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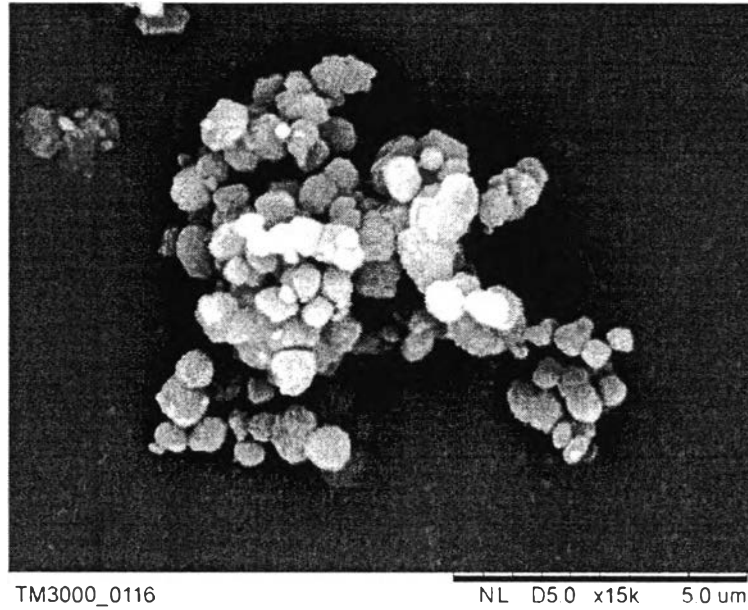
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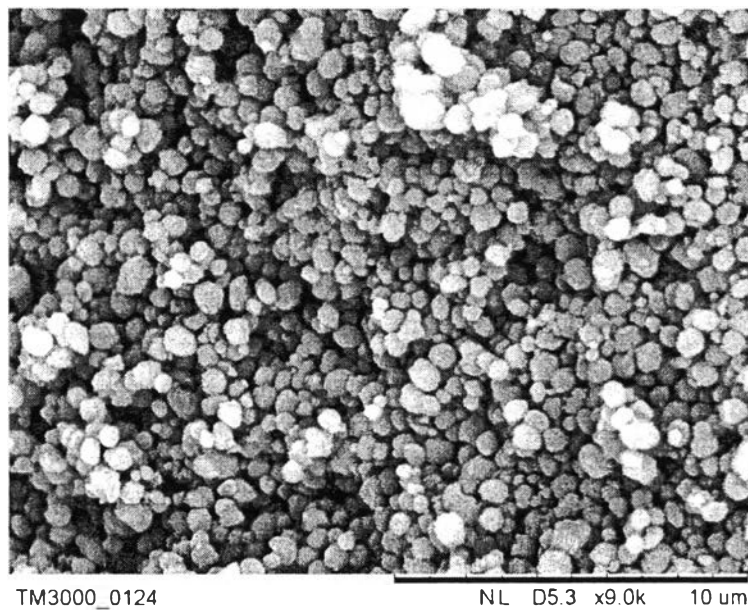
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## APPENDICES

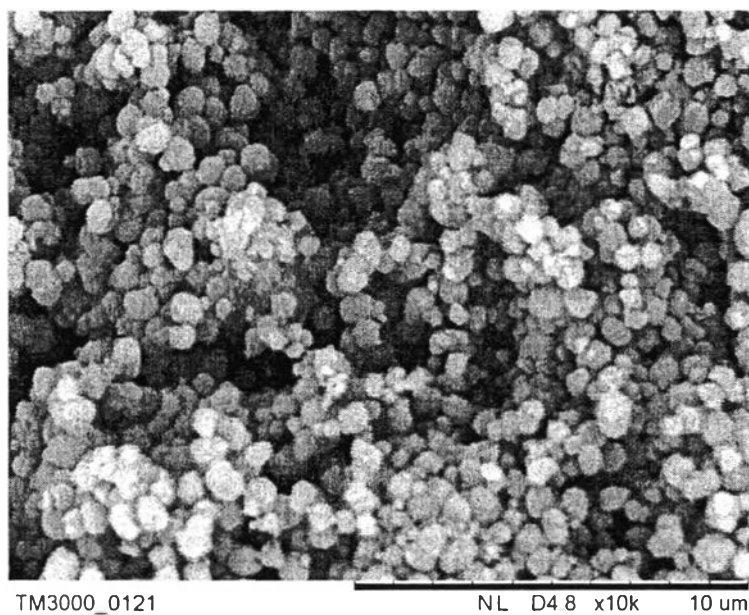
### Appendix A Scanning Electron Microscopy Micrographs



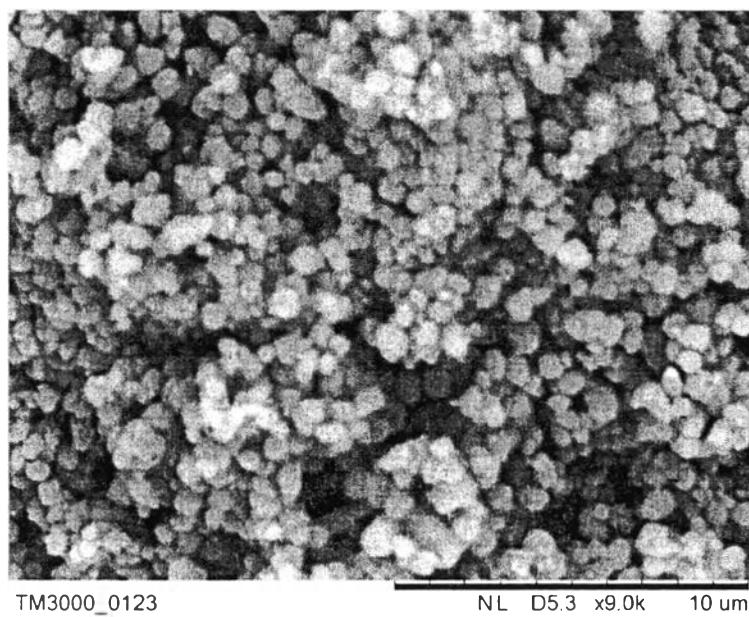
**Figure A1** SEM image of HZ11(75) (15.0 kV×10.0k).



