

REFERENCES

- Addach, H., Berçot, P., Rezrazi, M., and Wery, M. (2005) Hydrogen permeation in iron at different temperatures. Materials Letters, 59(11), 1347-1351.
- Al Raisi, A.Y. and Gardner, T.Q. (2007, November 4-9) Surface and fluid phase transport effects on hydrogen permeability through palladium-based membranes. Paper presented at 07 AIChE Annual Meeting, Utah, USA.
- Bird, R.B., Stewart, W.E., and Lightfoot, E.N. (2001) Transport Phenomena. New York: John Wiley.
- Burrill, K.A. and Cheluguet, E.L. (1998, September 7-11) Corrosion of CANDU outlet feeder pipes. Paper presented at 1998 JAIF International Conference, Japan Atomic Industrial Forum on Water Chemistry in Nuclear Power Plants, Kashiwazaki, Japan.
- Callister, W.D. (1991) Material Science and Engineering: An Introduction 2nd ed. New York: John Wiley.
- Cheng, Y.F. and Steward, F.R. (2004) Corrosion of carbon steels in high-temperature water studied by electrochemical techniques. Corrosion Science, 46(10), 2405-2420.
- Chung, H. (2010) A review of CANDU feeder wall thinning. Nuclear Engineering And Technology, 42(5), 568-575.
- Dooley, R.B. and Chexal, V.K. (2000) Flow-accelerated corrosion of pressure vessels in fossil plants. International Journal of Pressure Vessels and Piping, 77(2-3), 85-90.
- Environmental News Service, Issue No.9 Summer. (July, 2005). Greenpeace co-founded says nuclear energy is 'only option'. 19 September 2014. <<http://www.euronuclear.org/e-news/e-news-9/greenpeace.htm>>
- Fontana, M.G. (1986) Corrosion Engineering. Singapore: McGraw Hill.
- Gadgeel, V. and Johnson, D. (1979) Gas-phase hydrogen permeation and diffusion in carbon steels as a function of carbon content from 500 to 900 K. Journal of Materials for Energy Systems, 1(2), 32-40.
- Gorman, J.K. and Nardella, W.R. (1962) Hydrogen permeation through metals. Vacuum, 12(1), 19-24.

- Grant, D.M., Cummings, D.L., and Blackburn, D.A. (1988) Hydrogen in 316 steel — diffusion, permeation and surface reaction. Journal of Nuclear Materials, 152(2–3), 139-145.
- Gunter, W.D., Myers, J., and Girsperger, S. (1987) Hydrogen: Metal Membranes. Hydrothermal Experimental Techniques. New York: Wiley.
- Hadam, U. and Zakroczymski, T. (2009) Absorption of hydrogen in tensile strained iron and high-carbon steel studied by electrochemical permeation and desorption techniques. International Journal of Hydrogen Energy, 34(5), 2449-2459.
- Hannay, N.B. (1967) Solid State Chemistry. New Jersey: Prentice-Hall.
- Homhuandee, P. (2008) Transport through carbon steel of hydrogen produced by flow-accelerated corrosion. M.S. Thesis, The Petroleum and Petrochemical College, Chulalongkorn University, Bangkok, Thailand.
- Kain, V., Roychowdhury, S., Ahmedabadi, P., and Barua, D.K. (2011) Flow accelerated corrosion: Experience from examination of components from nuclear power plants. Engineering Failure Analysis, 18(8), 2028-2041.
- Kongvarhodom, C. (2014) Measurement of hydrogen diffusion through carbon steel under different operating conditions associated with the development of a hydrogen effusion probe to measure metal corrosion rates. Ph.D. Dissertation, The University of New Brunswick, New Brunswick, Canada.
- Lang, L.C. (2000) Modelling the corrosion of carbon steel feeder pipes in CANDU reactors. M.S. Thesis, The University of New Brunswick, New Brunswick, Canada.
- Lee, S.K., Yun, S.H., Joo, H.G., and Noh, S.J. (2014) Deuterium transport and isotope effects in type 316L stainless steel at high temperatures for nuclear fusion and nuclear hydrogen technology applications. Current Applied Physics, 14(10), 1385-1388.
- Leelasangai, C. (2009) Measurement of the hydrogen diffusion through various steels with and without oxide film. M.S. Thesis, The Petroleum and Petrochemical College, Chulalongkorn University, Bangkok, Thailand.

