	1.92	4.29
200	1967	865.0	7.87	0.659	0.14	1.65	16.19	1.93	3.89

APPENDIX B

THERMAL CONDUCTIVITY OF HEAT

PIPE CONTAINER AND WICK MATERIALS

Material	Thermal Conductivity (W/m ^o C)
Aluminium	205
Brass	113
Copper (0 - 100 ^o C)	394
Glass	0.75
Nickel (0 - 100 ^o C)	88
Mild Steel	45
Stainless Steel (Type 304)	17.3
Teflon	0.17



APPENDIX C

DIMENSIONAL EQUIVALENTS AND PHYSICAL CONSTANTS

DIMENSIONAL EQUIVALENTS

Length	1 ft = 12 in. = 30.48 cm = 0.3048 m 1 m = 100 cm = 39.37 in. = 3.28 ft
Mass	1 lbm = 0.03108 slug = 453.59 g = 0.45359 kg 1 kg = 1000 g = 0.06852 slug = 2.205 lbm
Time	1 hr = 3600 sec 1 sec = 2.778×10^{-4} hr
Force	1 lbf = 4.448×10^5 dyne = 4.448 N 1 N = 10^5 dyne = 0.2249 lbf
Angle	1 degree = 1.745×10^{-2} rad 1 rad = 57.30 degrees
Temperature	1 deg F = 1 deg R = 0.5556 deg C = 0.5556 deg K 1 deg K = 1 deg C = 1.8 deg R = 1.8 deg F deg F = 1.8 deg C + 32 deg C = 0.5556(deg F - 32) deg R = deg F + 459.69 deg K = deg C + 273.16 deg R = 1.8 deg K deg K = 0.5556 deg R
Energy	1 Btu = 777.66 ft-lbf = 252 cal = 1.054×10^{10} erg = 1054 J 1 J = 10^7 erg = 0.239 cal = 0.7375 ft-lbf = 9.485×10^{-4} Btu
Power	1 Btu/hr = 2.778×10^{-4} Btu/sec = 2.929×10^6 erg/sec = 0.2929 W 1 W = 10^7 erg/sec = 9.481×10^{-4} Btu/sec = 3.414 Btu/hr
Pressure	1 lbf/ft ² = 6.944×10^{-3} lbf/in. ² = 478.8 dyne/cm ² = 47.88 N/m ²

	$1 \text{ lbf/in.}^2 = 144 \text{ lbf/ft}^2 = 68,948 \text{ dyne/cm}^2 = 6894.8 \text{ N/m}^2$ $1 \text{ N/m}^2 = 10 \text{ dyne/cm}^2 = 1.450 \times 10^{-4} \text{ lbf/in.}^2 = 2.089 \times 10^{-2} \text{ lbf/ft}^2$
Area	$1 \text{ ft}^2 = 144 \text{ in.}^2 = 929 \text{ cm}^2 = 0.0929 \text{ m}^2$ $1 \text{ m}^2 = 10^4 \text{ cm}^2 = 1550 \text{ in.}^2 = 10.76 \text{ ft}^2$
Volume	$1 \text{ ft}^3 = 1728 \text{ in.}^3 = 2.832 \times 10^4 \text{ cm}^3 = 0.02832 \text{ m}^3$ $1 \text{ m}^3 = 10^6 \text{ cm}^3 = 6.102 \times 10^4 \text{ in.}^3 = 35.31 \text{ ft}^3$
Density	$1 \text{ gal (U.S. liquid)} = 0.13368 \text{ ft}^3 = 0.003785 \text{ m}^3$ $1 \text{ lbm/ft}^3 = 0.03108 \text{ slug/ft}^3 = 1.602 \times 10^{-2} \text{ g/cm}^3 = 16.02 \text{ kg/m}^3$ $1 \text{ kg/m}^3 = 10^{-3} \text{ g/cm}^3 = 0.00194 \text{ slug/ft}^3 = 0.06242 \text{ lbm/ft}^3$
Viscosity (dynamic)	$1 \text{ lbm/ft-hr} = 8.634 \times 10^{-6} \text{ slug/ft-sec} = 4.134 \times 10^{-3} \text{ g/cm-sec} = 4.134 \times 10^{-4} \text{ kg/m-sec}$ $1 \text{ kg/m-sec} = 10 \text{ g/cm-sec} = 2.089 \times 10^{-2} \text{ slug/ft-sec} = 2.419 \times 10^3 \text{ lbm/ft-hr}$
Thermal conductivity	$1 \text{ Btu/ft-hr-F} = 2.778 \times 10^{-4} \text{ Btu/ft-sec-F} = 1.730 \times 10^5 \text{ erg/cm-sec-K} = 1.730 \text{ W/m-K}$ $1 \text{ W/m-K} = 10^5 \text{ erg/cm-sec-K} = 1.606 \times 10^{-4} \text{ Btu/ft-sec-F} = 0.578 \text{ Btu/ft-hr-F}$
Surface tension	$1 \text{ lbf/ft} = 1.459 \times 10^4 \text{ dyne/cm} = 14.59 \text{ N/m}$ $1 \text{ N/m} = 10^3 \text{ dyne/cm} = 0.06854 \text{ lbf/ft}$
Latent heat of vaporization	$1 \text{ Btu/lbm} = 32.174 \text{ Btu/slug} = 2.32 \times 10^7 \text{ erg/g} = 2.324 \times 10^3 \text{ J/kg}$ $1 \text{ J/kg} = 10^4 \text{ erg/g} = 1.384 \times 10^{-2} \text{ Btu/slug} = 4.303 \times 10^{-4} \text{ Btu/lbm}$
Heat transfer coefficient	$1 \text{ Btu/ft}^2\text{-hr-F} = 5.674 \times 10^3 \text{ erg/cm}^2\text{-sec-K} = 5.674 \text{ W/m}^2\text{-K}$ $1 \text{ W/m}^2\text{-K} = 10^3 \text{ erg/cm}^2\text{-sec-K} = 0.1762 \text{ Btu/ft}^2\text{-hr-F}$

PHYSICAL CONSTANTS

Gravitational acceleration (standard), g	$g = 32.174 \text{ ft/sec}^2 = 980.7 \text{ cm/sec}^2 = 9.807 \text{ m/sec}^2$
Universal gas constant, \bar{R}	$\bar{R} = 1545.2 \text{ ft-lbf/lbm-mol-R} = 1.987 \text{ Btu/lbm-mol-R} = 8.314 \times 10^7 \text{ erg/g-mol-K} = 8.314 \times 10^3 \text{ J/kg-mol-K}$
Mechanical equivalent of heat, J	$J = 777.66 \text{ ft-lbf/Btu} = 4.184 \times 10^7 \text{ erg/cal} = 1 \text{ N-m/J}$
Stefan-Boltzman constant, σ	$\sigma = 0.1713 \times 10^{-8} \text{ Btu/ft}^2\text{-hr-R}^4 = 5.670 \times 10^{-5} \text{ erg/cm}^2\text{-sec-K}^4 = 5.670 \times 10^{-8} \text{ W/m}^2\text{-K}^4$