**Figure A2** SEM image of P/HZ11(75) (15.0 kV×10.0k).

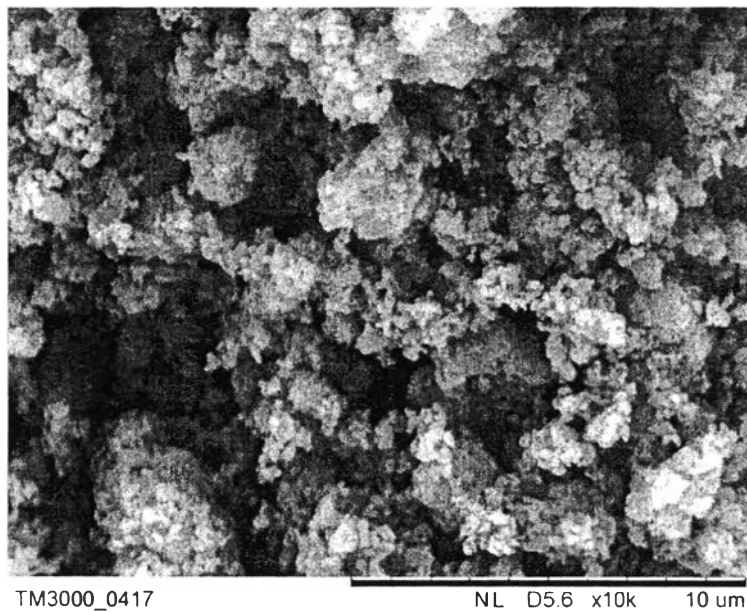


**Figure A3** SEM image of Sb/HZ11(75) (15.0 kV×10.0k).

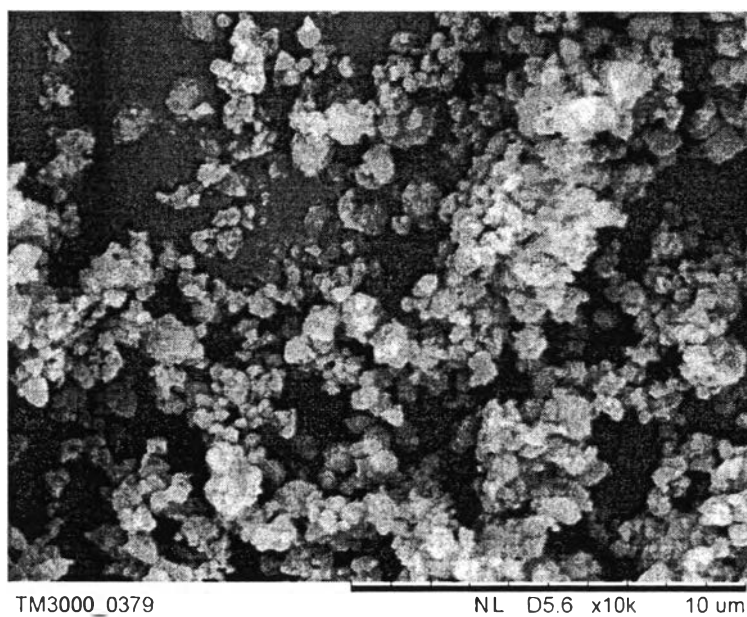


**Figure A4** SEM image of Bi/HZ11(75) (15.0 kV×10.0k).

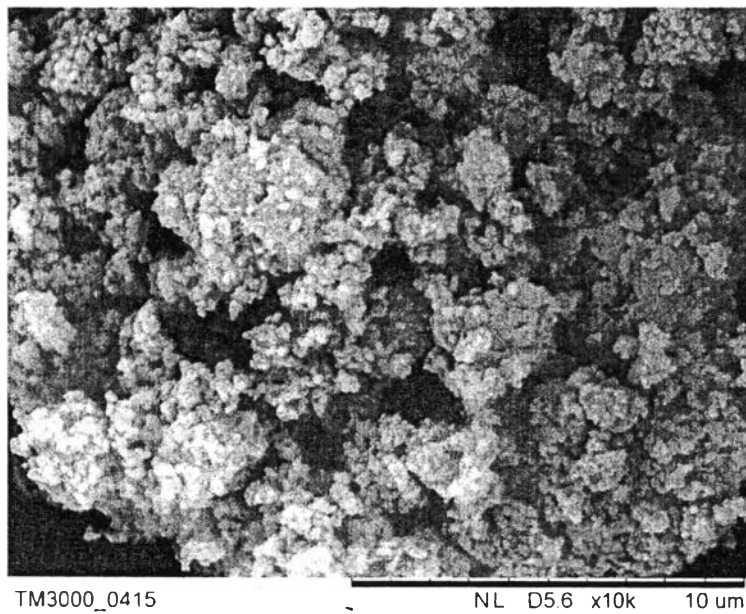




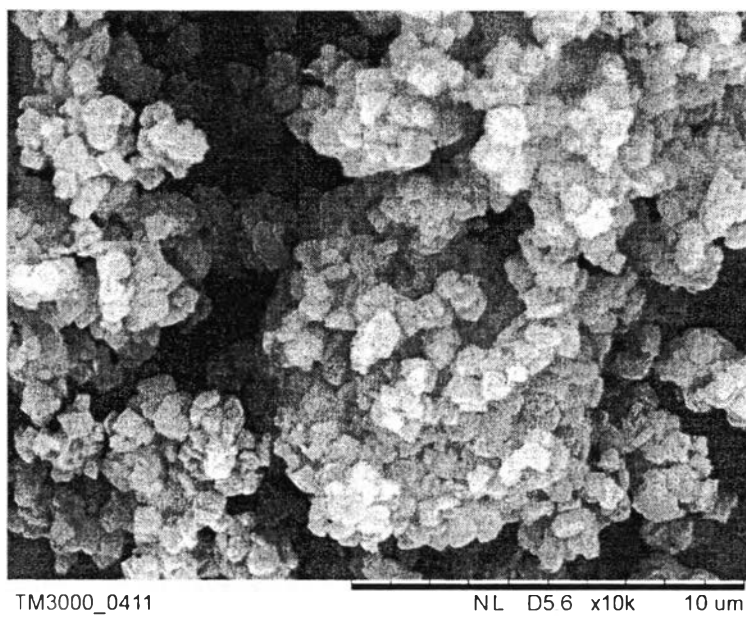
**Figure A5** SEM image of HZ5(30) (15.0 kV×10.0k).



**Figure A6** SEM image of HZ5(80) (15.0 kV×10.0k).



**Figure A7** SEM image of HBeta(27) (15.0 kV×10.0k).



**Figure A8** SEM image of HY(30) (15.0 kV×10.0k).

## Appendix B Product Distribution and Product Yield Calculations

$$\text{Yield (wt \%)} = \frac{\text{Total weight of any products}}{\text{Total weight of converted bioethanol}} \times 100$$

**Table B1** Product distribution and product yields from HZ5(30), P/HZ5(30), Sb/HZ5(30), and Bi/HZ5(30) catalysts

Catalyst	HZ5(30)	P/HZ5(30)	Sb/HZ5(30)	Bi/HZ5(30)
Ethanol conversion (wt %)	99.5	99.0	99.3	97.8
Feed ethanol (ml/h)	2.00	2.00	2.00	2.00
Feed ethanol (ml)	16.6	17.5	17.5	17.7
Feed ethanol (g)*	13.1	13.8	13.8	14.0
Converted ethanol (g)	13.1	13.7	13.7	13.7
Product distribution (g)				
Oil	0.92	0.48	1.55	2.56
Gas	9.64	9.60	10.3	8.0
Water	2.49	3.63	1.85	3.09
Other**	0.06	0.13	0.10	0.31
Product yield (wt %)				
Oil	7.07	3.52	11.3	18.7
Gas	73.9	70.0	75.2	58.6
Water	19.1	26.4	13.5	22.6

\*Ethanol concentration is 99.5 v/v %

\*\*Unconverted bio-ethanol

**Table B2** Product distribution and product yields from HBeta(27), P/HBeta(27), Sb/HBeta(27), and Bi/HBeta(27) catalysts

Catalyst	HBeta(27)	P/HBeta(27)	Sb/HBeta(27)	Bi/ HBeta(27)
Ethanol conversion (wt %)	96.7	99.1	98.5	99.7
Feed ethanol (ml/h)	2.00	2.00	2.00	2.00