- Lister, D.H., Gauthier, P., Goszcyński, J., and Slade, J. (1998, October 13-16) The accelerated corrosion of CANDU primary piping. Paper presented at Proceeding of the JAIF International Conference on water chemistry in nuclear power plants, Kashiwazaki, Japan.
- Lister, D.H., Liu, L., Feicht, A., Khatibi, M., Cook, W., Fujiwara, K., Kadoi, E., Ohira, T., Takiguchi, H., and Uchida, S. (2007, August 19-23) Effects of dissolved oxygen on flow-accelerated corrosion in feedwater systems. Paper presented at 13th International Conference on Environmental Degradation of Materials in Nuclear Power Systems, Ontario, Canada.
- Lister, D.H., Slade, J., and Arbeau, N. (1997, June 8-11) The accelerated corrosion of CANDU outlet feeders - observations, possible mechanisms and potential remedies. Paper presented at CNS proceedings of the 1997 CNA/CNS annual conference on powering Canada's future, Toronto, Canada.
- Lister, D.H., Steward, F.R., Cook, W.G., and Slade, J. (2001, June 10-13) Experiments on feeder thinning and their implications for CANDU reactors. Paper presented at The 22nd Annual Canadian Nuclear Society Conference, Toronto, Canada.
- Marchi, C.S., Somerday, B.P., and Robinson, S.L. (2007) Permeability, solubility and diffusivity of hydrogen isotopes in stainless steels at high gas pressures. International Journal of Hydrogen Energy, 32(1), 100-116.
- McKeen, K., Justason, A., and Lalonde, M. (2010, February 15-18) Sealing Of Non-Intrusive Vacuum Hydrogen Probe At Temperatures Up To 500 Degrees C. Paper presented at NACE International Corrosion Conference and Expo, Texas, USA.
- McKeen, K., Lalonde, M., Scott, A., and Ross, J. (2007, June 3-6) Hydrogen effusion probe development and installation at the Point Lepreau generating station. Paper presented at The 28th Annual Conference of the Canadian Nuclear Society and 31st Annual Student Conference of the Canadian Nuclear Society and the Canadian Nuclear Association, Saint John, New Brunswick, Canada.

- Norgate, T., Haque, N., and Koltun, P. (2013) The impact of uranium ore grade on the greenhouse gas footprint of nuclear power. Journal of Cleaner Production. 1-8.
- Petrucci, R.H., Harwood, W.S., and Herring, F.G. (2002) General Chemistry: Principles and Modern Applications 8th ed. New Jersey: Prentice-Hall.
- Pisarev, A., Shestakov, V., Kulsartov, S., and Vaitonene, A. (2001) Surface effects in diffusion measurements: Deuterium permeation through Martensitic steel. Physica Scripta. 2001(T94), 121-127.
- Potter, E.C. and Mann, G.M.W. (1961, April 10-15) Oxidation of Mild Steel in High-temperature Aqueous Systems. Paper presented at First International Congress on Metallic Corrosion, London, England.
- Potter, E.C. and Mann, G.M.W. (1963, March 11-15) Mechanism of Magnetite Growth on Low - Carbon Steel in Steam and Aqueous Solutions up to 550 Degrees C. Paper presented at 2nd International Congress on Metallic Corrosion, New York, USA.
- Robertson, W. and Thompson, A. (1980) Permeation measurements of hydrogen trapping in 1045 steel. Metallurgical Transactions A. 11(4), 553-557.
- She, Y., Emerson, S.C., Magdefrau, N.J., Opalka, S.M., Thibaud-Erkey, C., and Vanderspurt, T.H. (2014) Hydrogen permeability of sulfur tolerant Pd-Cu alloy membranes. Journal of Membrane Science. 452, 203-211.
- Silbert, M.D. (2002, October 14-17) Flow-Accelerated Corrosion in Boilers and Cooling Systems. Paper presented at NACE - Niagara Frontier Section Corrosion Conference, New York, USA.
- Sovacool, B.K. (2008) Valuing the greenhouse gas emissions from nuclear power: A critical survey. Energy Policy. 36(8), 2950-2963.
- Steed, R.G. (2006) Nuclear Power: In Canada and Beyond. Ontario: General Store Publishing House.
- Steward, S.A. (1983) Review of hydrogen isotope permeability through materials. California: Lawrence Livermore National Laboratory.
- Stone, J.M. (1981, September 21-23) Deuterium permeation and surface effects. Paper presented at International Conference on Environmental Degradation of Engineering Materials, Virginia, USA.

