# n-OCTANE AROMATIZATION ON Pt SUPPORTED ON NOVEL ZEOLITES



Supak Trakarnroek

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By:	Supak Trakarnroek
Program:	Petrochemical Technology
Thesis Advisors:	Prof. Somchai Osuwan
	Prof. Daniel E.Resasco
	Assoc. Prof. Thirasak Rirksomboon
	Dr. Siriporn Jongpatiwut

Accepted by the Petroleum and Petrochemical College, Chulalongkorn University, in partial fulfilment of the requirements for the Degree of Doctor of Philosophy.

> Nartiyo Genumit College Director

(Assoc. Prof. Nantaya Yanumet)

**Thesis Committee:** 

Sumath alwady A.D.

(Assoc. Prof. Sumaeth Chavadej)

Foult

(Assoc. Prof. Thirasak Rirksomboon)

esasco

(Prof. Daniel E. Resasco)

(Prof. Somchai Osuwan)

J (in

(Dr. Siriporn Jongpatiwnt)

(Assoc. Prof. Vissanu Meeyoo)

ary

(Asst. Prof. Apanee Luengnaruemitchai)

### ABSTRACT

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KL zeolites with cylindrical shape are effective catalyst supports for noctane aromatization, but the effectiveness strongly depends on the channel length of the zeolite crystallite as well as Pt dispersion and location of the Pt cluster. The different Pt/KL catalysts in the series were compared in the aromatization of n-octane at 500°C and atmospheric pressure. It was found that the catalysts with shorter channel length exhibited improved activity, selectivity, and catalyst life. In addition, the catalysts with shorter channels had a much lower extent of secondary hydrogenolysis. Consequently, more C8 aromatics are preserved in the product and less benzene and toluene are produced compared to the catalysts with longer channels. In the case that the inactive metal was added into Pt/KL catalysts, it was found that the addition of tin improved the stability of the Pt/KL catalyst by inhibiting the adsorption of dehydrogenated species which is the intermediate for formation of coke. Furthermore, the selectivity to C8-aromatics products is increased but the secondary hydrogenolysis reaction, which occurred inside the pore of KL zeolite, is decreased. In addition, it was found that Co1Pt1Sn prepared by vapor phase co-impregnation method yielded a high fraction of alloy phase compared to Seq1Pt1Sn and Seq1Sn1Pt which were prepared by vapor phase sequential impregnation method. As a result, ColPt1Sn gave the highest activity and C8aromatics selectivity among the Pt-Sn catalysts investigated. Moreover, it was observed that OX molecules were produced more compared to without addition of tin because of electronic effect. As a result, the EB/OX ratio was lower than unity.

# บทคัดย่อ

สุภัค ตระการฤกษ์ : ปฏิกิริยาอะโรมาไทเซชันของนอร์มัลออกเทนบนโลหะ แพลททินัมที่อยู่บนซีโอไลด์ชนิดใหม่ (n-Octane Aromatization on Pt Supported on Novel Zeolites) อ. ที่ปรึกษา : ศ. สมชาย โอสุวรรณ ศ. แดเนียล อีรีซัสโก รศ. คร. ธีรศักดิ์ ฤกษ์ สมบูรณ์ และ คร. ศิริพร จงผาติวุฒิ 112 หน้า