Feed ethanol (ml)	16.9	16.0	17.3	16.6
Feed ethanol (g)*	13.3	12.6	13.7	13.1
Converted ethanol (g)	12.9	12.5	13.5	13.1
Product distribution (g)				
Oil	0.21	0.55	0.68	0.62
Gas	10.5	9.71	9.52	9.30
Water	2.13	2.23	3.27	3.14
Other**	0.44	0.12	0.20	0.04
Product yield (wt %)				
Oil	1.60	4.43	5.06	4.74
Gas	80.7	70.9	69.4	68.0
Water	16.3	16.3	23.9	23.0

\*Ethanol concentration is 99.5 v/v %

\*\*Unconverted bio-ethanol

**Table B3** Product distribution and product yields from HY(30), P/HY(30), Sb/HY(30), and Bi/HY(30) catalysts

Catalyst	HY(30)	P/HY(30)	Sb/HY(30)	Bi/HY(30)
Ethanol conversion (wt %)	99.5	99.0	99.3	97.8
Feed ethanol (ml/h)	2.00	2.00	2.00	2.00
Feed ethanol (ml)	17.0	17.2	17.2	15.6
Feed ethanol (g)*	13.4	13.6	13.6	12.3
Converted ethanol (g)	13.4	13.5	13.5	12.1
Product distribution (g)				
Oil	0.46	0.48	0.62	0.72
Gas	11.1	11.6	10.4	8.79
Water	1.79	1.36	2.49	2.56
Other**	0.07	0.13	0.10	0.28
Product yield (wt %)				
Oil	3.47	3.55	4.62	6.00
Gas	85.0	84.9	75.7	64.3
Water	13.7	9.9	18.2	18.7

\*Ethanol concentration is 99.5 v/v %

\*\*Unconverted bio-ethanol

**Table B4** Product distribution and product yields from HZ5(80), P/HZ5(80), Sb/HZ5(80), and Bi/HZ5(80) catalysts

Catalyst	HZ5(80)	P/HZ5(80)	Sb/HZ5(80)	Bi/HZ5(80)
Ethanol conversion (wt %)	97.7	99.1	98.1	99.0
Feed ethanol (ml/h)	2.00	2.00	2.00	2.00
Feed ethanol (ml)	15.9	15.5	15.8	16.0
Feed ethanol (g)*	12.6	12.3	12.5	12.6
Converted ethanol (g)	12.3	12.2	12.2	12.5
Product distribution (g)				
Oil	1.50	0.54	1.71	2.31
Gas	7.97	9.31	8.55	8.34
Water	2.82	2.31	1.96	1.86
Other**	0.29	0.11	0.23	0.13
Product yield (wt %)				
Oil	12.17	4.45	14.01	18.50
Gas	61.1	67.9	62.3	61.0
Water	21.6	16.8	14.3	13.6