- Tomlinson, L. (1981) Mechanism of corrosion of carbon and low alloy ferritic steels by high temperature water. Corrosion, 37(10), 591-596.
- Tomlinson, L. and Cory, N.J. (1989) Hydrogen emission during the steam oxidation of ferritic steels: Kinetics and mechanism. Corrosion Science, 29(8), 939-965.
- Yuan, X.X., Pandey, M.D., and Bickel, G.A. (2008) A probabilistic model of wall thinning in CANDU feeders due to flow-accelerated corrosion. Nuclear Engineering and Design, 238(1), 16-24.

APPENDICES

Appendix A Parameters of Hydrogen Accumulation Loop

Table A1 Volume of accumulation loop

Components	Volume (cm³)	Method
Pressure transducer	1.5	Supplier
Valve	0.8	Supplier
VCR Tee	1.32	Calculated
Silver tubing (1/3 outside furnace)	7.54	Calculated
VCR blind fitting	0.11	Calculated
Cup 1	0.297	Calculated
Cup 2	0.185	Calculated
Cup 3	2.07	Calculated
Cup 4	1.76	Calculated
Cup 5	0.297	Calculated
Cup 6	0.185	Calculated
Cup 7	2.07	Calculated
Cup 8	1.76	Calculated

Table A2 Parameters of cups

Component	Outer Diameter (m)	Perimeter of the Cup on the Tube Surface (m)	Surface Area of Pipe under the Cup (m²)
Cup 1	6.35×10^{-3}	0.0200	8.025×10^{-5}
Cup 2	$6.35 \cdot 10^{-3}$	0.0200	7.391×10^{-5}
Cup 3	$12.70 \cdot 10^{-3}$	0.0399	$2.129 \cdot 10^{-4}$
Cup 4	12.70×10^{-3}	0.0399	2.025×10^{-4}
Cup 5	6.35×10^{-3}	0.0200	8.025×10^{-5}
Cup 6	6.35×10^{-3}	0.0200	7.391×10^{-5}
Cup 7	12.70×10^{-3}	0.0399	2.129×10^{-4}
Cup 8	12.70×10^{-3}	0.0399	2.025×10^{-4}

Appendix B Calculations of Surface Area of Pipe under the Cup, Cup Volume, Cup Perimeter, Surface Area of Cup inside the Cup, and Mean Temperature