ซีโอไลต์แอลที่มีรูปร่างทรงกระบอกเป็นตัวรองรับที่มีประสิทธิภาพในการเป็นตัวเร่ง ปฏิกิริยาสำหรับปฏิกิริยาอะโรมาไทเซชันของนอร์มัลออกเทน อย่างไรก็ตามประสิทธิผลของ ้ตัวเร่งปฏิกิริยาขึ้นอยู่กับความยาวของท่อซีโอไลต์ การกระจายตัวของโลหะแพลททินัม และ ตำแหน่งของโลหะแพลททินัม ในงานนี้ได้ใช้ตัวเร่งปฏิกิริยา Pt/KL ชนิดต่างๆมาเปรียบเทียบ ความเป็นตัวเร่งปฏิกิริยาของปฏิกิริยาอะ โรมาไทเซชันของนอร์มัลออกเทน ที่อุณหภูมิ 500°C ณ ความคันบรรยากาศ ผลการทคลองพบว่า ตัวเร่งปฏิกิริยาที่มีความยาวของท่อสั้นให้ความว่องไวใน การเป็นตัวเร่งปฏิกิริยาคี มีความเลือกเฉพาะกับผลิตภัณฑ์ที่ต้องการเป็นอย่างคี และมีอายุการใช้ ้งานนาน นอกจากนี้ยังลดการเกิดปฏิกิริยาไฮโครจีโนไลซีส ส่งผลให้ได้ผลิตภัณฑ์ที่เป็น C8 อะโร มาติกมาก พร้อมทั้งลดการเกิดของเบนซินและ โทลูอีนเมื่อเทียบกับตัวเร่งปฏิกิริยาที่มีท่อยาวกว่า ในกรณีที่เติมโลหะที่ไม่ว่องไวลงบนตัวเร่งปฏิกิริยา Pt/KL ผลการทคลองพบว่าการเติมโลหะ ดีบุกช่วยปรับปรุงความเสถียรของตัวเร่งปฏิกิริยาเนื่องจากโลหะดีบุกช่วยยับยั้งการดูดซับของ โมเลกุลจำพวกดีไฮโรจีเนทซึ่งเป็นตัวกลางในการเกิดโค้ก และมีความเลือกเฉพาะกับผลิตภัณฑ์ที่ เป็น C8 อะ โรมาติกมากขึ้น รวมทั้งลดการเกิดปฏิกิริยาไฮโครจีโนไลซีสซึ่งเกิดขึ้นในรูพรุนของซึ โอไลต์ อีกทั้งพบว่าตัวเร่งปฏิกิริยา Pt-Sn/KL ที่เตรียมจากการเติมโลหะแพลททินัมและคีบุก พร้อมกันมีเฟสที่เป็น PtSn อัลลอยค์มากกว่าตัวเร่งปฏิกิริยา Pt-Sn/KL ที่เตรียมจากการเติม โลหะแพลททินัมและดีบุกแบบลำดับ ส่งผลให้ตัวเร่งปฏิกิริยา Pt-Sn/KL ชนิดนี้มีความว่องไว และมีความเลือกเฉพาะกับผลิตภัณฑ์ที่เป็น C8 อะโรมาติกมากกว่าตัวเร่งปฏิกิริยาชนิดอื่นๆ นอกจากนี้ยังพบว่า ออร์ โทไซลีน (OX) เกิดได้ง่ายกว่าการเกิดเอทิลเบนซิน(EB) อันเป็นผล เนื่องมาจากการถ่ายโอนอิเล็กตรอนจากโลหะคีบุกไปยังโลหะแพลททินัม ส่งผลให้ อัตราส่วน EB/OX มีค่าน้อยกว่า 1

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- 6.7 The variation of (a) n-octane conversion and (b) C8aromatics selectivity with time on stream of Co1Pt1Sn and Pt-Sn/SiO<sub>2</sub>; reaction conditions: temperature =  $500^{\circ}$ C, pressure = 1 atm, WHSV = 5 h<sup>-1</sup>, and H<sub>2</sub>:HC = 6:1.
- 6.8 The variation C8-aromatics selectivity with n-octane conversion of Co1Pt1Sn and Pt-Sn/SiO<sub>2</sub>; reaction conditions: temperature =  $500^{\circ}$ C, pressure = 1 atm, WHSV = 0.5-5 h<sup>-1</sup>, and H<sub>2</sub>:HC = 6:1.
- 6.9 The variation of (a) totalenes yield and (b) hydrogenolysis product yield with n-octane conversion of 1Pt, Co1Pt1Sn and Pt-Sn/SiO<sub>2</sub>; reaction conditions: temperature = 500°C, pressure = 1 atm, WHSV = 5 h<sup>-1</sup>, and H<sub>2</sub>:HC = 6:1.
- 6.10 The variation of n-octane conversion with time on stream of various Sn/Pt ratios of the bimetallic Pt-Sn/KL catalysts prepared by vapor phase co-impregnation; reaction conditions: temperature =  $500^{\circ}$ C, pressure = 1 atm, WHSV =  $5 \text{ h}^{-1}$ , and H<sub>2</sub>:HC = 6:1.
- 6.11 The variation of (a) total aromatics selectivity and (b) C8aromatics selectivity with time on stream of various Sn/Pt ratios of the bimetallic Pt-Sn/KL catalysts prepared by vapor phase co-impregnation; reaction conditions: temperature =  $500^{\circ}$ C, pressure = 1 atm, WHSV = 5 h<sup>-1</sup>, and H<sub>2</sub>:HC = 6:1.
- 6.12 The variation of benzene selectivity with n-octane conversion of various Sn/Pt ratios of the bimetallic Pt-Sn/KL catalysts prepared by vapor phase co-impregnation; reaction conditions: temperature = 500°C, pressure = 1 atm, WHSV

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 $= 0.5-5 h^{-1}, and H_2:HC = 6:1.$ 100 6.13 The variation of EB/OX ratio with Sn/Pt ratios of the bimetallic Pt-Sn/KL catalysts prepared by vapor phase coimpregnation; reaction conditions: temperature = 500°C, pressure = 1 atm, WHSV = 5 h^{-1}, and H\_2:HC = 6:1.
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