\*Ethanol concentration is 99.5 v/v %

\*\*Unconverted bio-ethanol

**Table B5** Product distribution and product yields from HZ11(75), P/HZ11(75), Sb/HZ11(75), and Bi/HZ11(75) catalysts

Catalyst	HZ11(75)	P/ HZ11(75)	Sb/ HZ11(75)	Bi/ HZ11(75)
Ethanol conversion (wt %)	95.5	98.0	95.6	96.8
Feed ethanol (ml/h)	2.00	2.00	2.00	2.00
Feed ethanol (ml)	15.6	17.9	15.6	15.9
Feed ethanol (g)*	12.3	14.2	12.3	12.5
Converted ethanol (g)	11.8	13.9	11.7	12.1
Product distribution (g)				
Oil	0.52	0.61	0.46	0.55
Gas	7.93	10.8	8.86	9.72
Water	3.30	2.52	2.43	1.85
Other**	0.55	0.28	0.54	0.41
Product yield (wt %)				
Oil	4.41	4.38	3.92	4.53
Gas	60.8	78.4	64.5	71.1
Water	25.3	18.4	17.7	13.5

\*Ethanol concentration is 99.5 v/v %

\*\*Unconverted bio-ethanol

























## Appendix D Compositions in Liquid Products

**Table D1** Oil compositions from HZ5(30), P/HZ5(30), Sb/HZ5(30), and Bi/HZ5(30) catalysts

Component	Composition (wt%)			
	HZ5(30)	P/HZ5(30)	Sb/HZ5(30)	Bi/HZ5(30)
Oxygenate	0.18	18.60	0.29	1.27
Non-aromatic	10.45	5.27	2.55	3.71
Benzene	1.28	7.48	0.56	0.25
Toluene	3.70	4.98	7.25	5.30
o-Xylene	6.52	6.10	1.37	7.48
m-Xylene	9.87	2.59	8.58	7.73
p-Xylene	4.66	2.55	4.30	5.04
Ethylbenzene	1.03	1.29	3.55	1.98
C9	26.35	2.23	38.78	28.62
C10+	35.96	48.92	32.77	38.61
BTEX/total aromatics	0.30	0.33	0.26	0.29
p-Xylene/total aromatics	0.172	0.102	0.168	0.181

**Table D2** Oil compositions from HBeta(27), P/HBeta(27), Sb/HBeta(27), and Bi/HBeta(27) catalysts

Component	Composition (wt %)			
	HBeta(27)	P/HBeta(27)	Sb/HBeta(27)	Bi/HBeta(27)
Oxygenate	1.03	3.63	1.02	1.43
Non-aromatic	0.00	0.00	0.44	0.57
Benzene	30.02	29.25	8.95	14.76
Toluene	34.83	27.40	21.66	23.73
o-Xylene	9.26	3.80	11.06	9.32
m-Xylene	10.67	5.56	14.91	11.86
p-Xylene	8.33	4.46	10.90	9.96
Ethylbenzene	1.18	1.41	3.32	3.15
C9	2.70	4.51	16.44	15.29
C10+	1.97	19.97	11.30	9.93
BTEX/total aromatics	0.95	0.75	0.72	0.74
p-Xylene/total aromatics	0.088	0.062	0.154	0.137

**Table D3** Oil compositions from HY(30), P/HY(30), Sb/HY(30), and, Bi/HY(30) catalysts

Component	Composition (wt %)			
	HY(30)	P/HY(30)	Sb/HY(30)	Bi/HY(30)
Oxygenate	0.71	7.31	7.38	13.87
Non-aromatic	3.52	1.87	1.27	1.10
Benzene	44.90	45.62	42.81	32.81
Toluene	31.34	18.00	21.38	19.08
o-Xylene	4.40	3.88	5.32	6.31
m-Xylene	5.12	4.02	6.19	6.20
p-Xylene	3.85	2.92	4.75	5.16
Ethylbenzene	1.27	1.02	1.38	1.35
C9	0.88	2.66	1.86	5.13
C10+	4.00	12.69	7.67	8.98
BTEX/total aromatics	0.95	0.83	0.90	0.83
p-Xylene/total aromatics	0.042	0.039	0.058	0.073

**Table D4** Oil composition from HZ5(80), P/HZ5(80), Sb/HZ5(80), and Bi/HZ5(80) catalysts

Component	Composition (wt %)			
	HZ5(80)	P/ HZ5(80)	Sb/ HZ5(80)	Bi/ HZ5(80)
Oxygenate	0.01	25.94	0.00	0.14
Non-aromatic	9.76	0.00	15.00	22.6
Benzene	0.24	0.00	3.39	0.00
Toluene	9.54	1.76	29.47	9.61
o-Xylene	15.24	7.70	5.04	3.92
m-Xylene	14.80	2.74	2.54	2.62
p-Xylene	5.79	6.93	6.43	6.14
Ethylbenzene	5.08	2.75	16.52	12.8
C9	25.49	7.75	13.62	15.5
C10+	14.05	44.43	8.00	26.6
BTEX/total aromatics	0.56	0.30	0.75	0.53
p-Xylene/total aromatics	0.114	0.317	0.101	0.175