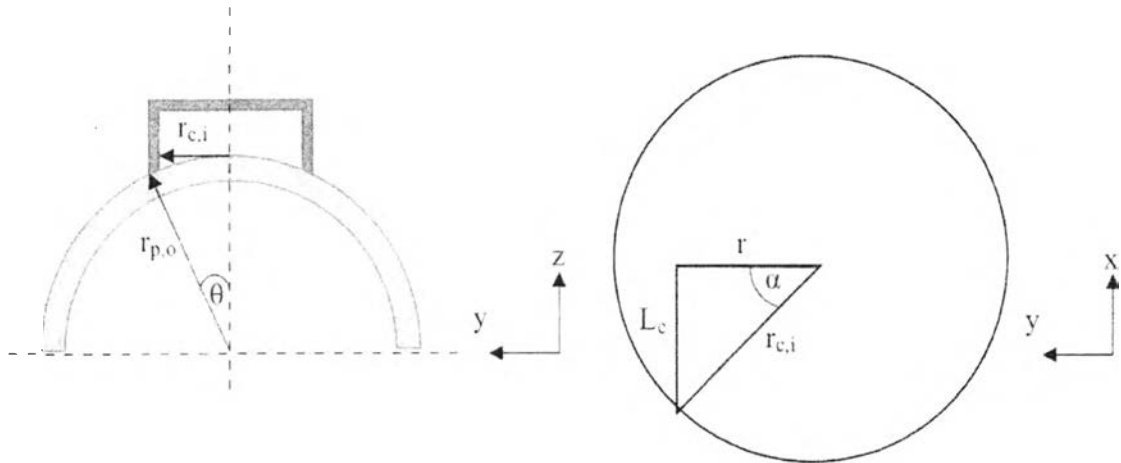


Figure B1 Schematic of cup mounted on a carbon steel pipe for the calculation of surface area under the cup.

The surface area of pipe under the cup was determined based on the outer diameter of pipe as shown in Equation B.1 where a quarter of the geometry is considered due to symmetry. The surface area of pipe under the cup is, thus, four times this integration.

$$A = \int_0^{\sin^{-1}\left(\frac{r}{r_{p,o}}\right)} L_c r_{p,o} d\theta \quad (\text{B.1})$$

where

- A = outer surface area of pipe which is under the cup (m^2)
- $r_{c,i}$ = inner radius of cup (m)
- $r_{p,o}$ = outer radius of pipe (m)
- L_c = length around the edge of the cup as a function of α (m)
- r = radius direction (m)

The length around the edge of the cup as a function of α , L_c , can be determined from Equation B.2 where α was found as a function of θ through Equations B.3-B.5.

$$L_c = r_{c,i} \sin \alpha \quad (\text{B.2})$$

$$\sin \theta = \frac{r}{r_{p,o}} \quad (\text{B.3})$$

$$\cos \alpha = \frac{r}{r_{c,i}} \quad (\text{B.4})$$

$$\alpha = \cos^{-1} \left(\frac{r_{p,o} \sin \theta}{r_{c,i}} \right) \quad (\text{B.5})$$

Therefore, Equation B.1 becomes as Equation B.6:

$$A = \int_0^{\sin^{-1} \left(\frac{r_{c,i}}{r_{p,o}} \right)} r_{p,o} r_{c,i} \sin \left(\cos^{-1} \left(\frac{r_{p,o} \sin \theta}{r_{c,i}} \right) \right) d\theta \quad (\text{B.6})$$

The volume of cup (V_{cup}) was calculated by the summation of cylindrical cup volume based on the minimum height of the cup ($V_{\text{cup,min}}$) and the remaining element volume of the cup (V_{element}).

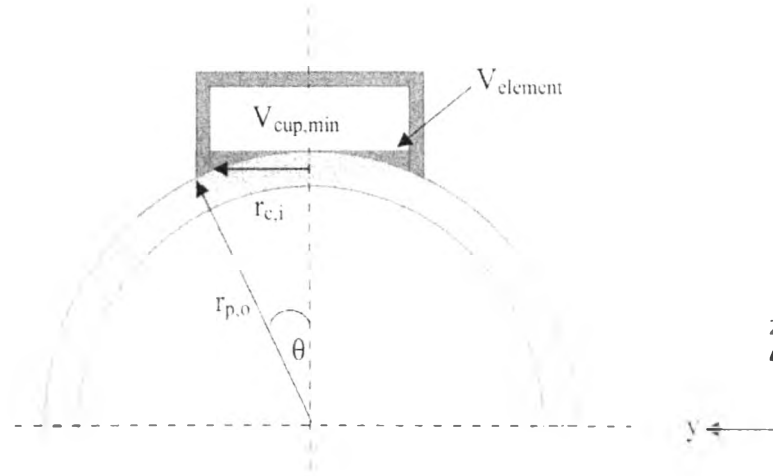


Figure B2 Schematic of cup mounted on a carbon steel pipe showing the breakdown of the cup volume.

The volume of element (V_{element}) is the product of the length, the height and the width of the element based on a quarter of the geometry which are shown in Equations B.7-B.9.