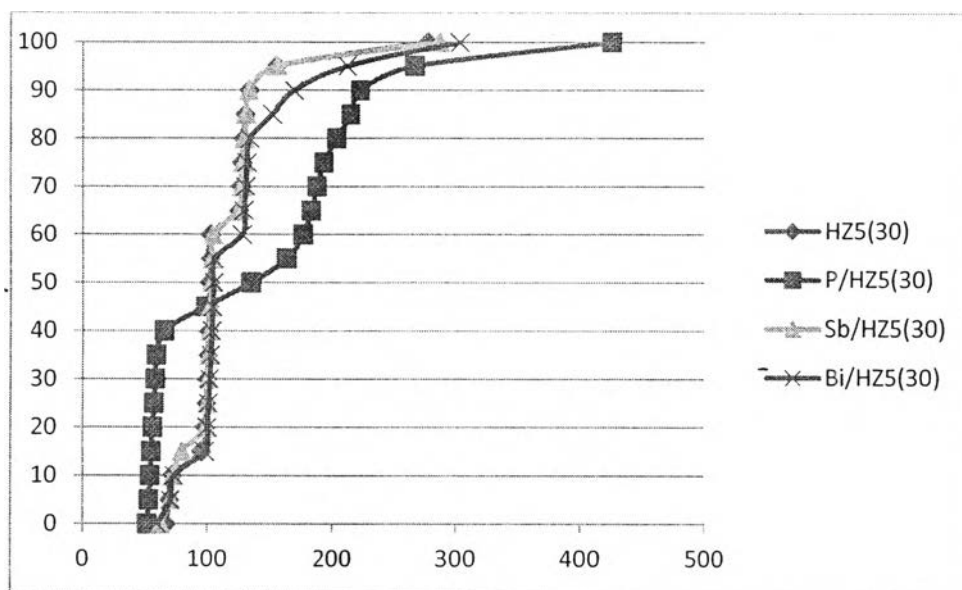
**Table D5** Oil composition from HZ11(75), P/HZ11(75), Sb/HZ11(75), and Bi/HZ5(75) catalysts

Component	Composition (wt %)			
	HZ11(75)	P/ HZ11(75)	Sb/ HZ11(75)	Bi/ HZ11(75)
Oxygenate	0.04	7.03	0.03	0.00
Non-aromatic	14.0	12.85	1.77	3.89
Benzene	1.98	3.19	15.03	8.21
Toluene	2.94	0.05	29.40	9.25
o-Xylene	12.83	9.74	10.66	21.81
m-Xylene	22.1	13.58	22.04	23.22
p-Xylene	13.2	15.86	9.77	4.78
Ethylbenzene	5.2	11.71	4.94	11.12
C9	22.2	18.50	6.36	17.14
C10+	5.57	7.49	0.00	0.59
BTEX/total aromatics	0.68	0.68	0.94	0.82
p-Xylene/total aromatics	0.226	0.293	0.106	0.061

## Appendix E True Boiling Point Curves

**Table E1** True boiling point curves from HZ5(30), P/HZ5(30), Sb/HZ5(30), Bi/HZ5(30)

% OFF	Boiling point (°C)			
	HZ5(30)	P/HZ5(30)	Sb/HZ5(30)	Bi/HZ5(30)
0	67.2	51.8	62.3	59.9
5	70	53.1	70.9	70.9
10	72.4	54.1	72.8	73.7
15	95.8	55.2	80.3	98.8
20	98.8	56.3	99.4	100.4
25	99.6	57.4	100.5	101.5
30	100.3	58.4	101.3	102.4
35	100.9	59.5	102	103.2
40	101.4	65.9	102.7	104
45	101.9	99.1	103.3	104.7
50	102.4	134.9	103.8	105.3
55	102.8	163.2	104.3	105.9
60	103.2	176.2	104.9	127.9
65	125.4	182.8	125.4	129.2
70	127	187.6	127.7	130.4
75	127.9	192.9	128.7	131.4
80	128.6	203.7	129.6	133.6
85	130.3	215.2	130.7	151.4
90	133.2	223.4	132.9	168.7
95	154.8	267.8	155.3	212.4
100	278.2	424.9	287.3	303.4



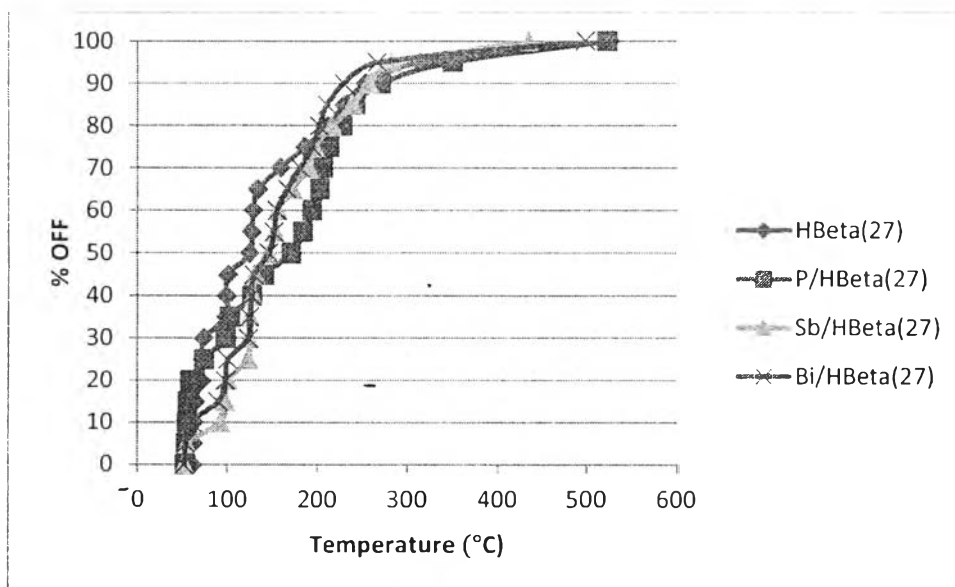
**Figure E1** True boiling point curves from HZ5(30), P/HZ5(30), Sb/HZ5(30), Bi/HZ5(30).