Length of element: $r_{c,i} \sin \alpha \quad (\text{B.7})$

$$\text{Height of element:} \quad r_{p,o} - \sqrt{r_{p,o}^2 - r^2} \quad (\text{B.8})$$

$$\text{Width of element:} \quad dr \quad (\text{B.9})$$

$$\text{Therefore,} \quad dV = (r_{p,o} \sin \alpha) \left(r_{p,o} - \sqrt{r_{p,o}^2 - r^2} \right) dr \quad (\text{B.10})$$

In order to solve Equation B.10, α must be determined as a function of r which is already defined as shown in Equation B.4. The volume of element and cup volume are, thus, as in Equations B.11-B.12.

$$V_{\text{element}} = \int_0^{r_{c,o}} \left(r_{p,o} - \sqrt{r_{p,o}^2 - r^2} \right) \left(r_{c,o} \sin \left(\cos^{-1} \frac{r}{r_{c,o}} \right) \right) dr \quad (\text{B.11})$$

$$V_{\text{cup}} = V_{\text{cup min}} + 4V_{\text{element}} \quad (\text{B.12})$$

where

$$V_{\text{element}} = \text{remaining element volume of the cup (m}^3\text{)}$$

$$V_{\text{cup}} = \text{cup volume (m}^3\text{)}$$

$$V_{\text{cup min}} = \text{cylindrical cup volume based on the minimum height of the cup (m}^3\text{)}$$

The perimeter of cup can be determined from Equation B.13 where a quarter of the geometry is considered due to symmetry. The cup perimeter is thus four times this integration.

$$p_c = \int_0^{\frac{\pi}{2}} s d\theta \quad (\text{B.13})$$

where

$$p_c = \text{perimeter of cup (m)}$$

$$s = \text{distance between the center of cup and edge of cup (m) as shown in}$$

Figure B.3 which can be calculated from Equation B.14 which a and B can be solved by Equations B.15 and B.16.

$$s^2 = a^2 + r_{c,o}^2 \quad (\text{B.14})$$

where

$$a = \sqrt{r_{p,o}^2 - B^2} - \sqrt{r_{p,o}^2 - r_{c,o}^2} \quad (\text{B.15})$$

and

$$B = r_{c,o} \cos \theta \quad (\text{B.16})$$

where

$r_{c,o}$ = outer radius of cup (m)

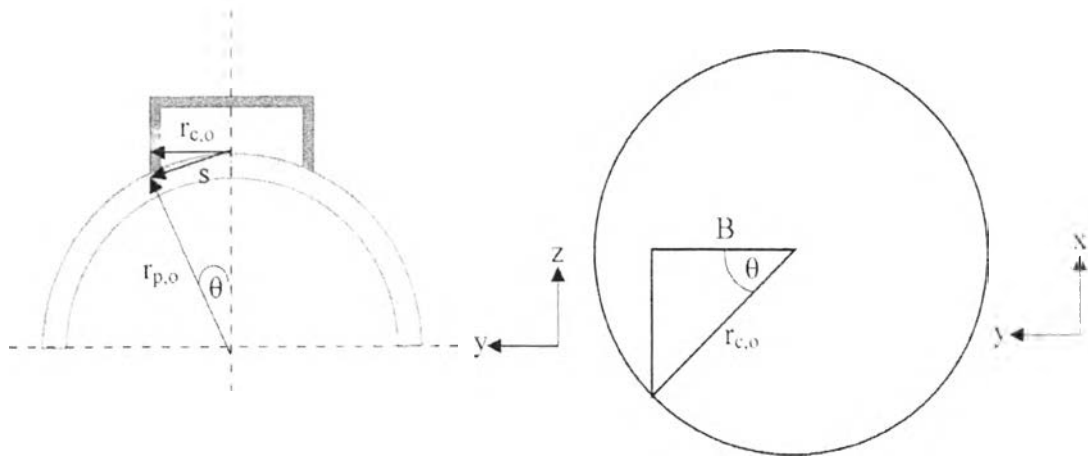


Figure B3 Schematic of cup mounted on a carbon steel pipe for the calculation of the perimeter of the cup.