**Table E2** Petroleum cuts obtained from the HZ5(30), P/HZ5(30), Sb/HZ5(30), Bi/HZ5(30).

Fraction	Boiling point (°C)	wt %			
		HZ5(30)	P/HZ5(30)	Sb/HZ5(30)	Bi/HZ5(30)
Gasoline	<149	93.66	52.49	93.59	84.33
Kerosene	149-232	4.47	38.48	4.31	11.75
Gas oil	232-343	1.87	6.42	2.09	3.92
LVGO	343-371	0.00	0.89	0.00	0.00
HVGO	>371	0.00	1.72	0.00	0.00

**Table E3** True boiling point curves from HBeta(27), P/ HBeta(27), Sb/ HBeta(27), Bi/ HBeta(27)

% OFF	Boiling point (°C)			
	HBeta(27)	P/HBeta(27)	Sb/HBeta(27)	Bi/HBeta(27)
0	62.3	53.3	52.6	52.4
5	63.4	54.3	55.6	54.3
10	64.4	55.4	93.2	61
15	65.5	56.5	98.3	90.4
20	72.2	59.3	101.2	98.4
25	73.3	75	123.3	101
30	74.8	98.6	124	123.7
35	99.2	103.4	125.4	124.8
40	99.6	127.5	128.3	126.9
45	101.2	140.9	130.3	129.3
50	125.1	171.3	146.1	145.6
55	126.8	184.3	152.6	151.2
60	129	194.7	156	154.7
65	133.4	203.3	172.5	166.1
70	159.2	207.1	190	180.4
75	186	214.1	196.7	193.8
80	212.2	228.6	216.8	201.8
85	230	243	239.5	210.8
90	254.3	270.9	257.6	230.1
95	314	349.3	283.5	267.2
100	524.7	522.1	434.8	498.3



**Figure E2** True boiling point curves from HBeta(27), P/ HBeta(27), Sb/ HBeta(27), Bi/ HBeta(27) catalysts.

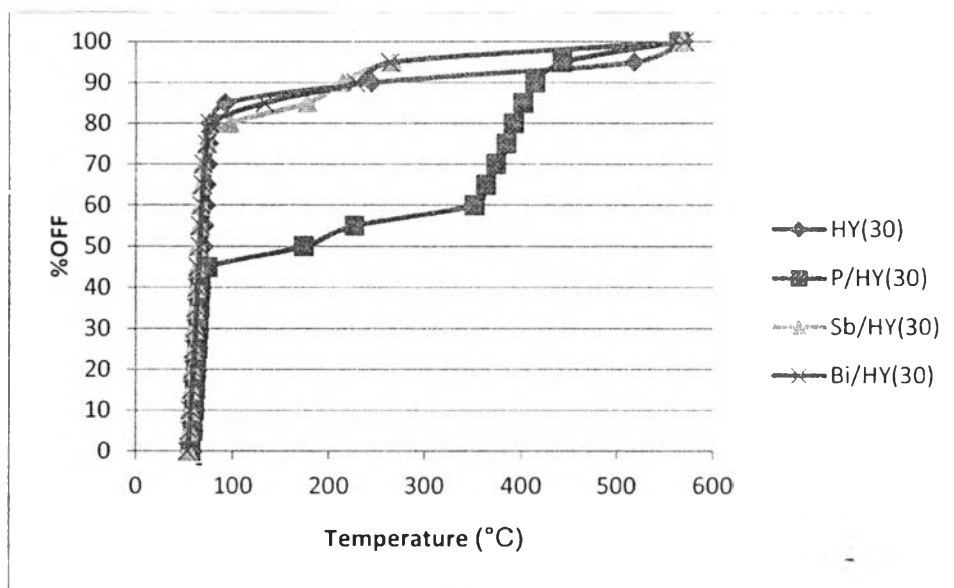
**Table E4** Petroleum cuts obtained from HBeta(27), P/ HBeta(27), Sb/ HBeta(27), Bi/ HBeta(27) catalysts.

Fraction	Boiling point (°C)	wt %			
		HBeta(27)	P/ HBeta(27)	Sb/ HBeta(27)	Bi/ HBeta(27)
Gasoline	<149	68.02	46.33	52.23	53.04
Kerosene	149-232	17.39	6.03	31.12	37.22
Gas oil	232-343	10.28	29.86	13.62	6.38
LVGO	343-371	0.66	6.98	0.93	0.61
HVGO	>371	3.65	10.80	2.11	2.75



**Table E5** True boiling point curves from HY(30), P/HY(30), Sb/HY(30), and Bi/HY(30) catalysts.

% OFF	Boiling point (°C)			
	HY(30)	P/ HY(30)	Sb/ HY(30)	Bi/ HY(30)
0	58.2	56.3	52.8	52.6
5	59.9	58.6	54.3	55
10	61	59.9	55.4	56.1
15	62.1	61	56.5	57.6
20	63.2	62.1	57.6	58.6
25	64.2	63.2	58.6	59.7
30	65.3	64.2	59.7	60.8
35	66.4	65.3	60.8	61.9
40	67.5	66.4	61.9	62.9
45	68.5	73.9	62.9	64
50	69.6	174.2	64	65.1
55	70.7	226.6	65.1	66.2
60	71.7	352.3	66.2	67.2
65	72.8	363.8	67.2	68.3
70	73.9	374.4	68.3	69.4
75	75	384.6	73.3	72.2
80	76	392.2	97.1	75.4
85	91.9	402	177.9	133.1
90	243.9	414.2	214.3	227.6
95	518.6	442.4	267	263.4
100	569.1	564.6	568	570.1



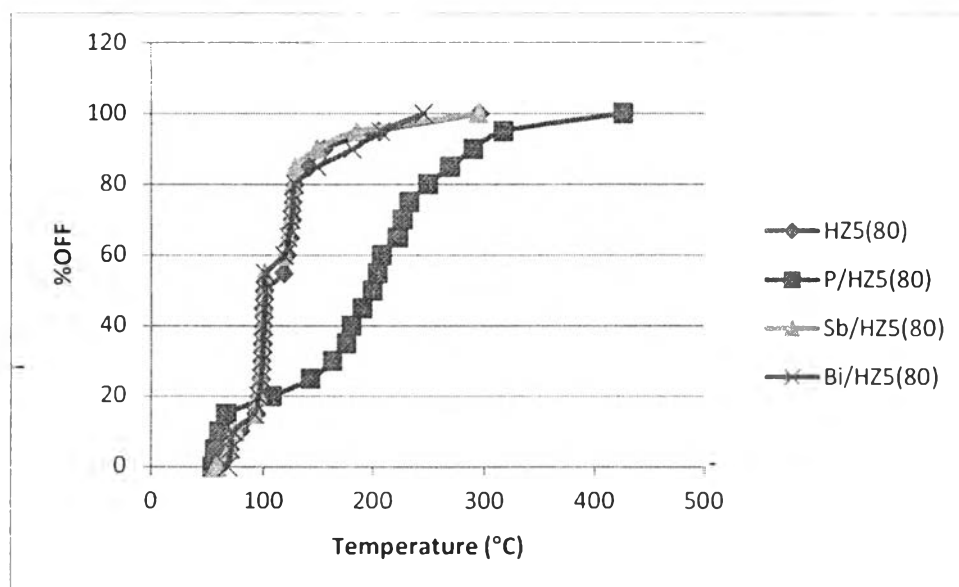
**Figure E3** True boiling point curves from HY(30), P/HY(30), Sb/HY(30), and Bi/HY(30) catalysts.

**Table E6** Petroleum cuts obtained from HY(30), P/HY(30), Sb/HY(30), and Bi/HY(30) catalysts.

Fraction	Boiling point (°C)	wt %			
		HY(30)	P/HY(30)	Sb/HY(30)	Bi/HY(30)
Gasoline	<149	86.88	48.74	83.21	85.84
Kerosene	149-232	2.73	6.77	8.47	4.77
Gas oil	232-343	2.20	4.11	4.58	5.68
LVGO	343-371	0.51	8.77	0.47	0.46
HVGO	>371	7.69	31.60	3.27	3.25

**Table E7** True boiling point curves from HZ5(80), P/HZ5(80), and Sb/HZ5(80), Bi/HZ5(80) catalysts

% OFF	Boiling point (°C)			
	HZ5(80)	P/HZ5(80)	Sb/HZ5(80)	Bi/HZ5(80)
0	61.7	55	58.2	68.1
5	70.5	57.1	70.5	70.9
10	79.7	61.2	74.8	73
15	93.7	67	92.4	91.5
20	96.5	107.7	-95.4	95.6
25	98.1	143.2	97.5	98.1
30	98.8	163.3	98.5	98.8
35	99.4	176.1	99.2	99.5
40	99.9	180.7	99.7	100.1
45	100.4	190.5	100.2	100.6
50	100.9	200	100.7	101.2
55	118.4	204.6	101.1	101.7
60	121.9	207.9	119	118.7
65	124.5	222.2	122.3	122.6
70	126.3	226.4	124.8	125.5
75	127	232.4	126.4	126.7
80	128.6	249.1	127.5	128.6
85	141.8	268.6	129	149.3
90	155.2	289.6	148.8	181.7
95	205.5	317.1	185.7	206.8
100	295.2	425.6	294.3	245



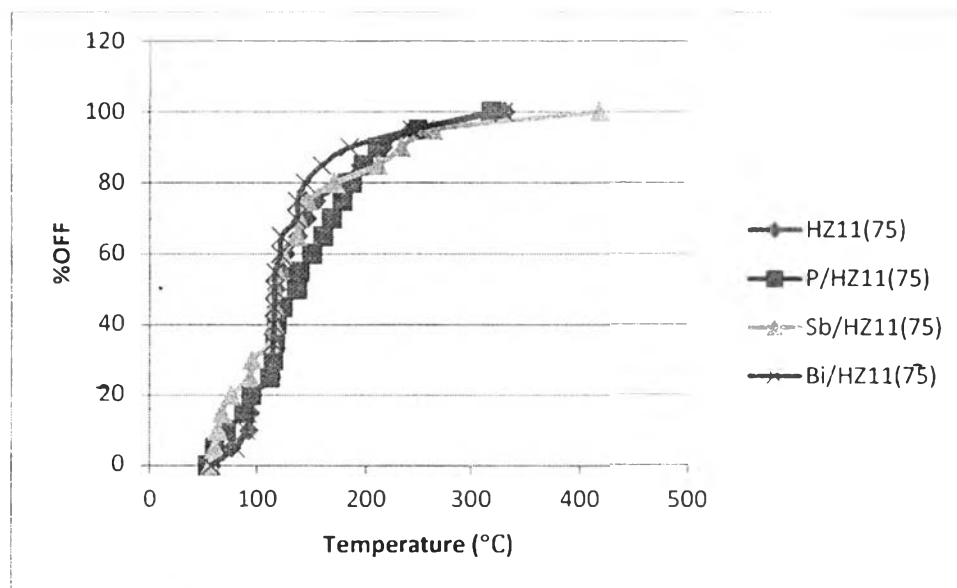
**Figure E4** True boiling point curves from HZ5(80), P/HZ5(80), Sb/HZ5(80), and Bi/HZ5(80) catalysts.