Therefore, Equation B.13 becomes as Equation B.17.

$$p_c = \int_0^{\frac{\pi}{2}} \left(r_{p,o}^2 + \left(\sqrt{r_{p,o}^2 - r_{c,o}^2 \cos^2 \theta} - \sqrt{r_{p,o}^2 - r_{p,o}^2} \right)^2 \right)^{1/2} d\theta \quad (\text{B.17})$$

The surface area of cup inside the cup can be determined by Equation B.18 where a quarter of geometry is considered due to the symmetry. Consequently, the surface area of side wall inside the cup is four times this integration.

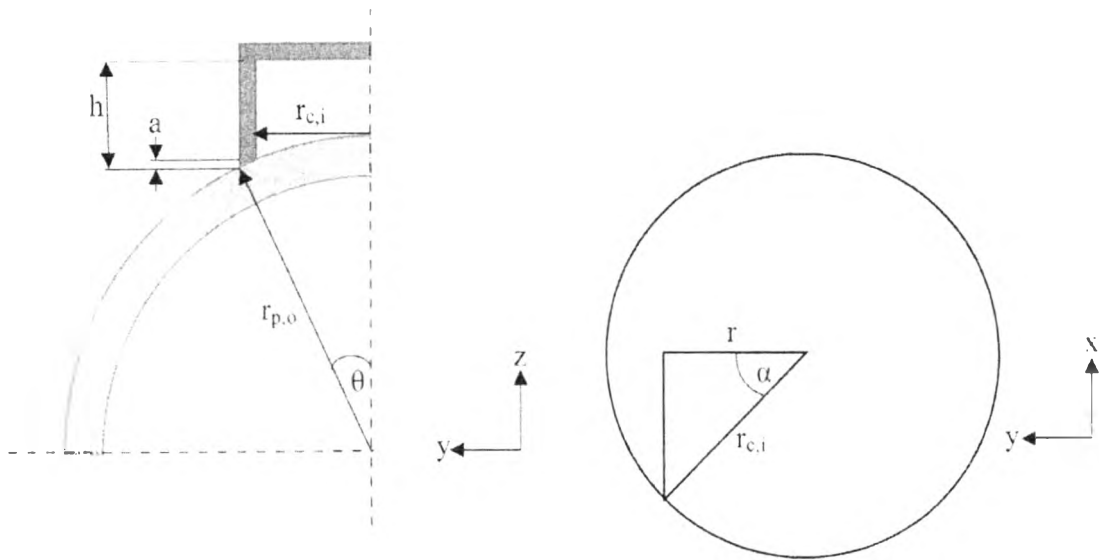


Figure B4 Schematic of cup mounted on a carbon steel pipe for the calculation of surface area of cup inside the cup.

$$A_c = \int_0^{\frac{\pi}{2}} (h-a)r_c d\alpha \quad (\text{B.18})$$

where

A_c = surface area of cup inside the cup (m^2)

h = height of cup (m)

a = height of element (m)

Equation B.18 shows that the surface area of cup inside the cup is based on the height of cylindrical element which can be calculated from the height of element (a) and height of cup as shown in Equation B.19 where a and r can be calculated from Equations B.20 and B.21.

$$\text{Height of cylindrical element:} \quad h - a \quad (\text{B.19})$$

where

$$a = \sqrt{r_{p,o}^2 - r^2} - \sqrt{r_{p,o}^2 - r_{c,i}^2} \quad (\text{B.20})$$

and

$$r = r_{c,i} \cos \alpha \quad (\text{B.21})$$

Therefore, Equation B.18 becomes Equation Equation B.22.

$$A_c = \int_0^{\frac{\pi}{2}} \left[h - \left(\sqrt{r_{p,o}^2 - (r_{c,i} \cos \alpha)^2} - \sqrt{r_{p,o}^2 - r_{c,i}^2} \right) \right] r_{c,i} d\alpha \quad (\text{B.22})$$

The above integrals were solved numerically.