**Table E8** Petroleum cuts obtained from HZ5, 1BiHZ5, 2BiHZ5, 3BiHZ5, and 4BiHZ5 catalysts

Fraction	Boiling point (°C)	wt %			
		HZ5(80)	P/HZ5(80)	Sb/HZ5(80)	Bi/HZ5(80)
Gasoline	<149	84.1	69.0	69.8	69.9
Kerosene	149-232	11.3	23.3	24.5	22.7
Gas oil	232-343	1.73	5.46	3.28	4.87
LVGO	343-371	0.44	0.79	0.68	0.70
HVGO	>371	2.44	1.49	1.68	1.84

**Table E9** True boiling point curves from HZ11(75), P/HZ11(75), and Sb/HZ11(75), Bi/HZ11(75) catalysts

% OFF	Boiling point (°C)			
	HZ11(75)	P/HZ11(75)	Sb/HZ11(75)	Bi/HZ11(75)
0	58.2	54.3	56.9	57.4
5	77.3	60.6	60.8	80.6
10	92.6	71.7	63.4	90.4
15	93.9	88.3	67.5	91.5
20	96.9	95.2	76	94.5
25	113.8	112.7	93.9	112.3
30	116	115.6	96	114.2
35	116.9	117.3	113.7	115.1
40	117.6	118.5	115.7	115.7
45	118	124.1	116.2	116.2
50	118.6	137.1	116.6	116.6
55	123.9	139.4	118.6	117
60	127.1	150.8	123.3	121.7
65	138.1	160.9	137	122.8
70	145.9	168.7	137.9	136.6
75	154.8	178.4	146.1	137.3
80	176	187.2	170.8	144.6
85	195.1	198	211.8	159.8
90	216.3	210.8	233.5	184.8
95	242.8	249.4	264.4	243.5
100	331.1	318.5	418.6	329.7

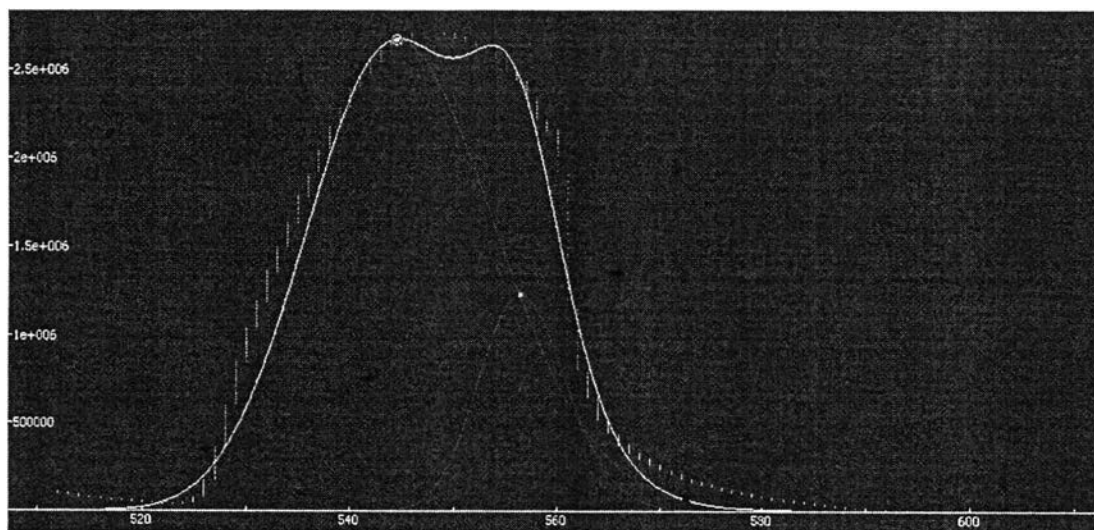


**Figure E5** True boiling point curves from HZ11(75), P/HZ11(75), Sb/HZ11(75), and Bi/HZ11(75) catalysts.

**Table E10** Petroleum cuts obtained from HZ11(75), P/HZ11(75), Sb/HZ11(75), and Bi/HZ11(75) catalysts

Fraction	Boiling point (°C)	wt %			
		HZ11(75)	P/HZ11(75)	Sb/HZ11(75)	Bi/HZ11(75)
Gasoline	<149	71.74	59.21	90.03	81.45
Kerosene	149-232	21.22	33.54	7.10	12.57
Gas oil	232-343	7.04	7.25	2.87	5.98
LVGO	343-371	0.00	0.00	0.00	0.00
HVGO	>371	0.00	0.00	0.00	0.00

## Appendix F Xylene Isomer Spectra From GCxGC-MS/TOF



**Figure F1** Deconvoluted peak of *m,p*-xylene from using GC×GC-MS/TOF.

Deconvoluted peak area = 2,621,351,427

*p*-Xylene peak area = 736,872,132

*m*-Xylene peak area = 1,884,479,295

wt.% of *p,m*-Xylene = 20.34 wt.%

wt.% of *p*-Xylene =  $20.34 \times (736,872,132 / 2,621,351,427) = 5.73$  wt.%

wt.% of *m*-Xylene =  $20.34 \times (1,884,479,295 / 2,621,351,427) = 14.6$  wt.%

## CURRICULUM VITAE

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**Proceedings:**

1. Kittikarnchanaporn, J. , Jitkarnka, S. (2014). Effects of SiO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub> Ratio of HZSM-5 with Antimony Oxide Promoter for Dehydration of Bio-ethanol to Hydrocarbons. Proceedings of The 5<sup>th</sup> Research Symposium on Petrochemical and Materials Technology and The 20<sup>th</sup> PPC Symposium on Petroleum, Petrochemicals, and Polymers, Bangkok, Thailand.
2. Kittikarnchanaporn, J. and Jitkarnka, S. (2014). Distillate Range of Hydrocarbon Production from Bio-ethanol Dehydration Using HY, HBeta, and HZSM-5 as Supports of Phosphorus Oxide. Proceedings of The 17<sup>th</sup> Conference Process Integration, Modelling and Optimisation for Energy Saving and Pollution Reduction, Prague, Czech Republic.