For inner height (h_{in}) can be calculated by Equation B.23.

$$h_m = h - \left(\sqrt{r_{p,o}^2 - r_{c,i}^2} - \sqrt{r_{p,o}^2 - r_{c,o}^2} \right) \quad (\text{B.23})$$

For mean temperature calculation, the ideal gas law is used as shown in Equation B.24-B.25, but due to the configuration of the test apparatus as shown in Figure 3.1, some parts of the hydrogen containing volume consisting of pressure transducers, valves, VCR tees, VCR blind fittings and one-third of silver tubing are outside the furnace. The mean temperature is, then, calculated by based on the volume of hydrogen at a given temperature for components that are inside and outside the furnace as shown in Equation B.26-B.28.

Ideal gas law: $PV' = nRT$ (B.24)

$$n = \frac{PV'}{RT} = \frac{P}{R} \times \frac{V'}{T_{mean}} \quad (\text{B.25})$$

So, $n_{\text{total}} = n_{in} + n_{out}$ (B.26)

Then, $\frac{V'}{T_{mean}} = \frac{V'_{in}}{T_{in}} + \frac{V'_{out}}{T_{out}}$ (B.27)

Therefore, $T_{mean} = \frac{V'}{\frac{V'_{in}}{T_{in}} + \frac{V'_{out}}{T_{out}}}$ (B.28)

where

n_{total} = total moles hydrogen gas (mole)

n_{in} = number of moles of hydrogen gas accumulated in the components which are inside the furnace (mole)

n_{out} = number of moles of hydrogen gas accumulated in the components which are outside the furnace (mole)

T_{mean} = absolute mean temperature (K)

V' = total hydrogen gas volume (m^3)

V'_{in} = hydrogen gas volume accumulated in the components which are inside the furnace (m^3)

V_{out} = hydrogen gas volume accumulated in the components which are outside the furnace (m^3)

Although the temperature may vary to some degree along the length of the silver tubing which has one-third of the length outside the furnace, the total volume of silver tubing is minimal so it is assumed that the hydrogen within this volume has a constant temperature gradient.

Appendix C Parameters of Hydrogen Accumulation Loop after Redesign of the Cups

Table C1 Volume of accumulation loop when the cups were redesigned

Components	Volume (cm³)	Method
Pressure transducer	1.5	Supplier
Valve	0.8	Supplier
VCR Tee	1.32	Calculated
Silver tubing (1/3 outside furnace)	7.54	Calculated
VCR blind fitting	0.235	Calculated
Cup 1	0.119	Calculated
Cup 2	0.119	Calculated
Cup 3	0.267	Calculated
Cup 4	0.267	Calculated
Cup 5	0.119	Calculated
Cup 6	0.119	Calculated
Cup 7	0.267	Calculated
Cup 8	0.267	Calculated

Table C2 Parameters of new cups

Component	Outer Diameter (m)	Perimeter of the Cup on the Tube Surface (m)	Surface Area of Pipe under the Cup (m²)
Cup 1	$21 \cdot 10^{-3}$	0.0660	2.409×10^{-4}
Cup 2	23×10^{-3}	0.0723	2.692×10^{-4}
Cup 3	23×10^{-3}	0.0723	2.992×10^{-4}
Cup 4	$25 \cdot 10^{-3}$	0.0786	3.307×10^{-4}
Cup 5	$11 \cdot 10^{-3}$	0.0346	$1.228 \cdot 10^{-4}$
Cup 6	21×10^{-3}	0.0660	2.409×10^{-4}
Cup 7	13×10^{-3}	0.0409	$1.653 \cdot 10^{-4}$
Cup 8	$23 \cdot 10^{-3}$	0.0723	2.992×10^{-4}

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Proceeding:

1. Santiwiparat, P.; Steward, F.R.; Lister, D.L.; Cook, W.G.; and Rirksomboon, T. (2015, May 31 – June 3) Modelling hydrogen permeation in a hydrogen effusion probe for monitoring corrosion of carbon steels. Proceedings of The 35th Annual Conference of Canadian Nuclear Society and the 39th Annual Student Conference of the Canadian Nuclear Society and the Canadian Nuclear Association. New Brunswick, Canada.